## Supporting Information

# Selective synthesis of *para*-xylene and light olefins from $CO_2/H_2$ in the presence of toluene

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#### **Experimental Section**

#### **Catalyst Preparation**

ZnCr metal oxide with a Zn/Cr molar ratio of 2/1 (named as ZnCr) was prepared using a coprecipitation method.<sup>1</sup> Briefly, certain amounts of Zn(NO<sub>3</sub>)<sub>2</sub> and Cr(NO<sub>3</sub>)<sub>3</sub> were dissolved in distilled water, and then (NH<sub>4</sub>)<sub>2</sub>CO<sub>3</sub> aqueous solution was added to form precipitate. After being aged at 70 °C for 3 h, the precipitate was centrifuged and washed with distilled water. After being dried at 110 °C for 12 h, the precipitate was finally calcined at 500 °C for 4 h.

H-ZSM-5 with different SiO<sub>2</sub>/Al<sub>2</sub>O<sub>3</sub> ratio were purchased from Nankai University Catalyst Co.. Phosphorus modification ZSM-5 was carried out by impregnating the pristine ZSM-5 powder (Z5-pristine, SiO<sub>2</sub>/Al<sub>2</sub>O<sub>3</sub> ratio = 146) with H<sub>3</sub>PO<sub>4</sub> aqueous solution. After stayed at room temperature for 12 h, the sample was dried at 110 °C for 12 h and calcined at 550 °C for 4 h. The obtained samples were denoted as *x*P/Z5, where *x* represented the content of P (wt%).

Silica modification on Z5-pristine or 3P/Z5 was carried out by a chemical liquid deposition method using polysiloxane (Dow Corning-550) as the silica source, a molecule larger than the pore size of H-ZSM- $5.^2$  In detail, 8g Dow Corning-550 was dissolved in 40 ml n-hexane and 6 g ZSM-5 was introduced into the solution. After the solvent was evaporated at room temperature, the solid was dried at 110 °C for 5 h and calcined at 600 °C for 4 h. The obtained samples were denoted as (3P/)Z5-Siy, where y represented the cycle of silica deposition.

The ZnCr-ZSM-5 composite catalyst was obtained by mixing well the metal oxides and zeolites with a granule size 40-60 mesh (equivalent to 250-380  $\mu$ m) with a mass ratio of 1/1 unless otherwise stated.

#### **Catalyst Characterization**

X-ray diffraction (XRD) patterns were recorded on a PANalytic X'Pert Pro-1 instrument at 40 mA and 40 kV using Cu K<sub> $\alpha$ </sub> as the radiation source ( $\lambda = 0.1541$  nm). The specific surface area was analyzed by N<sub>2</sub> adsorption at -196 °C over QuadraSorb SI instrument (Quantachrome). All samples were evacuated at 300 °C for 6 h prior to measurements. SEM and EDS mapping were carried out on a JEOL JSM-7900F. The samples were ultrasonically suspended in ethanol and placed onto a carbon film supported over a Cu grid. The acidity of ZSM-5 was characterized by NH<sub>3</sub> temperature-programmed desorption (NH<sub>3</sub>-TPD) on a Micromeritics AutoChem 2910 instrument, following the previously reported procedure. <sup>2</sup>

The external acid sites were characterized by adsorption of 2,6-di-tert-butyl-pyridine (2,6-DTBPy).<sup>2</sup> The self-supported samples were first evacuated at 450 °C for 1.5 h and cooled down to 150 °C inside the *in situ* IR cell. 2,6-DTBPy was then introduced into the cell. After adsorption for 10 min, the cell was evacuated for 1 h before IR spectra were recorded. Single-pulse <sup>27</sup>Al MAS experiments were carried out with a  $\pi/8$  pulse length of 0.5 µs and a recycle delay of 0.5 s at 14.1 T and 12 kHz MAS. The chemical shifts were referenced to 1 M Al(NO<sub>3</sub>)<sub>3</sub> aqueous solution.

#### **Catalytic reaction**

300 mg ZnCr-ZSM-5 was loaded in a fixed-bed reactor and heated to the desired temperature under H<sub>2</sub>. A mixture of CO<sub>2</sub> and H<sub>2</sub> containing 5% Ar as the internal standard for GC analysis was introduced using a mass flow controller and toluene was injected with a pump (Elite P230). The reaction was operated at H<sub>2</sub>/CO<sub>2</sub> = 3, 4 MPa and 390 °C, and a gas hourly space velocity of H<sub>2</sub>/CO<sub>2</sub>/Ar (GHSV<sub>CO2/H2</sub>) = 15,000 ml/g/h, a weight hourly space velocity of toluene (WHSV<sub>toluene</sub>) = 0.87 h<sup>-1</sup> unless otherwise stated. The products were analyzed by an on-line GC Agilent 7890 B equipped with a thermal conductivity detector (TCD) and a flame ionization detector (FID). Hydrocarbons were separated in a HP-FFAP column and a HP-Al/S capillary column and analyzed by FID, while Ar, CO, CO<sub>2</sub>, C<sub>2</sub>H<sub>4</sub> and C<sub>2</sub>H<sub>6</sub> were separated in a Porapak Q column and a 5A molecular sieve column and analyzed by TCD.

 $CO_2$  conversion,  $X_{CO2}$ , was calculated according to

$$X_{CO2} = \frac{CO_{2 inlet} - CO_{2 outlet}}{CO_{2 inlet}} \times 100\%$$
(1)

where  $CO_2$  inlet and  $CO_2$  outlet were the moles of  $CO_2$  at the inlet and outlet of the reactor, respectively.

Toluene conversion,  $X_{\rm T}$ , was obtained according to

$$X_{T} = \left(1 - \frac{7 \times C_{7} H_{8 \text{ outlet}}}{\sum_{6}^{n} (nC_{n}H_{m \text{ outlet}})}\right) \times 100\%$$
(2)

where  $C_n H_{m outlet}$  represented moles of aromatics at the outlet.

CO selectivity, Sco, was obtained according to

$$S_{CO} = \frac{CO_{outlet}}{CO_{2inlet} - CO_{2outlet}} \times 100\% \quad (3)$$

where *CO*<sub>outlet</sub> was the mole of CO at the outlet.

The selectivity of hydrocarbon  $C_nH_m({}^{S_{C_nH_m}})$  was calculated according to:

$$S_{C_n H_m} = \frac{n C_n H_m \text{ outlet}}{\sum_{1}^{n} (n C_n H_m \text{ outlet})} \times 100\% \quad (4).$$



Fig. S1. (a) XRD pattern and (b) N<sub>2</sub> adsorption-desorption isotherm of ZnCr oxide.



Fig. S2. SEM images of (a) Z5-pristine; (b) 3P/Z5; and (c) 3P/Z5-Si3.



Fig. S3. <sup>27</sup>Al NMR spectra of phosphorus-modified ZSM-5.



Fig. S4. XRD pattern of 3P/Z5- Si3.



**Fig. S5.** Fractions of *para*-ethyltoluene and 1,2,4-trimethylbenzene in  $C_{9+}$  aromatics. Reaction conditions are the same as those in Fig. 7.



**Fig. S6.** (a) Xylenes distribution and (b) aliphatics distribution over ZnCr-Z5-Si1 and ZnCr-3P/Z5-Si1. Reaction conditions is the same as in Fig. 7.

Zeolite	X <sub>CO2</sub> (%)	S <sub>CO</sub> (%)	X <sub>T</sub> (%)	S <sub>Aro.</sub> (%)
Z5-pristine	22.0	70.4	31.4	97.3
3P/Z5	21.3	74.7	25.7	92.6
3P/Z5-Si1	23.7	73.0	18.8	87.7
3P/Z5-Si2	23.2	75.5	11.2	75.5
3P/Z5-Si3	20.9	74.0	10.6	69.5

Table S1. CO<sub>2</sub> hydrogenation in the presence of toluene over ZnCr-modified ZSM-5.

Reation conditions: ZnCr/ZSM-5 = 1/1 mass ratio, granule mixing, 40-60 mesh,  $GHSV_{CO2/H2} = 15000$  ml/g/h,  $WHSV_{toluene} = 0.87$  h<sup>-1</sup>, 390 °C, 4 MPa,  $H_2/CO_2 = 3/1$ .

### Reference

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