# Electronic Supplementary Information 

# A Noble Metal Seed-Mediated Approach to General and Mild Synthesis of Non-noble Metal Nanoparticles Stabilized by A MetalOrganic Framework for Highly Efficient Catalysis 

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Fig. S1 As a representative, the synthesis progress for Ag-doped Ni/MIL-101 can be visibly monitored by the obvious color evolution in the solution: (a) The pale green $\mathrm{Ag}^{+} \mathrm{Ni}^{2+} / \mathrm{MIL}-101$ aqueous solution before the reduction by $\mathrm{NH}_{3} \mathrm{BH}_{3}$; (b) the deep green aqueous solution obtained at the beginning of the hydrolysis of $\mathrm{NH}_{3} \mathrm{BH}_{3}$, in which only the $\mathrm{Ag}^{+}$was reduced to Ag NPs as seeds. The generated very few bubbles are due to the presence of tiny amount of Ag NPs ; (c) then the color became darker and darker gradually within a few minutes during the hydrogen generation and reduction process, and the bubbles becomes more and bigger, revealing that the reduction of $\mathrm{Ni}^{2+} \mathrm{NPs}$ to Ni NPs covered on the pre-formed Ag seeds, thus to afford Ag-doped Ni/MIL-101.


Fig. S2 (a, c) HAADF-STEM images and (b, d) the corresponding EDS spectra for as-synthesized Ag-doped Ni/MIL-101 sample. The point 1 in (a) and 2 in (c) lie in middle and edge of Ag-doped Ni NPs, respectively. The Cu and Cr signals originate from Cu grid and MIL-101 support, respectively. The EDS spectra for point 1 and 2 marked for Ag -doped Ni NPs only show the element Ni because the content of Ag is too low to be detectable.


Fig. S3 TEM image of (a) Ag-doped Ni/MIL-101 (reduced by $\mathrm{NH}_{3} \mathrm{BH}_{3}$ ) with $\mathrm{Ag} / \mathrm{Ni}$ molar ratio of $1 / 200$, (b) PVP-stabilized Ni NPs (reduced by $\mathrm{NaBH}_{4}$, inset: HRTEM image for Ni NP) (c) Ni/MIL-101 (reduced by $\mathrm{NaBH}_{4}$ ), (d) Ag/MIL-101 (reduced by $\mathrm{NH}_{3} \mathrm{BH}_{3}$ ), and (e) pure Ag-doped Ni (1/200) NPs without stabilizer. (f) HRTEM image of pure Ag-doped Ni NP , in which the lattice fringes with 0.206 nm spacing are assigned to the (111) plane of the face-centered cubic (fcc) Ni. (g) $\mathrm{Ni}^{2+} / \mathrm{MIL}-101$ and (h) PVP-stabilized $\mathrm{Ag} @ \mathrm{Ni}$ core-shell NPs (reduced by $\mathrm{NH}_{3} \mathrm{BH}_{3}$ ) with $\mathrm{Ag} / \mathrm{Ni}$ molar ratio of $1 / 1$ (inset: HRTEM image for $\mathrm{Ag} @ \mathrm{Ni}$ NP).


Fig. S4 PXRD patterns of (a) Ag-doped Ni/MIL-101 reduced by $0.6 \mathrm{M} \mathrm{NaBH}_{4}$ or
$\mathrm{NH}_{3} \mathrm{BH}_{3}$ aqueous solution, (b) simulated MIL-101, as-synthesized MIL-101, Agdoped Ni/MIL-101, Pd-doped Co/MIL-101, Pd-doped Ni/MIL-101, Pt-doped Ni/MIL-101, Pt-doped Co/MIL-101 and Au-doped Ni/MIL-101 with noble/non-noble metal molar ratio from $1 / 100$ to $1 / 200$, and (c) simulated MIL-101, as-synthesized MIL-101, Ag/MIL-101, and Ag-doped Ni/MIL-101 with various molar ratios of Ag and Ni.


Fig. S5 $\mathrm{N}_{2}$ sorption isotherms of (a) as-synthesized MIL-101, Pd-doped Co/MIL-101, Pd-doped Ni/MIL-101, Pt-doped Ni/MIL-101, Pt-doped Co/MIL-101 and Au-doped Ni/MIL-101 with the corresponding surface areas of 3660, 2347, 2711, 2250, 2328, $2941 \mathrm{~m}^{2} / \mathrm{g}$, respectively. (b) $\mathrm{N}_{2}$ sorption isotherms of as-synthesized MIL-101, $\mathrm{Ag} / \mathrm{MIL}-101$ and Ag -doped $\mathrm{Ni} / \mathrm{MIL}-101$ with $\mathrm{Ag} / \mathrm{Ni}$ molar ratios of $10 / 1,1 / 1,1 / 5$, $1 / 50,1 / 100$ and $1 / 200$ at 77 K , with the corresponding surface areas of 3660,2456 , 2034, 2142, 2452, 2453, 2490, 2460, $2753 \mathrm{~m}^{2} / \mathrm{g}$, respectively. Filled and open symbols represent adsorption and desorption branches, respectively.


Fig. S6 Plots of time $v s$ volume of hydrogen generated from the catalytic hydrolysis of $\mathrm{NH}_{3} \mathrm{BH}_{3}$ over (a) Pd-doped Ni/MIL-101, (b) Pd-doped Co/MIL-101, (c) Pt-doped Ni/MIL-101, (d) Pt-doped Co/MIL-101, (e) Au-doped Ni/MIL-101 catalysts with different noble/non-noble metals molar ratios, and (f) Pd-doped Fe/MIL-101 (1:100) at $25^{\circ} \mathrm{C}$. The Fe species has inferior activity compared to Ni and Co . Therefore, only catalytic study over Pd-doped Fe/MIL-101 (1:100) was conducted.

Table S1. Catalytic reaction rate constant $k$ and TOF value of Ag-doped Ni/MIL-101 catalysts with different $\mathrm{Ag} / \mathrm{Ni}$ ratios for hydrolytic dehydrogenation of $\mathrm{NH}_{3} \mathrm{BH}_{3}$ (TOF $\left.=\mathrm{k} /\left(\mathrm{V}_{0} \cdot \mathrm{n}_{\text {metal }}\right), \mathrm{V}_{0}=24 \mathrm{~L} / \mathrm{mol}, \mathrm{T}=25^{\circ} \mathrm{C}\right)$.

| $\mathrm{n}_{\mathrm{Ag}}: \mathrm{n}_{\mathrm{Ni}}$ <br> $\left(\mathrm{mol}: \mathrm{mol}^{2}\right)$ | K <br> $\left(\mathrm{mL}_{\mathrm{H} 2} \cdot \mathrm{~min}^{-1}\right)$ | TOF <br> $\left(\mathrm{mol}_{\mathrm{H} 2} \cdot \mathrm{~mol}_{\mathrm{metal}^{-1}} \cdot \mathrm{~min}^{-1}\right)$ |
| :---: | :---: | :---: |
| $10: 1$ | 7.31 | 21.2 |
| $5: 1$ | 8.94 | 20.3 |
| $1: 1$ | 7.62 | 24.8 |
| $1: 50$ | 10.8 | 30 |
| $1: 100$ | 7.21 | 20 |
| $1: 150$ | 6.51 | 18.1 |
| $1: 200$ | 7.28 | 20.2 |



Fig. S7 Plots of TOF value of hydrogen release versus Ag-doped Ni/MIL-101 catalysts with various $\mathrm{Ag} /(\mathrm{Ag}+\mathrm{Ni})$ molar ratios. Reaction conditions: 0.875 mmol ammonia borane, $20 \mathrm{~mL} \mathrm{H} \mathrm{H}_{2} \mathrm{O},(\mathrm{Ag}+\mathrm{Ni}) / \mathrm{NH}_{3} \mathrm{BH}_{3}=0.017$ in molar ratio for all catalysts.


Fig. S8 Plots of time versus the volume of hydrogen generated from the hydrolysis of ammonia borane catalyzed by the Ag -doped $\mathrm{Ni} / \mathrm{MIL}-101$ catalyst with $\mathrm{Ag} / \mathrm{Ni}$ atomic ratio of $1 / 200$ at different temperatures. It can be seen that the lower the reaction temperature, the longer the initiation period. After the initiation process, a rapid and almost linear hydrogen evolution can be observed.


Fig. S9 Plots of $\ln (\mathrm{K})$ versus $1 / \mathrm{T}$ of hydrogen generated from ammonia borane ( 0.875 mmol, 20 ml ) in the presence of Ag-doped $\mathrm{Ni} / \mathrm{MIL}-101$ catalyst with $\mathrm{Ag} / \mathrm{Ni}$ molar ratio of $1 / 200\left((\mathrm{Ag}+\mathrm{Ni}) / \mathrm{NH}_{3} \mathrm{BH}_{3}=0.017\right.$ in molar ratio $)$ at $25,30,35$ and $40{ }^{\circ} \mathrm{C}$ and the calculated activation energy is $25 \mathrm{~kJ} / \mathrm{mol}$.


Fig. S10 Plots of time versus the volume of hydrogen generated from the hydrolysis of ammonia borane over Ag -doped $\mathrm{Ni} /$ MIL-101 catalyst with $\mathrm{Ag} / \mathrm{Ni}$ molar ratio of $1 / 200$ at different concentrations of ammonia borane $\left(\left[\mathrm{NH}_{3} \mathrm{BH}_{3}\right]=0.875 \mathrm{mmol}, \mathrm{T}=\right.$ $25^{\circ} \mathrm{C}$ ), indicating that the catalytic hydrolysis of ammonia borane is of zero order with respect to the substrate concentration. It can be seen that the initiation process is dependent on the $\mathrm{NH}_{3} \mathrm{BH}_{3}$ concentration while other reaction conditions are fixed. The higher $\mathrm{NH}_{3} \mathrm{BH}_{3}$ concentration is, the shorter initiation period.

Table S2. Performance comparison of Ag-doped Ni/MIL-101 catalyst with various catalysts.

| Catalyst | $\underset{\mathrm{kJ} \cdot \mathrm{~mol}^{-1}}{\mathrm{Ea}}$ | $\underset{\left(\mathrm{mol}_{\mathrm{H} 2} \cdot \text { mol }_{\text {metal }}{ }^{-1} \cdot \mathrm{~min}^{-1}\right)}{\text { TOF }}$ | Ref. |
| :---: | :---: | :---: | :---: |
| $\begin{gathered} \text { Ag-doped Ni/MIL- } \\ 101(\mathrm{Ag} / \mathrm{Ni} \text { molar } \\ \text { ratio }=1 / 200) \\ \hline \end{gathered}$ | 25 | 20.2 | This work |
| PSMA-Ni | 38.12 | 10.1 | 1 |
| zeolite confined palladium (0) | 56 | 5.6 | 2 |
| $\mathrm{Ni} / \mathrm{SiO}_{2}$ | 34 | 13.2 | 3 |
| Ag-Ni/C | 52 | - | 4 |
| $\mathrm{Ni}_{0.97}-\mathrm{Pt}_{0.03}$ | 57 | - | 5 |
| VP stabilized Au@Co core-shell | - | 13.6 | 6 |
| CVD-Ni/ZIF-8 | - | 14.2 | 7 |
| $\mathrm{Ni} / \gamma-\mathrm{Al}_{2} \mathrm{O}_{3}$ | - | 1.7 | 8 |
| $\mathrm{Pt} / \mathrm{Al}_{2} \mathrm{O}_{3}$ | 21 | - | 9 |
| Ag@CoNi/graphene | 47 | - | 10 |

Table S3. Inductively coupled plasma atomic emission spectrometry (ICP-AES) analysis results for catalysts. The results have confirmed that the actual ratios of noble/non-noble metals are very close to the nominal values.

| Nanoparticles | Metal content (\%) | $\mathrm{n}_{\text {noble }} / \mathrm{n}_{\text {non-noble }}(\mathrm{mol} / \mathrm{mol})$ |  |
| :---: | :---: | :---: | :---: |
|  |  | Actual value | Nominal value |
| Ag-doped Ni | 1.81 | $1 / 167$ | $1 / 200$ |
| Pd-doped Ni | 1.51 | $1 / 210$ | $1 / 200$ |
| Pd-doped Co | 1.75 | $1 / 144$ | $1 / 150$ |
| Pt-doped Ni | 1.43 | $1 / 85$ | $1 / 100$ |
| Pt-doped Co | 1.73 | $1 / 96$ | $1 / 100$ |
| Au-doped Ni | 1.63 | $1 / 88$ | $1 / 100$ |

Experimental process for ICP characterization: First, the instrument was preheated for about 30 min . Second, sample treatment: 10 mg of sample was dissolved in 3 mL concentrated $\mathrm{HNO}_{3}$ followed by heating to $80^{\circ} \mathrm{C}$ to remove organics. The residue was dissolved with $1 \mathrm{~mL} \mathrm{HNO}_{3}$ and some water, and then continuously adding water to make solution volume to 10 mL (a constant volume). Third, work curve was made and the metal ions in solution were measured.


Fig. S11 PXRD patterns for Ag-doped Ni/MIL-101 catalyst with $\mathrm{Ag} / \mathrm{Ni}$ molar ratio of $1 / 200$ and the catalyst after 5 cycles of $\mathrm{NH}_{3} \mathrm{BH}_{3}$ hydrolysis, revealing the wellretained crystallinity and framework structure of MIL-101, and also the absence of aggregation of tiny Ag-doped Ni NPs in both catalysts before and after five runs of recycling experiments.

## References

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