

**Supplementary information**

Macroscopic assembly style of catalysts significantly determining their efficiency for  
converting CO<sub>2</sub> to gasoline

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Table S1. Reaction performances of Fe–Zn–Zr@HZSM-5 core–shell catalysts with different SiO<sub>2</sub>/Al<sub>2</sub>O<sub>3</sub> molar ratios of HZSM-5 on CO<sub>2</sub> hydrogenation.

Catalysts	CO <sub>2</sub> conv. (%)	Selectivity (mol%)			Hydrocarbon distribution (C-mol %)			I-C <sub>5+</sub> /C <sub>5+</sub> (%)	Aromatics /C <sub>5+</sub> (%)
		CO	Oxy	HC	C <sub>1</sub>	C <sub>2-4</sub>	C <sub>5+</sub>		
Fe–Zn–Zr@HZSM-5(38)	22.5	42.0	0.0	58.0	1.3	53.3	45.4	75.4	19.7
Fe–Zn–Zr@HZSM-5(50)	21.2	42.8	0.1	57.1	1.5	42.3	56.2	90.6	6.4
Fe–Zn–Zr@HZSM-5(100)	22.5	83.0	14.7	2.3	69.2	20.3	10.5	87.6	0.0
Fe–Zn–Zr/HZSM-5(50)	19.7	45.1	0.0	54.9	1.4	55.0	43.6	74.4	19.9

5.0 MPa; 340 °C; 6 h; 3000 ml/g/h; H<sub>2</sub>/CO<sub>2</sub>/N<sub>2</sub>=72/24/4; Fe–Zn–Zr:HZSM-5=4:1 (weight ratio).

Oxy=oxygen compounds (MeOH+Me<sub>2</sub>O); HC=hydrocarbon.

I-C<sub>5+</sub>=C<sub>5+</sub> isoalkanes; C<sub>5+</sub>=C<sub>5+</sub> hydrocarbons.

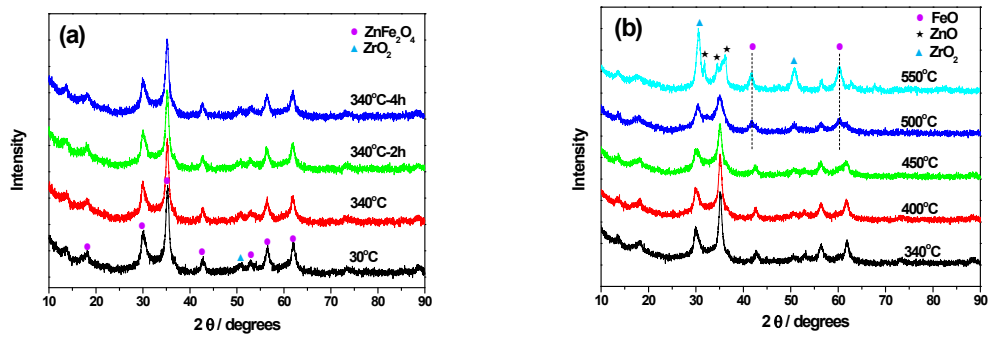


Fig. S1. In situ XRD patterns of Fe–Zn–Zr core. (a) Reduced at 340 °C with different time, (b) Reduced at different temperature and keep 0.5 h.

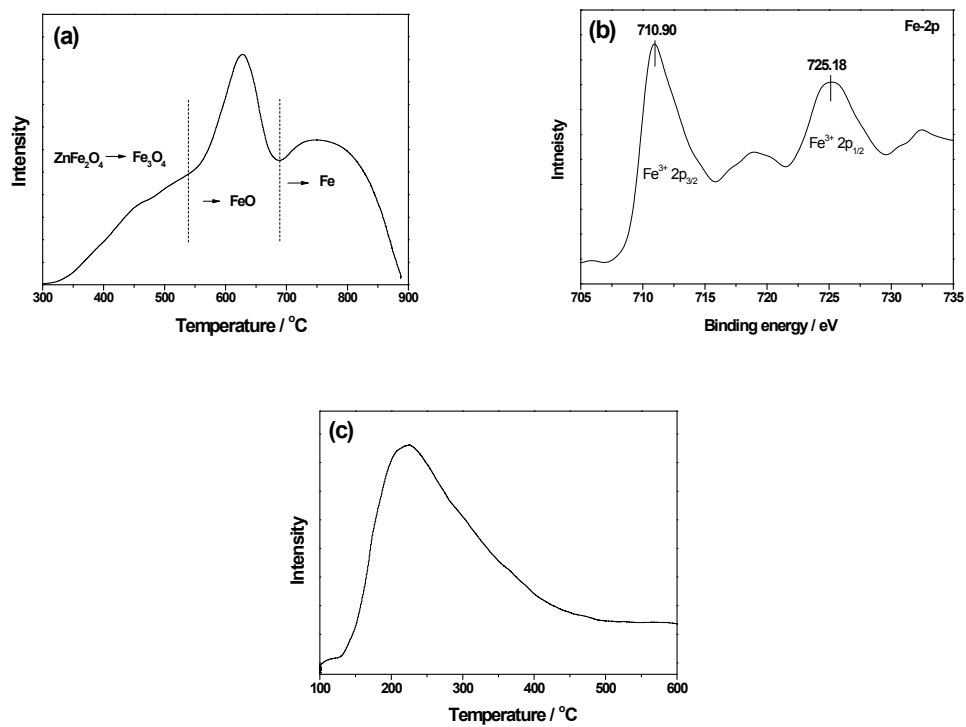


Fig. S2. (a) H<sub>2</sub>-TPR (b) XPS, and (c) NH<sub>3</sub>-TPD profiles of Fe-Zn-Zr core.

Table S2. Peak areas integrated from NH<sub>3</sub>-TPD profiles of the different samples.

Samples	Total acid sites <sup>a</sup> (μmol/g)	Weak acid sites <sup>b</sup> (μmol/g)	Mediate acid sites <sup>b</sup> (μmol/g)	Strong acid sites <sup>b</sup> (μmol/g)
Fe-Zn-Zr	93.5	28.4	65.1	0.0
HZSM-5(100)	69.7	36.1	0.0	33.6
HZSM-5(50)	280.9	152.5	0.0	128.4
HZSM-5(38)	440.0	237.4	0.0	202.6
Fe-Zn-Zr@HZSM-5(100) <sup>c</sup>	55.3	12.7	28.4	14.2
Fe-Zn-Zr@HZSM-5(50) <sup>c</sup>	86.8	29.7	30.1	27.0
Fe-Zn-Zr@HZSM-5(38) <sup>c</sup>	92.0	35.6	24.1	32.3
Fe-Zn-Zr/HZSM-5(50) <sup>c</sup>	107.7	45.0	24.7	38.0

<sup>a</sup> Determined by NH<sub>3</sub>-TPD.

<sup>b</sup> Quantified by deconvolution of the NH<sub>3</sub>-TPD profiles with Gaussian peaks ( $R^2 > 0.99$ ).

<sup>c</sup> Fe-Zn-Zr:HZSM-5=4:1(weight ratio)

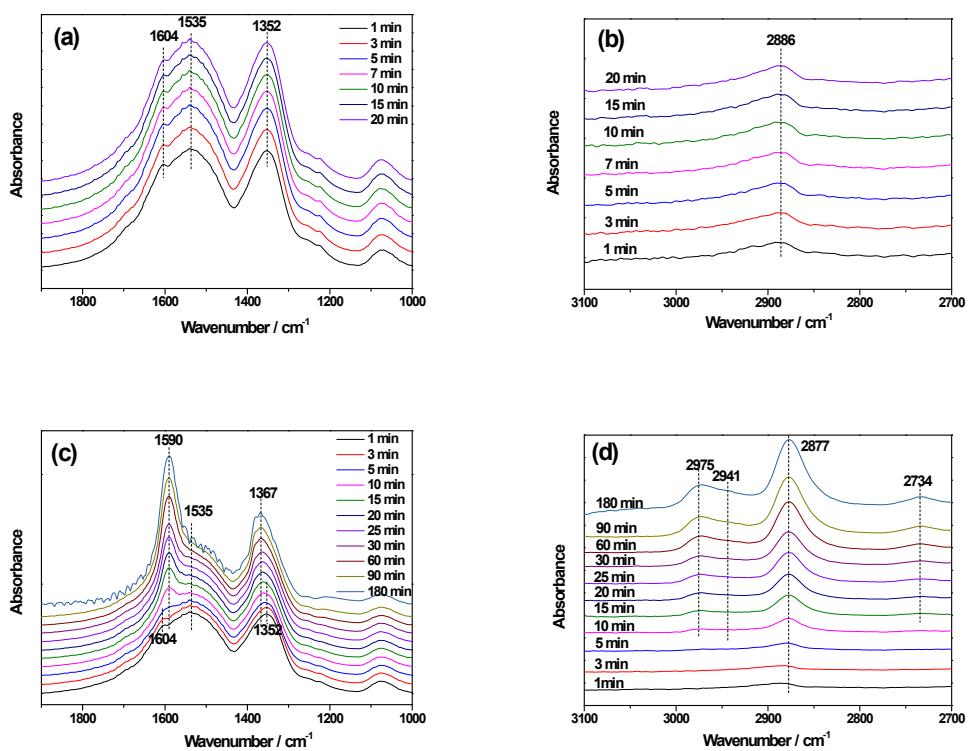


Fig. S3. In situ DRIFT spectra of (a,b) CO<sub>2</sub> adsorption and (c,d) CO<sub>2</sub> hydrogenation on Fe-Zn-Zr core.

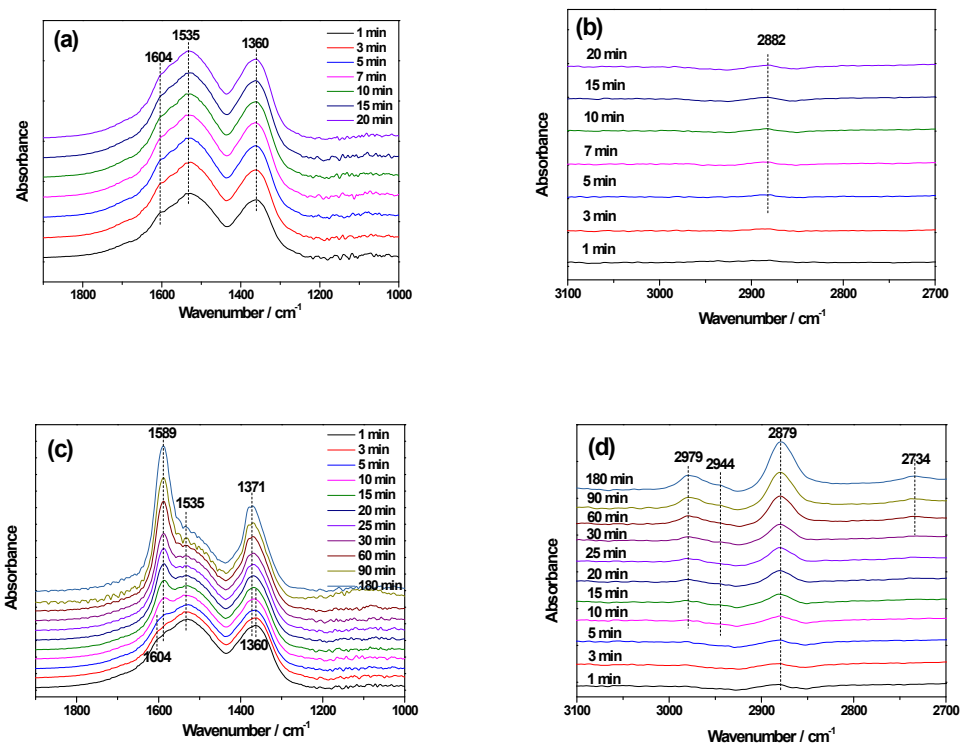


Fig. S4. In situ DRIFT spectra of (a,b) CO<sub>2</sub> adsorption and (c,d) CO<sub>2</sub> hydrogenation on Fe-Zn-Zr@HZSM-5(50) core-shell catalyst with Fe-Zn-Zr and HZSM-5 weight ratio of 6:1.

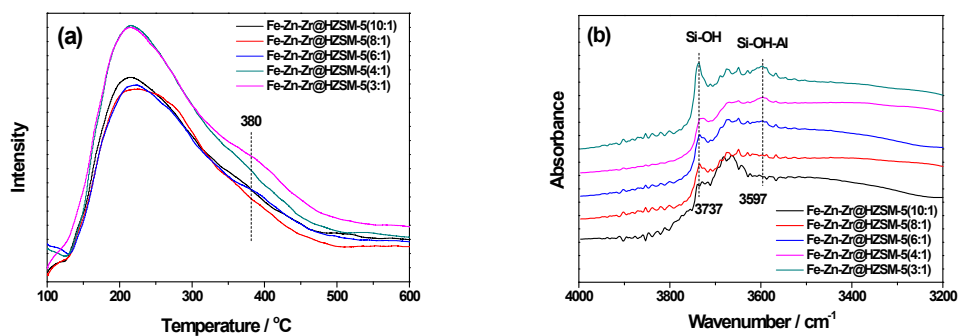


Fig. S5. NH<sub>3</sub>-TPD profiles (a) and DRIFT spectra in the OH stretching region (b) of Fe-Zn-Zr@HZSM-5(50) core-shell catalysts with different Fe-Zn-Zr and HZSM-5 weight ratios.



Table S3. Bulk contents and peak areas integrated from NH<sub>3</sub>-TPD profiles of Fe–Zn–Zr@HZSM-5(50) core–shell catalysts with different Fe–Zn–Zr and HZSM-5 weight ratios.

Samples	Fe–Zn–Zr:HZSM-5 (weight ratio) <sup>a</sup>	Total acid Sites <sup>b</sup> (μmol/g)	Weak acid Sites <sup>c</sup> (μmol/g)	Mediate acid Sites <sup>c</sup> (μmol/g)	Strong acid Sites <sup>c</sup> (μmol/g)
Fe–Zn–Zr@HZSM-5(10:1)	17.3:1	73.0	19.8	33.9	19.3
Fe–Zn–Zr@HZSM-5(8:1)	14.7:1	72.0	19.6	32.1	20.3
Fe–Zn–Zr@HZSM-5(6:1)	13.3:1	64.1	21.9	20.7	21.5
Fe–Zn–Zr@HZSM-5(4:1)	7.9:1	86.8	29.7	30.1	27.0
Fe–Zn–Zr@HZSM-5(3:1)	6.3:1	95.7	34.2	24.2	37.3

<sup>a</sup> Determined by ICP.

<sup>b</sup> Determined by NH<sub>3</sub>-TPD.

<sup>c</sup> Quantified by deconvolution of the NH<sub>3</sub>-TPD profiles with Gaussian peaks ( $R^2 > 0.99$ ).

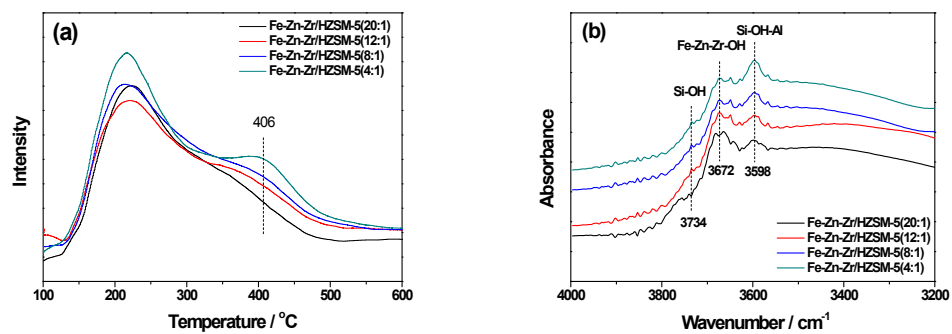


Fig. S6. NH<sub>3</sub>-TPD profiles (a) and DRIFT spectra in the OH stretching region (b) of Fe-Zn-Zr/HZSM-5(50) granular-mixing catalysts with different Fe-Zn-Zr and HZSM-5 weight ratios.

Table S4. Peak areas integrated from NH<sub>3</sub>-TPD profiles of Fe–Zn–Zr/HZSM-5(50) granular-mixing catalysts with different Fe–Zn–Zr and HZSM-5 weight ratios.

Samples	Total acid sites <sup>a</sup> (μmol/g)	Weak acid sites <sup>b</sup> (μmol/g)	Mediate acid sites <sup>b</sup> (μmol/g)	Strong acid sites <sup>b</sup> (μmol/g)
Fe–Zn–Zr/HZSM-5(20:1)	90.5	29.1	34.8	26.6
Fe–Zn–Zr/HZSM-5(12:1)	77.6	28.2	18.8	30.6
Fe–Zn–Zr/HZSM-5(8:1)	91.8	29.7	27.7	34.4
Fe–Zn–Zr/HZSM-5(4:1)	107.7	45.0	24.7	38.0

<sup>a</sup> Determined by NH<sub>3</sub>-TPD.

<sup>b</sup> Quantified by deconvolution of the NH<sub>3</sub>-TPD profiles with Gaussian peaks ( $R^2 > 0.99$ ).

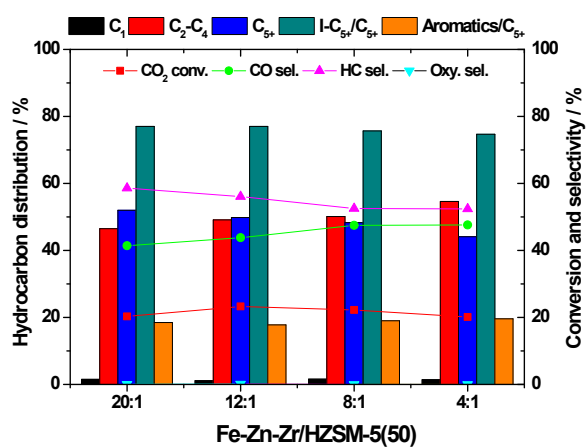


Fig. S7. CO<sub>2</sub> conversion and hydrocarbon distribution of CO<sub>2</sub> hydrogenation to gasoline over Fe–Zn–Zr/HZSM-5(50) granular–mixing catalysts with different Fe–Zn–Zr and HZSM-5 weight ratios. (Reaction conditions: 5.0 MPa; 340 °C; 2 h; 3000 ml/g/h; H<sub>2</sub>/CO<sub>2</sub>/N<sub>2</sub>=72/24/4.)

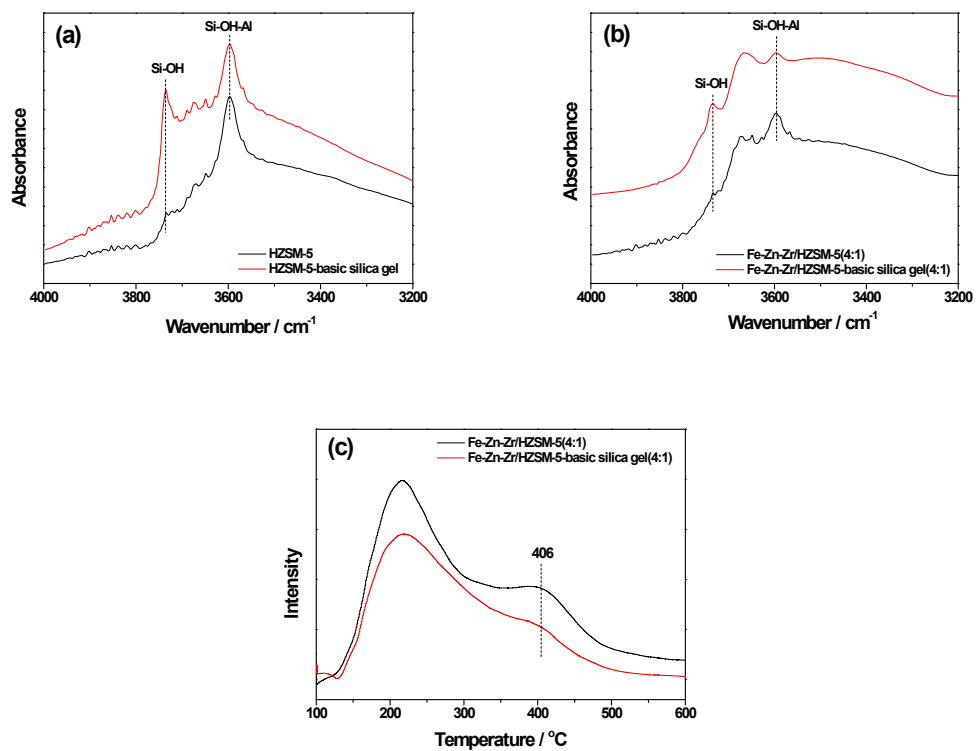


Fig. S8. Characterizations of HZSM-5(50) zeolite and Fe-Zn-Zr/HZSM-5(4:1) granular-mixing catalysts with  $\text{SiO}_2/\text{Al}_2\text{O}_3$  of 50 before and after soaking by basic silica gel: (a, b) DRIFT spectra in the OH stretching region, (c)  $\text{NH}_3$ -TPD profiles.

Table S5. Peak areas integrated from NH<sub>3</sub>-TPD profiles of Fe–Zn–Zr/HZSM-5(50) granular–mixing catalysts before and after soaking by basic silica gel.

Samples	Total acid sites <sup>a</sup> (μmol/g)	Weak acid sites <sup>b</sup> (μmol/g)	Mediate acid sites <sup>b</sup> (μmol/g)	Strong acid sites <sup>b</sup> (μmol/g)
Fe–Zn–Zr/HZSM-5(4:1)	107.7	45.0	24.7	38.0
Fe–Zn–Zr/HZSM-5-basic silica gel(4:1)	77.6	28.5	19.2	29.9

<sup>a</sup> Determined by NH<sub>3</sub>-TPD.

<sup>b</sup> Quantified by deconvolution of the NH<sub>3</sub>-TPD profiles with Gaussian peaks ( $R^2 > 0.99$ ).

Table S6. Reaction performances of Fe–Zn–Zr@HZSM-5(50) core–shell catalyst (Fe–Zn–Zr:HZSM-5=6:1) on CO<sub>2</sub> hydrogenation.

Space velocity (mL/g/h)	CO <sub>2</sub> conv.(%)	Selectivity (C-mol%)			Hydrocarbon distribution (C-mol %)			I-C <sub>5+</sub> /C <sub>5+</sub> (%)	Aromatics/C <sub>5+</sub> (%)
		CO	Oxy	HC	C <sub>1</sub>	C <sub>2</sub> -C <sub>4</sub>	C <sub>5+</sub>		
3000	22.8	39.1	0.1	60.9	2.2	39.8	58.0	91.5	6.0
20000	12.3	34.3	5.0	60.7	2.4	44.0	53.7	89.6	7.1

5.0 MPa; 340 °C; 2 h; H<sub>2</sub>/CO<sub>2</sub>/N<sub>2</sub>=72/24/4.

Oxy=oxygen compounds (MeOH+Me<sub>2</sub>O); HC=hydrocarbon.

I-C<sub>5+</sub>=C<sub>5+</sub> isoalkanes; C<sub>5+</sub>=C<sub>5+</sub> hydrocarbons.

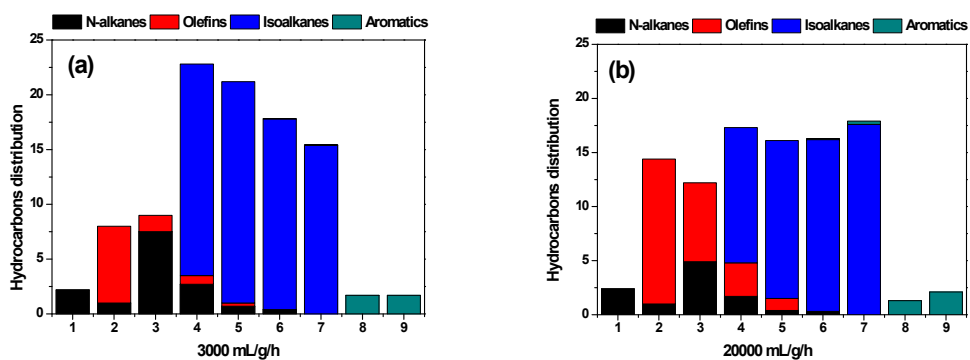


Fig. S9. Hydrocarbon distribution of Fe-Zn-Zr@HZSM-5(50) core-shell catalyst (Fe-Zn-Zr:HZSM-5=6:1) on CO<sub>2</sub> hydrogenation with different space velocity. (a) 3000 mL/g/h, (b) 20000 mL/g/h.



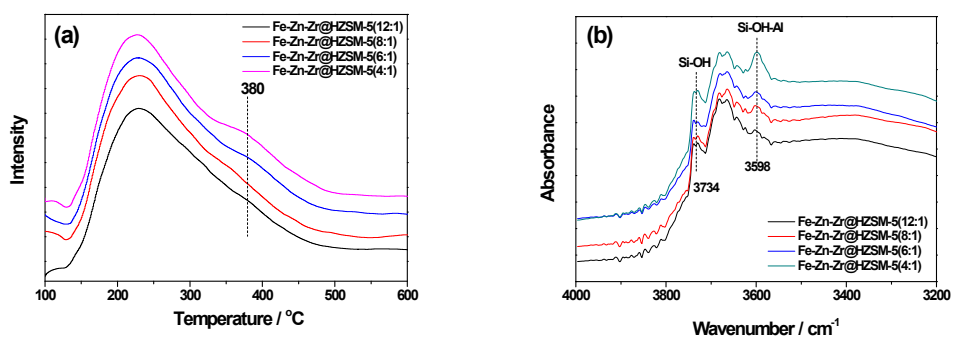


Fig. S10. NH<sub>3</sub>-TPD profiles (a) and DRIFT spectra in the OH stretching region (b) of Fe-Zn-Zr@HZSM-5(38) core-shell catalysts with different Fe-Zn-Zr and HZSM-5 weight ratios.

Table S7. Peak areas integrated from NH<sub>3</sub>-TPD profiles of Fe–Zn–Zr@HZSM-5(38 ) core–shell catalysts with different Fe–Zn–Zr and HZSM-5 weight ratios.

Samples	Total acid sites <sup>a</sup> (μmol/g)	Weak acid sites <sup>b</sup> (μmol/g)	Mediate acid sites <sup>b</sup> (μmol/g)	Strong acid sites <sup>b</sup> (μmol/g)
Fe–Zn–Zr@HZSM-5(12:1)	89.1	34.2	32.8	22.1
Fe–Zn–Zr@HZSM-5(8:1)	83.5	29.1	31.5	22.9
Fe–Zn–Zr@HZSM-5(6:1)	88.5	27.2	33.3	28.0
Fe–Zn–Zr@HZSM-5(4:1)	92.0	35.6	24.1	32.3

<sup>a</sup> Determined by NH<sub>3</sub>-TPD.

<sup>b</sup> Quantified by deconvolution of the NH<sub>3</sub>-TPD profiles with Gaussian peaks ( $R^2 > 0.99$ ).