1	Supporting Information
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5	Effect of the Blocking Sites Phenomenon on the
6	Heterogeneous Reaction of Pyrene with N <sub>2</sub> O <sub>5</sub> /NO <sub>3</sub> /NO <sub>2</sub>
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20	<b>1.</b> Collecting and analyzed of products
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Figure S1. The schematic diagram of collecting procedure

# 23 2. The partitioning ratio of PY

The particulate PY and gas-phase PY were microfiber filter (25 mm diameter, 0.7 μm pore-size, Whatman)—liquid nitrogen washing (Figure S2). The collected PY were extracted with ~20 ml dichloromethane and analyzed using GC-MS. The partitioning ratio of pyrene between the gas and particle phase under our experimental condition was estimated to 0.2 be according to the relative signal intensities of gasphase and particulate PY observed using GC-MS.





32 Figure S2. The schematic diagram of collecting procedure



33



#### 35 3. Estimation of Oxidants Concentrations

#### 36 3.1 Estimation of initial N<sub>2</sub>O<sub>5</sub> concentration

The amount of  $N_2O_5$  delivered in experiments was determined by the temperature of the  $N_2O_5$  trap (243 K in our experiments) and its vapor pressure under this temperature. The initial gas-phase  $N_2O_5$  concentration in the chamber was calculated using the equation (2).

41 
$$[N_2 O_5]_0 = \frac{qt T_{chamber} P_t}{V_{chamber} T_{bathe} P_0}$$
(1)

42  $[N_2O_5]_0$  is the initial N<sub>2</sub>O<sub>5</sub> concentration,  $P_t$  and  $P_0$  is the vapor pressure of 43 N<sub>2</sub>O<sub>5</sub> (~40 Pa) at 243 K and the standard atmospheric pressure (~101306 Pa), 44 respectively.  $V_{chamber}$  represents the volume of the reaction chamber used in our 45 experiment, respectively.  $T_{chamber}$  and  $T_{bathe}$  are the temperatures of the chamber (286 46 K) and the cooling bath (243 K). q is the flow rate of N<sub>2</sub> (~0.6 L min<sup>-1</sup>), t is the filling 47 time (3~5 min).

### 48 3.2 Estimation of the $[NO_3]/[N_2O_5]$ ratio in the absence of $O_3$

The NO<sub>3</sub> concentration in the chamber was estimated by probing the decay of the isoprene. ~200 ppbv isoprene was added into the chamber before introducing  $N_2O_5/NO_3/NO_2$  mixture. The decay of isoprene was on-line monitored using VUV-GTOFMS (Figure S4). The NO<sub>3</sub> radical concentration in the absence of O<sub>3</sub> are calculated with the following equations (3–6).

54 
$$NO_3 + Isoprene \rightarrow \Pr oducts$$
  $k_I = 7.0 \times 10^{-13} \text{ cm}^3 \text{ molecule}^{-1} \text{ s}^{-1}$  (2)

55 
$$-\frac{d[Isoprene]}{dt} \rightarrow k_1[Isoprene][NO_3]$$
(3)

56 
$$In\left(\frac{[Isoprene]_{t}}{[Isoprene]_{0}}\right) = -k_{1}[NO_{3}]t$$
(4)

57 
$$[NO_3] = \frac{In\left(\frac{[Isoprene]_t}{[Isoprene]_0}\right)}{-k_1 t}$$
(5)

58 *t* is the reaction time. ([Isoprene]<sub>*t*</sub>/[Isoprene]<sub>0</sub>) is the loss ratio of isoprene during 59 this period. The average NO<sub>3</sub> radical concentrations in the reaction processes was 60 calculated to be  $\sim 3.0 \times 10^{10}$  molecules cm<sup>-3</sup>.



61

62 Figure S4. The isoprene decay curves by exposure to  $N_2O_5/NO_3/NO_2$ . The error bars

63 are obtained from three duplicate experiments.

Based on the obtained NO<sub>3</sub> level and the temperature dependent equilibrium constant  $K_{eq}$  shown in equation (7) (Sander et al., 2003), the N<sub>2</sub>O<sub>5</sub> concentration was calculated to be ~2.0 × 10<sup>14</sup> molecules cm<sup>-3</sup>.

67 
$$K_{eq} = \frac{[N_2 O_5]}{[NO_2][NO_3]} = 3 \times 10^{-27} \exp(10990/T)$$
(7)

68 [N<sub>2</sub>O<sub>5</sub>], [NO<sub>3</sub>], and [NO<sub>2</sub>] are the concentrations of N<sub>2</sub>O<sub>5</sub>, NO<sub>3</sub>, and NO<sub>2</sub>, respectively.

# 69 **3.3 Estimation of the [NO<sub>3</sub>]/[N<sub>2</sub>O<sub>5</sub>] ratio in the presence of O<sub>3</sub>**

The NO<sub>3</sub> radical concentration in the presence of O<sub>3</sub> could not be estimated according to the decay of isoprene because part of isoprene was also consumed by O<sub>3</sub> in the chamber. Although the  $N_2O_5(g) \longrightarrow NO_2(g) + NO_3(g)$  reaction was derived to NO<sub>3</sub> radical using O<sub>3</sub>, the new equilibrium in the N<sub>2</sub>O<sub>5</sub>/NO<sub>3</sub>/NO<sub>2</sub> system was assumed to be established in the presence of O<sub>3</sub>. Both NO<sub>3</sub> radical and N<sub>2</sub>O<sub>5</sub> concentration could be calculated using the following equation:

76 
$$\frac{[N_2O_5]^*}{[NO_2]^*[NO_3]^*} = \frac{[N_2O_5] - k_{O_3 + NO_2}[O_3][NO_2]^*}{[NO_2]^*([NO_3] + k_{O_3 + NO_2}[O_3][NO_2]^*)} = K_{eq}$$
(8)

where  $[N_2O_5]^*$ ,  $[NO_3]^*$ , and  $[NO_2]^*$  are the concentrations of  $N_2O_5$ ,  $NO_3$ , and  $NO_2$ , respectively, in the new equilibrium system.  $k_{O_3+NO_2}[O_3][NO_2]^*$  is the production rate of the NO<sub>3</sub> radical ( $k_{O_3+NO_2} = 1.4 \times 10^{-13} \exp(-2490/T)$ )(Atkinson et al., 2004). Based on the iteration method,  $[NO_3]^*$ ,  $[N_2O_5]^*$ ,  $[NO2]^*$ , the  $[NO_3]/[N_2O_5]$  ratio have been calculated and shown in Table 1.

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