# Supplementary Information

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Text S1 Determination of iron ion concentration

The iron ion concentration in the solution was determined by o-phenanthroline chromogenic method. Ferrous ion could form a red complex with colorless phenanthroline. The complex had a strong characteristic absorption peak at 510 nm, which could be detected by UV spectrophotometer. When determining the concentration of Fe<sup>2+</sup> or total iron ion, 0.5 mL hydrochloric acid amine solution (100 mg/L) or water was added to 0.5 mL sample to be tested, then 0.5 mL phenanthroline solution (1 g/L) and 0.5 mL sodium acetate solution (mass fraction 10%) were added. Then the solution was shaken evenly for color development and the absorbance of the sample was determined.

#### Text S2 LC-MS Analysis

The intermediates were isolated using an ACQUITY UPLC® BEH C18 column (2.1 × 50 mm, 1.7  $\mu$ m). A mobile phase including formic acid (A) and acetonitrile (B) was used. Sample Cone: 30-60 V; Extraction Cone: 30-60 V; Source temperature: 120 °C; Desolvation temperature: 350 °C; Cone Gas: 50 L/h; Desolvation Gas: 800 L/h. According to the mass-to-charge (*m/z*) value, the LC-MS chromatogram of the intermediate product of MO degradation was shown in Fig. S7.

## Text S3 Energy efficiency

In order to quantitatively evaluate the energy efficiency under different systems, the conversion rate per unit time per unit current was calculated according to Equation (S1-1), which was expressed as EE (A<sup>-1</sup>min<sup>-1</sup>):

$$EE = \frac{d_r}{I \times t} \tag{S1-1}$$

Where I (A) was the current, t (min) was the degradation time,  $d_r$  (%) was final degradation rate, and EE (A<sup>-1</sup>min<sup>-1</sup>) was energy efficiency.



Fig. S1 Degradation experimental device diagram.



Fig. S2 Determination of Fe ion concentration in sample reaction process.



Fig. S3 Comparison of the performance with different methods.



Fig. S4 Effect of different reaction conditions on performance of Fe-MOFs (a) MO concentration;

(b) discharge voltage; (c) catalyst addition amount; (d)  $H_2O_2$  addition amount; (e) pH.



Fig. S5 Recyclability and reusability tests.



Fig. S6 Effect of capture agents on MO degradation during plasma/Fenton-like process.



Fig. S7 LC-MS chromatograms corresponding to the intermediates of MO degradation.

TA/Fe molar ratio	Average particle size /(nm)
1:1	49
1:2	24
1:3	17
1:4	23

Table S1 Average particle size of Fe-MOFs with different TA/Fe molar ratios

**Table S2** Composition of Fe-MOFs with different TA/Fe molar ratios

TA/Fe	EDS v	vt%
molar ratio	Fe	0
1:1	24.19	75.81
1:2	32.61	67.39
1:3	43.39	56.61
1:4	28.31	71.69

Table S3 Surface and pore structure of Fe-MOFs with different TA/Fe molar ratios

TA/Fe	Surface area	Average pore size	Pore volume	
molar ratio	(m <sup>2</sup> ·g <sup>-1</sup> )	(nm)	(cm <sup>3</sup> ·g <sup>-1</sup> )	
1:1	3.123	3.816	0.007	
1:2	20.864	3.411	0.154	
1:3	32.021	17.186	0.210	
1:4	19.992	3.410	0.131	

Table S4 Binding energies of Fe2p, O1s, and C1s for Fe-MOFs

TA/Fe	Binding energy /(eV)										
molar	Fe 2p						C1s			O1s	
ratio	Fe <sup>2+</sup>	Fe <sup>3+</sup>	satellite	Fe <sup>2+</sup>	Fe <sup>3+</sup>	C1s A	C1s	C1s B	O1s	O1s A	
	2p <sub>3/2</sub>	2p <sub>3/2</sub>	peak	$2p_{1/2}$	$2p_{1/2}$						
1:1	711.17	712.94	717.02	724.48	726.46	284.54	285.34	288.91	531.44	532.18	
1:2	711.40	713.36	717.51	724.81	726.74	284.72	285.73	288.67	531.25	531.97	
1:3	711.11	712.72	716.18	724.47	726.10	284.68	285.61	288.64	531.24	532.00	
1:4	711.08	712.49	715.59	724.01	726.00	284.70	285.80	288.64	531.31	532.09	

TA/Fe	Proportion /(%)					
molar ratio	Fe <sup>2+</sup>	Fe <sup>3+</sup>	Fe <sup>2+</sup> /Fe <sup>3+</sup>	[O] <sub>s</sub> /([O] <sub>l</sub> +[O] <sub>s</sub> )		
1:1	46.85	45.36	1.03	42.89		
1:2	43.21	38.22	1.13	43.96		
1:3	46.83	39.94	1.17	44.00		
1:4	42.27	46.85	0.90	42.61		

**Table S5** Proportion of different valence elements of Fe-MOFs with different TA/Fe

 molar ratios

systems	catalyst	pollutants	pН	pollutants concentration (mg/L)	pollutants treatment capacity (mL)	catalyst addition amount (g/L)	Reaction time (min)	Degradation rate (d <sub>r</sub> ) (%)	EE (A <sup>-1</sup> min <sup>-1</sup> )	Refer ences
DBD plasma/Fenton- like	Fe-MOFs	МО	3	200	200	1.0	8	96.4	8.03	This work
PDP/Fenton	FeSO <sub>4</sub> ·7H <sub>2</sub> O	Bisphenol A	5.5	4.566	600	2.0	30	97	2.16	[11]
GAD/Fenton	ZVI (Fe <sup>0</sup> )	Acid Orange 7	7.4	63	400	26	25	80	0.64	[13]
Electro Fenton	pyrite	tyrosol	3	41	250	1.0	60	96	5.33	[38]
Electro Fenton	FeSO <sub>4</sub> ·7H <sub>2</sub> O	chloroquine drug	3	125	400	0.01	300	100	5.56	[39]
Electro Fenton	iron plate electrode	diisobutyl phthalate	4	10	500	-	45	93	2.07	[40]

 Table S6 Comparison of degradation ability by different systems

Relative molecular mass	Structure
304.07	
290.06	
261.03	
172.99	-0,38-ОН
172.00	
156.99	-o <sub>3</sub> s
138.01	O2N OH
110.03	но—————————————————————————————————————
107.07	
106.04	N=NH
93.05	NH2

 Table S7 Degradation intermediate

## References

F. Dai, X.R. Fan, G.R. Stratton, C.L. Bellona, T.M. Holsen, B.S. Crimmins, X.Y.
 Xia, S.M. Thagard, *J. Hazard. Mater.* 2016, 308, 419-429.
 https://doi.org/10.1016/j.jhazmat.2016.01.068.

C.M. Du, L.L. Zhang, J. Wang, C.R. Zhang, H.X. Li, Y. Xiong, *Plasma Chem. Plasma P.* 2010, 30, 855-871. https://doi.org/10.1007/s11090-010-9249-0.

S. Ammar, M.A. Oturan, L. Labiadh, A. Guersalli, R. Abdelhedi, N. Oturan, E. Brillas, *Water Res.*, 2015, 74, 77-87. http://dx.doi.org/10.1016/j.watres.2015.02.006.

S. Midassi, A. Bedoui, N. Bensalah, *Chemosphere.*, 2020, 260, 127558.
 https://doi.org/10.1016/j.chemosphere.2020.127558.

40. Z.Q. Yang, H.L. Chen, J.H. Wang, Q.F. Yuan, F. Wang, B.H. Zhou, *J. Environ. Chem. Eng.*, 2020, 8, 104057. https://doi.org/10.1016/j.jece.2020.104057.