

Improved hydrogenation function (Pt@SOD) incorporated inside sulfided (NiMo) hydrocracking catalyst

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Supplementary information

Table S1: Selectivity of various hydrocarbons over NiMo-Pt@SOD@ZSM-5 catalyst (at $\geq 99\%$ jatropha oil conversion).

Temp	H ₂ /HC	<C ₈	C ₉ -C ₁₄	C ₁₅	C ₁₆	C ₁₇	C ₁₈	C ₁₈₊
380	500	3.11	1.59	8.16	10.97	35.35	34.95	3.18
400	500	5.3	2.35	2.78	9.39	39.35	34.95	5.82
420	500	0.37	3.51	9.02	10.77	37.3	35.94	3.12
380	1000	7.81	11.77	7.97	12.44	23.25	30.38	6.3
400	1000	3.68	3.79	5.76	12.79	28.2	42.83	2.8
420	1000	7.33	10.22	7.15	12.83	22.96	32.25	7.22
450	1000	19.07	26.8	6.47	12.34	10.86	18.18	6.31
380	1500	3.74	7.09	5.21	15.29	16.16	47.29	5.23
420	1500	11.88	17.4	7.21	13.37	15.51	25.28	8.5
450	1500	27.69	29.4	7.27	10.74	10.03	12.43	1.22
380	2000	3.65	5.81	4.61	15.21	15.8	49.36	5.5
400	2000	7.38	13.96	5.94	15.38	13.42	36.5	7.48
420	2000	10.19	18.89	4.79	10.69	8.03	19.51	7.89
450	2000	21.58	25.36	5.88	13.63	11.04	19.64	2.85
380	250	1.67	3.8	6	11.8	31.1	43.8	1.68

Table S2: Composition of effluent gas

H ₂	CH ₄	CH ₃ -CH ₃	CH ₂ =CH ₂	CH ₃ CH ₂ CH ₃	CO ₂	CO
88.57 ^a	0.69	0.28	0.006	1.23	6.74	2.45
93.7 ^b	0.79	0.32	0.003	1.05	2.46	1.192

a: H₂/HC, 250, T: 380°C, Lhsv:1, P:80, b: H₂/HC, 1000, T: 420°C, Lhsv:1, P:80.

Figure: S1: Geometrically optimized H₂ (a), SOD (b), Pt (c, 0.4 nm), Pt (d, 0.57 nm), and hydrogen adsorbed SOD (e, f)

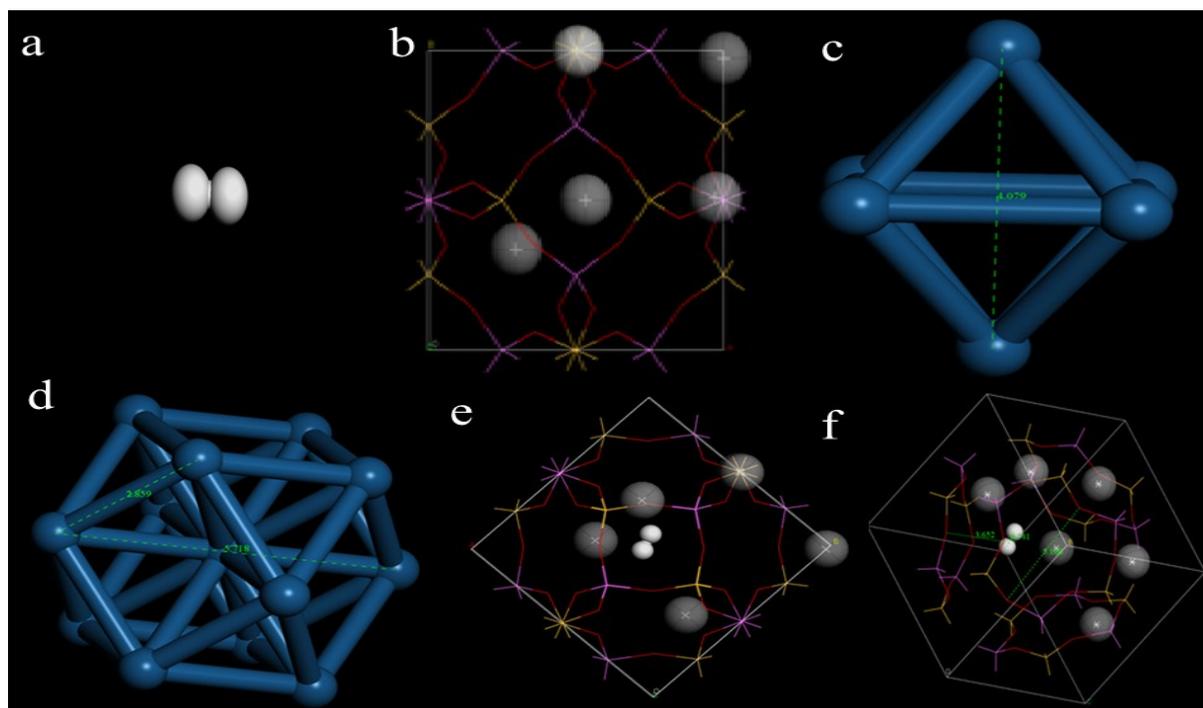


Figure S4: EDX analysis of Pt@SOD

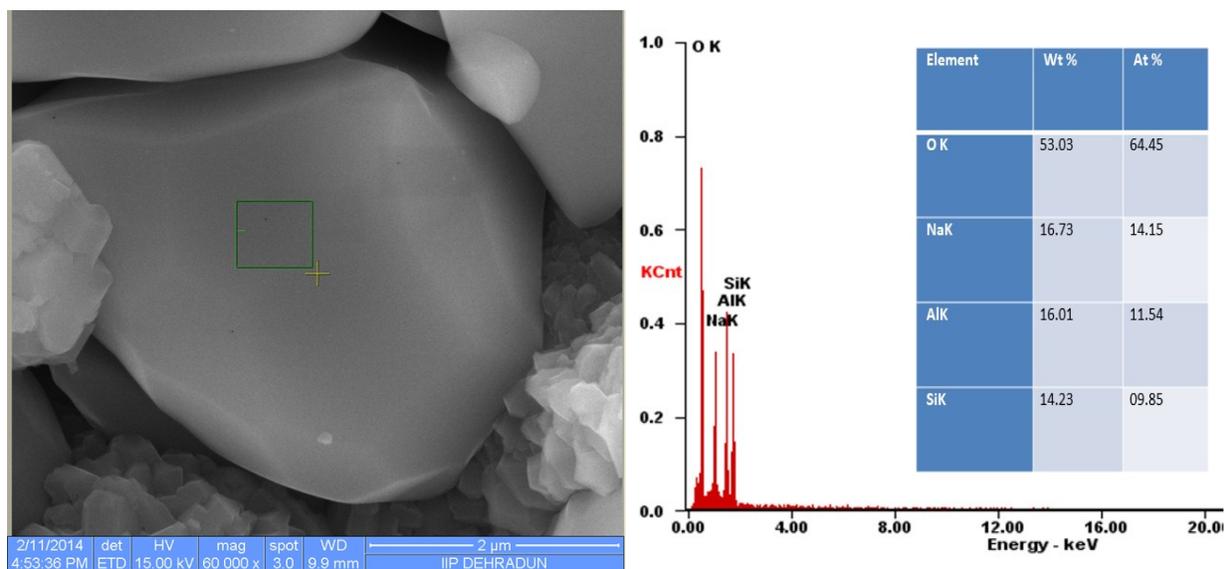


Figure S5: Influence of reaction temperature on yield of various products (H_2/HC ratio 500, P 80, GL: Gasoline, KR: Kerosene, DL: Diesel).

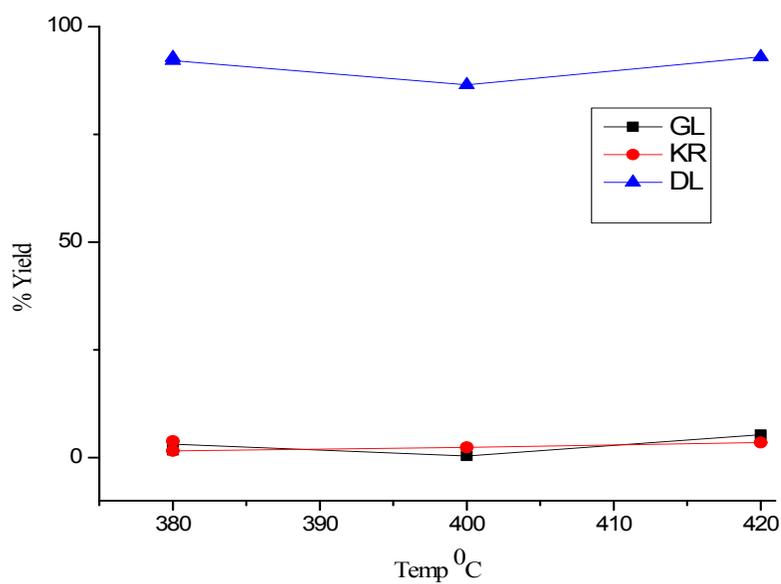


Figure S6: Influence of reaction temperature on yield of various products (H₂/HC ratio 1000, P 80, GL: Gasoline,KR: Kerosene, DL:Diesel, HVY: Oligomers).

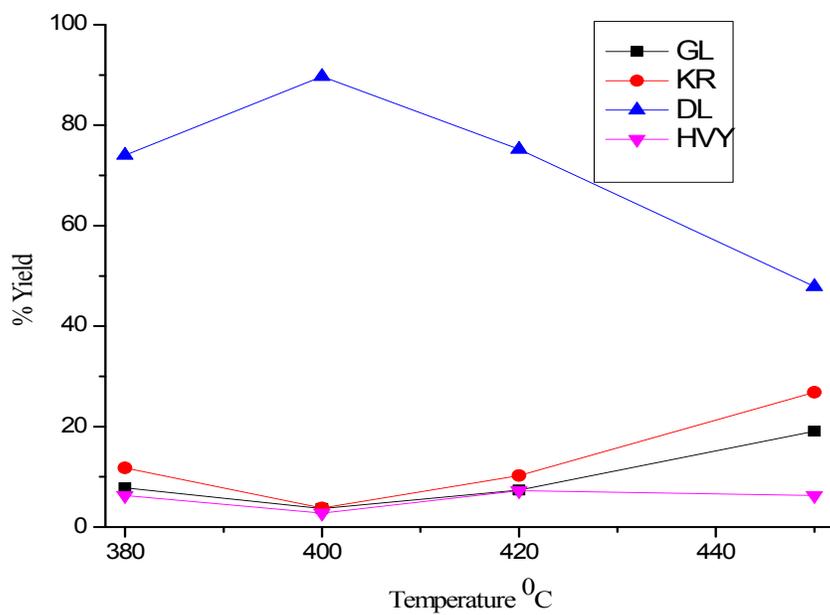


Figure S7: Influence of reaction temperature on yield of various products (H₂/HC ratio 1500, P 80 bar, GL: Gasoline, KR: Kerosene, DL:Diesel, HV: Oligomers).

