SUPPLEMENTARY INFORMATION

Cerium promotion on the hydrocarbons resistance of Cu-SAPO-34 NH₃-SCR monolith catalyst

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Fig. S1. The NO_x conversion and N_2O formation of the H-SAPO-34 and Ce-x supported material. Feed condition: 350 ppm NH₃, 350 ppm NO, 8% O₂, 5 vol% H₂O and N₂ balance, GSHV: 30,000 h⁻¹.

sample	Ce (wt%)	Si (wt%)	Al (wt%)	P (wt%)
Ce-1.3	1.2	2.9	20.2	18.1
Ce-1.9	1.9	3.1	19.5	17.5
Ce-2.6	2.6	2.7	19.8	17.9

Table S1. The chemical composition of Ce-x.

The NO_x conversion of the H-SAPO-34 and Ce-x supported materials were shown in Fig. S1, and the chemical composition of Ce-x were listed in Table S1. For the

supported materials, it could be found that the H-SAPO-34 supported material showed no NH₃-SCR activity, and the NO_x conversion at temperature above 300 °C was negative. In addition, after the Ce doping, the Ce-x supported materials also showed little NH₃-SCR activity at temperature below 300 °C, indicating that the cerium species was not the active sites for CuCe-x catalysts at the temperature below 300 °C. Furthermore, at the temperature above 300 °C, the NO_x conversion of Ce-x catalysts increased with the content of Ce increasing, until the content of Ce reached 1.9 wt%, suggesting that the NO_x conversion of CuCe-x catalysts may be improved by Ce adding. It could be found that the amount of N₂O formation of Ce-x catalyst increased as the content of Ce increasing, and the maximum concentrations of N₂O formation of Ce-x catalysts were not higher than 10 ppm, indicating that the selectivity of NO_x to N₂ of Ce-x catalysts were high.