

## **Appendix A. Supplementary data**

### **Understanding the role of redox property and NO adsorption over MnFeO<sub>x</sub> for NH<sub>3</sub>-SCR**

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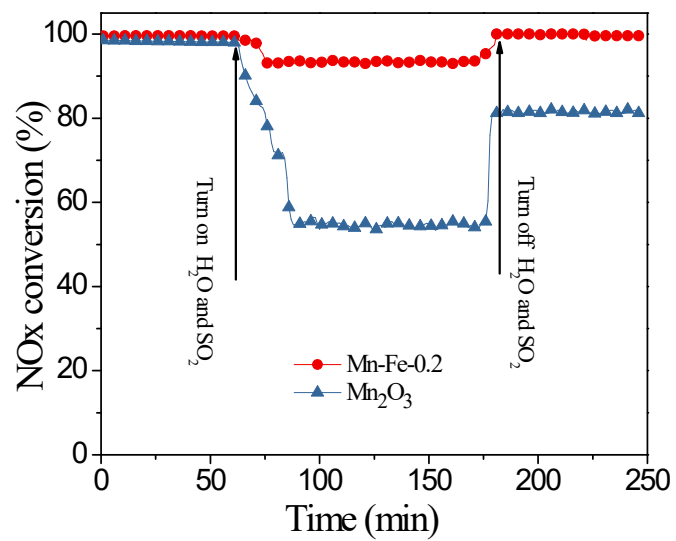


Fig. S1. H<sub>2</sub>O and SO<sub>2</sub> tolerance test of the Mn<sub>2</sub>O<sub>3</sub> and Mn-Fe-0.2 catalysts at 100 °C

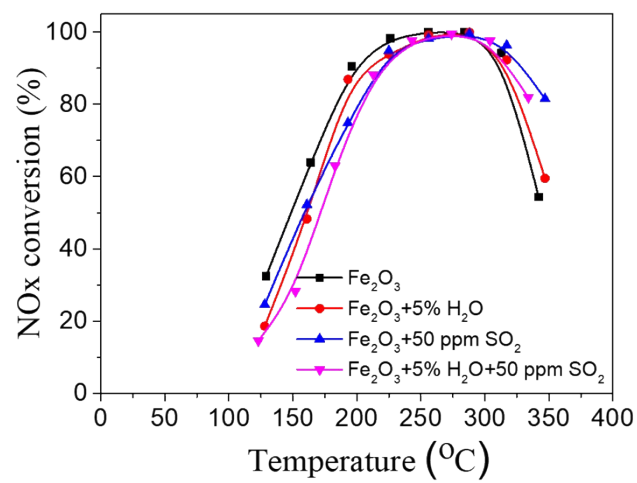


Fig. S2. Effect of H<sub>2</sub>O or/and SO<sub>2</sub> on the activities of Fe<sub>2</sub>O<sub>3</sub>.

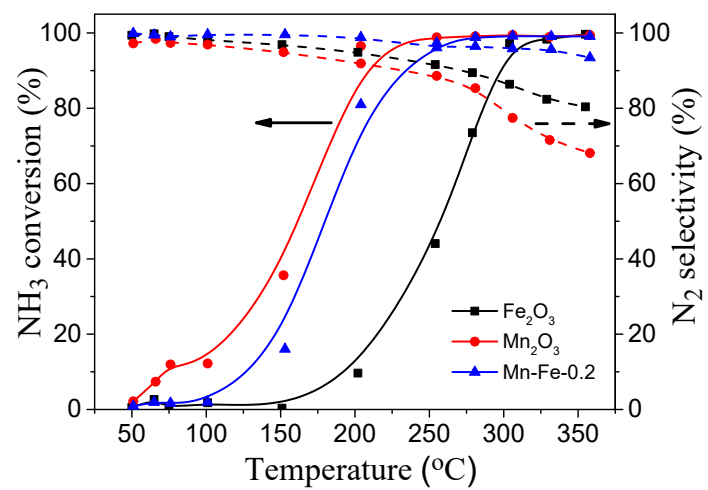


Fig. S3. NH<sub>3</sub> oxidation profiles of Mn<sub>2</sub>O<sub>3</sub>, Fe<sub>2</sub>O<sub>3</sub>, and Mn-Fe-0.2

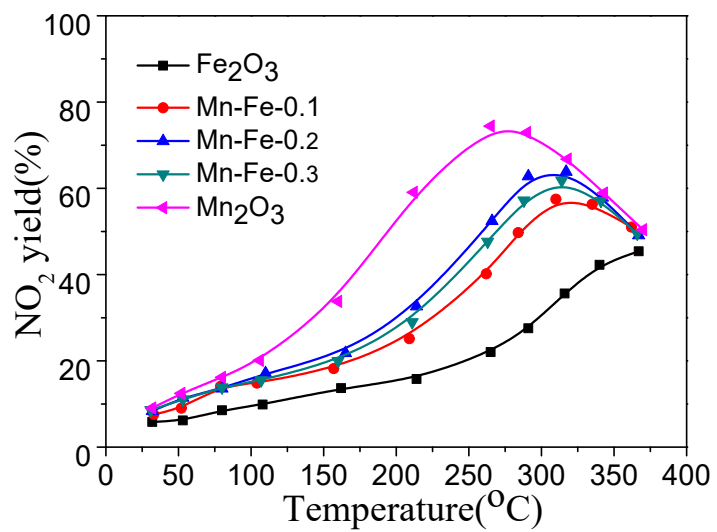


Fig. S4. The NO<sub>2</sub> yield during NO oxidation.

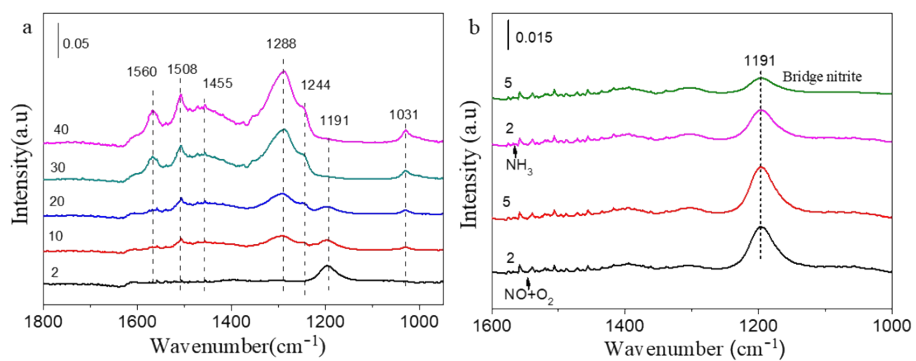


Fig. S5. In situ DRIFT spectra of Mn-Fe-0.2 catalysts exposed to 500 ppm NO + 5 vol % O<sub>2</sub>/Ar (50 mL/min) (a) , and then switched to 500 ppm NH<sub>3</sub>/Ar (50 mL/min) (b) at 50 °C.

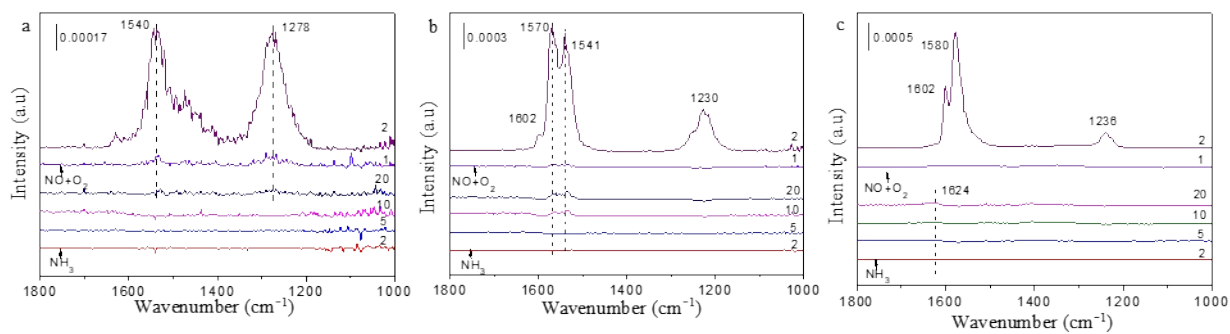


Fig. S6. In situ DRIFT spectra of the Mn<sub>2</sub>O<sub>3</sub> (a), Fe<sub>2</sub>O<sub>3</sub> (b), and Mn-Fe-0.2 (c) catalysts exposed to 500 ppm NH<sub>3</sub>/Ar (50 mL/min), and then switched to 500 ppm NO + 5 vol % O<sub>2</sub>/Ar (50 mL/min) at 300 °C.

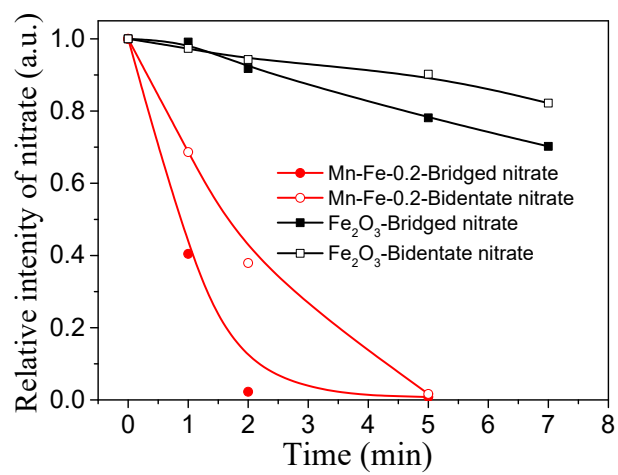


Fig. S7. Relative intensity of nitrate consumption over time on different samples at 300 °C.



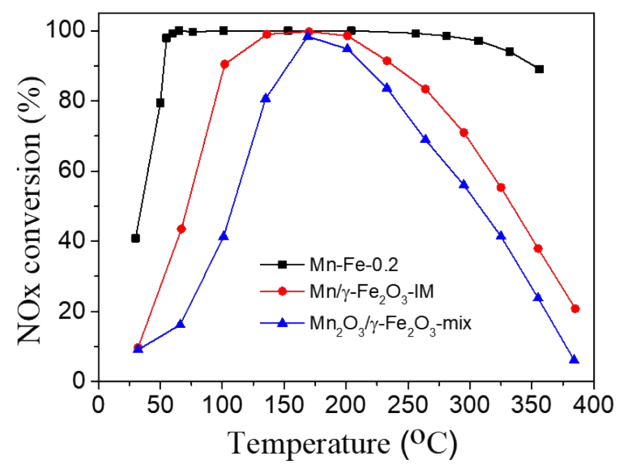


Fig. S8. NO<sub>x</sub> conversion as a function of temperature over MnFe catalysts prepared by different methods.

Table S1. The H<sub>2</sub> consumption amount of the Mn-Fe catalysts.

Catalyst	The practical H <sub>2</sub> consumption amount of $\alpha$ (mmol/g) <sup>a</sup>	The total theoretical H <sub>2</sub> consumption amount (mmol/g) <sup>b</sup>	The difference value between the theoretical and practical H <sub>2</sub> consumption amount (mmol/g)
Fe <sub>2</sub> O <sub>3</sub>	1.91	18.80	6.95
Mn-Fe-0.1	2.29	17.56	6.16
Mn-Fe-0.2	2.04	16.63	5.21
Mn-Fe-0.3	2.47	15.78	2.84
Mn <sub>2</sub> O <sub>3</sub>	2.15	6.33	0.32

<sup>a</sup> Calculated via H<sub>2</sub>-TPR results.

<sup>b</sup> Calculated via ICP results.