

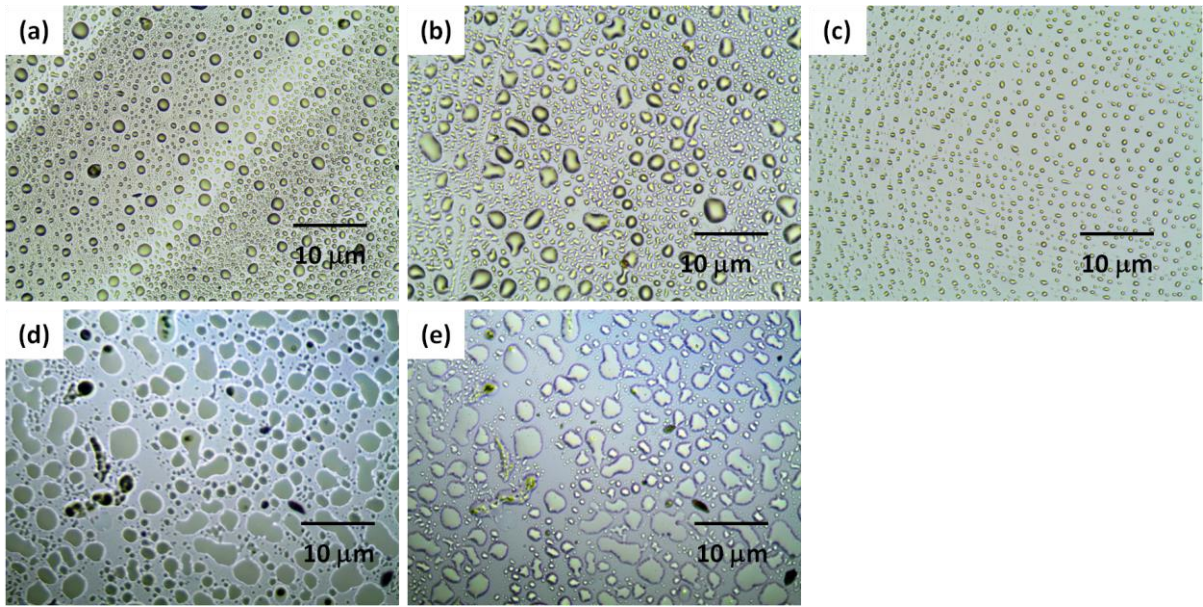
**Preferential water remediation of cationic dyes using structurally engineered novel organoselenium based self-assembled constructs**

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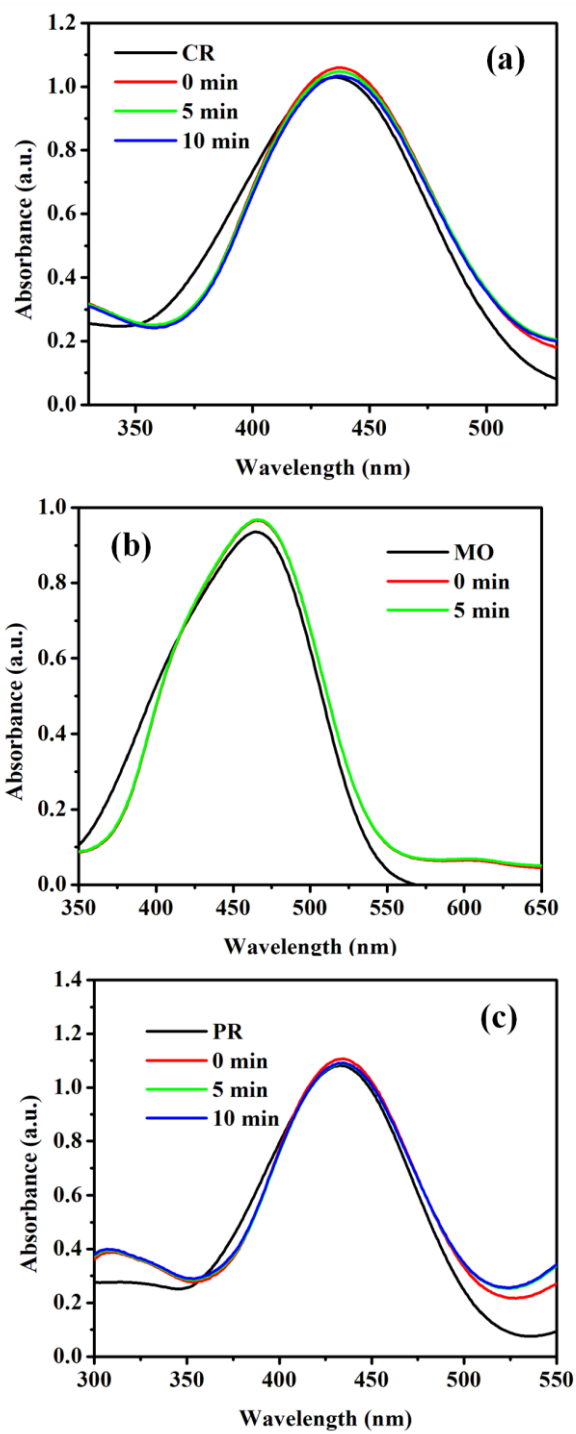
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**Fig. S1** Optical microscopic images of self-assembled IPSeX1 in (a) Acetone (b) Methanol (c) Dichloromethane (d) Acetonitrile (e) 1,4-dioxane



**Fig. S2** Absorption spectra of (a) CR (b) MO and (c) PR.

The equilibrium adsorption capacity,  $q_e = \frac{C_0 - C_e}{W} \times V$

For CV, Dye adsorption capacity at equilibrium: 0.01 mg adsorbent

$$q_e = \frac{(5-2.90) \mu\text{g/mL} \times (10^{-3} \text{ mg} / 10^{-3} \text{ L}) \times 1 \text{ mL} \times 10^{-3} \text{ L}}{0.01 \text{ mg} \times 10^{-3} \text{ g}}$$

$q_e = 210 \text{ mg/g}$  for CV

For MB, Dye adsorption capacity at equilibrium: 0.01 mg adsorbent

$$q_e = \frac{(5-3.515) \mu\text{g/mL} \times (10^{-3} \text{ mg} / 10^{-3} \text{ L}) \times 1 \text{ mL} \times 10^{-3} \text{ L}}{0.01 \text{ mg} \times 10^{-3} \text{ g}}$$

$q_e = 148.5 \text{ mg/g}$  for MB

Fig. S3 Dye adsorption capacity at equilibrium for CV and MB

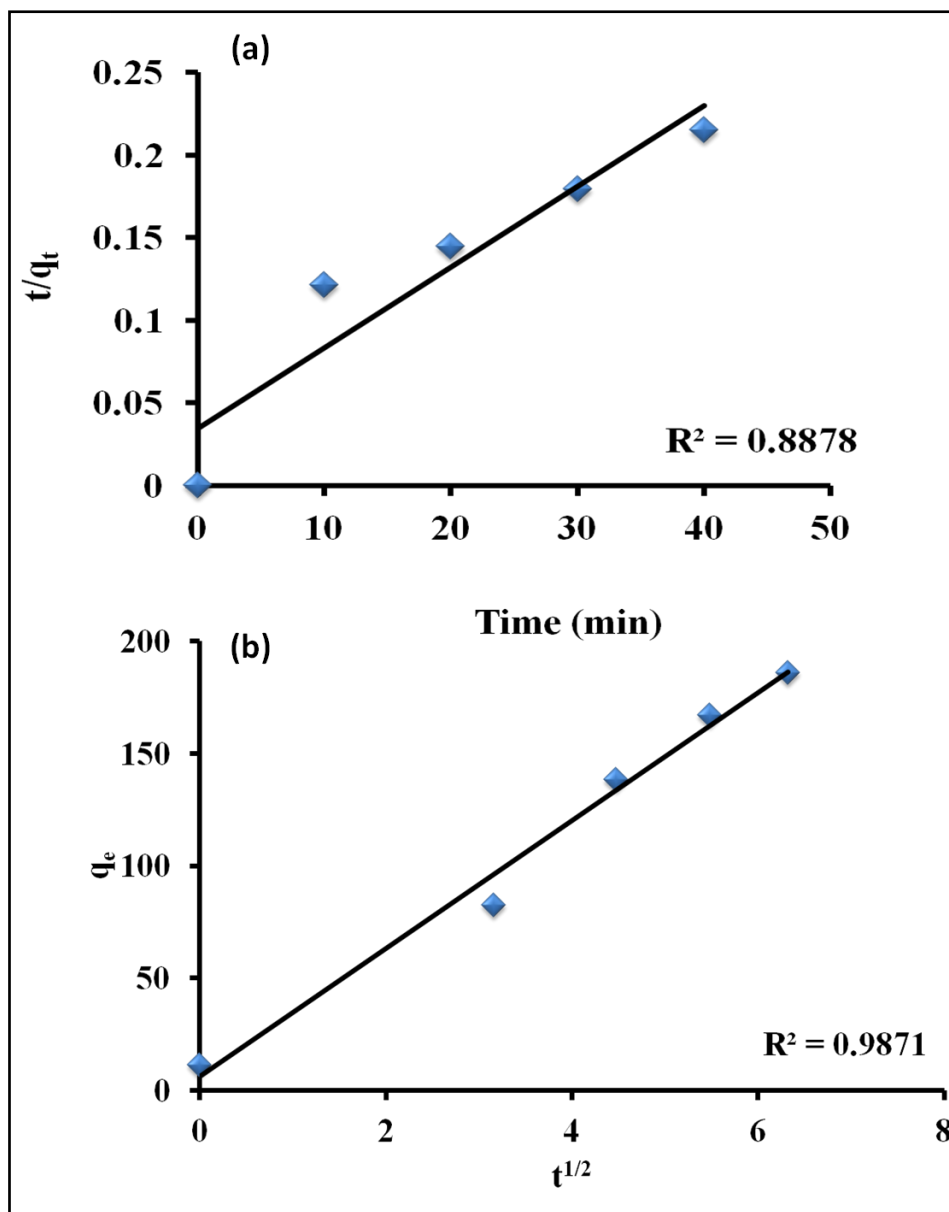


Fig. S4 (a) Pseudo second order (b) Intraparticle diffusion model for adsorption of CV

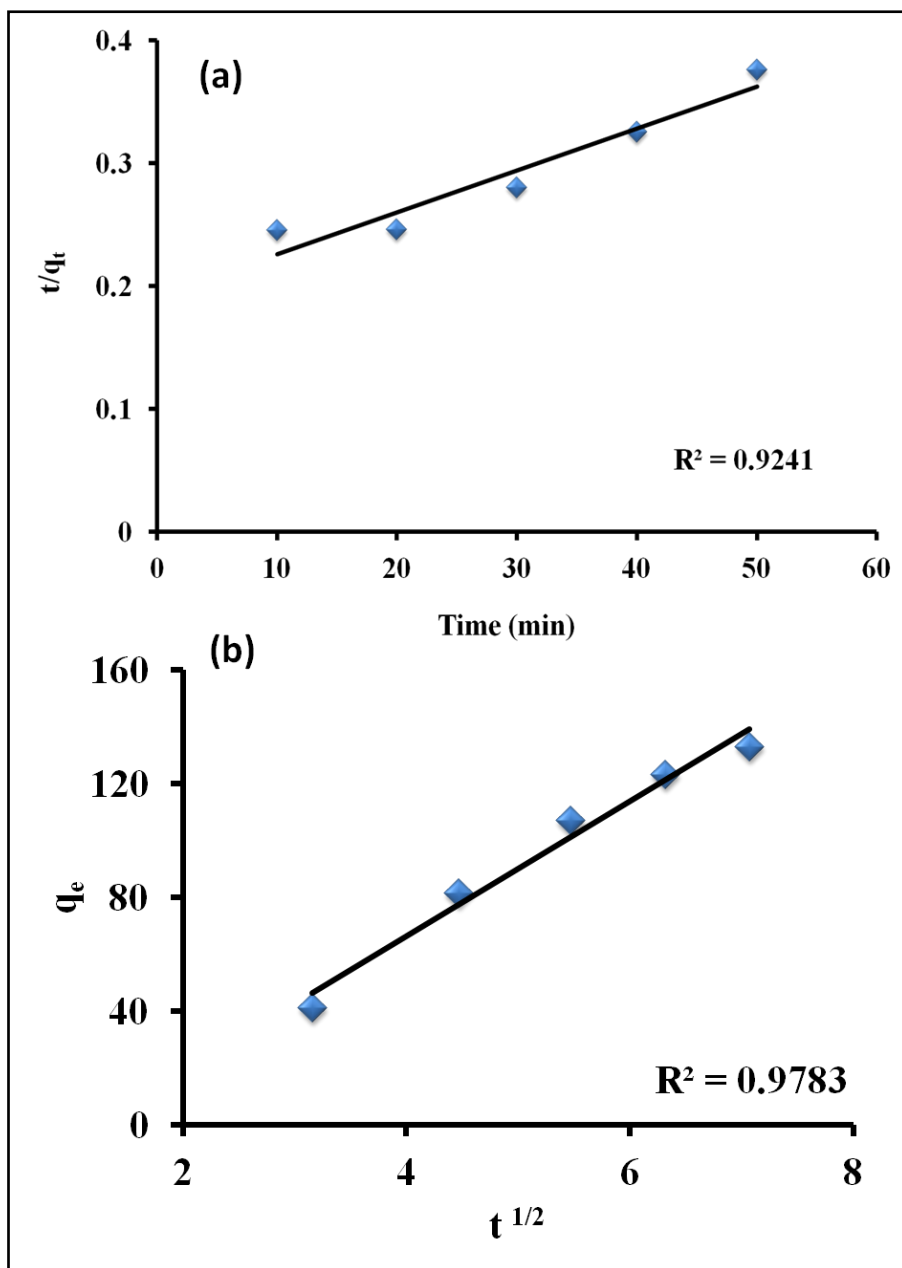
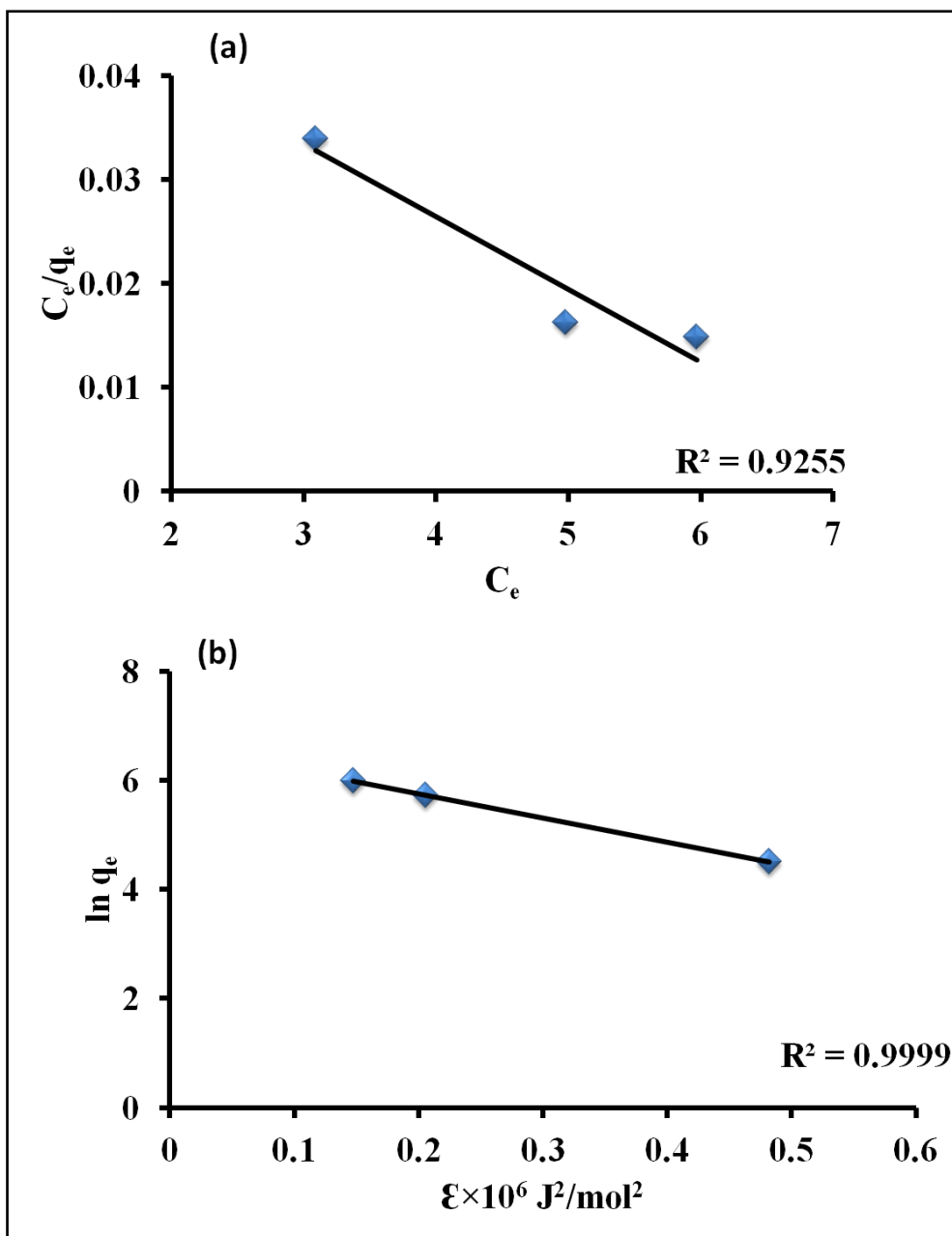


Fig. S5 (a) Pseudo second order (b) Intraparticle diffusion model for adsorption of MB



**Fig. S6** (a) Langmuir adsorption isotherm (b) D-R adsorption isotherm for CV



### Adsorption Isotherms for CV:

**Freundlich adsorption isotherm:**

$$\ln q_e = \frac{1}{n} \ln C_e + \ln K_F$$

$$R^2 = 0.991$$

**From the graph  $\ln q_e$  versus  $\ln C_e$ ,**

$$y = 2.3168x + 1.9202$$

$$\frac{1}{n} = 2.3168; \quad n = 0.431$$

$$K_F = 6.822$$

**D-R adsorption isotherm:**

$$\ln q_e = \ln q_m - \beta \epsilon^2$$

**From the graph  $\ln q_m$  versus  $\epsilon^2$**

$$y = -4.4251x + 6.6426$$

$$R^2 = 0.9999$$

$$\beta = 4.4251, \quad E = 1/(2\beta)^{1/2}$$

**Energy of adsorption = 0.475 KJ/ mol**

$$\ln q_m = 6.6426$$

$$q_m = 767.08 \text{ mg/g}$$

**Fig. S7** Maximum dye adsorption capacity,  $q_m$  for CV using Freundlich and D-R adsorption isotherm

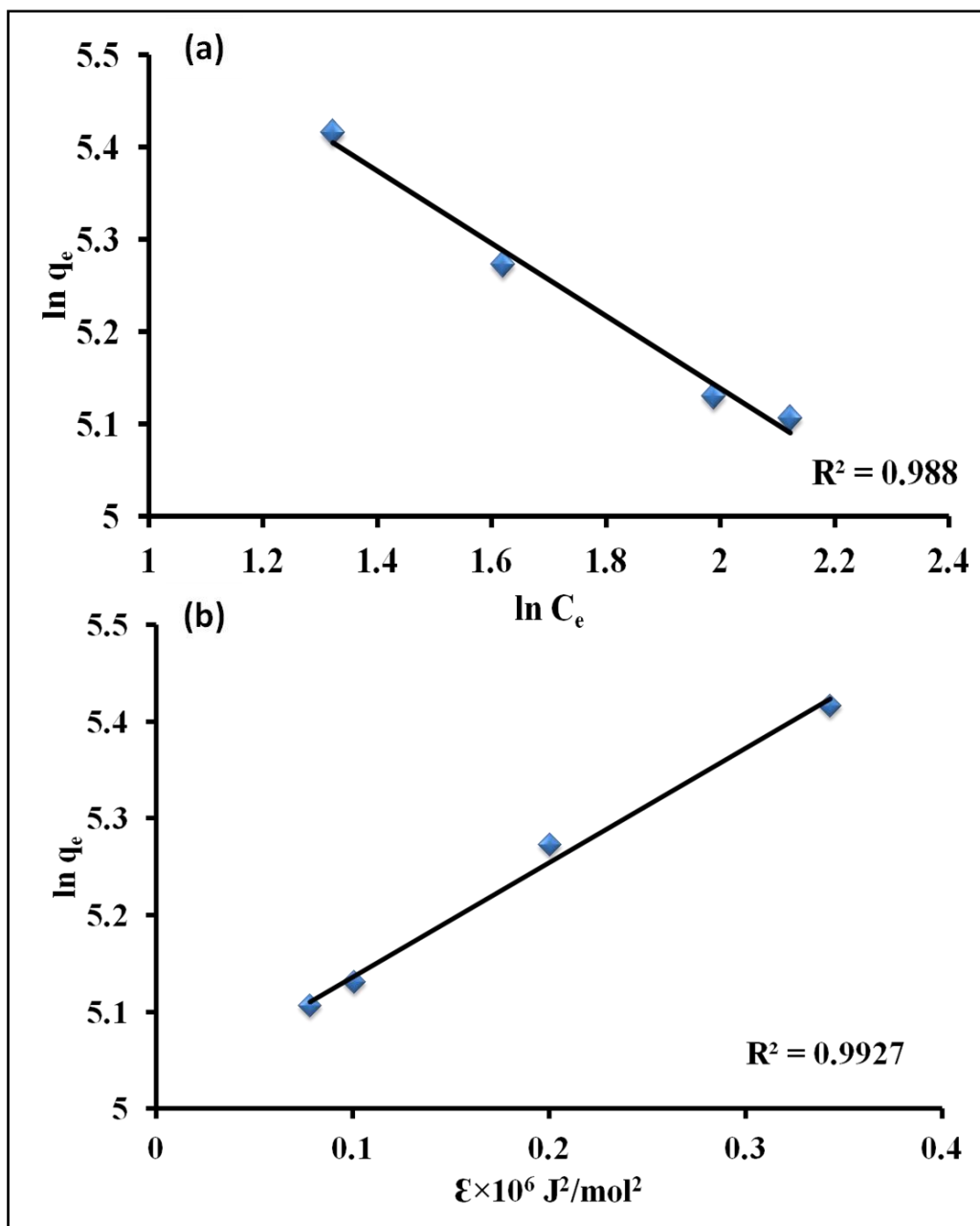


Fig. S8 (a) Freundlich adsorption isotherm (b) D-R adsorption isotherm for MB

**Adsorption Isotherms for MB:**

**Langmuir adsorption isotherm:**

$$\frac{C_e}{q_e} = \frac{1}{K_L q_m} + \frac{C_e}{q_m}$$

**From the graph  $C_e / q_e$  versus  $q_e$**

$$y = 0.0074x - 0.0114$$

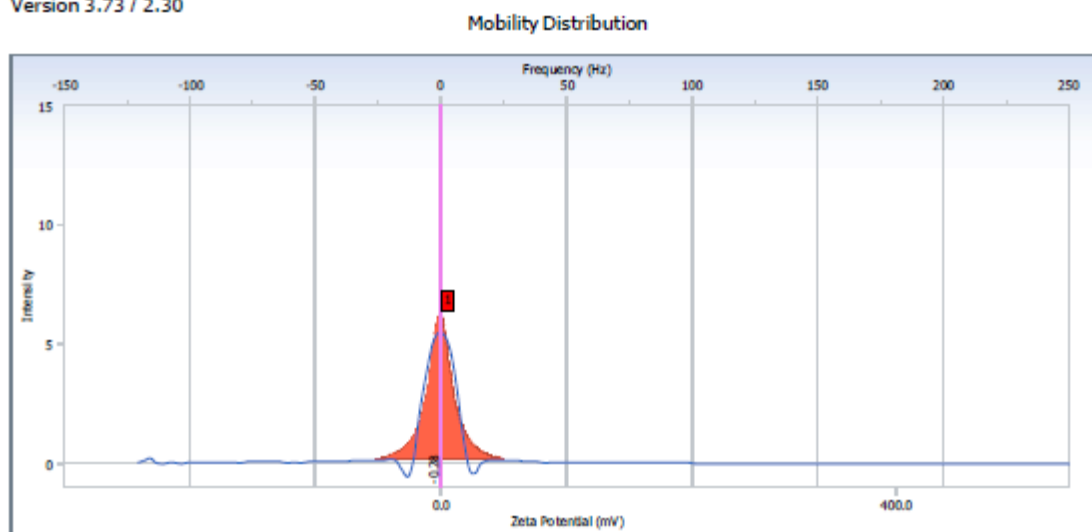
$$\text{Slope} = \frac{1}{q_m} = 0.0074$$

**Maximum adsorption capacity for MB,  $q_m = 135.13\text{mg/g}$**

**Fig. S9** Maximum dye adsorption capacity,  $q_m$  for MB using Langmuir adsorption isotherm

pH Value	Dye adsorption capacity (mg/g)	
	CV	MB
2	17.5	15.2
5	20.8	19.9
7	195.4	180.78
9	350.8	302.6
12	389.6	323.3

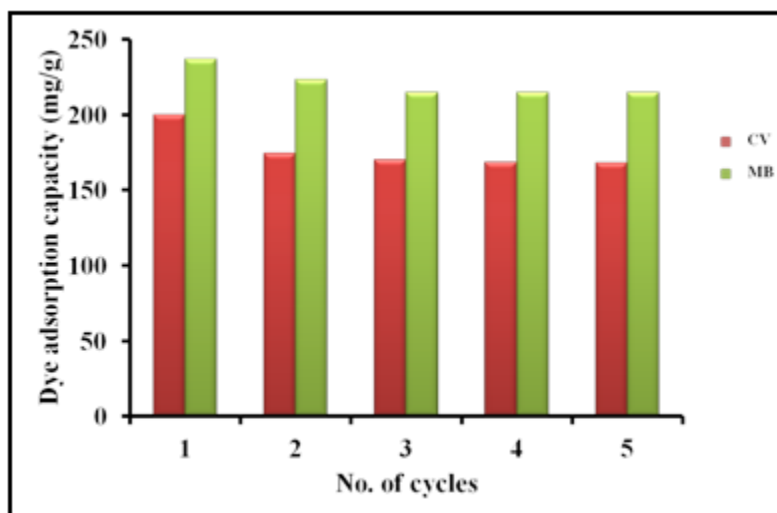
**Table S1.** Dye adsorption capacity of CV and MB at different pH values (2-12).



Measurement Results

Zeta Potential	: -0.28	(mV)	Doppler shift	: -0.12	(Hz)
Mobility	: -1.575e-006	(cm <sup>2</sup> /Vs)	Base Frequency	: 120.6	(Hz)
Conductivity	: 0.0490	(mS/cm)	Conversion Equation	: Smoluchowski	

**Fig. S10** Zeta potential analysis of surface of self-assembled fibrils of IPSeX1



**Fig. S11** Recyclability of peptide fibrils for the adsorption of CV and MB