

Supplementary Information

1. Experimental Section

1.1 Catalyst preparation and evaluation

We synthesized the $\text{Ni}_x\text{Mo}_y\text{P}_1$ oxidic precursors by stirring an aqueous solution of $\text{Ni}(\text{NO}_3)_2 \cdot 6\text{H}_2\text{O}$, $(\text{NH}_4)_6\text{Mo}_7\text{O}_{24} \cdot 4\text{H}_2\text{O}$ and $(\text{NH}_4)_2\text{HPO}_4$ with a given molar ratio of $\text{Ni}:\text{Mo}:\text{P}=x:y:1$ ($x,y=0, 0.3, 0.6$ and 1) at room temperature (RT) for 1 h. In order to dissolve the precipitate, a few drops of nitric acid were added in the solutions. The solutions were dried in air at $110\text{ }^\circ\text{C}$ for overnight to form $\text{Ni}_x\text{Mo}_y\text{P}_1$ oxidic precursors. The synthesis of phosphides in $\text{CH}_4\text{-CO}_2$ and the reforming reaction were carried out in a fixed-bed micro-reactor with an inner diameter of 10 mm at atmospheric pressure. The $\text{Ni}_x\text{Mo}_y\text{P}_1$ oxidic precursors (0.2 g) were heated under a flow of CH_4 and CO_2 ($\text{CH}_4/\text{CO}_2 = 1$, 30 ml min^{-1}) from RT to $900\text{ }^\circ\text{C}$ at a rate of $10\text{ }^\circ\text{C min}^{-1}$ and then the temperature was kepted at $900\text{ }^\circ\text{C}$ for 0-30 h. In addition, the $\text{Ni}_1\text{Mo}_1\text{P}_1$ oxidic precursors (0.2 g) were also heated under a flow of H_2 (30 ml min^{-1}) from RT to $650\text{ }^\circ\text{C}$ at a rate of $10\text{ }^\circ\text{C min}^{-1}$ and then the temperature was kepted at $650\text{ }^\circ\text{C}$ for 2 h. Finally, the resulting sample was suffered from passivation process in a flow of $1\%\text{O}_2/\text{Ar}$ for 12 h. Prior to the reaction, the catalyst prepared in H_2 was preheated to $900\text{ }^\circ\text{C}$ under an H_2 flow and then a flow of CH_4 and CO_2 ($\text{CH}_4/\text{CO}_2 = 1$, 30 ml min^{-1}) was allowed to pass through the catalyst. The conversions of CH_4 and CO_2 , and selectivity of H_2 were defined as follows ($n_{i,\text{in}}$ = the initial molar fraction of component i in the feed, $n_{i,\text{out}}$

= the final molar fraction of component i in the gaseous effluent):

$$X_{CH_4}(\%) = \frac{n_{CH_4,in} - n_{CH_4,out}}{n_{CH_4,in}} \times 100$$

$$X_{CO_2}(\%) = \frac{n_{CO_2,in} - n_{CO_2,out}}{n_{CO_2,in}} \times 100$$

$$S_{H_2} = \frac{n_{H_2,out}}{2(n_{CH_4,in} - n_{CH_4,out})} \times 100$$

1.2 Catalyst characterization

X-ray diffraction (XRD) was conducted using an X-ray diffractometer (X'Pert Pro MPD) equipped with a Cu K α source. X-ray photoelectron spectroscopy (XPS) was carried out using a Kratos Axis ultra (DLD) equipped with Al K α X-ray source. The binding energies (± 0.2 eV) were referenced to the C 1s peak at 284.8 eV due to adventitious carbon. SEM and TEM images were acquired using a scanning electron microscopy (SEM, Hitachi S-4800) and transmission electron microscope (Philips Tecna 10). BET surface area of the samples was measured by a Nova 4200e (Quantachrome) instrument. CHN analysis was performed using a Heraeus CHN-O-Rapid analyzer. H₂-TPR experiments were carried out in a quartz tube micro-reactor. The effluent gases were monitored by means of a GC thermal conductivity detector. Before each H₂-TPR run, the oxidic precursors (10 mg) was heated from RT to 120 °C in He and maintained at this temperature for 30 min. After being cooled to RT, the sample was heated from 30 °C to 1000 °C at a rate of 4 °C/min in a gas mixture of 10% H₂/Ar (80 ml min⁻¹). CO₂ and CH₄ dissociation studies were performed using a

flow of 2%CO₂(2%CH₄)/Ar (50 ml min⁻¹). Prior to the dissociation reaction, the sample was preheated to 900 °C under an H₂ flow and then the gas mixtures were allowed to pass through the sample. The change of CH₄ and CO₂ during reaction was monitored using gas chromatography (GC).

2. Results

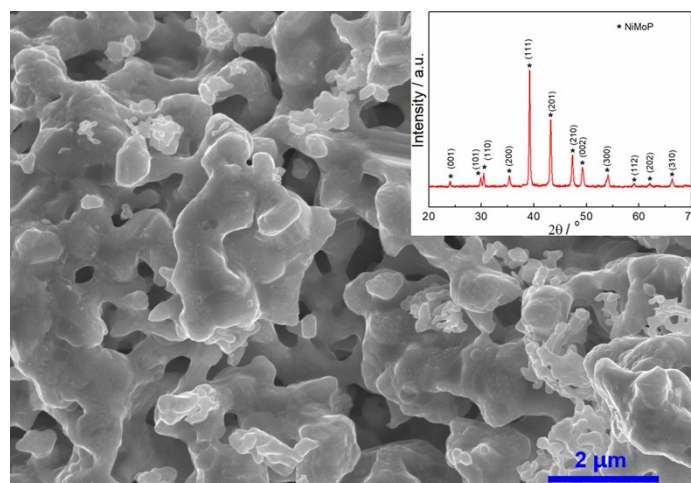


Fig. S1 SEM image of H₂-NiMoP sample. The inset shows the XRD pattern of the sample.

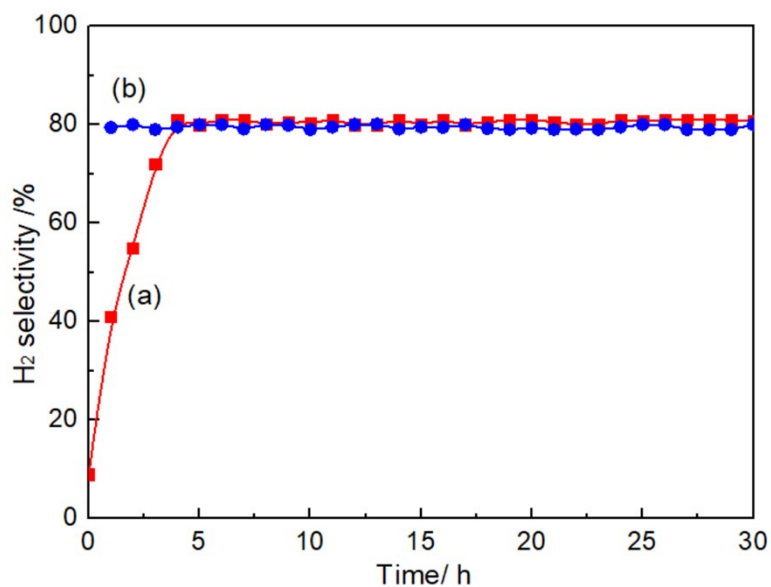


Fig. S2 H₂ selectivity over the (a) Ni₁Mo₁P₁ precursors and (b) H₂-NiMoP in DRM. Reaction conditions: CH₄:CO₂=1:1, WHSV=9000 cm³ g⁻¹ h⁻¹, reaction pressure= 1 atm, reaction temperature=900 °C.

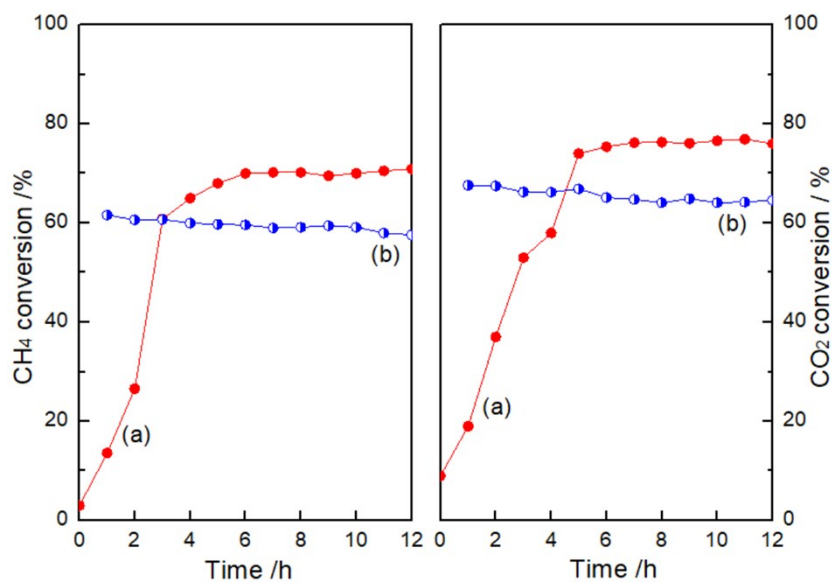


Fig. S3 CH₄ and CO₂ conversions over the (a) Ni₁Mo₁P₁ precursor and (b) H₂-NiMoP in DRM. Reaction conditions: CH₄:CO₂=1:1, WHSV=24000 cm³ g⁻¹ h⁻¹, reaction pressure= 1 atm, reaction temperature=900 °C.

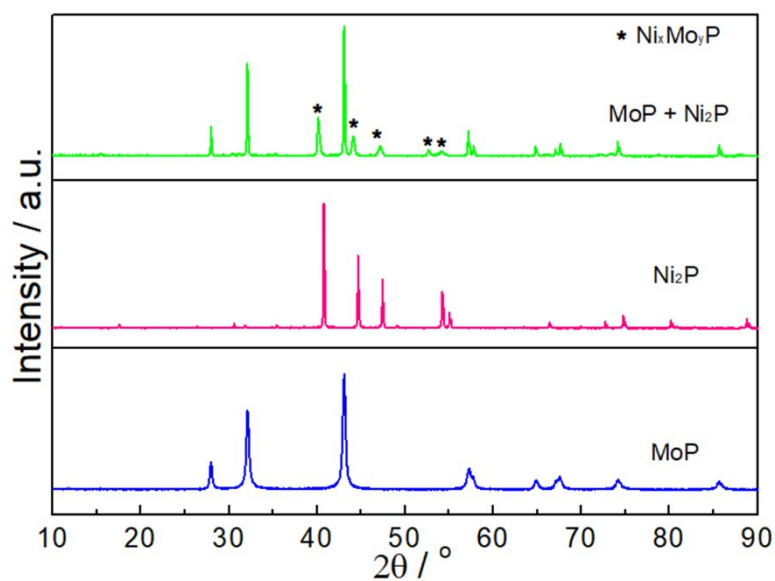


Fig. S4 XRD pattern of mechanical mixture of Ni₂P and MoP (Ni:Mo=1:1) treated in H₂ at 800 °C for 1 h. The patterns of Ni₂P and MoP are also shown for comparison.