

**Open metal sites(OMSs) and Lewis basic sites(LBSs) -functionalized copper-organic framework with high CO<sub>2</sub> uptake performance and highly selective CO<sub>2</sub>/N<sub>2</sub> and CO<sub>2</sub>/CH<sub>4</sub> separation**

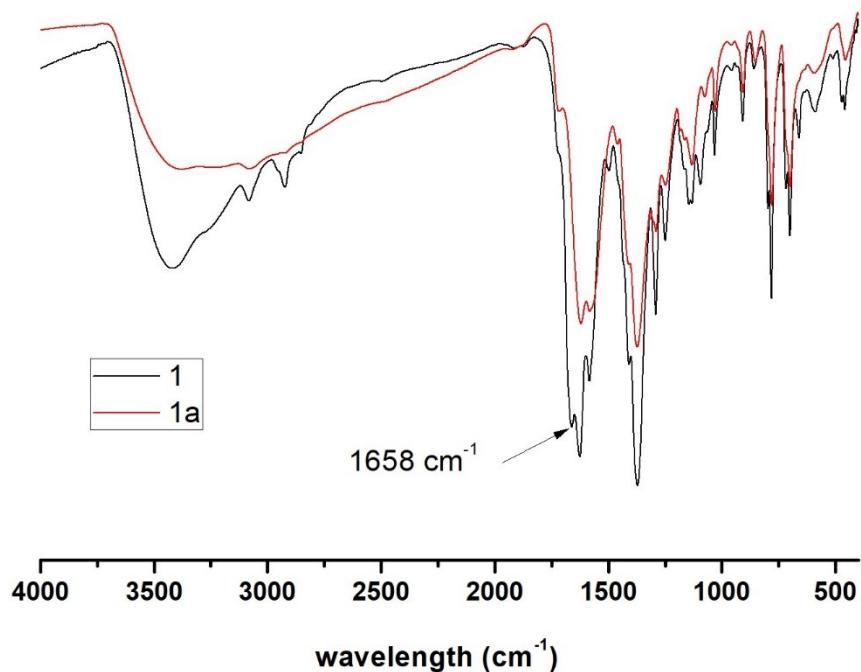
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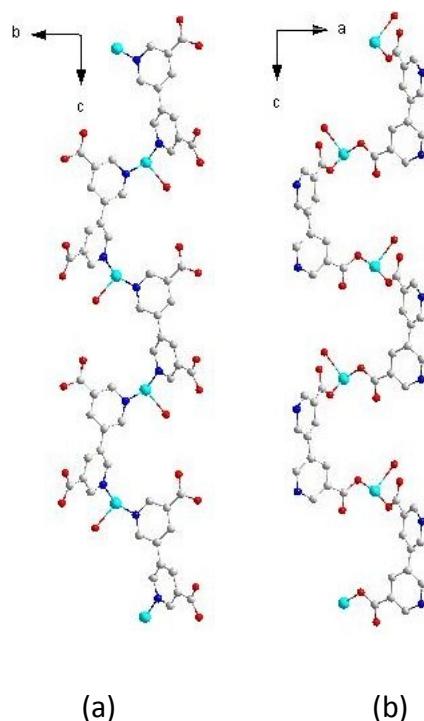
**Table S1.** Selected Bond Lengths (Å) and Angles (deg) for Complex **1<sup>a</sup>**

<b>1</b>			
Cu1-N1#1	1.98(5)	Cu1-N2	2.003(9)
Cu1-O5	2.11(7)	Cu2-O2	1.945(15)
Cu2-O4#2	1.974(16)	Cu2-O6	2.20(6)
N1#1-Cu1-N1#3	80(5)	N1#1-Cu1-N2#4	160.6(15)
N1#3-Cu1-N2#4	95(2)	N2-Cu1- N2#4	83.5(16)
N1#1-Cu1-O5	97.4(18)	N1#3-Cu1-O5	97(2)
N2-Cu1-O5	101.9(17)	O2-Cu2-O2#5	86.2(13)
O2-Cu2-O4#6	88.7(9)	O2-Cu2-O4#7	167.4(7)
O4#6-Cu2-O4#7	93.9(13)	O2-Cu2-O6	99.5(11)
O4#6-Cu2-O6	92.7(10)		

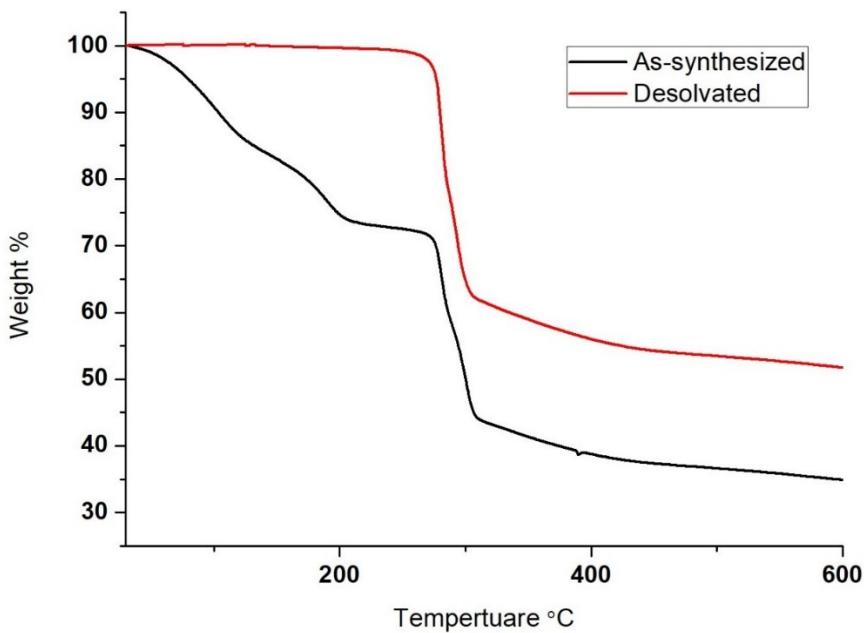
<sup>a</sup> Symmetry transformations used to generate equivalent atoms: #1 x, -y+1/2, z+1/2; #2 -x+1/2, -y+1, z-1/2; #3 -x+1, -y+1/2, z+1/2; #4 -x+1, y, z; #5 x, -y+1, z; #6 -x+1/2, y, z-1/2, #7 -x+1/2, -y+1, z-1/2.



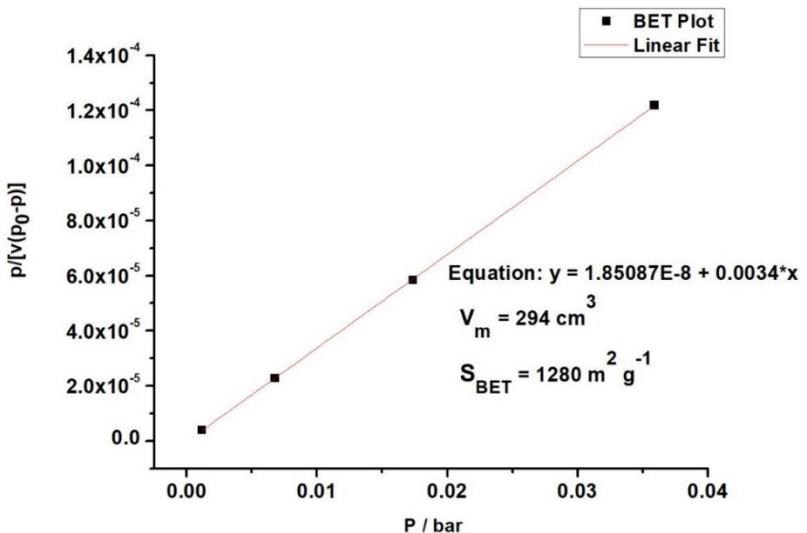
**Fig. S1** The FT-IR spectra of **1** and **1a**. The characteristic C=O vibration at  $1658\text{ cm}^{-1}$  of DMA in **1** is absent in **1a**, indicating the complete removal of DMA.



**Fig. S2** The zigzag 1D chains along c-axis, with Cu1-Cu1 distance of  $7.736\text{ \AA}$  for (a) and Cu2-Cu2 distance of  $7.770\text{ \AA}$  for (b).



**Fig. S3** TGA curves



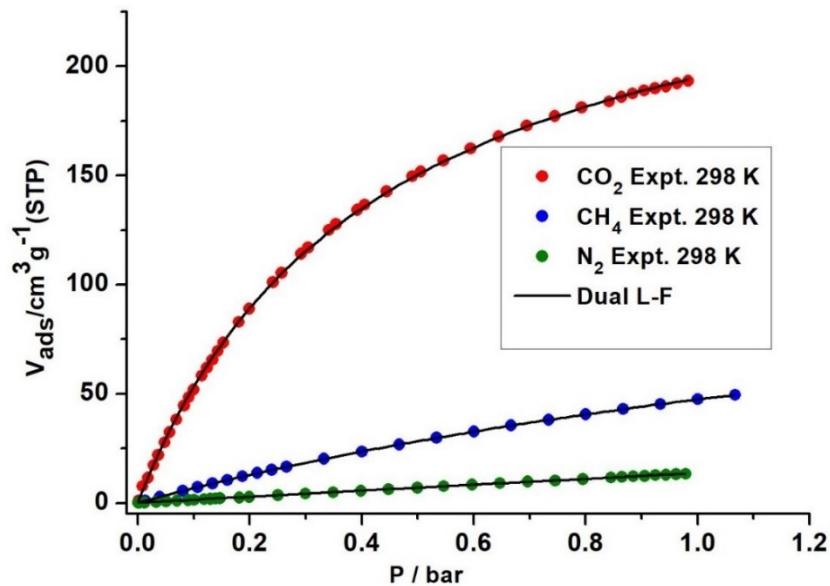
**Fig. S4** The BET plot calculated from  $\text{N}_2$  isotherm of **1a**

**Table S2** Comparison of the best  $\text{CO}_2$  adsorption performances of MOFs. Note: the highest values of each parameter were highlighted in boldface.

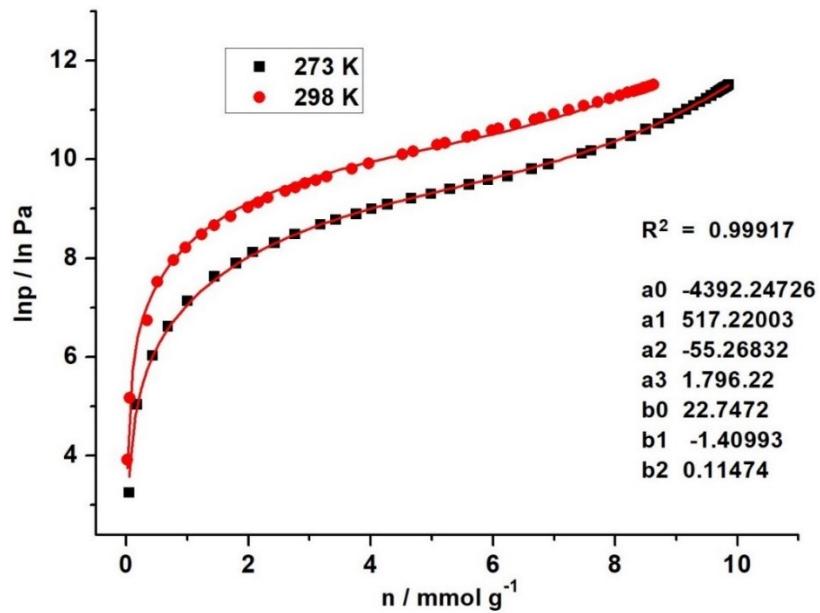
MOF (common name)	$D_c$ ( $\text{g cm}^{-3}$ )	CO <sub>2</sub> uptake at 298 K and 1 bar		Ref
		(mmol g <sup>-1</sup> )	(mmol cm <sup>-3</sup> )	

Mg-MOF-74	0.920	<b>8.6</b>	7.912	S1
MAF-X27ox	1.354	6.70	9.07	S2
MAF-X25ox	1.227	7.14	8.76	S2
FJI-H14	1.167	7.63	8.91	S3
[Cu <sub>2</sub> (BPDC) <sub>2</sub> ]	1.147	<b>8.6</b>	<b>9.86</b>	<b>This work</b>
Co <sub>2</sub> (dobdc)	1.177	6.96 <sup>#1</sup>	8.20 <sup>#1</sup>	S4
Ni <sub>2</sub> (dobdc)	1.194	5.8 <sup>#1</sup>	6.93 <sup>#1</sup>	S4
SIFSIX-2-Cu-i	1.246	5.41	6.74	S5
MAF-66	1.128	5.0	5.6	S6
HKUST-1	0.879	4.86	4.27	S7
bio-MOF-11	1.234	5.0	6.17	S8

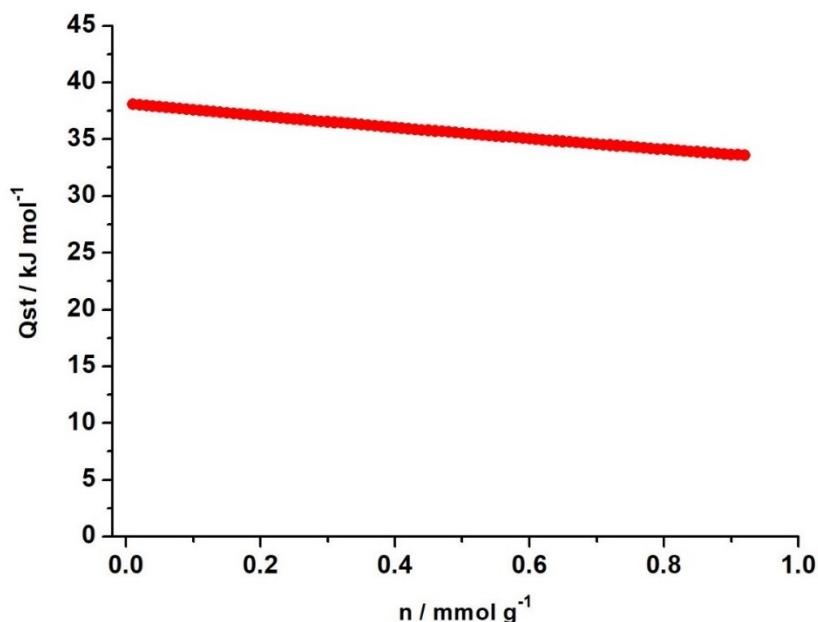
dobdc = 4,4'-dioxido-3,3'biphenyldicarboxylate; SIFSIX= SiF<sub>6</sub><sup>2-</sup> anions. <sup>#1</sup> 296 K.



**Fig. S5** The adsorption isotherms of CO<sub>2</sub>, CH<sub>4</sub> and N<sub>2</sub> at 298 K along with the dual-site Langmuir Freundlich (DSLF) fits.



(a)



(b)

**Fig. S6** (a) The calculated virial equation isotherms parameters fit to the experimental  $\text{CO}_2$  data of **1a**. (b) The isosteric adsorption enthalpy for **1a**.

#### $\text{CO}_2/\text{N}_2$ and $\text{CO}_2/\text{CH}_4$ Selectivity Prediction by IAST Model

The experimental isotherm data for pure CO<sub>2</sub> was fitted using a dual Langmuir-Freundlich (L-F) model (equation (1)) and the experimental isotherm data for pure N<sub>2</sub> or CH<sub>4</sub> was fitted using Langmuir-Freundlich (L-F) model (equation (2)):

$$q = \frac{M_1 * K_1 * p}{1 + K_1 * p} + \frac{M_2 * K_2 * p}{1 + K_2 * p} \quad (1)$$

$$q = \frac{M * K * p}{1 + K * p} \quad (2)$$

Where q and p are adsorbed amounts and the pressure of component i, respectively.

The adsorption selectivities for binary mixtures of CO<sub>2</sub>/N<sub>2</sub> and CO<sub>2</sub>/CH<sub>4</sub> were respectively calculated using the Ideal Adsorption Solution Theory (IAST), defined by

$$S_{i/j} = \frac{x_i * y_i}{x_j * y_j}$$

Where x<sub>i</sub> is the mole fraction of component i in the adsorbed phase and y<sub>i</sub> is the mole fraction of component i in the bulk.

### Estimation of the isosteric heats of gas adsorption

A virial-type<sup>59</sup> expression comprising the temperature-independent parameters *a<sub>i</sub>* and *b<sub>i</sub>* was employed to calculate the enthalpies of adsorption for CO<sub>2</sub> (at 273 and 298 K) on **1a**. In each case, the data were fitted using the equation:

$$\ln P = \ln N + 1/T \sum_{i=0}^m a_i N^i + \sum_{j=0}^n b_j N^j$$

Here, *P* is the pressure expressed in Pa, *N* is the amount adsorbed in mmol g<sup>-1</sup>, *T* is the temperature in K, *a<sub>i</sub>* and *b<sub>j</sub>* are virial coefficients, and *m*, *n* represent the number of coefficients required to adequately describe the isotherms (*m* and *n* were gradually increased until the contribution of extra added *a* and *b* coefficients was deemed to be statistically insignificant towards the overall fit, and the average value of the squared deviations from the experimental values was minimized). The values of the virial

coefficients  $a_0$  through  $a_m$  were then used to calculate the isosteric heat of adsorption using the following expression.

$$Q_{st} = -R \sum_{i=0}^m a_i N^j$$

$Q_{st}$  is the coverage-dependent isosteric heat of adsorption and  $R$  is the universal gas constant.

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