

Supporting Information

Heterogeneous catalytic ozonation of ciprofloxacin in aqueous solution using a manganese-modified silicate ore

Lisha Luo^{ab}, Donglei Zou^a, Dongwei Lu^{c*}, Bingjing Xin^b, Ming Zhou^b, Xuedong Zhai^c and Jun Ma^{c*}

^a Key Laboratory of Ministry of Education for Groundwater Resources and Environment, College of New Energy and Environment, Jilin University, Changchun 130000, P. R. China

^b Jilin Institute of Chemical Technology, Jilin 130022, P. R. China

^c State Key Laboratory of Urban Water Resource and Environment, Harbin Institute of Technology, Harbin 150090, PR China. E-mail: lvdongwei@hit.edu.cn

Table S1 BET of the SO and MnSO

Sample	BET ($\text{m}^2 \text{g}^{-1}$)	Pore volume ($\text{cm}^3 \text{g}^{-1}$)	Average pore size (nm)
SO	75.56	0.24	12.95
MnSO	59.11	0.16	10.9

Table S2 First-order kinetic parameters of the CIP removal during different oxidation processes

	k (min^{-1})	R^2
SO/O ₂	0.014	0.9934
MnSO/O ₂	0.009	0.9940
O ₃	0.025	0.9993
SO/O ₃	0.043	0.9955
MnSO/O ₃	0.083	0.9968

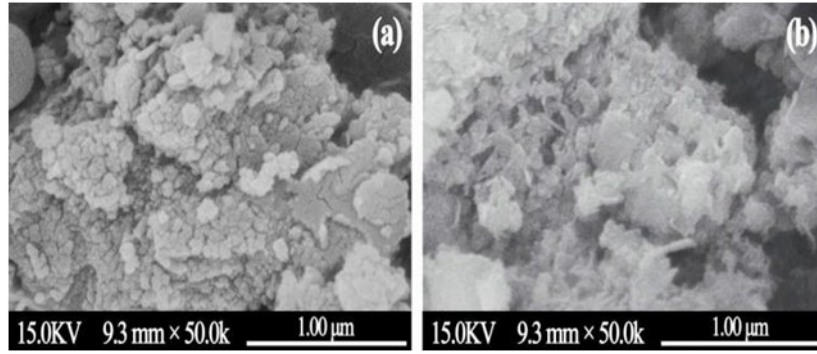


Fig. S1 SEM images of the samples SO (a) and MnSO (b).

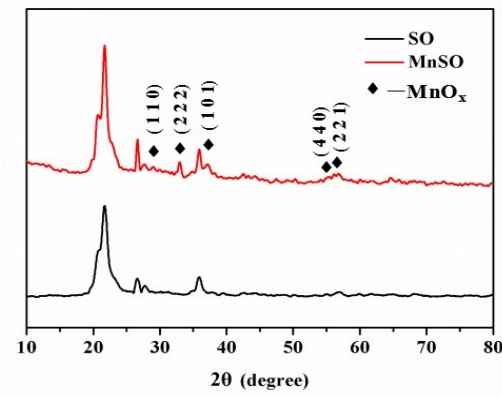


Fig. S2 XRD of the SO and MnSO catalyst.

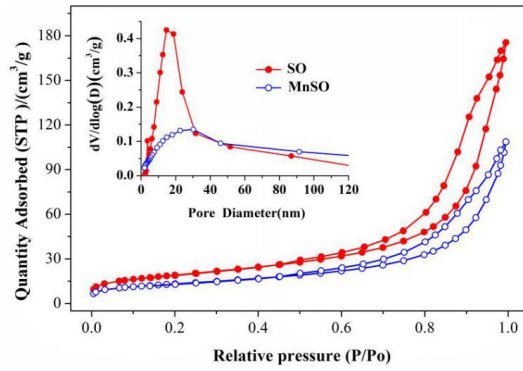


Fig. S3 N₂ adsorption-desorption isotherms of the SO and MnSO

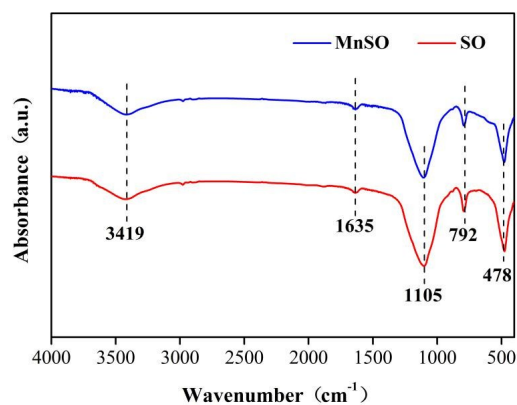


Fig. S4 FTIR spectra of SO and MnSO.

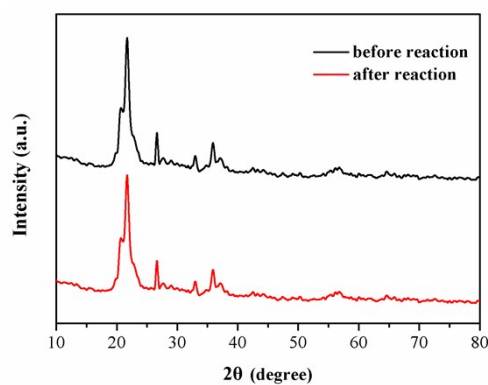


Fig. S5 XRD of MnSO before and after catalytic ozonization of CIP

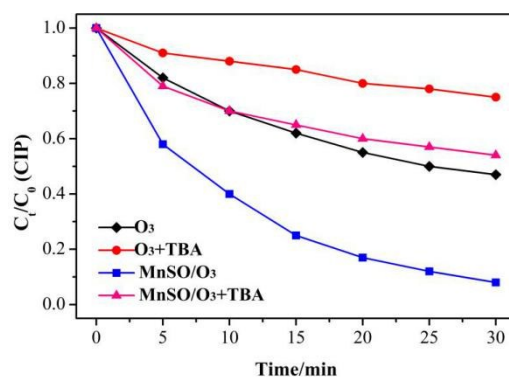


Fig. S6 Effect of TBA on CIP degradation.

(experimental conditions: pH = 7.0, $C_0 = 20 \text{ mg L}^{-1}$; ozone gas flow rate = 0.3 L min^{-1} ; ozone gas concentration = 0.4 mg min^{-1} ; catalyst dose = 0.5 g L^{-1} ; $T = 20 \text{ }^\circ\text{C}$; TBA = 100 mg L^{-1}).

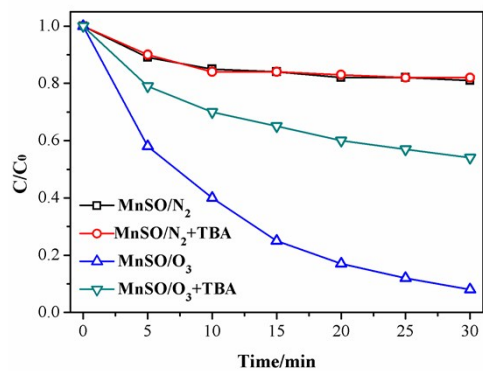


Fig. S7 The system of replace O₃ by N₂ on CIP degradation.

(experimental conditions: pH = 7.0, C₀ = 20 mg L⁻¹; N₂ flow rate = 0.3 L min⁻¹; catalyst dose = 0.5 g L⁻¹; T = 20 °C; ozone gas flow rate = 0.3 L min⁻¹; ozone gas concentration = 0.4 mg min⁻¹; TBA=100 mg L⁻¹).