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# **Supporting Information**

# Unraveling the interactions of reductants and reaction path over Cu-

# ZSM-5 for model coal-gas-SCR via transient reaction study

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#### S1. XRD results

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Fig. S1. XRD spectra of Cu based catalyst with different topology structure.

**Fig. S2.** H<sub>2</sub> signal (a), CO signal (b), CH<sub>4</sub> signal (c) of Cu-ZSM-5 catalyst at different adsorption conditions.

Fig. S3. MS signals of Cu-ZSM-5 catalyst at different reaction conditions.

**Fig. S4.** In situ DRIFTS spectra of (a)  $H_2$ , (b) CO, (c)  $CH_4$ , (d)  $CO + H_2$ , (e)  $CH_4 + H_2$ , (f)  $CH_4 + CO$ , and (g)  $CH_4 + CO + H_2$  reacted with pre-adsorbed NO + O<sub>2</sub> on Cu-ZSM-5 catalyst at 250°C

as a function of time.

Fig. S5. In situ DRIFTS spectra of (a) NO +  $H_2$  +  $O_2$ , (b) NO + CO +  $O_2$ , (c) NO +  $CH_4$  +  $O_2$ , (d) NO + CO +  $H_2$  +  $O_2$ , (e) NO +  $CH_4$  +  $H_2$  +  $O_2$ , (f) NO +  $CH_4$  + CO +  $O_2$  and (g) NO +  $CH_4$  + CO

+ H\_2 + O\_2 on Cu-ZSM-5 catalyst at 250  $^{\rm o}\text{C}$  as a function of time.

Fig. S6. In situ DRIFTS spectra of (a) NO + CO + H<sub>2</sub> + O<sub>2</sub>, (b) stop CO + H<sub>2</sub>, (c) NO + CH<sub>4</sub> + H<sub>2</sub> + O<sub>2</sub>, (d) stop CH<sub>4</sub> + H<sub>2</sub>, (e) NO + CH<sub>4</sub> + CO + O<sub>2</sub>, (f) stop CH<sub>4</sub> + CO (e) NO + CH<sub>4</sub> + CO + H<sub>2</sub> + O<sub>2</sub> and (f) stop CH<sub>4</sub> + CO + H<sub>2</sub> on Cu-ZSM-5 catalyst at 250 °C as a function of time.

Fig. S7. In situ DRIFTS spectra in the range of 2400-2000 cm<sup>-1</sup> (a) stop H<sub>2</sub>, (b) stop CO, (c) stop CH<sub>4</sub>, (d) stop CO + H<sub>2</sub>, (e) stop CH<sub>4</sub> + H<sub>2</sub>, (f) stop CH<sub>4</sub> + CO and (g) stop CH<sub>4</sub> + CO + H<sub>2</sub> on Cu-ZSM-5 catalyst at 250 °C as a function of time.

Fig. S8. In situ DRIFTS spectra of (a) NO + H<sub>2</sub> + O<sub>2</sub>, (b) stop H<sub>2</sub>, (c) NO + CO + O<sub>2</sub>, (d) stop CO,
(e) NO + CH<sub>4</sub> + O<sub>2</sub> and (f) stop CH<sub>4</sub> on Cu-ZSM-5 catalyst at 250 °C as a function of time.

Fig. S9. In situ DRIFTS spectra on Cu-ZSM-5 catalyst at 250 °C under different reaction condition.

Fig. S10. In situ DRIFTS spectra on Cu-ZSM-5 catalyst at 350 °C under different reaction condition.

Table S1. Observed species in the reaction process as identified by IR.

 Table S2. Reaction steps of various SCR reactions.

## S1. XRD results



Fig. S1. XRD spectra of Cu based catalyst with different topology structure.

As shown in **Fig. S1**, five kinds of zeolite catalyst with different topology structure exhibit complete diffraction peak according to the database of IZA <sup>1</sup>, which indicated that the modification process did not deteriorate zeolite structure. In addition, the characteristic signals of CuO species ( $2\theta$ =35.5 and 38.8°) are not observed in all patterns, suggesting that CuO species were highly dispersed on the zeolite.



#### **S2. TPD results**

Fig. S2.  $H_2$  signal (a), CO signal (b),  $CH_4$  signal (c) of Cu-ZSM-5 catalyst at different adsorption conditions.

In order to explore the competitive adsorption between reductants, the H<sub>2</sub>, CO,

and CH<sub>4</sub> signal at different adsorption conditions were monitored. As shown in **Fig. S2**, after introducing CO + H<sub>2</sub> and CH<sub>4</sub> + H<sub>2</sub> for co-adsorption, the intensity of H<sub>2</sub> signal greatly decreased, which indicated that CO and CH<sub>4</sub> were regarded as an inhibitor for the H<sub>2</sub> adsorption. Moreover, the H<sub>2</sub> signal in the flow of CO + H<sub>2</sub> is weaker than that of CH<sub>4</sub> + H<sub>2</sub>, indicating that the inhibition effect of CO is stronger than CH<sub>4</sub> which may be due to the strong adsorption ability of CO. As for CO and CH<sub>4</sub> adsorption, the introduction of external reducing agent has little effect on its adsorption.



### **S3. TPSR results**

Fig. S3. MS signals of Cu-ZSM-5 catalyst at different reaction conditions.

## S4. In situ DRIFTS results



Fig. S4. In situ DRIFTS spectra of (a)  $H_2$ , (b) CO, (c)  $CH_4$ , (d)  $CO + H_2$ , (e)  $CH_4 + H_2$ , (f)  $CH_4 + H_2$ , (h)  $CH_4 + H_2$ , (

CO, and (g)  $CH_4 + CO + H_2$  reacted with pre-adsorbed NO + O<sub>2</sub> on Cu-ZSM-5 catalyst at 250 °C

as a function of time.



Fig. S5. In situ DRIFTS spectra of (a) NO +  $H_2$  +  $O_2$ , (b) NO + CO +  $O_2$ , (c) NO + CH<sub>4</sub> +  $O_2$ , (d)

 $NO + CO + H_2 + O_2$ , (e)  $NO + CH_4 + H_2 + O_2$ , (f)  $NO + CH_4 + CO + O_2$  and (g)  $NO + CH_4 + CO$ 

+  $H_{2}$  +  $O_{2}$  on Cu-ZSM-5 catalyst at 250  $^{o}\mathrm{C}$  as a function of time.



Fig. S6. In situ DRIFTS spectra of (a) NO + CO +  $H_2$  +  $O_2$ , (b) stop CO +  $H_2$ , (c) NO + CH<sub>4</sub> +  $H_2$ 

 $+ O_{2}$ , (d) stop  $CH_{4} + H_{2}$ , (e)  $NO + CH_{4} + CO + O_{2}$ , (f) stop  $CH_{4} + CO$  (e)  $NO + CH_{4} + CO + H_{2} + CO$ 

 $O_2$  and (f) stop  $CH_4 + CO + H_2$  on Cu-ZSM-5 catalyst at 250 °C as a function of time.



Fig. S7. In situ DRIFTS spectra of (a) stop  $H_2$ , (b) stop CO, (c) stop  $CH_4$ , (d) stop CO +  $H_2$ , (e)

stop  $CH_4 + H_2$ , (f) stop  $CH_4 + CO$  and (g) stop  $CH_4 + CO + H_2$  on Cu-ZSM-5 catalyst at 250 °C as

a function of time.



**Fig. S8.** In situ DRIFTS spectra of (a)  $NO + H_2 + O_2$ , (b) stop  $H_2$ , (c)  $NO + CO + O_2$ , (d) stop CO,

(e) NO +  $CH_4$  +  $O_2$  and (f) stop  $CH_4$  on Cu-ZSM-5 catalyst at 250 °C as a function of time.



Fig. S9. In situ DRIFTS spectra on Cu-ZSM-5 catalyst at 250 °C under different reaction conditions.

In order to investigate the effect of  $H_2$  on the generation of intermediate species in CO-SCR process, the catalyst first was exposed to the flow of NO + CO + O<sub>2</sub> for reaction, and then  $H_2$  was introduced in the reaction. As shown in **Fig. S9**, when exposed the catalyst to NO + CO + O<sub>2</sub> reaction system, a band at 2280 cm<sup>-1</sup> was appeared in spectra, which could be ascribed to NCO species, which is an important intermediate species in CO-SCR reaction <sup>2</sup>. However, after introducing  $H_2$  for reaction, the intensity of this band vanished, which means that addition of  $H_2$  could reduce the amount of NCO species, thus the presence of  $H_2$  may change the reaction route in CO-SCR process.



Fig. S10. In situ DRIFTS spectra on Cu-ZSM-5 catalyst at 350 °C under different reaction conditions.

To investigate the inhibitory effect of CO on the generation of  $NH_x$  species from  $H_2$ , the catalyst was first exposed to the flow of  $NO + H_2 + O_2$  for reaction, and then CO was added into the reaction. As shown in **Fig. S10**, a peak at 1640 cm<sup>-1</sup> attributed to  $NH_4^+$  species appeared after introduction of  $H_2$ <sup>3</sup>, which indicated that  $NH_4^+$  species was formed in the SCR process. However, after injecting CO, the intensity of 1640 cm<sup>-1</sup> weakened to almost disappear, indicating CO could have an obvious inhibition on the formation of  $NH_x$  species.

Wavenumber (cm <sup>-1</sup> )	Species and mode	Ref.
1143	Adsorbed NO	4
1255	Bridged nitrates	4
1439	Nitrites	5
2155	NO <sup>+</sup> species	6
964	Bidentate carbonates	7
1372	Monodentate carbonate	8
2109/2155	Cu <sup>+</sup> (CO) carbonyl	9, 10
2195	$Cu^+(CO)_2$ carbonyl	11
2346/2360	Adsorbed CO <sub>2</sub>	12
1285	Coordinated NH <sub>3</sub>	13
3015	Adsorbed CH <sub>4</sub>	14
3580	Si-OH-A1	15
3650	Cu-OH	15

Table S1. Observed species in the reaction process as identified by IR.

Reaction type	Reaction steps	No.
	$NO + * \rightarrow NO^*$	R1
	$O_2 + * \rightarrow O_2^*$	R2
	$NO^* + * \rightarrow N^* + O^*$	R3
NO adsorption	$O_2^* + * \rightarrow O^* + O^*$	R4
and nitrate	$N^* + N^* \rightarrow N_2 + 2^*$	R5
formation	$NO^* + N^* \rightarrow N_2O + 2^*$	R6
	$NO^* + O_2^* \rightarrow NO_2^* + O^*$	R7
	$NO^* + O_2^{-*} \rightarrow NO_3^{-*} + *$	R8
	$N_2 O^{\boldsymbol{*}} \rightarrow N_2 + O^{\boldsymbol{*}}$	R9
H <sub>2</sub> -SCR	$H_2 + * \rightarrow H_2 *$	Ral
	$H_2^* \rightarrow 2H^*$	Ra2
	$N^* + H^* \rightarrow NH^* + *$	Ra3
	$\mathrm{NH}^{*} + \mathrm{H}^{*} \rightarrow \mathrm{NH}_{2}^{*} + ^{*}$	Ra4
	$\rm NH_2{}^{\textstyle *} + \rm H{}^{\textstyle *} \rightarrow \rm NH_3{}^{\textstyle *} + {}^{\textstyle *}$	Ra5
	$O^* + H^* \rightarrow OH^* + *$	Ra6
	$OH^* + H^* \rightarrow H_2O + 2^*$	Ra7
	$NO_2^* + H_2^* \rightarrow ONH^* + OH^*$	Ra8
	$ONH^* + NO^* + H^* \rightarrow N_2 + H_2O + O^* + 2^*$	Ra9
	$ONH^* + NO^* + H^* \rightarrow N_2O^* + H_2O + 2^*$	Ra10
	$4NH_3 + 4NO + 2O_2 \rightarrow 4N_2 + 6H_2O$	Ra11
	$2NH_3 + NO + NO_2 \rightarrow 2N_2 + 3H_2O$	Ra12
CO-SCR	$CO + * \rightarrow CO*$	Rb1
	$N^* + CO^* \rightarrow NCO^* + *$	Rb2
	$NO_2^* + CO^* \rightarrow NCO^* + O_2^*$	Rb3
	$\mathrm{CO}^{\boldsymbol{*}} + 2\mathrm{NO}_{2}^{\boldsymbol{*}} \rightarrow \mathrm{N}_{2} + \mathrm{CO}_{2} + 3\mathrm{O}^{\boldsymbol{*}}$	Rb4
	$NCO^* + NO^* \rightarrow N_2 + CO_2 + 2^*$	Rb5
	$CO^* + O^* \rightarrow CO_2 + 2^*$	Rb6
	$2NCO^* + 3H_2O \rightarrow 2NH_3 + 2CO_2 + O^*$	Rb7
	$NCO^* + NO_2^* \rightarrow N_2 + CO_2 + * + O^*$	Rb8
CH <sub>4</sub> -SCR	$CH_4^* + O^* \rightarrow CH_3^* + OH^*$	Rc1
	$\mathrm{CH}_3{}^* + \mathrm{O}{}^* \to \mathrm{CH}_2{}^* + \mathrm{OH}{}^*$	Rc2
	$NO^* + CH_3^* \rightarrow CH_3NO^* + *$	Rc3
	$4CH_3NO + 2NO + 4O_2 \rightarrow 3N_2 + 6H_2O + 4CO_2$	Rc4
	$CH_4 + 2O_2 \rightarrow CO_2 + 2H_2O$	Rc5
	$2NO + CH_4 + O_2 \rightarrow N_2 + CO_2 + 2H_2O$	Rc6

 Table S2. Reaction steps of various SCR reactions.

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