

## Supplementary Information

### Synthesis of dimethyl carbonate from CO<sub>2</sub> and methanol over hydrophobic Ce/SBA-15 catalyst

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Scale bars are 2 nm.

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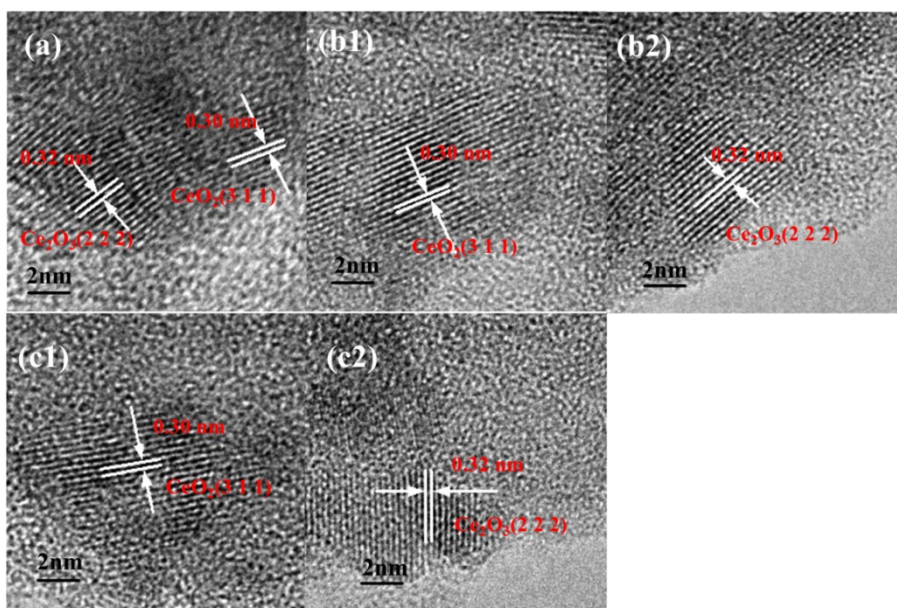
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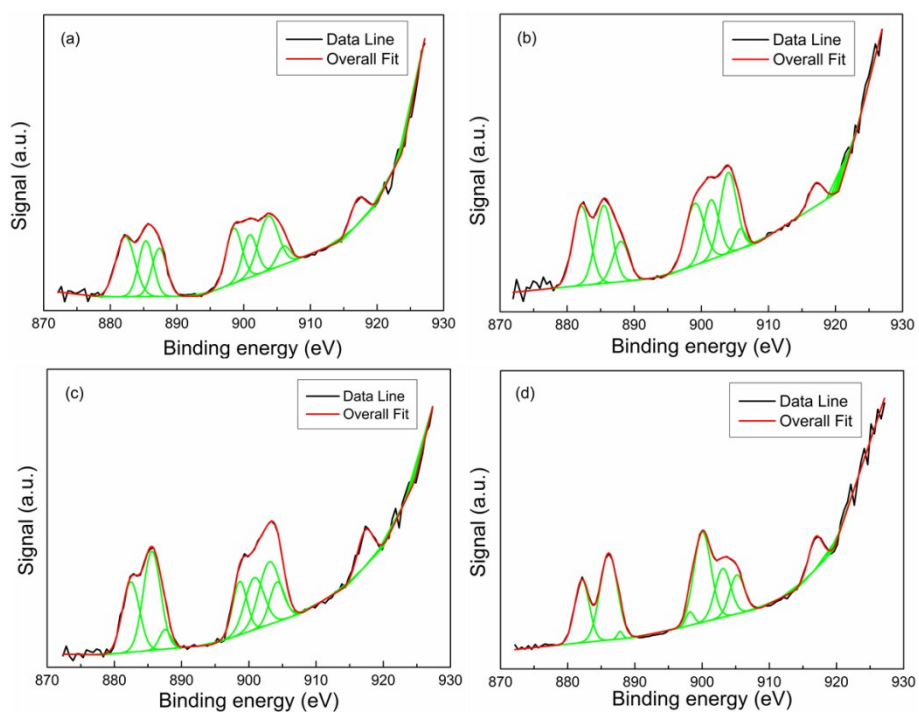
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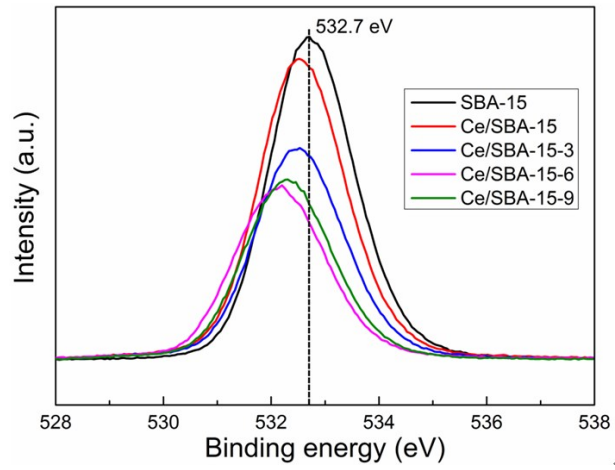
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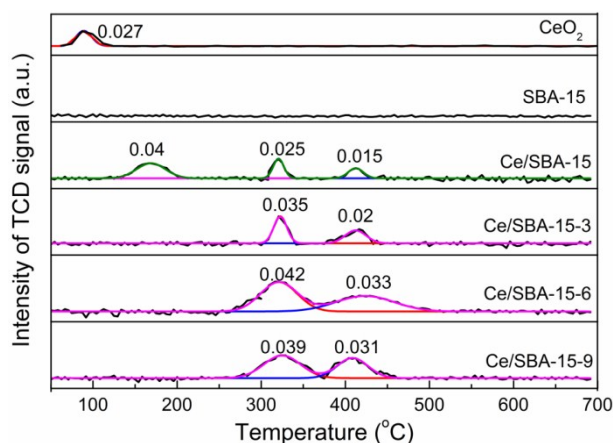
**Fig. S1.** TEM images of catalysts for SBA-15 (a); Ce/SBA-15 (b1, b2); Ce/SBA-15-6 (c1, c2). Scale bars are 2 nm.



**Fig. S2.** Ce 3d XPS spectra of the catalysts: Ce/SBA-15 (a); Ce/SBA-15-3 (b); Ce/SBA-15-6 (c); Ce/SBA-15-9 (d).



**Fig. S3.** O1s spectra of SBA-15, Ce/SBA-15 and Ce/SBA-15-X (X=3, 6, 9) catalysts.

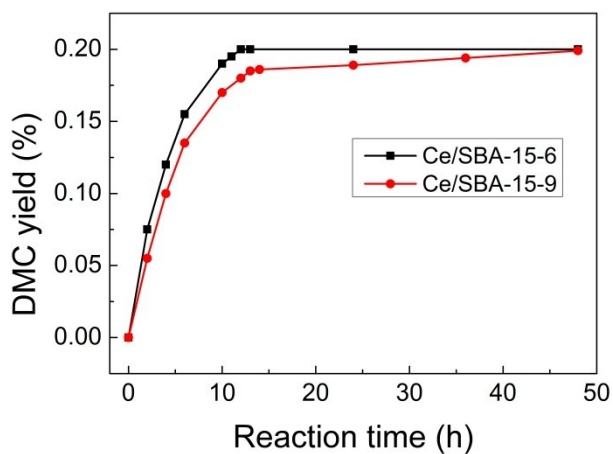


**Fig. S4.** CO<sub>2</sub>-TPD profiles of CeO<sub>2</sub>, SBA-15, Ce/SBA-15 and Ce/SBA-15-X (X=3, 6, 9) catalysts. Adsorption amount of CO<sub>2</sub> was measured by the volumetric methods, the unit “mmol·gcat<sup>-1</sup>”

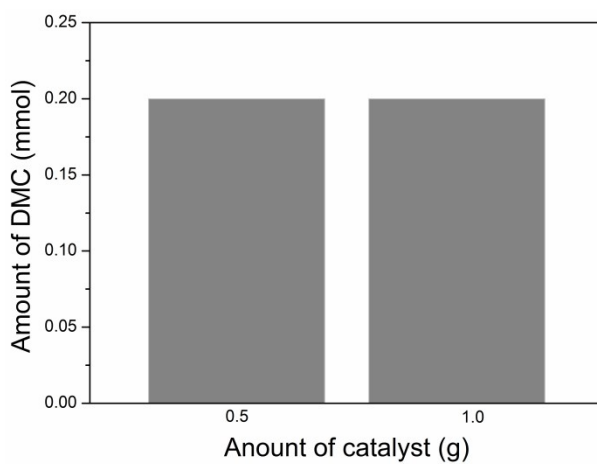
In order to evaluate the desorbed CO<sub>2</sub> amount excluding CO<sub>2</sub> derived from the organic species on SBA-15, the samples were desorbed directly without CO<sub>2</sub> adsorption after the Ar purification, and then the obtained value was used as curve( i ).

The detailed procedure was as follows: Temperature programmed desorption of CO<sub>2</sub> (CO<sub>2</sub>-TPD) were carried out on the GAM 200 Mass Spectrometer for the measurement of the acidity- basicity of the catalysts. Each sample (50 mg) was placed in the quartz reactor and pretreated in an Ar flow (40 mL min<sup>-1</sup>) at 500 °C for 1 h. the purified samples was then cooled to 50 °C, followed by an Ar purge for 1 h to remove the physisorbed CO<sub>2</sub>. The desorption process was performed at a heating rate of 10 °C min<sup>-1</sup> from 50 °C to 500 °C and the evolved CO<sub>2</sub> was monitored with a thermal conductivity detector (TCD), and quantitatively analyzed by the external standard method.

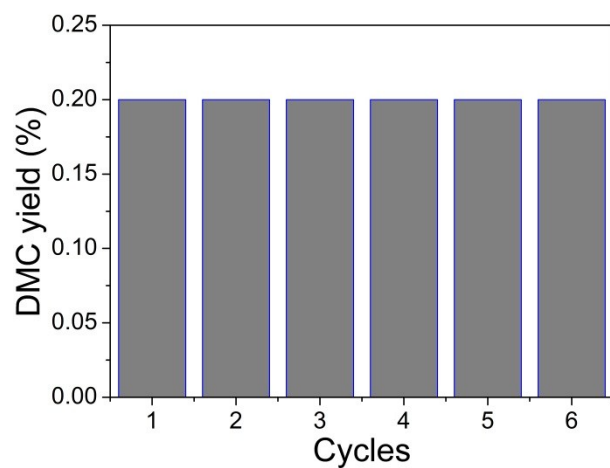
Furthermore, the samples with CO<sub>2</sub> adsorption were desorbed (the detailed procedure was as the “**2.2 Physical Characterization**”) were used as the curve( ii ). Then, curve( ii ) subtracted curve( i ) equaled to the results curve and shown in the **Fig. S4**.



**Fig. S5.** Effects of the reaction time on DMC yield over Ce/SBA-15-6 and Ce/SBA-15-9 catalysts. Reaction conditions: 130 °C; CH<sub>3</sub>OH weight, 6.4 g; CO<sub>2</sub>, 100 mmol; reaction pressure (P) = 10 MPa; catalyst weight, 0.5 g.



**Fig. S6.** DMC yield over Ce/SBA-15-6 catalyst with the different catalyst amount (0.5 g; 1.0 g). Reaction conditions: 130 °C; 12 h; CH<sub>3</sub>OH, 6.4 g; CO<sub>2</sub>, 100 mmol; reaction pressure (P) = 10 MPa;.



**Fig. S7.** DMC yield during recycling of Ce/SBA-15-6 as a catalyst, 12 h for each cycle. Reaction conditions: 130 °C; CH<sub>3</sub>OH weight, 6.4 g; CO<sub>2</sub>, 100 mmol; reaction pressure (P) = 10 MPa; catalyst weight, 0.5 g.