

## **Electronic Supplementary Information**

### **A microporous, amino acid functionalized Zn(II)-organic framework nanoflower for selective CO<sub>2</sub> capture and solvent encapsulation<sup>†</sup>**

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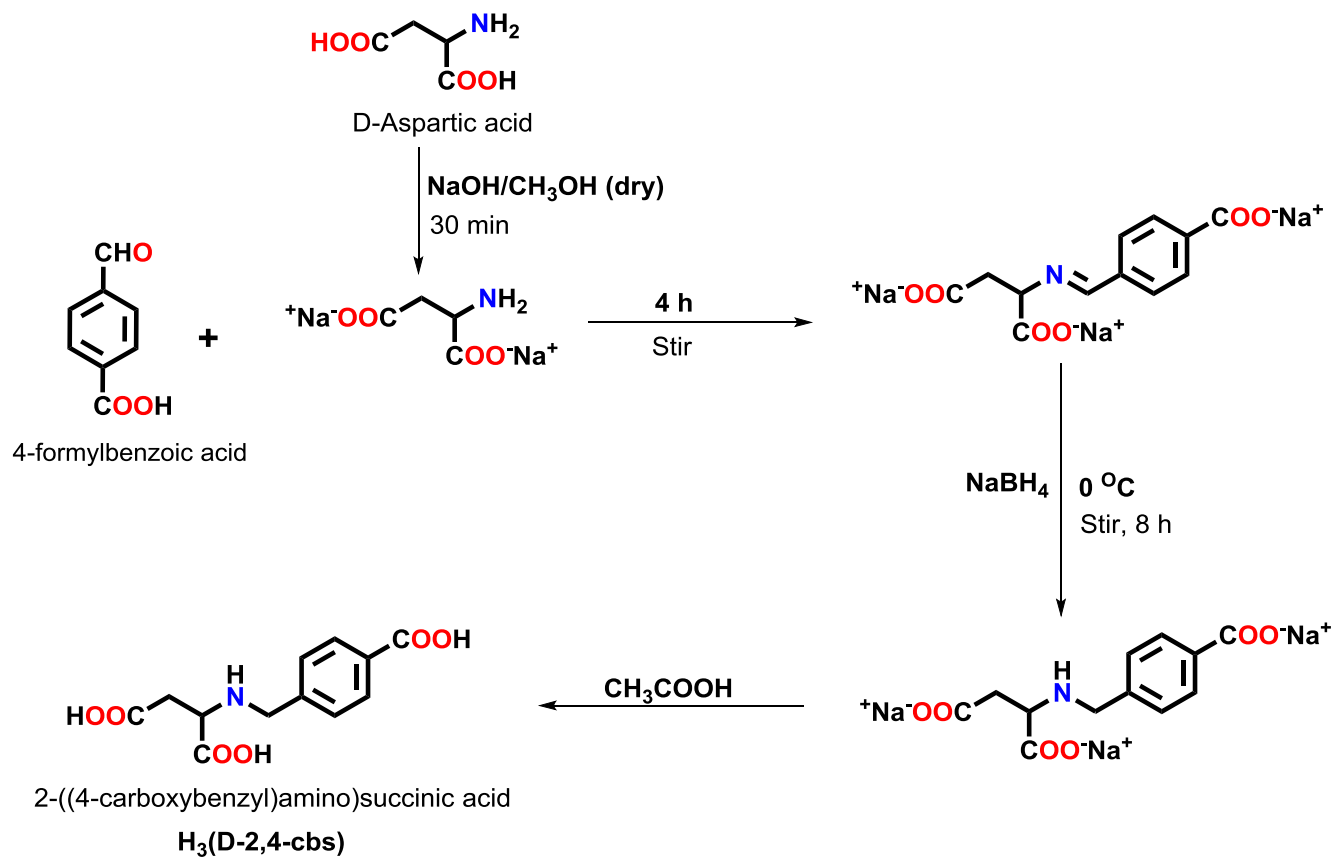
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**Scheme S1.** Synthesis of H<sub>3</sub>(D-2,4-cbs).

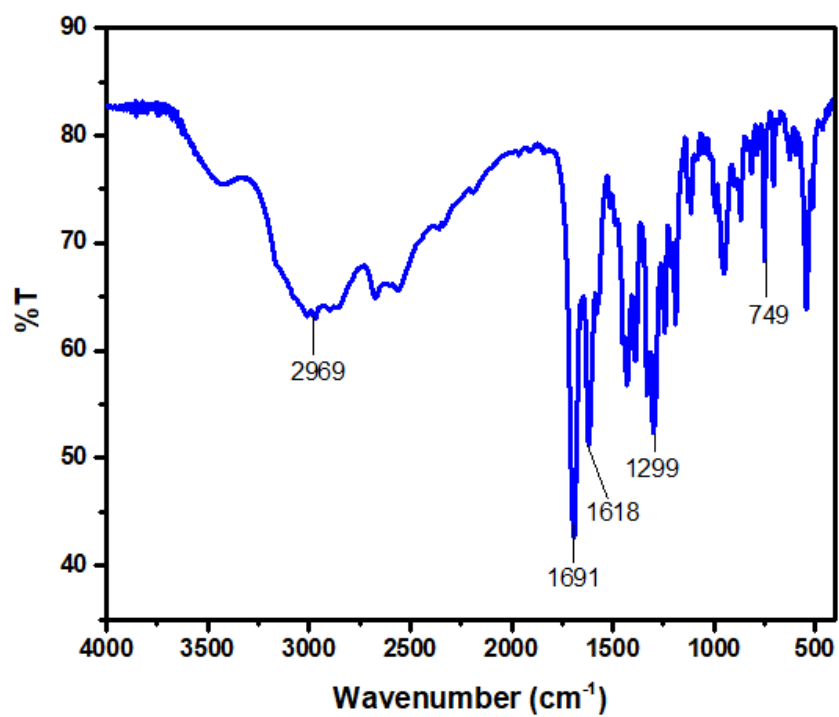


Fig. S1 FTIR spectrum of H<sub>3</sub>(D-2,4-cbs).

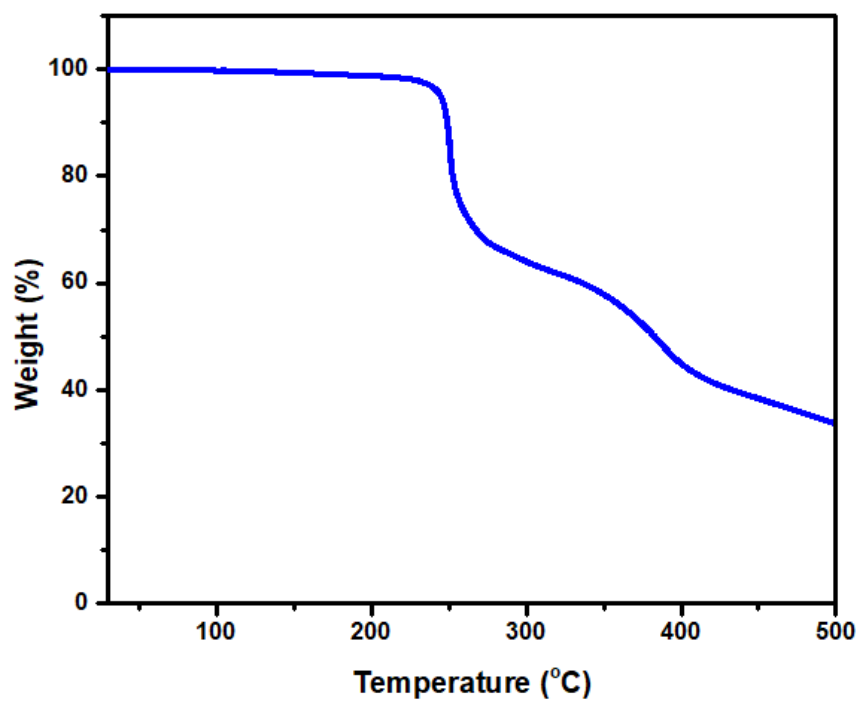
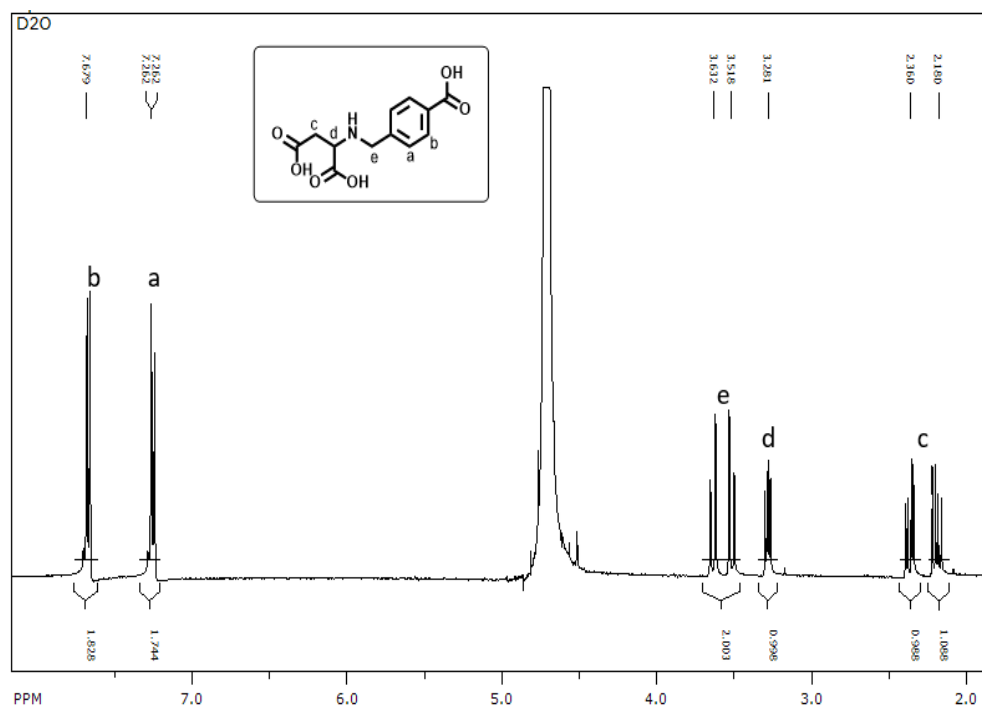
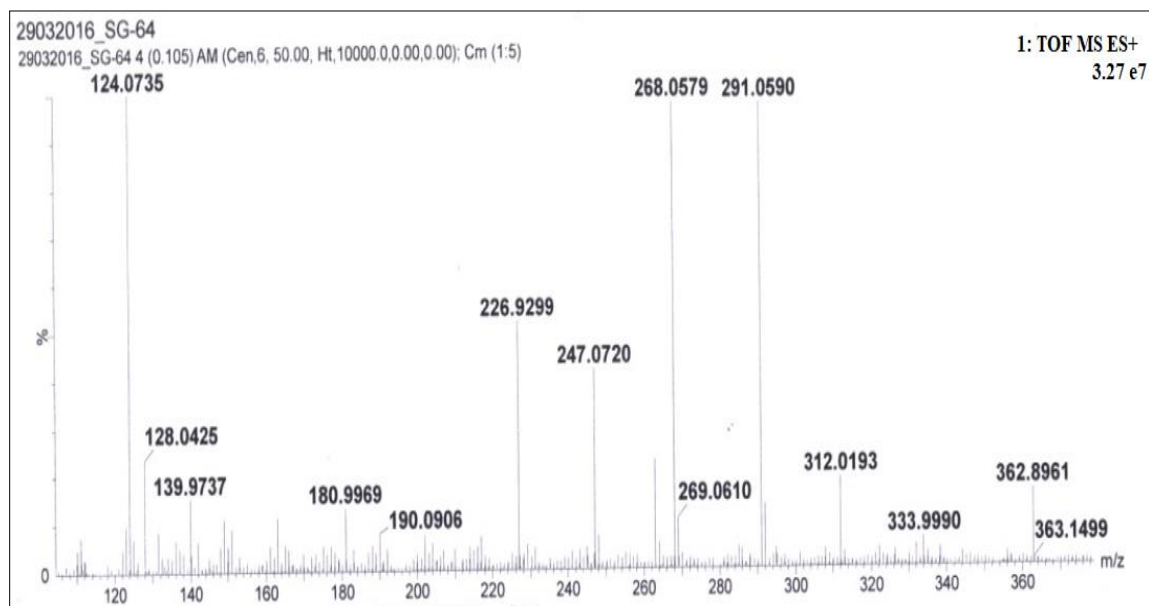


Fig. S2 TGA profile of H<sub>3</sub>(D-2,4-cbs).



**Fig. S3** <sup>1</sup>H NMR spectrum of H<sub>3</sub>(D-2,4-cbs) in D<sub>2</sub>O.



**Fig. S4** HRMS of H<sub>3</sub>(D-2,4-cbs).

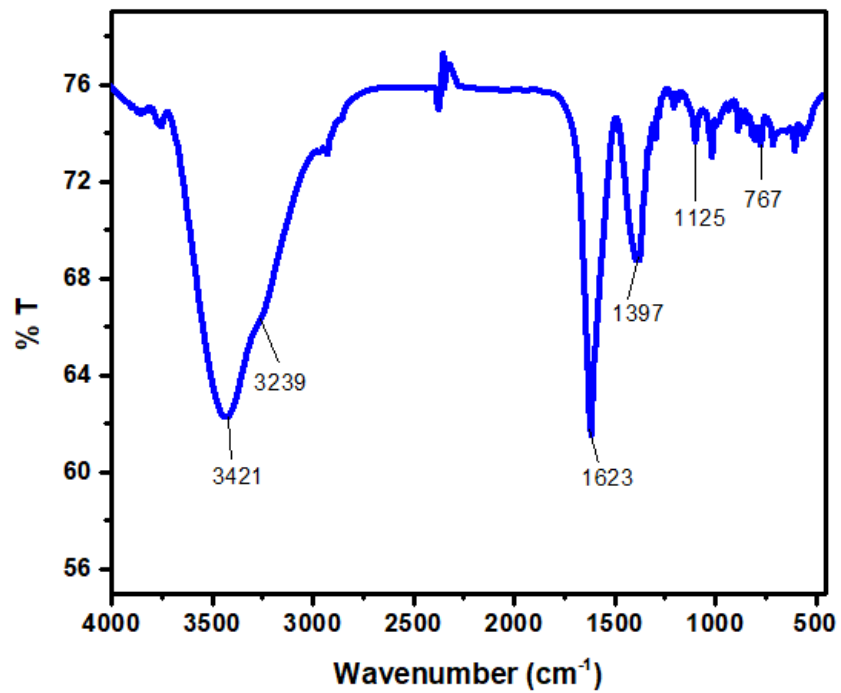


Fig. S5 FTIR spectrum of Zn-CBS.

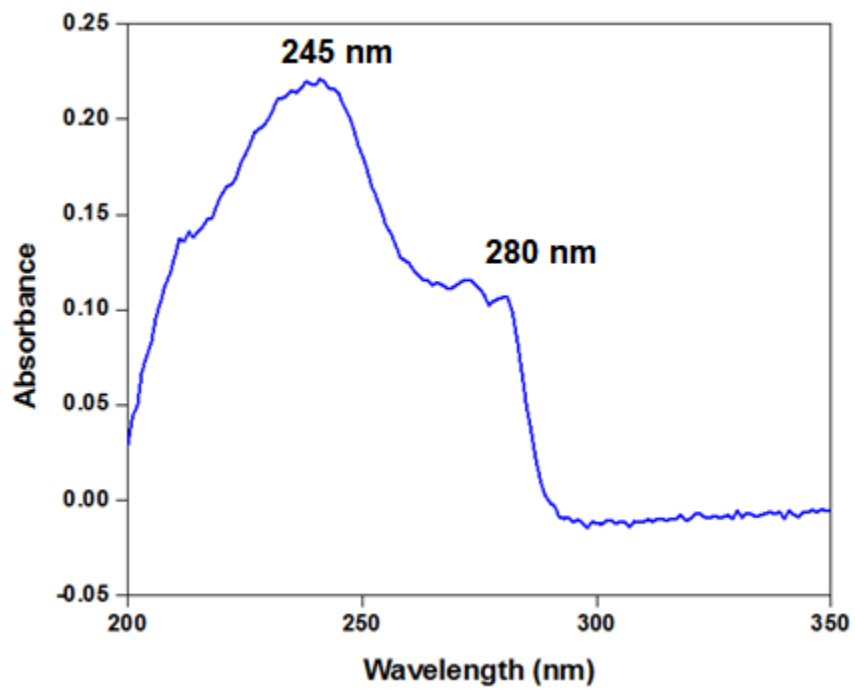


Fig. S6 Solid State diffuse reflectance spectrum of Zn-CBS.

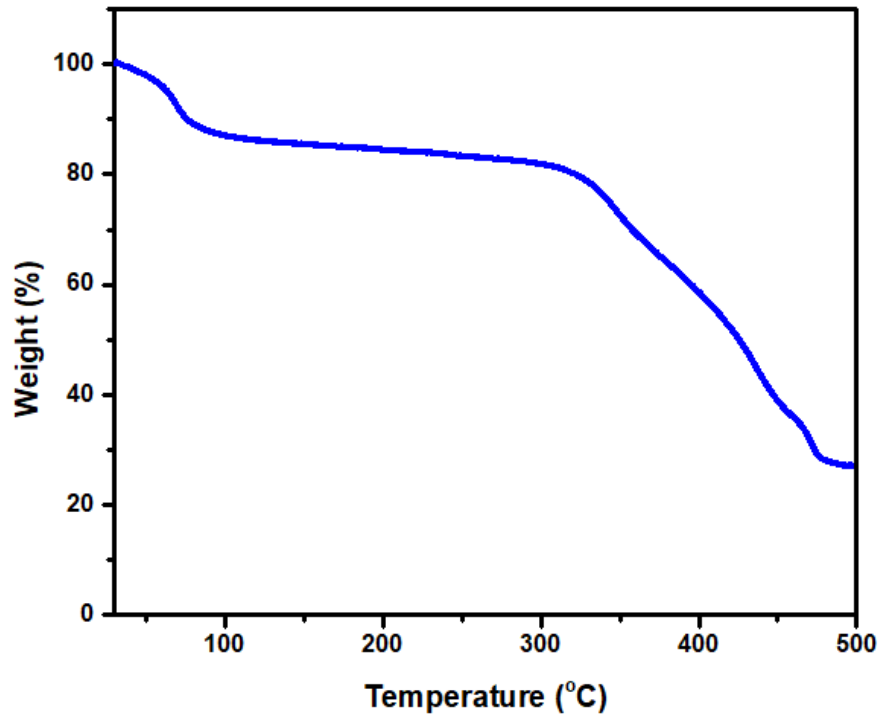


Fig. S7 TGA profile of Zn-CBS.

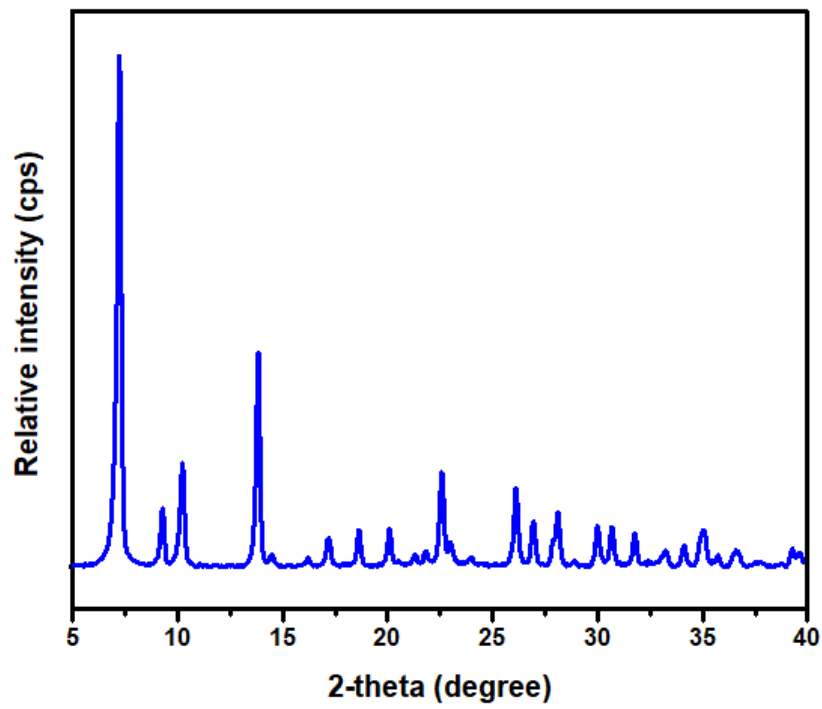
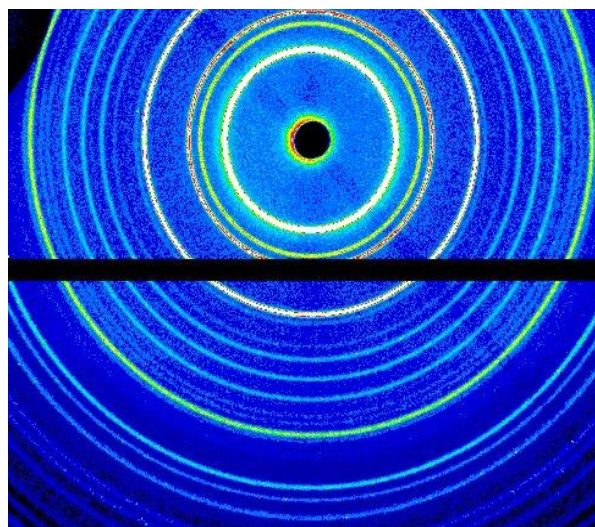
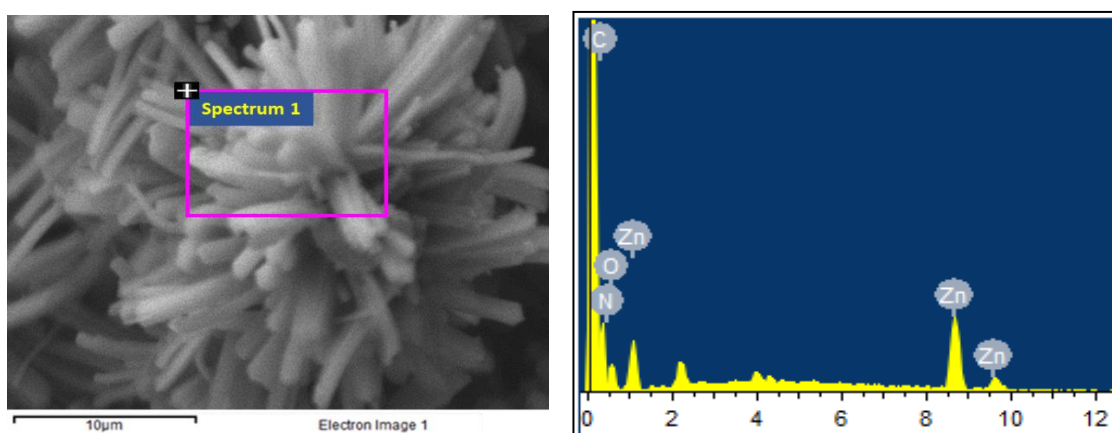


Fig. S8 PXRD pattern of Zn-CBS.



**Fig. S9** 2D WAX Map of Zn-CBS.



Element	Weight (%)	Atomic (%)
C K	33.5	47.5
N K	15.4	18.8
O K	25.5	27.1
Zn K	25.6	6.6
Total	100	

**Fig. S10** EDX analysis of Zn-CBS.



## Analysis of Sorption Isotherm

For this analysis, the BET equation is considered:

$$v = cv_m x / (1-x)[1 + (c-1)x]$$

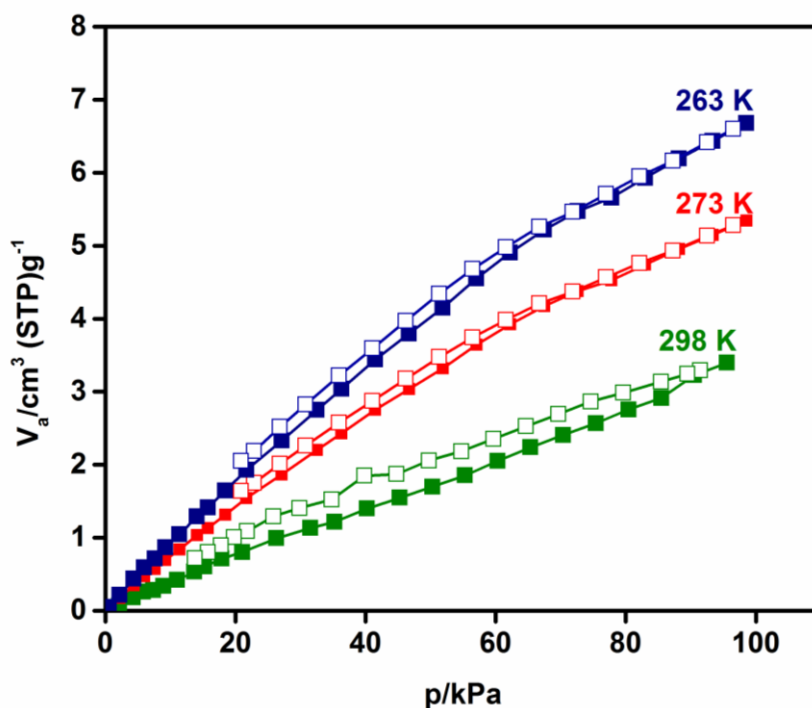
where,  $x = p/p_0$ ,  $v$  is the volume of nitrogen adsorbed per gram of **Zn-CBS** at STP,  $v_m$  is the monolayer capacity, and  $c$  is related to the heat of adsorption. It is noted that the line is fit to the low pressure isotherm data with range  $0.05 < x < 0.3$ .

The surface area is then calculated from:  $A = v_m \sigma_0 N_{av}$

where,  $\sigma_0$  is the cross-sectional area of nitrogen at liquid density (16.2 Å) and  $N_{av}$  is Avogadro's number.

These calculations are done through the "BET analysis" and "Langmuir analysis" function embedded in the Belsorp Adsorption/Desorption Data Analysis software version 6.3.1.0.

Pore size was calculated using microporous (MP) analysis method embedded in the Belsorp Adsorption/Desorption Data Analysis software.



**Fig. S11** N<sub>2</sub> sorption isotherms of **Zn-CBS** at 263 K, 273 K and 298 K.

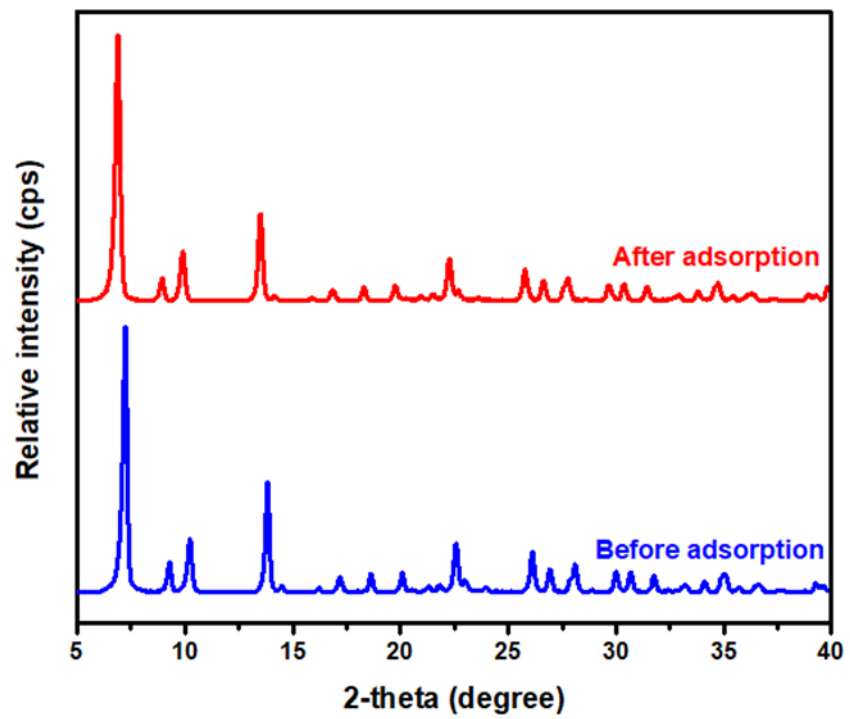


Fig. S12 PXRD pattern of before and after gas adsorption.

### **Calculation of Isothermic Heats of Adsorption:**

#### Using the Clausius-Clapeyron equation

Isothermic heats of adsorption ( $Q_{st}$ ) were calculated using the Clausius-Clapeyron equation based on pure-component isotherms collected at two different temperatures of 273 K and 298 K.  $Q_{st}$  is defined as:

$$Q_{st} = -R(\partial \ln x / \partial (1/T))_y$$

where,  $x$  is the pressure,  $T$  is the temperature,  $R$  is the gas constant and  $y$  is the adsorption amount.

These calculations are done through the “Heat of Adsorption” function embedded in the Belsorp Adsorption/Desorption Data Analysis software version 6.3.1.0.

**Table S1.** Comparison of BET surface area, H<sub>2</sub>, N<sub>2</sub>, CO<sub>2</sub> and CH<sub>4</sub> uptake, isosteric heat of adsorption for N<sub>2</sub>, CO<sub>2</sub> and CH<sub>4</sub> with literature reports.

Complex	BET surface area (m <sup>2</sup> g <sup>-1</sup> )	H <sub>2</sub> uptake at 77 K	N <sub>2</sub> uptake			CO <sub>2</sub> uptake				CH <sub>4</sub> uptake			Q <sub>st</sub> N <sub>2</sub>	Q <sub>st</sub> CO <sub>2</sub>	Q <sub>st</sub> CH <sub>4</sub>	Ref.
			298 K	273 K	263 K	298 K	273 K	263 K	195 K	298 K	273 K	263 K				
Zn-CBS	282	64	4.1	6.6	8.3	38.7	47.5	49.3	85.9	15.1	21.2	24.8	0.7	35	51.8	This work
[[Cd(ATAIA)]·4H <sub>2</sub> O] <sub>n</sub>	62	20.12				17.1	24.3							37.5		ACS Appl. Mat. Int., 2018, <b>10</b> , 25360-25371
TEA@bio-MOF-1	1220						4.16 mmol/g							26.5		JACS, 2010, <b>132</b> , 5578
TMA@bio-MOF-1	1460						4.446 mmol/g							23.9		
CPF-13		223.9				81	116							28.3		Chem. Mater., 2012, <b>24</b> , 2624-2626
JUC-141	1057		6.76	13.9		51.3	79.9			21.8	37.8		27.2	27.8	22.7	Inorg. chem., 2017, <b>56</b> , 6938-6942
MAF-2						19	49							27		JACS, 2009, <b>131</b> , 5516-5521
[Zn(atz) <sub>2</sub> ]	1014		29.4	50.1		99	140							26	19.5	Inorg. Chem. 2012, <b>51</b> , 9950-9955

Zn <sub>2</sub> (BDC) <sub>2</sub> (DABCO)	1725					13.7				5.3				20		<i>Microporous and mesoporous material</i> , 2010, <b>132</b> , 305
$((\text{CH}_3)_2\text{NH}_2)_{1.5} [\text{Zn}_3\text{L}_2(\text{HCOO})_{1.5}]_x\text{DMF}$	153.4			8.93			57.5				2.48					<i>J. Mater. Chem. A</i> , 2014, <b>2</b> , 17771-17778
SNU-150, SNU-77S, SNU-151, and SNU-100	1563, 3670, 1852		0.546, 0.40, 0.519, and 0.624 (wt%)			6.09, 3.94, 14.1, and 14.1	12.0, 8.21, 22.2, and 19.9		78.6, 169, 67.8, and 45.2	0.859, 0.62, 1.24, and 1.41	1.29, 1.20, 2.00, and 2.56				12.8, 14.3, 18.2, and 26.5	<i>Chem. Eur. J.</i> , 2013, <b>19</b> , 17432-17438
IITKGP-5	366		4	5.5		49	56.4			13.6	17		4.6	22.6	14.8	<i>Dalton Trans.</i> , 2017, <b>46</b> , 15280-15286
IITKGP-6	83.4		4.1	6.2		37.4	50.6			9.2	13.8		5.1	23	18.4	<i>Inorg. Chem.</i> , 2017, <b>56</b> , 13991-13997
IISERP-MOF20	945					3.5			9 mmol/g					26		<i>Inorg. Chem.</i> , 2018, <b>57</b> , 5267-5272

### CO<sub>2</sub> selectivity over N<sub>2</sub> and CH<sub>4</sub> - IAST selectivity calculation for CO<sub>2</sub>/N<sub>2</sub> and CO<sub>2</sub>/CH<sub>4</sub> mixture:

Gas selectivity for mixture of CO<sub>2</sub>/N<sub>2</sub> (15:85) and CO<sub>2</sub>/CH<sub>4</sub> (50:50) at different temperature were calculated based on the ideal absorbed solution theory (IAST) proposed by Myers and Prausnitz.<sup>S1</sup> In order to calculate the selective sorption ability of **Zn-CBS** towards the separation of binary mixed gases, the parameter fitted from the single component CO<sub>2</sub> and N<sub>2</sub> and CH<sub>4</sub> adsorption based on the Dual-Site Langmuir-Freundlich (DSLFL) model and different parameter were used given below.

$$y = \frac{q_{m1} b_1 p^{n1}}{1 + b_1 p^{n1}} + \frac{q_{m2} b_2 p^{n2}}{1 + b_2 p^{n2}}$$

where, p is the pressure of the bulk gas at equilibrium with the adsorbed phase (kPa); y is the adsorbed amount per mass of adsorbent (mmol/g), q<sub>m1</sub> and q<sub>m2</sub> are the saturation capacities of sites 1 and 2 (mmol/g); b<sub>1</sub> and b<sub>2</sub> are the affinity coefficients of sites 1 and 2, n<sub>1</sub> and n<sub>2</sub> represent the deviation from an ideal homogeneous surface.

The predicted adsorption selectivity is defined as

$$S = \left( \frac{\frac{x_1}{y_1}}{\frac{x_2}{y_2}} \right)$$

where, x<sub>i</sub> and y<sub>i</sub> are the mole fractions of component 1 (i = 1, 2) in the adsorbed and bulk phases, respectively. The IAST calculation was carried out for a binary mixture containing 15% CO<sub>2</sub> (y<sub>1</sub>) and 85% N<sub>2</sub> (y<sub>2</sub>) and 50% CO<sub>2</sub> (y<sub>1</sub>) and 50% CH<sub>4</sub> (y<sub>2</sub>), which is typical for flue gases and landfill gases, respectively.

(S1) A. L. Myers and J. M. Prausnitz, *AIChE J.*, 1965, **11**, 121-127.

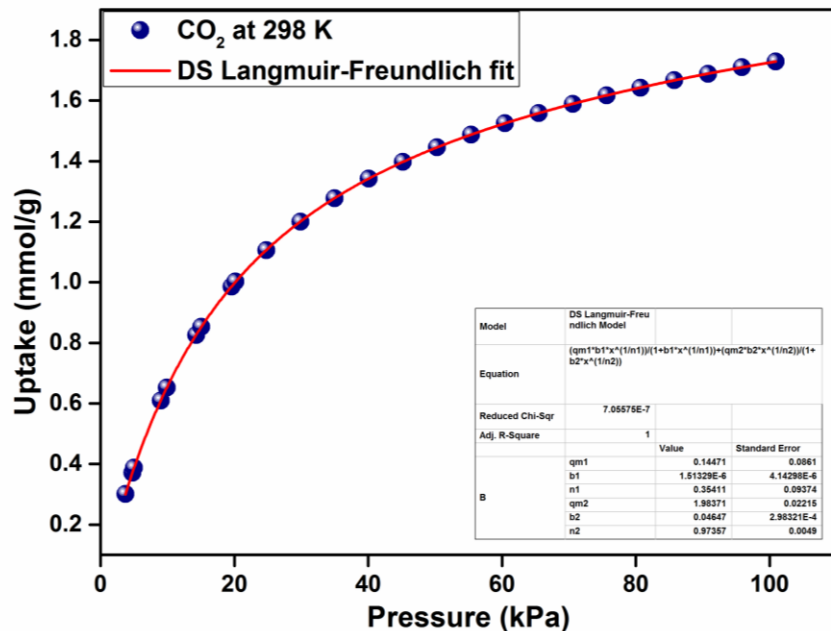


Fig. S13 Dual-site Langmuir-Freundlich fitted (red line) for CO<sub>2</sub> (blue circle) isotherm measure at 298 K.

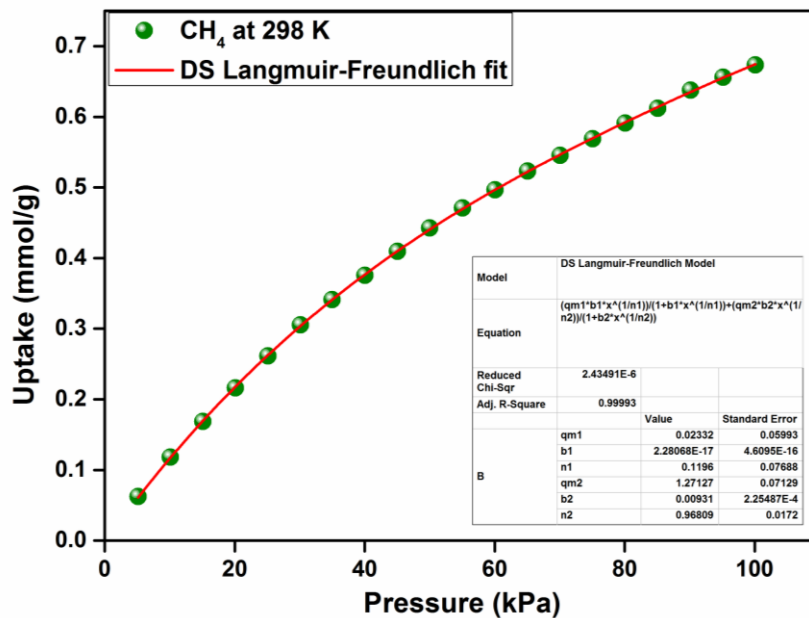


Fig. S14 Dual-site Langmuir-Freundlich fitted (red line) for CH<sub>4</sub> (green circle) isotherm measure at 298 K.

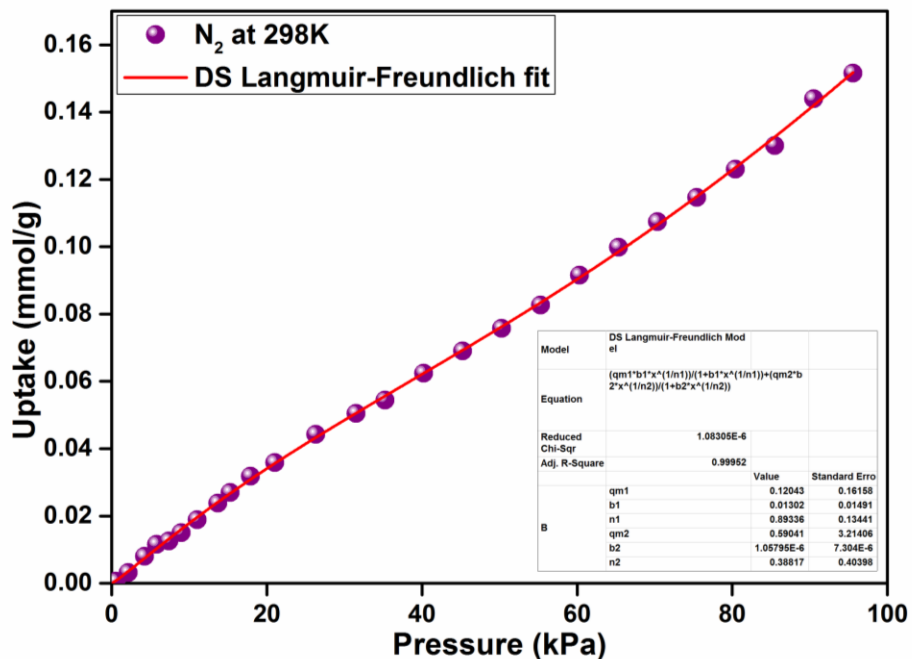


Fig. S15 Dual-site Langmuir-Freundlich fitted (red line) for N<sub>2</sub> (violet circle) isotherm measure at 298 K.

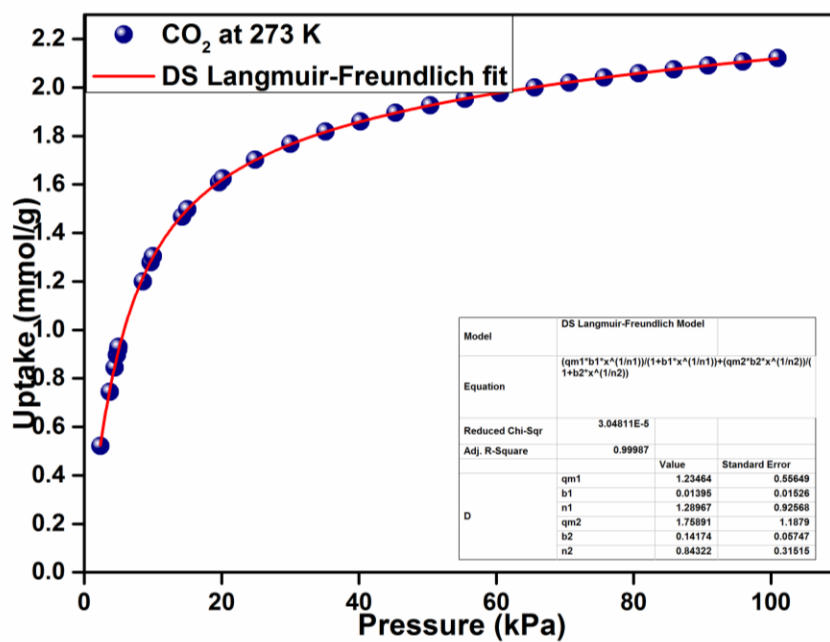


Fig. S16 Dual-site Langmuir-Freundlich fitted (red line) for CO<sub>2</sub> (blue circle) isotherm measure at 273 K.



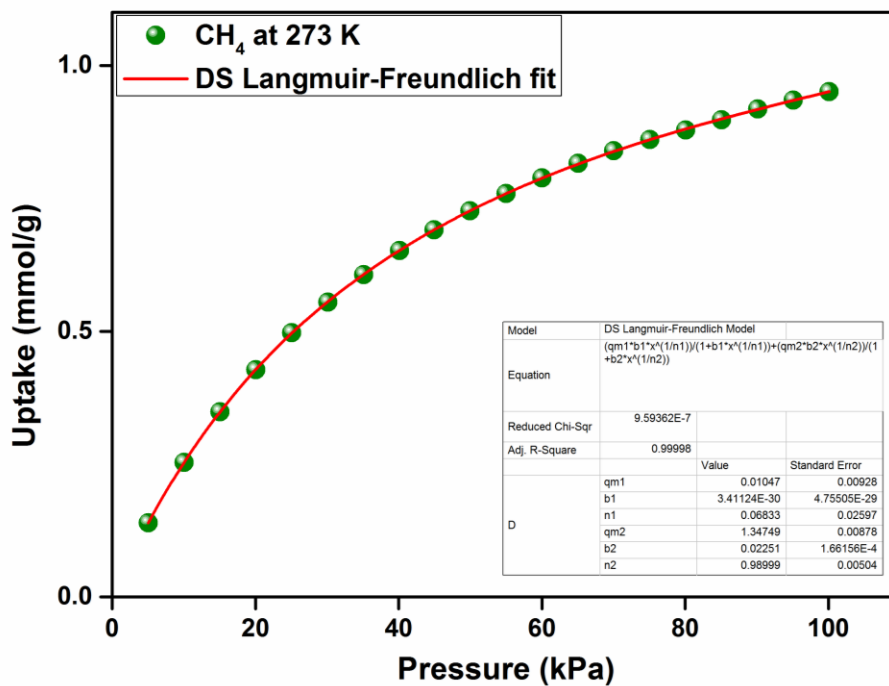


Fig. S17 Dual-site Langmuir-Freundlich fitted (red line) for CH<sub>4</sub> (green circle) isotherm measure at 273 K.

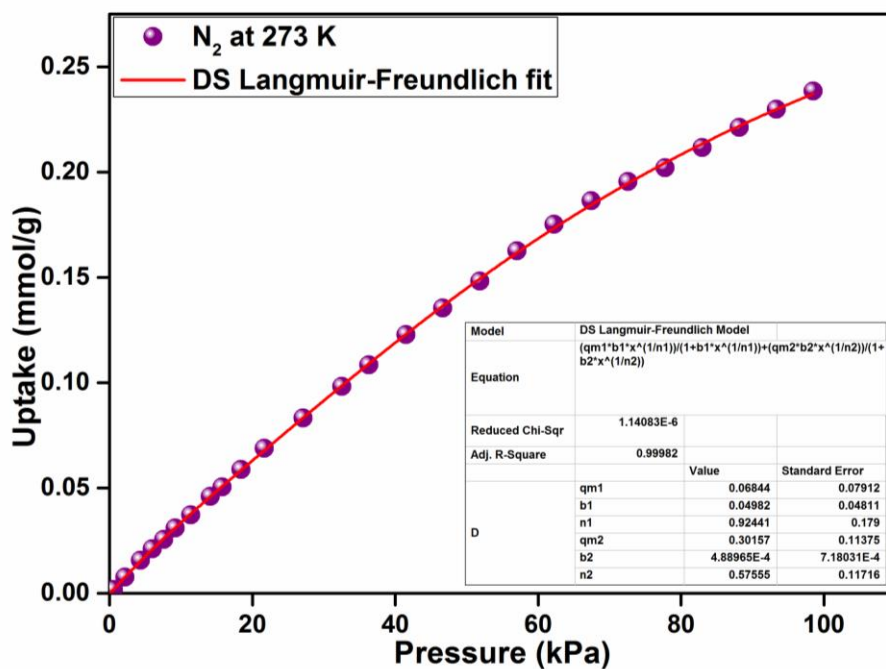


Fig. S18 Dual-site Langmuir-Freundlich fitted (red line) for N<sub>2</sub> (violet circle) isotherm measure at 273 K.

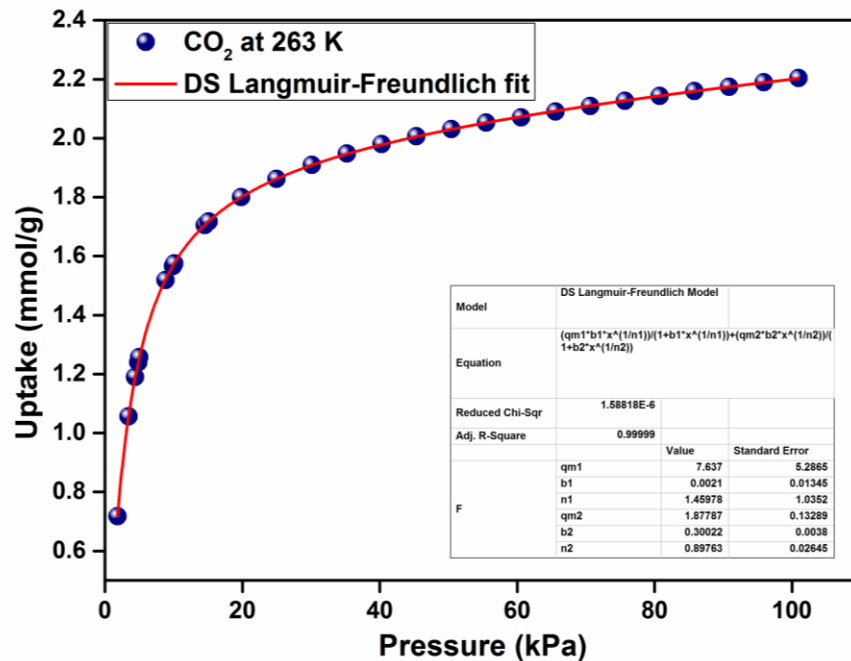


Fig. S19 Dual-site Langmuir-Freundlich fitted (red line) for CO<sub>2</sub> (blue circle) isotherm measure at 263 K.

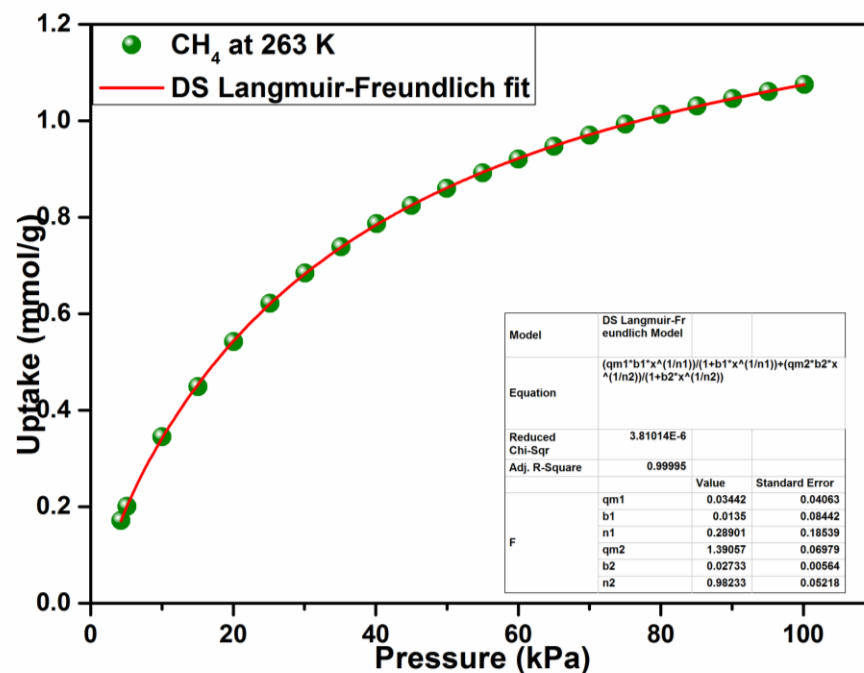
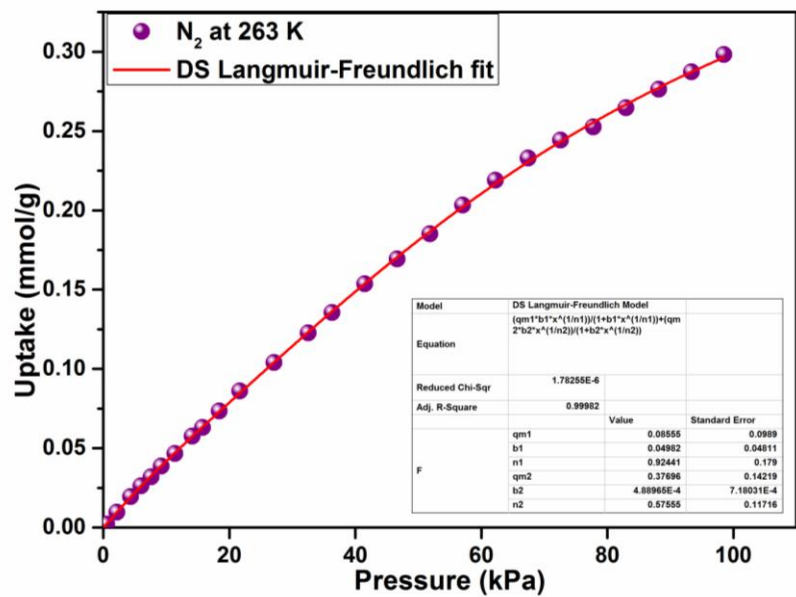


Fig. S20 Dual-site Langmuir-Freundlich fitted (red line) for CH<sub>4</sub> (green circle) isotherm measure at 263 K.



**Fig. S21** Dual-site Langmuir-Freundlich fitted (red line) for N<sub>2</sub> (violet circle) isotherm measure at 263 K.

**Table S2.** Summary of parameters for the DSLF isotherm model.

Parameter → Adsorbates ↓	$q_{m1}$ (mmol/g)	$b_1$ (1/kPa)	$n_1$	$q_{m2}$ (mmol/g)	$b_2$ (1/kPa)	$n_2$
CH <sub>4</sub> (298 K)	0.02332	2.2068E-17	0.1196	1.27127	0.00931	0.96809
CO <sub>2</sub> (298 K)	0.14471	1.51329E-6	0.35411	1.98371	0.04647	0.97357
N <sub>2</sub> (298 K)	0.12043	0.01302	0.89336	0.59041	1.05795E-6	0.38817
CH <sub>4</sub> (273 K)	0.01047	3.41124E-30	0.06833	1.34749	0.02251	0.98999
CO <sub>2</sub> (273 K)	1.23464	0.01395	1.28967	1.75891	0.14174	0.84322
N <sub>2</sub> (273 K)	0.06844	0.04982	0.92441	0.30157	4.88965E-4	0.57555
CH <sub>4</sub> (263 K)	0.03442	0.0135	0.28901	1.39057	0.02733	0.98233
CO <sub>2</sub> (263 K)	7.637	0.0021	1.45978	1.87787	0.30022	0.89763
N <sub>2</sub> (263 K)	0.08555	0.04982	0.92441	0.37696	4.88965E-4	0.57555

**Table S3.** Comparison for the selectivity of CO<sub>2</sub>/N<sub>2</sub> and CO<sub>2</sub>/CH<sub>4</sub> with literature reports.

Complex	Selectivity CO <sub>2</sub> /N <sub>2</sub> uptake			Selectivity CO <sub>2</sub> /CH <sub>4</sub> uptake			References
	298 K	273 K	263 K	298 K	273 K	263 K	
Zn-CBS	408	916	1832	12.2	17.2	24.5	This work
JUC-141	27.6	21.6		8.72	4.20		<i>Inorg. Chem.</i> , 2017, <b>56</b> , 6938-6942
SNU-150, SNU-77S, SNU-151, and SNU-100	5.4, 30, and 26.5			2.26, 7.20			<i>Chem. Eur. J.</i> , 2013, <b>19</b> , 17432–17438
[Zn(atz) <sub>2</sub> ]	225	403		5.8	7.5		<i>Inorg. Chem.</i> , 2012, <b>51</b> , 9950-9955
IITKGP-5	147.8	435.5		23.8	151.6		<i>Dalton Trans.</i> , 2017, <b>46</b> , 15280–15286
IITKGP-6	42.8	51.3		5.1	36		<i>Inorg. Chem.</i> , 2017, <b>56</b> , 13991-13997
IISERP-MOF20	250	220					<i>Inorg. Chem.</i> , 2018, <b>57</b> , 5267-5272
MAF-66	225	403		5.8	7.5		<i>Chem. Commun.</i> , 2014, <b>50</b> , 12101-12104
UTSA-49a	93.5	193.7		33.7	34.8		
(Me <sub>2</sub> NH <sub>2</sub> ) <sub>2</sub> [(In <sub>2</sub> X)]·9DMF·5H <sub>2</sub> O		250		5.6	6.4		<i>Inorg. Chem.</i> , 2013, <b>52</b> , 3127-3132
NOTT-202a	4.3	26.7		1.4	2.9		<i>Nat. Mater.</i> , 2012, <b>11</b> , 710-716
UTSA-15a, UTSA-20a, UTSA-25a, UTSA-33a, and UTSA-34a				14.2, 8.3, 9.4, 7.0, and 5.1			<i>Nat. Commun.</i> , 2012, <b>3</b> , 954-963

### **Density Functional Theory (DFT) and Configurational Bias Monte Carlo (CBMC) molecular simulation:**

Ligand H<sub>3</sub>(D-2,4-cbs) was optimized in DFT and put in a (1 x 1 x 1) cell for further calculation. The simulation boxes representing the ligand consist of (1 x 1 x 1) unit cells for CO<sub>2</sub>, N<sub>2</sub> and CH<sub>4</sub> (optimized). All the calculations were performed at 298 K at fixed pressure 1 bar. Interatomic interactions were modeled with standard Lennard-Jones potential and Columbic potentials. Lorentz-Berthelot mixing rules were employed to compute the Lennard-Jones parameters between unlike atom types. The pairwise interactions between host and guest atoms of the particular force field were analysed by utilizing the non-bonding parameter. The long-range part of electrostatic interactions was handled using the Ewald summation technique with a relative precision of 10<sup>-6</sup>. Periodic boundary conditions were applied in all three dimensions. For each state point, the CBMC simulation consists of 1 x 10<sup>7</sup> steps to guarantee equilibration, followed by 1 x 10<sup>7</sup> steps to sample the desired thermodynamic properties.

**Table S4.** Calculation of number of molecules absorbed per formula unit of Zn-CBS based on TGA.

<b>Solvent</b>	<b>Found (wt%)</b>	<b>Calculated (wt%)</b>	<b>Number of guest molecules</b>
Acetonitrile	15.0	14.6	3.75
Ethanol	15.0	15.2	3.5
Methanol	8.9	8.9	2.75
Tetrahydrofuran	12.5	12.3	1.75
Toluene	18.2	17.7	2.1
p-Xylene	14.7	15.0	1.5