

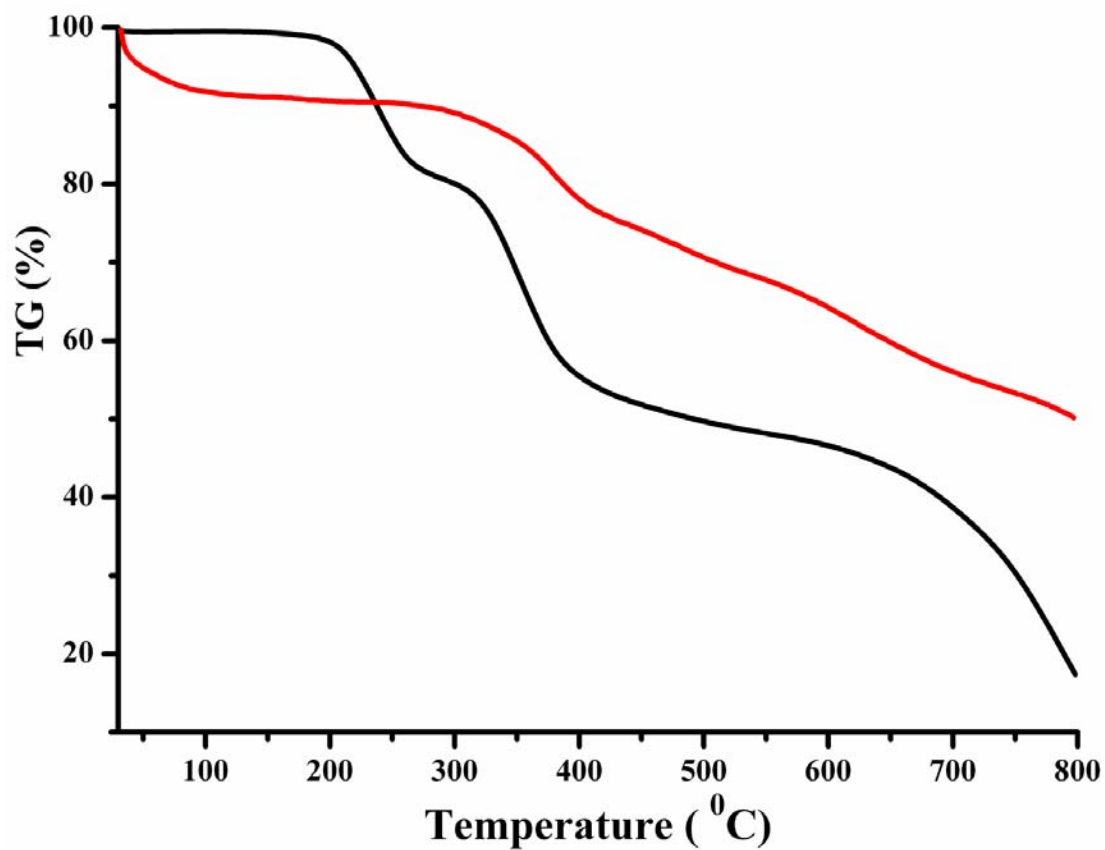
## Supporting Information

### **Enhancing CO<sub>2</sub> Adsorption enthalpy and Selectivity via Amino Functionalization of a Tetrahedral Framework Material**

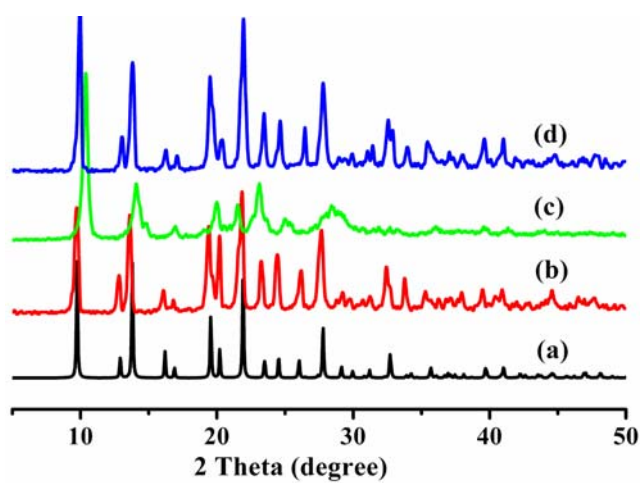
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*Figure S1.* The TGA diagram of **1** (a, black) and methanol exchanged sample (b, red).



*Figure S2.* The powder XRD patterns of **1**: (a) simulated; (b) experimental; (c) the activated samples after adsorption; (d) the activated samples soaked in DMF.

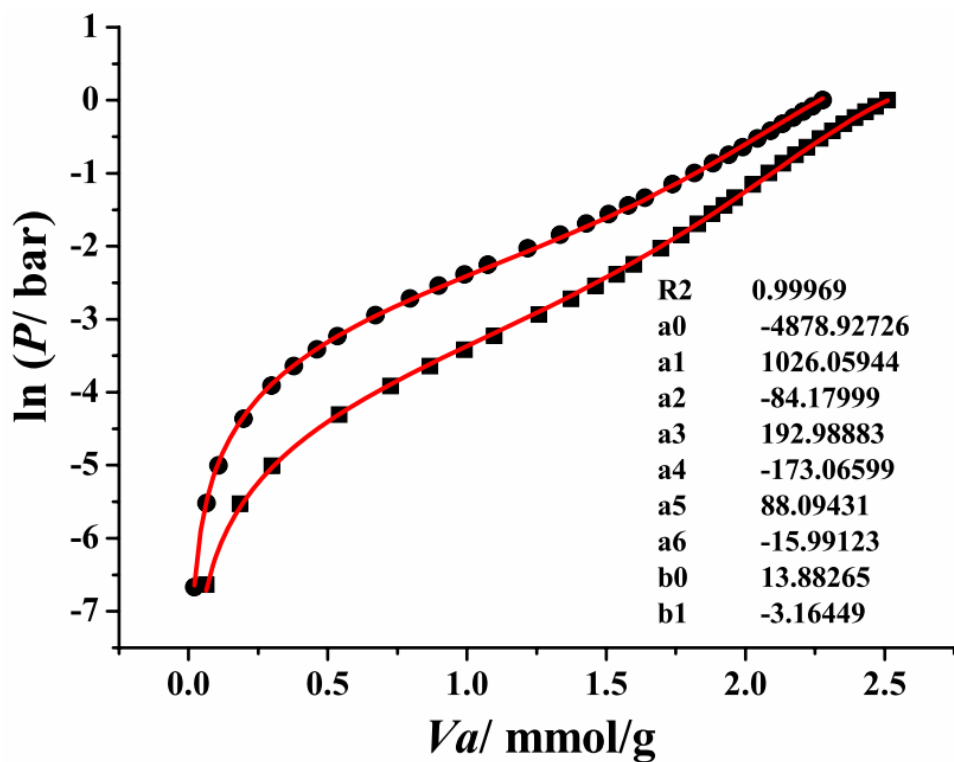


Figure S3. CO<sub>2</sub> adsorption isotherms for **1** fitting by virial method.

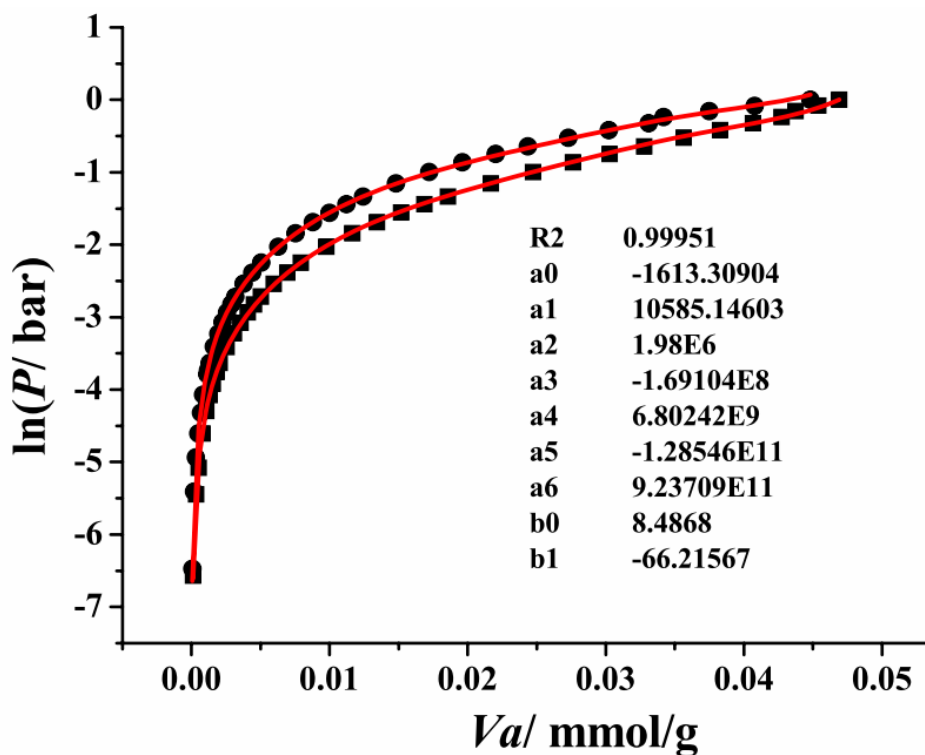


Figure S4. N<sub>2</sub> adsorption isotherms for **1** fitting by virial method.

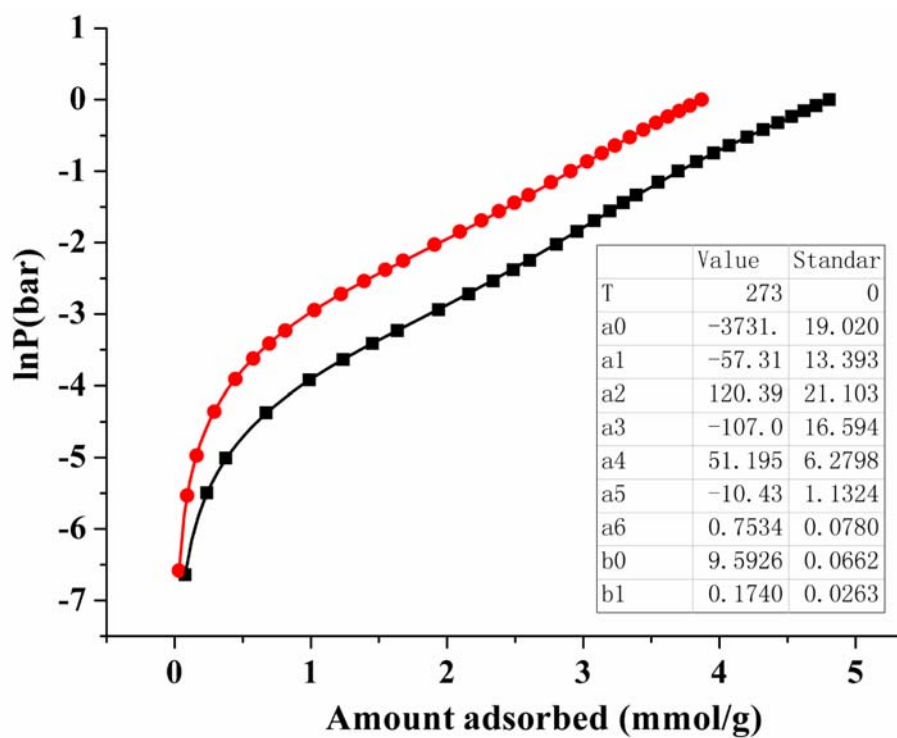


Figure S5. The CO<sub>2</sub> sorption isotherms for **TIF-A1** fitting by virial method.

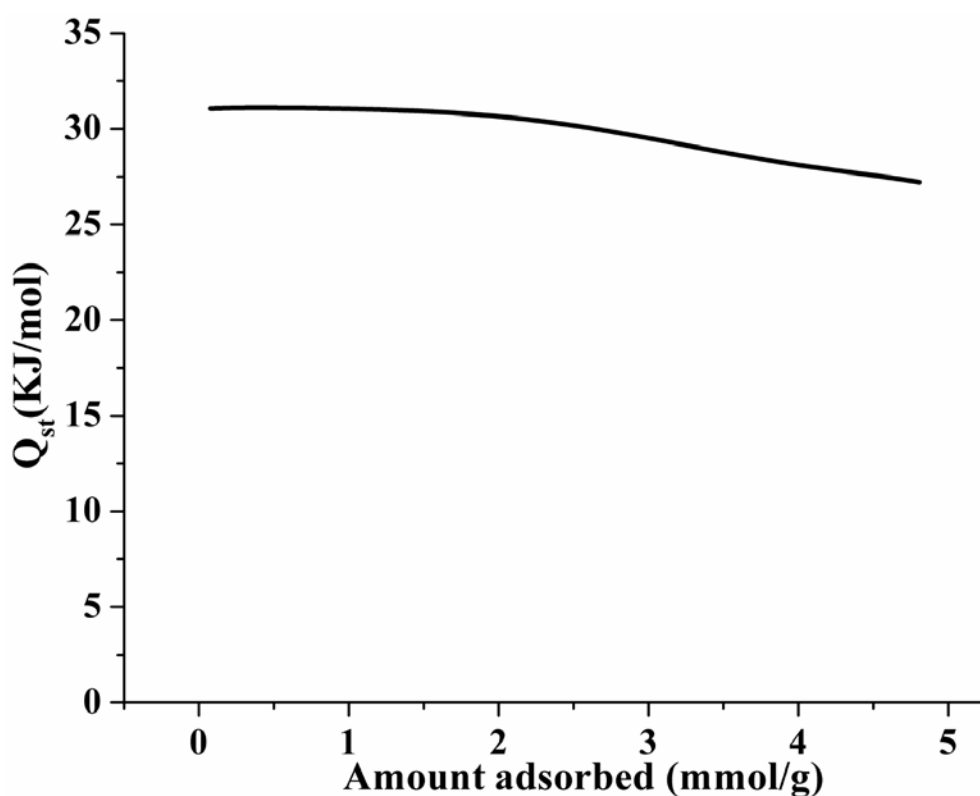


Figure S6. The isosteric heat of CO<sub>2</sub> adsorption for **TIF-A1** estimated by the virial equation.

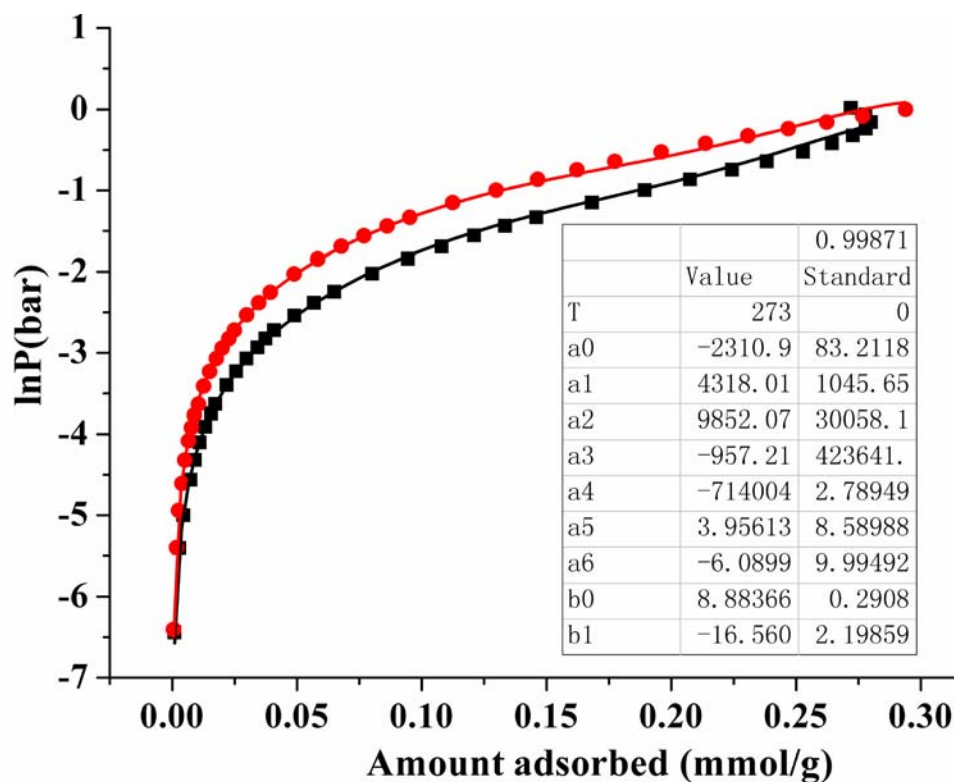


Figure S7. The N<sub>2</sub> sorption isotherms for TIF-A1 fitting by virial method.

#### Adsorption selectivity of CO<sub>2</sub>/N<sub>2</sub> calculation:

The CO<sub>2</sub> and N<sub>2</sub> sorption data for **1** and TIF-A1 measured up to 1 bar at 273 K and 298 K were fitted by the virial equation (Figure S3, S4, S5, S7).

$$\ln(P) = \ln(Va) + (a_0 + a_1 * Va + a_2 * Va^2 + \dots + a_6 * Va^6) / T + (b_0 + b_1 * Va) \quad (1)$$

Where  $P$  is pressure,  $Va$  is amount adsorbed,  $T$  is temperature, and  $a_0, a_1, a_2 \dots, a_6$  and  $b_0, b_1$  are temperature independent empirical parameters.

Henry's constant ( $K_H$ ) is calculated from where  $T$  is temperature.

$$K_H = \exp(-b_0) \cdot \exp(-a_0/T) \quad (2)$$

The Henry's Law selectivity ( $S_{ij}$ ) for gas  $i$  over  $j$  at 273K and 298 K is calculated from the following equation.

$$S_{ij} = K_{Hi} / K_{Hj} \quad (3)$$

#### References:

- (a) R. Banerjee, A. Phan, B. Wang, C. Knobler, H. Furukawa, M. O'Keeffe, and O. M. Yaghi, High-throughput synthesis of zeolitic imidazolate frameworks and application to CO<sub>2</sub> capture, *Science* 319 (2008) 939-943;

(b) B. Wang, A. P. Côté, H. Furukawa, M. O'Keeffe, and O. M. Yaghi, Colossal cages in zeolitic imidazolate frameworks as selective carbon dioxide reservoirs, *Nature* 453 (2008) 207-212;

(c) H. Kim, Y. Kim, M. Yoon, S. Lim, S. M. Park, G. Seo and K. Kim, Highly Selective Carbon Dioxide Sorption in an Organic Molecular Porous Materials, *J. Am. Chem. Soc.* 132 (2010) 12200-12202.