

Electronic Supporting Information

Cu/SAPO-34 prepared by a facile ball milling method for enhanced catalytic performance in selective catalytic reduction of NO_x with NH₃

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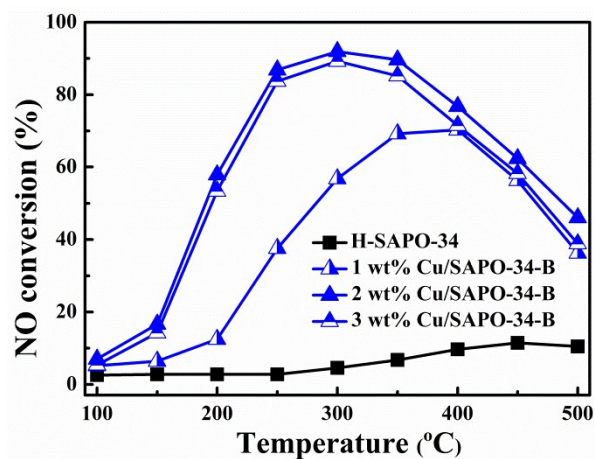


Fig. S1. NO conversion as a function of temperature over Cu/SAPO-34-B catalysts with different Cu loadings. Reaction conditions: $[\text{NO}] = [\text{NH}_3] = 500$ ppm, $[\text{O}_2] = 5\%$, N_2 balance, total flow rate 200 mL min^{-1} and GHSV = $200\,000 \text{ h}^{-1}$.

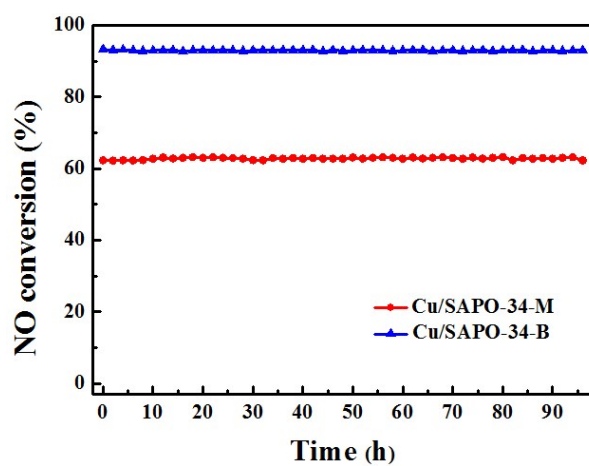


Fig. S2. NH₃-SCR lifetime tests of Cu/SAPO-34-M and Cu/SAPO-34-B at 400 and 350 °C, respectively. Reaction conditions: [NO] = [NH₃] = 500 ppm, [O₂] = 5%, N₂ balance, total flow rate 200 mL min⁻¹ and GHSV = 200 000 h⁻¹.

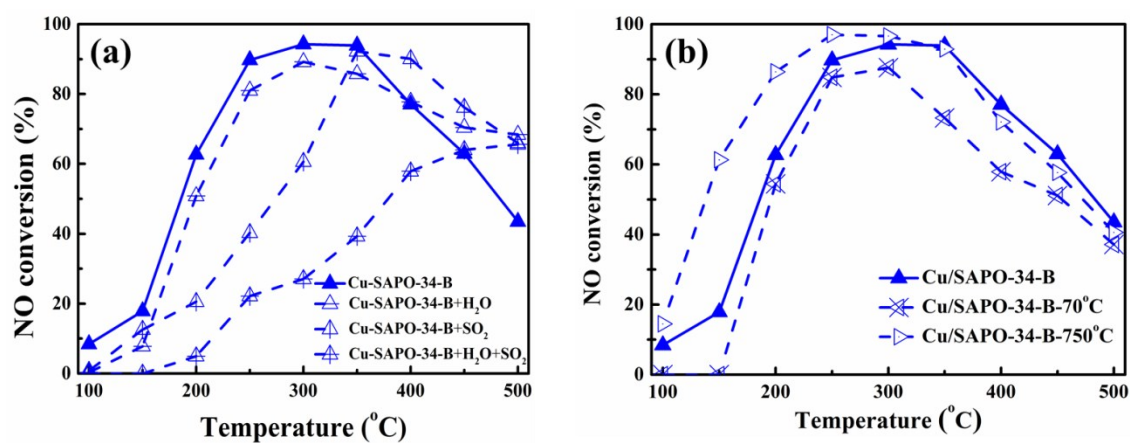


Fig. S3. (a) NO conversion as a function of temperature over Cu/SAPO-34-B catalyst in the presence of H₂O and SO₂. (b) NO conversion as a function of temperature over Cu/SAPO-34-B catalyst after hydrothermal treatments at high and low temperature. Reaction conditions: [NO] = [NH₃] = 500 ppm, [O₂] = 5%, [H₂O] = 5% (when used), [SO₂] = 100 ppm (when used), N₂ balance, total flow rate 200 mL min⁻¹ and GHSV = 200 000 h⁻¹.

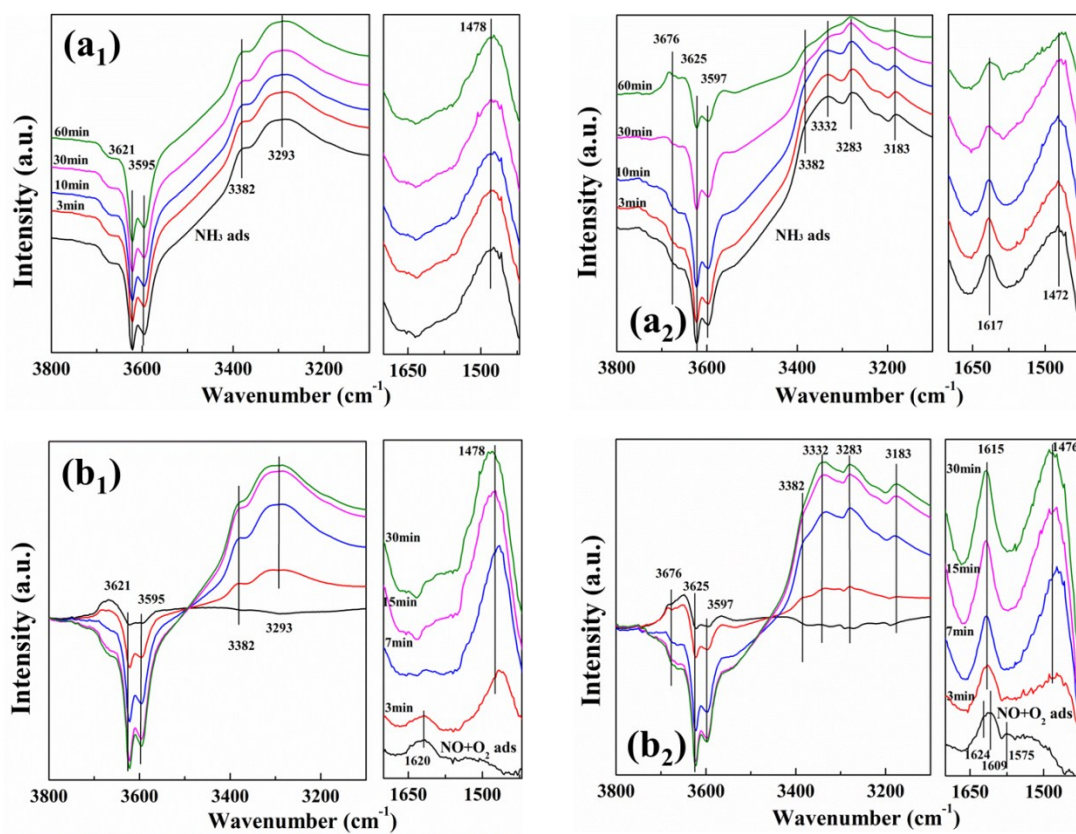


Fig. S4. Consumption of NH_4^+ ions and coordinated NH_3 at 150 °C upon passing $\text{NO}+\text{O}_2$ over Cu/SAPO-34-M (a₁) and Cu/SAPO-34-B (a₂) with preadsorbed NH_3 . Consumption of the adsorbed NO_x species at 150 °C upon passing NH_3 over Cu/SAPO-34-M (b₁) and Cu/SAPO-34-B (b₂) with preadsorbed $\text{NO}+\text{O}_2$.

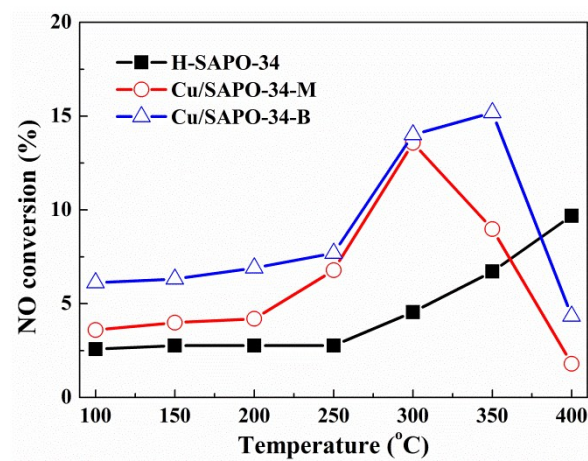


Fig. S5. NO conversion as a function of temperature over Cu/SAPO-34-M and Cu/SAPO-34-B samples before calcination. Reaction conditions: $[\text{NO}] = [\text{NH}_3] = 500 \text{ ppm}$, $[\text{O}_2] = 5\%$, N_2 balance, total flow rate 200 mL min^{-1} and GHSV = $200\,000 \text{ h}^{-1}$.