

Supplementary Materials

Toward lower cost cellulosic biofuel production using ammonia based pretreatment technologies

Mingjie Jin*, Leonardo da Costa Sousa, Christopher Schwartz, Yuxin He, Cory Sarks, Christa Gunawan, Venkatesh Balan*, Bruce E. Dale*

Biomass Conversion Research Laboratory (BCRL), Department of Chemical Engineering and Materials Science, Michigan State University, 3815 Technology Boulevard, Lansing, MI 48910, USA

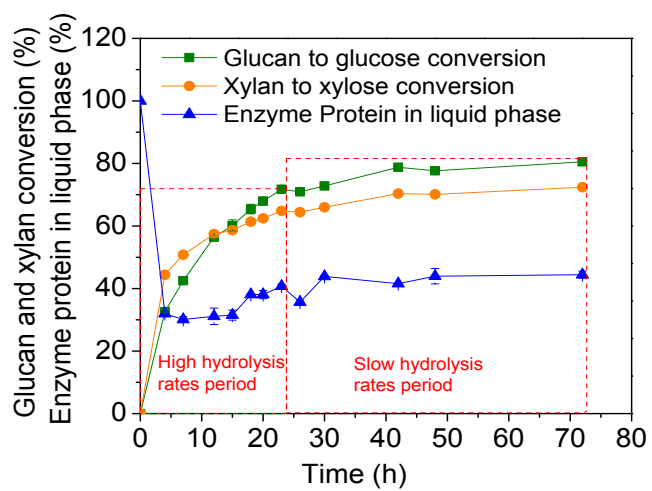
DOE Great Lakes Bioenergy Research Center, Michigan State University, East Lansing, MI 48824, USA

TM Trade mark of MBI, International (Lansing, Michigan)

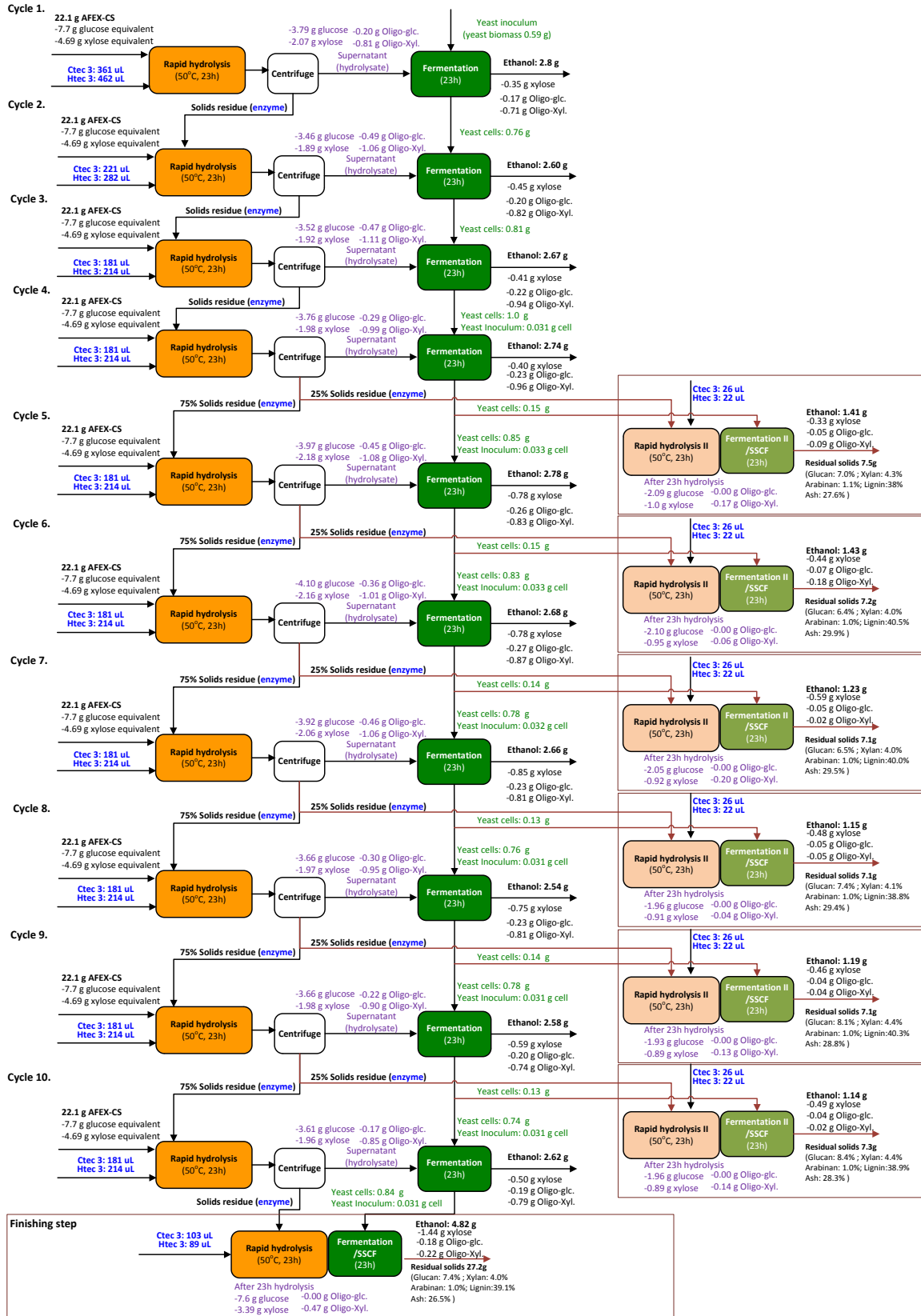
*Corresponding authors: jinmingji@egr.msu.edu, balan@egr.msu.edu, bdale@egr.msu.edu

Phone: 517-353-6777; Fax: 517-336-4615

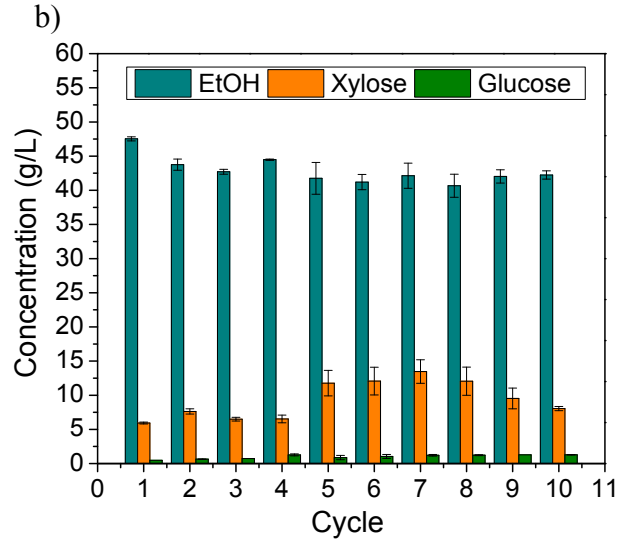
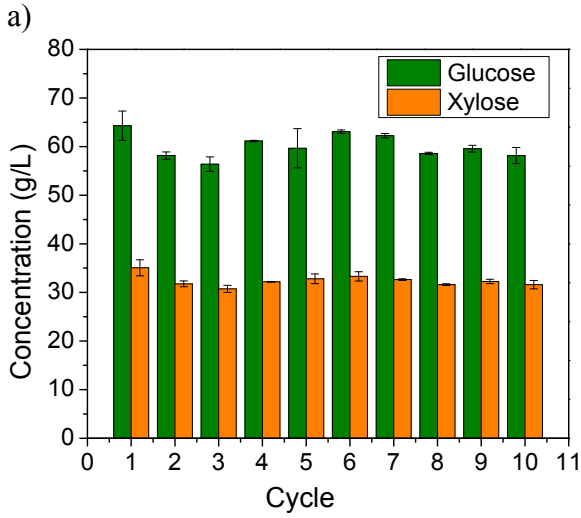
Supplementary Figure 1 Enzymatic hydrolysis profile on AFEX-CS at 7 wt.% glucan loading (22.1 wt.% solid loading) with an enzyme loading of 22 mg protein/g glucan showing rates slow down and enzyme adsorption profile.



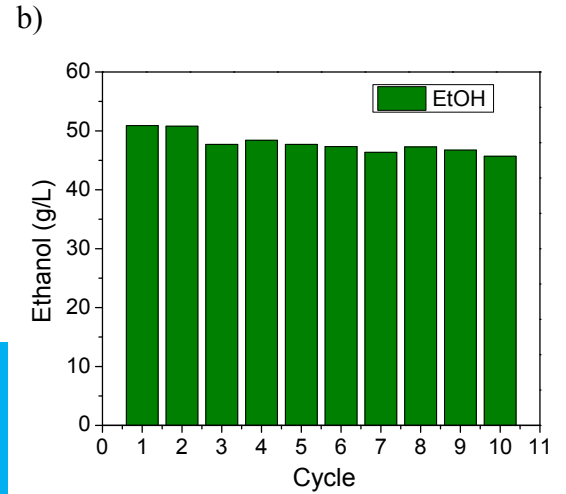
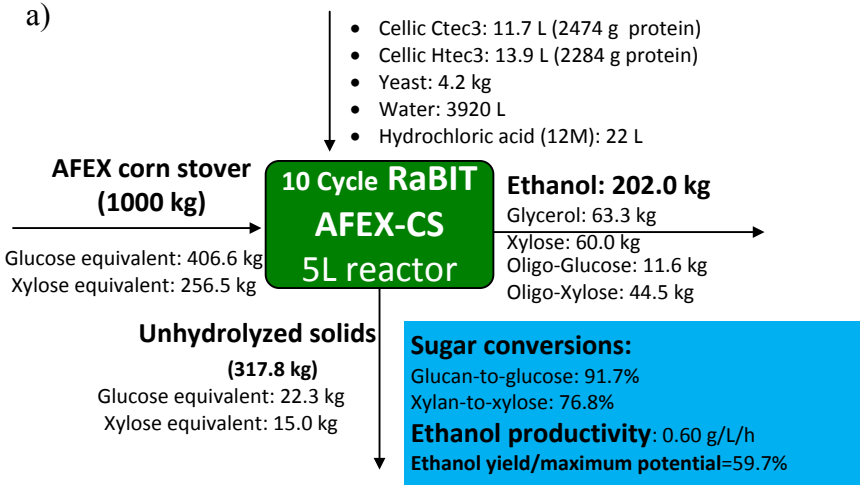
Supplementary Figure 2 Detailed mass balance of the ten-cycle shake flask RaBIT on AFEX-CS. The Fermentation II and the finishing step fermentation were performed in the hydrolysate with residual solids, which means they were actually simultaneous saccharification and co-fermentation (SSCF) and fermentable sugars were still being released during fermentation.



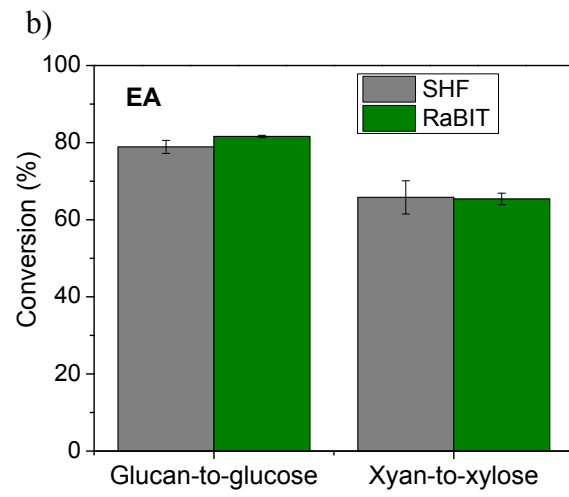
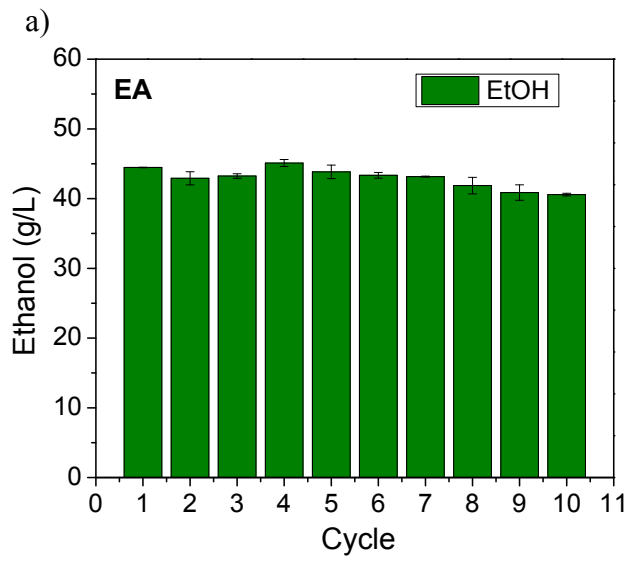
Supplementary Figure 3 Enzymatic hydrolysis and fermentation results of the ten-cycle shake flask RaBIT on AFEX-CS. a) sugar concentrations of each cycle in the main hydrolyzer showing consistent glucose and xylose released; b) ethanol and remaining sugar concentrations of each cycle in the main fermenter showing consistent ethanol (>40 g/L) produced.



Supplementary Figure 4 RaBIT performance on pelletized AFEX-CS in 5 L bioreactors. A glucan loading of 7.34 wt.% (20.0 wt.% solids loading) was applied. a) Mass balance of ten-cycle RaBIT in 5 L bioreactors; b) Ethanol concentrations produced from each cycle in the main fermenter.



Supplementary Figure 5 Ethanol concentrations produced in each RaBIT cycle on EA-CS in the main fermenter (a) and sugar conversion comparison between SHF and RaBIT (b).



Supplementary Table 1 Comparison of different substrates in enzyme recycling using RaBIT approach. Enzymatic hydrolysis were performed at 7 wt.% glucan loading in a 250 ml baffled flask with working loading of 100 g in total at 50 °C and 250 rpm. Avicel, Cellulose III, AFEX-CS, EA-CS and DA-CS were used as the substrates. To investigate the effect of lignin on enzyme recycling, AFEX-CS lignin residue obtained from enzymatically hydrolyzing AFEX-CS extensively was added to Avicel and Cellulose III at a loading of 4 g/7 g glucan (noted as Avicel + Lignin and Cellulose III + Lignin). Cellic Ctec3 were used for hydrolyzing Avicel, Avicel + lignin, Cellulose III and Cellulose III + Lignin at loadings of 11.9, 11.9, 6.0, and 6.0 mg protein/g glucan, respectively. Cellic Ctec3 and Htec3 were used for hydrolyzing AFEX-CS, EA-CS and DA-CS at loadings of 22.0 (Ctec3: 11.5 & Htec3: 10.5), 12.2 (Ctec3: 6.6 & Htec3: 5.6) and 15.4 (Ctec3: 11.8 & Htec3: 3.6) mg protein/g glucan. The enzymatic hydrolysis was performed for 23 h (Cycle 1) and then hydrolysate was centrifuged. Unhydrolyzed solids were recycled to the Cycle 2 hydrolysis. Enzymes were recycled together with unhydrolyzed solids to the Cycle 2. The amount of enzymes in supernatant, which were not recycled, was analyzed via 2D-quant method. The difference between total input enzyme and enzyme in the supernatant was counted as the enzyme recycled. The Cycle 2 enzymatic hydrolysis was set up as Cycle 1 expect that no enzyme was added for all cases expect the one shown in the last row of the table, in which 50% amount of the Cycle 1 enzyme was added. Experiments were performed in duplicates.

Substrate	Cycle 1		Enzyme recycle from Cycle 1 to Cycle 2 via unhydrolyzed solids		Cycle 2 w/o enzyme addition		% sugar yield of Cycle 2	
	Glucose (g/L)	Xylose (g/L)	Recycled enzyme (%)	Recycled enzyme due to moisture in solids (%)	Glucose (g/L)	Xylose (g/L)	Cycle 2 glucose concentration /Cycle 1 glucose concentration	Cycle 2 xylose concentration/ Cycle 1 xylose concentration
Avicel	29.4 ± 2.0	/	57.1% ± 0.8%	5.6% ± 0.0%	15.3 ± 0.8	/	52.0%	/
Avicel + Lignin	20.9 ± 2.1	/	89.5% ± 1.0%	2.7% ± 0.2%	15.5 ± 0.5	/	74.1%	/
Cellulose III	31.9 ± 0.9	/	50.4% ± 3.1%	5.3% ± 0.2%	8.9 ± 0.1	/	27.9%	/
Cellulose III + Lignin	21.9 ± 1.7	/	92.4% ± 0.7%	1.7% ± 0.2%	8.2 ± 0.6	/	37.6%	/
AFEX-CS	61.2 ± 1.4	33.7 ± 0.8	63.4% ± 1.5%	14.9% ± 0.1%	35.4 ± 0.3	22.3 ± 0.2	57.8%	66.2%
EA-CS	55.9 ± 0.5	32.3 ± 0.3	73.7% ± 4.7%	12.1% ± 1.4%	29.3 ± 1.2	23.7 ± 1.0	52.3%	73.3%
DA-CS	56.6 ± 0.1	2.2 ± 0.1	88.6% ± 0.2%	3.7% ± 0.1%	38.8 ± 0.4	1.4 ± 0.0	68.6%	61.9%
					Cycle 2 w/ 50% enzyme addition			
DA-CS	56.6 ± 0.1	2.2 ± 0.1	88.6% ± 0.2%	3.7% ± 0.1%	56.5 ± 0.1	2.2 ± 0.0	99.9%	98.5%