## **Electronic supplementary information**

## Synergistic activating effect of promoter and oxidant in single step conversion of methane into methanol over tailored polymer-Ag coordination complex.

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M = Ag/Fe/Cu

Scheme. S1. Synthetic path way of polymer-metal complexes and their possible structures



Fig. S1. Thermogravimetric analysis (TGA) spectra obtained for Ch and prepared catalysts

The TGA curve for 'Ch' gave two sharp peaks. One below 100 and other starts at 230 <sup>o</sup>C which are attributed to loss of moisture and functional groups respectively. A continues slow degradation of Ch was observed after 400 <sup>o</sup>C which informs that the 'Ch' forming carbon at higher temperatures. After complexation the temperature required for functional groups degradation was slightly high. This is because of the strong coordination of functional groups of Ch to metal.



Fig. S2. High resolution XPS spectra for different regions of Cuch (upper row) and FeCh (lower row)



Fig. S3. Transmission Electron Microscopy (TEM) images for (a,b) FeCh and (c,d) CuCh at different magnification



Fig. S4. Ion chromatogram obtained after analyzing liquid products.



Fig. S5. FESEM- Energy Dispersive X-Ray (EDX) spectroscopic analysis for prepared catalysts.

Field Emission Scanning Electron Microscopy (FESEM) images were recorded using a Sigma Z300 instrument equipped with an energy dispersive X-ray spectrometer (EDS).



Fig. S6. FESEM elemental mapping for prepared catalysts

Serial	Sample	Test Item	value	Unit
1	AgCh	Ag	20564.95	mg/Kg
2	FeCh	Fe	86038.45	mg/Kg
3	CuCh	Cu	84970.03	mg/Kg

## Table S1 (a). Metal concentration in catalysts detected by ICP-AES technique

Table S1 (b). C, H, N & S elemental concentration in catalysts

Serial	Sample	Mass (mg)	N (wt%)	C(wt%)	H(wt%)
1	Ch	1.781	7.45	41.27	7.31
2	AgCh	1.776	7.30	39.48	7.17
3	FeCh	1.768	6.41	34.85	6.26
4	CuCh	1.761	6.31	35.03	6.30

**Table S2.** Product quantification and percentage of  $CH_4$  conversion for different pristine materials usedfor catalyst preparation

Entry	Catalyst	oxidant <sup>.</sup>	Product formed (µmol)				CH <sub>4</sub>
			CH <sub>3</sub> OH	нсоон	CH <sub>3</sub> COOH	<b>CO</b> <sub>2</sub>	(%)
1	FeNO <sub>3</sub> .9H <sub>2</sub> O	$\mathrm{H}_{2}\mathrm{O}_{2}$	-	24	-	-	0.02
2	CuNO <sub>3</sub> .5H <sub>2</sub> O	$H_2O_2$	-	264	-	12.3	0.20
3	AgNO <sub>3</sub>	$H_2O_2$	-	490	-	15.2	0.38
4	Ch	$H_2O_2$	12	24	2	0	0.03



Fig. S7 (a) Effect of CH<sub>4</sub> pressure on the reaction: 150 mg catalyst, 3 hr, 60  $^{0}$ C (b) reusability data: 30 bar, 150 mg catalyst, 60  $^{0}$ C

Fig S7 (a) informs that, the  $3 \times 10^6$  Pa pressure is appropriate for the CH<sub>4</sub> to methanol conversion reaction using AgCh catalyst. A pressure higher than this, causes instability in the catalyst to bear pressure. The catalyst appeared to lose the coordination with metal after 3.5 10<sup>6</sup> Pa pressure. A cyclic performance of the AgCh catalyst is shown in Fig.S7 (b). There was continues decrease in catalytic activity. This may be due to loss in active sight which occurs in case of coordination complexes<sup>1</sup>.

Catalyst	Additives	Temperature (°C)	CH <sub>4</sub> conversion (%)	Methanol selectivity (%)	Ref.
Al/ZSM-5	Fe	50	0.2	22	[2]
Cu-Fe/ZSM-5	-	50	0.7	85	[2]
Cu/Silicates-1	-	50	0	0	[2]
Fe-Silicate	-	70	10.5	8	[2]
AgCh	[BMIM] <sup>+</sup> Cl <sup>-</sup>	60	4.5	0	This work
AgCh	[BMIM] <sup>+</sup> Cl <sup>-</sup> O <sub>2</sub>	60	4	54	This work
Au <sup>0</sup>	2% SO <sub>3</sub>	180	0	0	[3]
$Au^0$	3 M SeO <sub>3</sub> + 2% SO <sub>3</sub>	180	28	94	[3]
ZSM-5	-	50	1.1	11.6	[4]

Table S3. Catalysts comparison from literature for CH<sub>4</sub> conversion and methanol selectivity

Catalyst	Specifications	TON <sup>[a]</sup>	Ref.
Cu-ZSM-5	No solvent used	0.02	5
(Bipym)Pt <sup>II</sup> Cl <sub>2</sub>	H <sub>2</sub> SO <sub>4</sub> , Ionic liquid	0.5	6
Pd(OAc) <sub>2</sub> , NaNO <sub>2</sub> , O <sub>2</sub> , Benzoquinone	CF <sub>3</sub> COOH	3~7	7
FeCl <sub>3</sub>	aqueous	7	8
PdSO <sub>4</sub>	$H_2SO_4$	14.2	9
sMMO		19	10
AgCh	$H_2O_2$	22	This work
CuCh	$H_2O_2$	2	This work
FeCh	$H_2O_2$	3	This work
(FetBuPc) <sub>2</sub> N/SiO <sub>2</sub>	$H_2O_2$ , $H_2SO_4$	209	11
K <sub>2</sub> [PtCl <sub>4</sub> ]-CTF	30% Oleum	<250	12
AgCh	H <sub>2</sub> O <sub>2</sub> , [BMIM] <sup>+</sup> Cl <sup>-</sup>	301	This work
AgCh, O <sub>2</sub>	H <sub>2</sub> O <sub>2</sub> , [BMIM] <sup>+</sup> Cl <sup>-</sup>	266	This work
AgCh	H <sub>2</sub> O <sub>2</sub> , [BMIM] <sup>+</sup> Br <sup>-</sup>	144	This work
AgCh, O <sub>2</sub>	H <sub>2</sub> O <sub>2</sub> , [BMIM] <sup>+</sup> Br <sup>-</sup>	135	This work

Table S4. Catalysts comparison for CH<sub>4</sub> conversion to its oxygenates in terms of TON

[a] TON = Total moles of oxygenated produced/moles of Ag utilized for the reaction



Fig. S8. A rough diagram of the instrumentation used to carry out the reaction

## Notes and references

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