

Supplementary Material (ESI) for Catalysis Science & Technology

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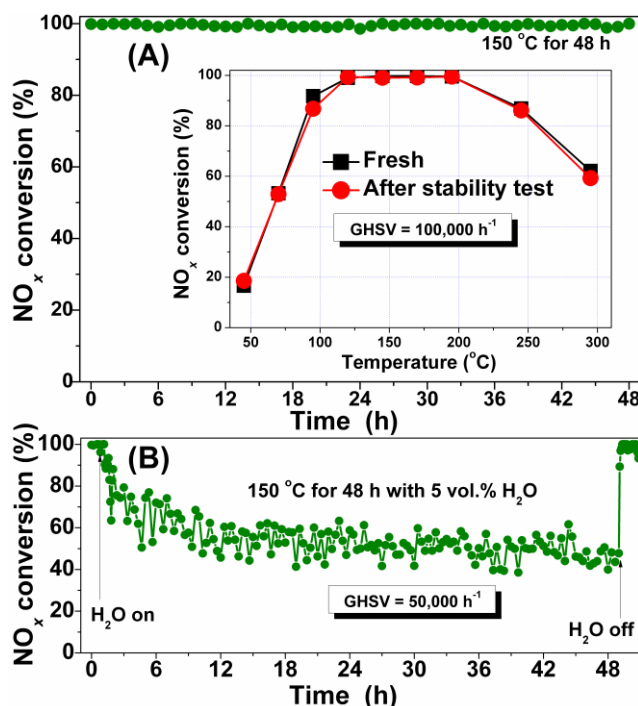
**Novel MnWO<sub>x</sub> catalyst with remarkable performance for low  
temperature NH<sub>3</sub>-SCR of NO<sub>x</sub>**

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## Electronic Supplementary Information

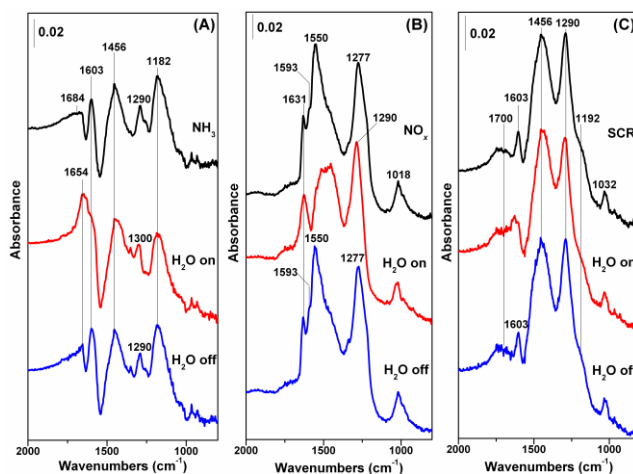
### The stability test of MnWO<sub>x</sub> catalyst in NH<sub>3</sub>-SCR reaction



**Fig. S1.** (A) The NO<sub>x</sub> conversion over MnWO<sub>x</sub> catalyst in NH<sub>3</sub>-SCR reaction at 150 °C for 48 h under GHSV of 100,000 h<sup>-1</sup> (inserted: the SCR activity of MnWO<sub>x</sub> catalysts before and after stability test as a function of temperature); (B) The NO<sub>x</sub> conversion over MnWO<sub>x</sub> catalyst in NH<sub>3</sub>-SCR reaction in the presence of 5 vol.% H<sub>2</sub>O at 150 °C for 48 h under GHSV of 50,000 h<sup>-1</sup>.

To better test the stability of MnWO<sub>x</sub> catalyst in the deNO<sub>x</sub> process, we also carried out the NH<sub>3</sub>-SCR reaction at 150 °C for 48 h under the GHSV of 100,000 h<sup>-1</sup>, and during the reaction period that we investigated the NO<sub>x</sub> conversion was always maintaining at 100% as shown in Fig. S1(A). After the stability test, we again tested the SCR performance of the used MnWO<sub>x</sub> catalyst in the whole temperature range, and no decline of SCR activity was observed at all comparing with the fresh catalyst. These results clearly indicate that the MnWO<sub>x</sub> catalyst is highly stable in the NH<sub>3</sub>-SCR reaction at low temperatures, which is advantageous to the practical use. We also carried out the stability test of MnWO<sub>x</sub> catalyst in the presence of 5 vol.% H<sub>2</sub>O at 150 °C for 48 h under the GHSV of 50,000 h<sup>-1</sup>. As we can clearly see, after the addition of H<sub>2</sub>O, the NO<sub>x</sub> conversion over MnWO<sub>x</sub> catalyst decreased from 100% to *ca.* 60% in nearly 12 h (possibly due the competitive adsorption of H<sub>2</sub>O and the slow deposition of ammonium nitrate onto catalyst surface) and then maintained at *ca.* 60% for the next 36 h. After the shutting off of H<sub>2</sub>O, the NO<sub>x</sub> conversion returned to 100% rapidly, indicating that the deactivation effect of H<sub>2</sub>O on the NH<sub>3</sub>-SCR activity of MnWO<sub>x</sub> catalyst at this temperature point is reversible. If operating at temperatures above 150 °C, this MnWO<sub>x</sub> catalyst can have long term stability even in the presence of water vapour.

### ***In situ* DRIFTS results about the influence of H<sub>2</sub>O on the NH<sub>3</sub>/NO<sub>x</sub> adsorption and NH<sub>3</sub>-SCR reaction over MnWO<sub>x</sub> catalyst**



**Fig. S2.** *In situ* DRIFTS results about the influence of H<sub>2</sub>O on (A) NH<sub>3</sub> adsorption, (B) NO<sub>x</sub> adsorption and (C) NH<sub>3</sub>-SCR reaction over MnWO<sub>x</sub> catalyst at 100 °C.

Peak assignments:

- (A) 1684/1654 and 1456 cm<sup>-1</sup> (NH<sub>4</sub><sup>+</sup>); 1603 and 1182 cm<sup>-1</sup> (coordinated NH<sub>3</sub>); 1290 cm<sup>-1</sup> (unknown assignment).
- (B) 1631 cm<sup>-1</sup> (bridging nitrate); 1593 and 1018 cm<sup>-1</sup> (bidentate nitrate); 1550 and 1277 cm<sup>-1</sup> (monodentate nitrate).
- (C) 1700 cm<sup>-1</sup> (NH<sub>4</sub><sup>+</sup>); 1603 and 1192 cm<sup>-1</sup> (coordinated NH<sub>3</sub>); 1456 and 1290 cm<sup>-1</sup> (surface ammonium nitrate species); 1032 cm<sup>-1</sup> (bidentate nitrate).