1 Electronic Supplementary Information

# 2 Molecular H<sub>2</sub>O promoted catalytic bicarbonate reduction with methanol

# 3 into formate over Pd<sub>0.5</sub>Cu<sub>0.5</sub>/C under mild hydrothermal conditions

4 Xiaoguang Wang,<sup>a</sup> Yang Yang,<sup>a</sup> Heng Zhong,<sup>\*,a,b,c</sup> Tianfu Wang,<sup>a,c</sup> Jiong Cheng,<sup>a</sup> and Fangming Jin<sup>\*,a,b,c</sup>

- 5 <sup>a</sup> School of Environmental Science and Engineering, State Key Lab of Metal Matrix Composites, Shanghai Jiao Tong
- 6 University, Shanghai 200240, China.
- 7 <sup>b</sup> Center of Hydrogen Science, Shanghai Jiao Tong University, Shanghai, 200240, China.
- 8 <sup>c</sup> Shanghai Institute of Pollution Control and Ecological Security, Shanghai 200092, P.R. China.
- 9 \*Fangming Jin: fmjin@sjtu.edu.cn; Heng Zhong: zhong.h@sjtu.edu.cn.
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#### **13 Experimental Section**

#### 14 Analytical methods

HPLC analysis was performed on an Agilent 1200 system, which is equipped with two KC-16 811 columns (SHODEX) for samples separation and a tunable UV/Vis absorbance detector 17 adjusted at 210 nm for samples detection. A 2 mmol/L  $HClO_4$  solution with a flow rate of 1.0 18 mL/min was used as the mobile phase.

19 QNMR analysis was performed on a Bruker Avance III 600 MHz NMR-Spectrometer, and 20 the quantitative estimation of products concentration was obtained using internal standard method 21 and reported results were based on the average values of at least three samples according to our 22 previous works.<sup>S1</sup>

For GC-MS analysis, a Hewlett-Packard model 7890A gas chromatograph system equipped with a model 5975C mass selective detector was used. The initial oven temperature in the gas chromatograph was 313 K, which was kept for 1 min, and then procedurally increased at a rate of 7 °C/min to a final temperature of 503 K and was held for 20 min. Samples were separated with a HP-INNOWAX polar capillary column (25 m long, 0.25 mm i.d., 0.5 μm film thickness) using helium as the carrier gas.

Gas samples were analyzed by a Hewlett-Packard model 5890 Series II Plus gas
chromatograph (GC-TCD) equipped with a packed column (TDX-01) using N<sub>2</sub> as the carrier gas.
X-ray diffraction (XRD) patterns were obtained on a Shimadzu XRD-6100 PC with a Cu Kα
radiation (λ = 1.54184 Å) in steps of 0.02° and an accumulation time of 0.6 s per step from 10 to
80° at 40 kV and 40 mA.

Transmission electron microscope (TEM) photographs were taken on JEOL JEM-2100F at an acceleration voltage of 200 Kv, and the sample stage is copper mesh ultra-thin carbon film.

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# 36 **Definition**

37 'Formate production efficiency' was used to evaluate the efficiency of  $HCO_3^{-}/CO_3^{2-}/CO_2$ 38 reduction with alcohol, which was defined as follow:

Formate production efficiency (%) = 
$$\frac{Produced formate from carbon source (mmol L^{-1})}{Initially added alcohol(mmol L^{-1})} \times 100\%$$

40 The  $HCO_3^{-}/CO_3^{2-}/CO_2$  generated formate was quantified by <sup>13</sup>C-qNMR with  $CH_3^{13}COOH$ 41 added to the samples as an internal standard since the -COOH group in  $H^{13}COOH$  and 42  $CH_3^{13}COOH$  has the nearest sensitivity in <sup>13</sup>C-qNMR.



44 Fig. S1 Schematic drawing of operando hydrothermal ATR-FTIR ((a) photo of high-temperature

- 45 and high-pressure ATR-FTIR reactor; (b) schematic drawing of whole system of operando high-
- 46 temperature and high-pressure ATR-FTIR).



**Fig. S2** SEM images of the as-prepared Pd/C (a, b),  $Pd_{0.5}Cu_{0.5}/C$  (c, d) and carbon black (e, f).





Fig. S3 SEM-EDS images of the as-prepared Pd/C (a-c) and Pd0.5Cu0.5/C (d-g).





52 Fig. S4 TEM images (a), HRTEM image (b), and TEM-EDS elemental mapping (c) of the as-

53 prepared Pd/C.



55 Fig. S5 HPLC chromatograms of methanol reacting with or without NaHCO<sub>3</sub> (reaction conditions:

56 0.1 mol/L CH<sub>3</sub>OH, 1 mol/L NaHCO<sub>3</sub>, 50% water filling, 180 °C, and 16 h).



58 **Fig. S6** <sup>13</sup>C-qNMR of the liquid sample after the reaction of NaH<sup>13</sup> $\underline{CO}_3$  with methanol 59 (CH<sub>3</sub><sup>13</sup> $\underline{COOH}$  was added as an internal standard to calculate the H<sup>13</sup> $\underline{COO}$ <sup>-</sup> concentration; reaction 60 conditions: 0.1 mol/L CH<sub>3</sub>OH, 1 mol/L NaH<sup>13</sup> $\underline{CO}_3$ , 50% water filling, 50 mg Pd<sub>0.5</sub>Cu<sub>0.5</sub>/C, 180 °C, 61 and 16 h).



63 Fig. S7 Effect of reaction temperature and time on the formate production efficiency
64 (reaction conditions: 0.1 mol/L CH<sub>3</sub>OH, 1 mol/L NaHCO<sub>3</sub>, 50% water filling, 50 mg
65 Pd<sub>0.5</sub>Cu<sub>0.5</sub>/C).





67 Fig. S8 Effect of catalyst amount on the formate production efficiency (reaction conditions: 0.1

68 mol/L CH<sub>3</sub>OH, 1 mol/L NaHCO<sub>3</sub>, 50% water filling, 180 °C, 16 h).



Fig. S9 Recycling test for the stability of  $Pd_{0.5}Cu_{0.5}/C$  catalyst (reaction conditions: 0.1 mol/L CH<sub>3</sub>OH, 1 mol/L NaHCO<sub>3</sub>, 50% water filling, 50 mg  $Pd_{0.5}Cu_{0.5}/C$ , 180 °C, and 16 h).



Fig. S10 SEM images (a, b), HRTEM images (c, d) and XRD spetra (e) of the Pd<sub>0.5</sub>Cu<sub>0.5</sub>/C
catalyst after reaction (reaction conditions: 0.1 mol/L CH<sub>3</sub>OH, 1 mol/L NaHCO<sub>3</sub>, 50%
water filling, 50 mg Pd<sub>0.5</sub>Cu<sub>0.5</sub>/C, 180 °C, and 16 h).





78 Fig. S11 XPS analyses of Cu 2p in PdCu alloy (a shoulder peak at 932.1 eV and 933.5 eV are

79 observed, which are assigned to Cu(0) and Cu(II) in PdCu alloy, respectively<sup>S2, S3</sup>).



Fig. S12 D-qNMR of the liquid sample after CH<sub>3</sub>OH (a), HCHO (b), and HCOO<sup>-</sup>(c) reacting with
D<sub>2</sub>O (reaction conditions: 0.1 mol/L reactant, 50% D<sub>2</sub>O filling, 50 mg Pd<sub>0.5</sub>Cu<sub>0.5</sub>/C, 180 °C, and
16 h).



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85 Fig. S13 HPLC spectra of NaHCO<sub>3</sub> reduction with different alcohols (reaction conditions: 0.1

86 mol/L alcohol, 1 mol/L NaHCO<sub>3</sub>, 50% water filling, 50 mg Pd<sub>0.5</sub>Cu<sub>0.5</sub>/C, 180 °C, and 16 h).



88 Fig. S14 Variation of the system pressure with reaction time (reaction conditions: 0.1 mol/L
89 CH<sub>3</sub>OH, 1 mol/L NaHCO<sub>3</sub>, 50% water filling and 0.5 g Pd<sub>0.5</sub>Cu<sub>0.5</sub>/C in 100 mL PARR reactor).

Entry	Catalyst*	wt.%		molar ratio
		Pd	Cu	of Pd/Cu
1	Pd <sub>0.75</sub> Cu <sub>0.25</sub> /C	6.09	1.17	3.11
2	Pd <sub>0.66</sub> Cu <sub>0.33</sub> /C	5.54	1.60	2.07
3	$Pd_{0.5}Cu_{0.5}/C$	4.46	2.68	0.98
4	Pd <sub>0.33</sub> Cu <sub>0.66</sub> /C	3.21	4.07	0.47
5	Pd <sub>0.25</sub> Cu <sub>0.75</sub> /C	2.44	4.67	0.31

Table S1 ICP-OES results of the catalysts with different Pd/Cu ratios.

\*The subscripted decimal represents the molar fraction of specific metal catalyst to the total metals.

reduction of Marico's with H2 on different catalysts.				
Catalyst	Formate yield (%)			
None	None			
Pd/C	37.7			
Cu/C	12.4			
$Pd_{0.5}Cu_{0.5}/C$	49.5			

Table S2 Formate yields obtained from the reduction of  $NaHCO_3$  with  $H_2$  on different catalysts.

Reaction conditions: 3 MPa H<sub>2</sub>, 1 mol/L NaHCO<sub>3</sub>, 50% water filling, 50 mg catalyst, 180 °C, and 16 h.

# 90 References

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