

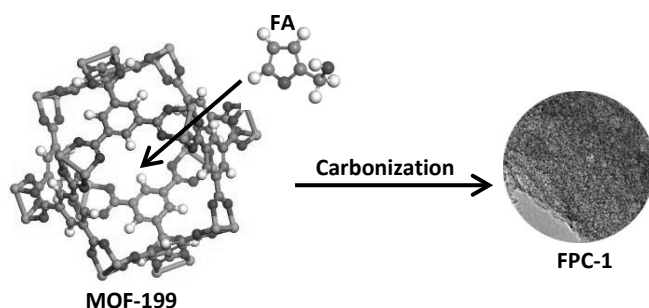
Supporting information for

Copper-Containing Porous Carbon Derived from MOF-199 for Dibenzothiophene Adsorption

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Scheme S.I.1 Schematic procedure for porous carbon from MOF-199

Figure captions:

Fig. S.I.1 Langmuir linear model of DBT on the FPC-1 in ALO, ARO and MIO, respectively.

Fig. S.I.2 Freundlich linear model of DBT on the FPC-1 in ALO, ARO and MIO, respectively.

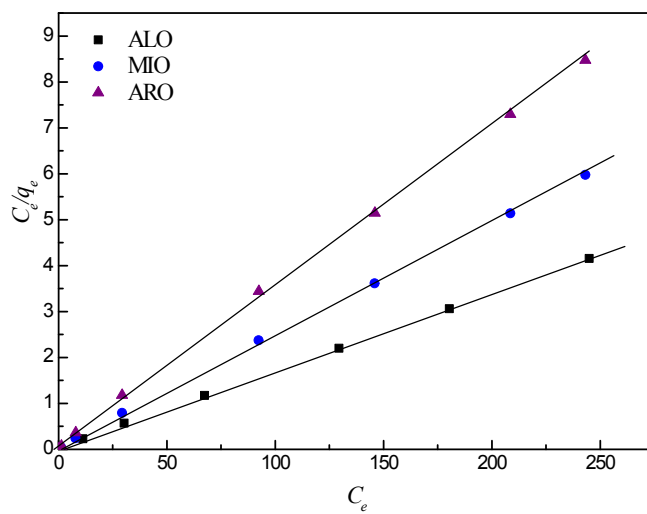


Fig. S.I.1 Langmuir linear model of DBT on the FPC-1 in ALO, ARO and MIO, respectively.

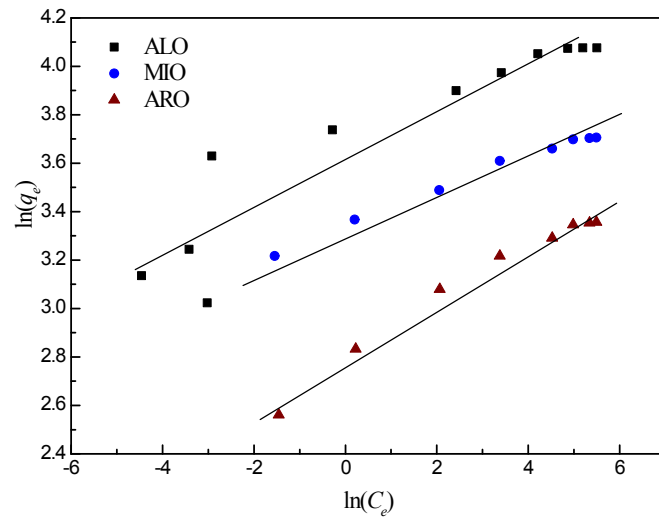


Fig. S.I.2 Freundlich linear model of DBT on the FPC-1 in ALO, ARO and MIO, respectively.

Table captions:**Table S.I.1** Comparison of sulfur adsorption capacity**Table S.I.2** Constants and correlation coefficients of Langmuir and Freundlich models.**Table S.I.1** Comparison of sulfur adsorption capacity

Adsorbents	Solvents	q_{max} ($\mu\text{gS/g}$)	References
FPC-1	ALO	59.1	this work
FPC-1	ARO	28.9	this work
FPC-1	MIO	40.9	this work
Activated carbon	n-octane	28.9	[31]
Cu(I)-Y zeolite	n-octane	32.6	[32]
Co-Y zeolite	n-octane	29.4	[32]
Ce/Ni-Y zeolite	n-octane	22.2	[33]
Activated Al_2O_3	n-hexane	21.0	[34]
CMK-3	n-hexane	10.9	[35]
ZIF-8-derived	n-hexane	26.7	[36]
ZIF-8-derived	n-hexane: Para-xylene (9:1)	22.2	[36]

*All the sulfur uptake capacity is the content of sulfur element ($\mu\text{gS/g}$).

Table S.I.2 Constants and correlation coefficients of Langmuir and Freundlich models.

Model oil	Langmuir				Freundlich		
	q_L (mg/g)	K_L (L/g)	R^2	R_L	K_f (L/mg)	$1/n$	R^2
ALO	59.10	1.12	0.9999	0.427	37.34	0.097	0.9324
ARO	28.87	0.78	0.9997	0.517	16.28	0.112	0.9883
MIO	40.87	0.55	0.9998	0.602	28.22	0.069	0.9957