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Electronic Supplementary Information

Facile, low-cost, and scalable fabrication of particle size and pore structure tuneable monodisperse mesoporous silica nanospheres as supports for advanced solid acid catalysts[†]

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Figure S1. Particle size distribution of MSN-*x* from TEM images shown in Figure 1. a) MSN-0.01, b) MSN-0.025, c) MSN-0.1, d) MSN-2.5, and 4) MSN-8.



Figure S2. NH₃-TPD profiles of the supported PTA catalysts on the as-synthesized MSN-*x* carriers. a) *x*=0.01, b)

x=0.025, c) *x*=0.1, d) *x*=2.5, e) *x*=8.

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Figure S3. N₂ adsorption-desorption isotherms (a) and the Barrett-Joyner-Halenda (BJH) pore size distribution from adsorption branch of the supported PTA catalysts on the diverse mesoporous silica nanospheres (MSN-*x*).



Figure S4. Catalytic performance of PTA/MSN-*x* catalysts (*x*=0.01, 0.025, 0.1, 2.5, and 8) for alkenylation of *p*-xylene with phenylacetylene. Reaction conditions: catalyst 0.8 g; $N_{p-xylene/Phen}$ 25:1; T_r 150 °C; P_s 1.0 MPa; *VHSV* 7.2 ml h⁻¹ g⁻¹cat; *TOS* 8 h.



Figure S5. Low-angle XRD patterns of 25 wt % PTA/MSN-0.025 catalyst and bare MSN support.



Figure S6. XRD patterns of the PTA/MSN-0.025, PTA/MCM-41, and bulk PTA.