Supplementary Information

NH3-SCR of NO with novel active, supported vanadium-containing Keggin-type heteropolyacid catalysts

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Characterization of HPA-n POMs

ICP-OES was used to determine the composition of the synthesized vanadium-substituted HPA-n Keggin-polyoxometalates. The results were adjusted considering one atom of phosphorous per Keggin unit according to the nature of the structure.

Table S1: Composition of the synthesized HPA-n polyoxometalates.

^a Determined via ICP-OES.

Solid state FTIR ATR of the as-synthesized HPA-n catalysts was recorded in order to validate that they contained the Keggin structure. [Figure](#page-1-0) S1 shows the FTIR spectra of the different HPA-n catalysts. All characteristic stretching vibrations of the Keggin oxoanion were observed at 1065 cm⁻¹ (v_{as} P-O_a), 959 cm⁻¹ (v_{as} Mo-O_d), 865 cm⁻¹ (v_{as} Mo-O_b-Mo) and 771 cm⁻¹ (v_{as} M- O_b -Mo). ¹

Figure S1: FTIR spectra of the synthesized HPA-n catalysts measured with a Jasco FT/IR-4100 spectrometer equipped with a PIKE GladiATR ATR-accessory.

Characterization of the supported HPA-n POM catalysts

ICP-OES analysis was used to determine the metal content in the different supported catalysts.

Table S2: ICP-OES results of supported HPA-n catalysts.

Characterization of the pure support materials

Specific surface area, pore volume and average pore diameter of all support materials were determined by N_2 -physisortion. Moreover, temperature-programmed desorption (TPD) of $NH₃$ measurements were performed to get more information regarding the acidity of the pure supports.

Support material	BET surface area $[m^2 g^{-1}]$	Pore vol. $[cm^3 \, g^{-1}]$	Av. pore diameter [Å]	Ads. $NH3$ [mmol g^{-1}]	T_{max} [°C]
ZrO ₂	132.0	0.16	47.93	0.51	192.5
TiO ₂	82.9	0.25	114.52	0.15	166.0
SiO ₂	441.9	0.72	62.44	0.08	297.4
Al ₂ O ₃	266.6	0.69	104.06	0.48	158.9
C	531.4	0.73	54.58	0.18	295.2

Table S3: Textural properties and NH₃-TPD results of the different support materials.

In-situ EPR measurements

Quantification of active vanadium was carried out by EPR in two replicates (see below) on fresh HPA-3/TiO₂, V₂O₅-HPA-0/TiO₂ and The HPA-3/Al₂O₃ by referencing to EPR measurements of VOSO₄ in K₂SO₄. The results show HPA-3/TiO₂ catalyst contained 0.18 ± 0.01 wt.% EPR active [VO]²⁺, while V₂O₅-HPA-0/TiO₂ contained 0.13 ± 0.08 wt.% EPR active [VO]²⁺. HPA-3/Al₂O₃ only gave a weak signal but it was estimated that it contained less than 0.05 wt.% EPR active [VO]²⁺. These amounts corresponded to 11, 8 and <4% of the total V measured by ICP being EPR active for the catalysts. The standard curves are given in Figure S2.

Figure S2: Standard curves for quantification of active vanadium by EPR at ambient conditions with no pre-treatment. Standards are shown as squares and samples as stars. The two curves represent two different series of measurements and are not directly comparable since the sample position and response differ between series.

A comparison of the EPR spectra of HPA-3/Al₂O₃ and the Al₂O₃ support itself showed that the signal observed at $g = 4.3$ and a broad signal at $g \approx 2$ was due to impurities on the support.

Figure S3: EPR spectra of the alumina support compared to HPA-3/Al₂O₃ recorded at ambient conditions with no pre-treatment.

A comparison of EPR spectra of the samples during operando SCR conditions is shown in Figure S4. The spectra showed a difference in EPR active species between the Al_2O_3 - and $TiO₂$ supported samples.

Figure S4: EPR spectra of the samples in 2.3 vol.% H_2O , 4.5 vol.% O_2 , 500 ppm NO and 550 ppm NH₃ at 250 °C in balance He. Red line is the HPA-3 on TiO₂, the blue line is V_2O_5 -HPA-0/TiO₂ and the black line is $HPA-3/Al₂O₃$.

Selected EPR spectra from each sample were simulated using Matlab with the EasySpin 5.2.23 program. Simulations and spectra are shown in Figures S5-S7. Three different EPR active species, A, B and C were observed on the HPA-3/TiO₂ and V_2O_5 -HPA-0/TiO₂ samples. The spin Hamiltonian values extracted from the simulated spectra of the reduced and oxidized samples are given in Table 2 of the main text. The simulations showed that for all the different conditions (SCR, NH₃, NO/NH₃, NO/O₂) much of the signal intensity could be assigned to the [VO]²⁺-species denoted C, which had a broad signal at $g = 1.96$ with unresolved hyperfine splitting and a large line width.

Figure S5: EPR spectra of HPA-3/TiO₂ (black lines) with the simulated spectra below (red lines). All flows were in balance He with 2.3 vol.% H₂O, and with 500 ppm NO, 550 ppm NH₃ and 4.5 vol.% O₂ when indicated.

The EPR spectrum of HPA-3/Al₂O₃ was compatible with a single vanadium species with varying intensity. The quantification of the signal for this sample was uncertain due to the low intensity of the initial spectrum and a non-vanadium impurity. Simulations and corresponding spectra are shown in Figure S7.

Figure S6: Recorded EPR spectra of V₂O₅-HPA-0/TiO₂ (black lines) with the simulated spectra below (red lines). All flows were in balance He with 2.3 vol.% H_2O , and with 500 ppm NO, 550 ppm NH₃ and 4.5 vol.% O₂ when indicated.

Figure S7: Top spectra: EPR spectra of HPA-3/Al₂O₃ (black lines) with the simulated spectra below (red lines). All flows were in balance He with 2.3 vol% $H₂O$, and with 500 ppm NO, 550 ppm NH₃ and 4.5 vol.% O_2 when indicated Bottom spectrum: Comparison of EPR spectra under NH₃ and under O_2 .

Exposure of samples to NH³ alone

All samples were exposed to the same experimental protocol: They were first heated to 200 °C in O_2 , then exposed to 550 ppm NH₃ and 2.3 vol.% H₂O in He at the same temperature and then heated to 250 °C in the same gas mixture. The exposure to $NH₃$ caused a significant increase in the intensity of the EPR signal for the HPA- $3/Al_2O_3$, see Figure S7, bottom. The increase corresponded to an increase in EPR active vanadium from less than 0.05 wt.% to a maximum of 0.43 wt.%. The resulting spectrum was axial and contained only one resolved EPR active vanadium species, with $g_z = 1.979$, $g_x = g_y = 1.927$ and $A_z = 190$, $A_x = A_y = 510$ MHz. After a few cycles between NO/NH₃ and NO/O₂ at 250 °C (see Figure 10 of the main text), the sample was exposed to $NH₃$ alone again. This time the intensity of the signal did not increase as much as before, and exposure to a mixture of $NO/NH₃$ did not increase the signal but rather decreased it a little, see Figure S9. Normally NO/NH_3 is considered the most reducing gas mixture and should give the highest intensity corresponding to the highest concentration of paramagnetic VO2+ .

Figure S8: Top: EPR spectra of samples in 4.5 vol.% O₂ and 2.3 vol.% H₂O in He at 200 °C (black lines). Bottom: The same samples after 30 min in 550 ppm NH₃ and 2.3 vol.% H₂O at 250 °C (red lines). The total flow was maintained at 200 mL min⁻¹ and the spectra were normalized with respect to the mass of the samples.

For the TiO₂ supported samples the same protocol was followed. Exposure to $NH₃$ initially caused a moderate increase of intensity to 0.25 wt.% EPR active $[VO]^2$ ⁺. The change was mainly in the broad unresolved signal at $g = 1.96$ (species C) and a slight broadening of the lines, whereas only small changes to features of species A and B was observed. The distribution of the three observed species for the HPA-3/TiO₂ changed slightly when exposed to $NH₃$. The increase in intensity was slow, however, and subsequent exposure to $NO/NH₃$ resulted in a faster and more significant increase.

Figure S9: Changes in amounts of EPR active vanadium at 250 °C in various conditions. Initial NH₃ represent the sample after exposure to 550 ppm $NH₃$ in 2.3 vol.% $H₂O$ and He balance on the sample that was heated in O_2 . NO/O₂ represent the sample exposed to 500 ppm NO and 4.5 vol.% O₂ in 2.3 vol.% H₂O and He balance. 2nd NH₃ represent the sample when exposed to 550 ppm NH₃ for 30 min after the sample had been exposed to $NO/O₂$ for the TiO₂ supported samples and after NO/NH₃ for the Al_2O_3 sample. NO/NH₃ represent the samples after exposure to 550 ppm NH₃ and 500 ppm NO in 2.3 vol.% H₂O and He balance after 20 min for the TiO₂ supported samples and 30 min for the Al₂O₃ sample.

$T = 250 °C$	X_{NO}	NNO.converted	n_v	TOF	k	
		mol $s-1$	mol	mol_{N2} /(mol _v s)	cm ³ (mol _{$\sqrt{5}$}) ⁻¹	mol $(s*mol_v)$
HPA-0	1%	2,84E-12				
HPA-1	7%	1,41E-11	3,86E-06	3,65E-06	1,70E+05	3,22E-03
HPA-2	19%	3,61E-11	7,82E-06	4,61E-06	2,29E+05	4,31E-03
HPA-3	25%	4,83E-11	1,20E-05	4,02E-06	2,08E+05	3,69E-03
HPA-4	26%	5,03E-11	1,62E-05	3,09E-06	$1,61E+05$	2,84E-03
HPA-5	33%	6,31E-11	2,06E-05	3,07E-06	1,67E+05	2,84E-03
HPA-6	36%	6,94E-11	2,51E-05	2,77E-06	$1,54E+05$	2,55E-03

Table S4: Summary of NO conversion (X_{NO}), amount of converted NO (n_{NO}, converted), amount of vanadium in the used catalyst (n_V), Turnover frequency (TOF), catalytic rate constant (k) and reaction rate (r) at 250 °C.

TOF was calculated using equation S1:

$$
TOF = \frac{h_{Products}}{n_{Vanadium}} = \frac{h_{NO, converted}}{n_{Vanadium}} \tag{S1}
$$

Reference:

1. Albert, J.; Lüders, D.; Bösmann, A.; Guldi, D. M.; Wasserscheid, P., Spectroscopic and electrochemical characterization of heteropoly acids for their optimized application in selective biomass oxidation to formic acid. *Green Chemistry* **2014,** *16* (1), 226-237.doi: 10.1039/C3GC41320A