

*Supplementary material for*

**Influence of La-doping on the CuO/ZrO<sub>2</sub> catalysts with  
different Cu content for hydrogenation of dimethyl oxalate  
to ethylene glycol**

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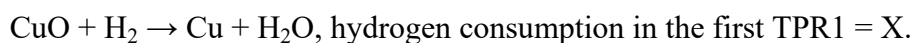
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**Table S1.** The input of raw materials needed for preparation of wCZ and wCLZ (g).

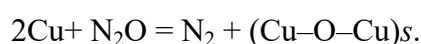
Catalyst	$\text{Cu}(\text{NO}_3)_2 \cdot 3\text{H}_2\text{O}$	$\text{La}(\text{NO}_3)_3 \cdot 6\text{H}_2\text{O}$	$\text{Zr}(\text{NO}_3)_4 \cdot 5\text{H}_2\text{O}$	SA
<b>5CZ/5CLZ</b>	<b>0.1888/0.1888</b>	<b>-/0.0312</b>	<b>3.2668/3.2259</b>	<b>4.6409/4.6172</b>
<b>10CZ/10CLZ</b>	<b>0.3775/0.3775</b>	<b>-/0.0312</b>	<b>3.0490/3.0081</b>	<b>4.5733/4.5489</b>
<b>20CZ/20CLZ</b>	<b>0.7550/0.7550</b>	<b>-/0.0312</b>	<b>2.6134/2.5726</b>	<b>4.4379/4.4141</b>
<b>28CZ/28CLZ</b>	<b>1.0570/1.0570</b>	<b>-/0.0312</b>	<b>2.2650/2.2241</b>	<b>4.3296/4.3057</b>
<b>33CZ/33CLZ</b>	<b>1.2458/1.2458</b>	<b>-/0.0312</b>	<b>2.0472/2.0063</b>	<b>4.2619/4.2382</b>
<b>39CZ/39CLZ</b>	<b>1.4723/1.4723</b>	<b>-/0.0312</b>	<b>1.7858/1.7450</b>	<b>4.1807/4.1573</b>
<b>58CZ/58CLZ</b>	<b>2.1895/2.1895</b>	<b>-/0.0312</b>	<b>0.9583/0.9174</b>	<b>3.9235/3.8986</b>

The exposed Cu surface area and Cu dispersion was measured by N<sub>2</sub>O oxidation and followed H<sub>2</sub> reduction. Generally, catalysts (60 mg) were first reduced in 5% H<sub>2</sub>/N<sub>2</sub> mixture at a flow rate of 30 mL min<sup>-1</sup> with a ramping rate of 10 °C min<sup>-1</sup> until 350 °C. The amount of hydrogen consumption in the first TPR (TPR1) was denoted as X. And then the reactor was purged with Ar to 50 °C. N<sub>2</sub>O (30 mL min<sup>-1</sup>) was injected to oxidize surface copper atoms to Cu<sub>2</sub>O at 50 °C for 15 min. Subsequently, the reactor was flushed with Ar to remove the oxidant. Finally, another TPR experiment was performed in 5% H<sub>2</sub>/N<sub>2</sub> at a flow rate of 30 mL min<sup>-1</sup>. Hydrogen consumption in the second TPR (TPR2) was denoted as Y. The dispersion of Cu and exposed Cu surface area were calculated according to the equations which were shown below:

Reduction of all copper atoms:



The decomposition of N<sub>2</sub>O on the surface of metallic copper:



Reduction of surface copper atoms only:



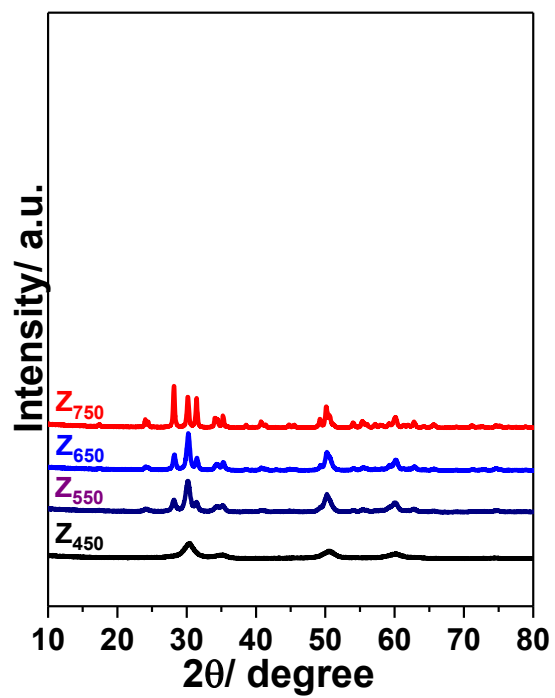
And the dispersion of Cu and exposed Cu surface area were calculated as [Eq. (1, 2)]:

$$D = \frac{2Y}{X} \times 100\% \quad (1)$$

$$S = \frac{2Y \times N_{av}}{X \times M_{Cu} \times 1.4 \times 10^{19}} = \frac{1353Y}{X} (m^2 - \text{Cu} / g - \text{Cu}) \quad (2)$$

where  $N_{av}$  is the Avogadro's constant,  $M_{Cu}$  is the relative atomic mass,  $1.4 \times 10^{19}$  comes from that an equal abundance of an average copper surface atom area of

0.0711 nm<sup>2</sup>, equivalent to  $1.4 \times 10^{19}$  copper atoms m<sup>-2</sup>.



**Figure S1.** XRD patterns of the ZrO<sub>2</sub> powders calcined at 450, 550, 650, and 750 °C.

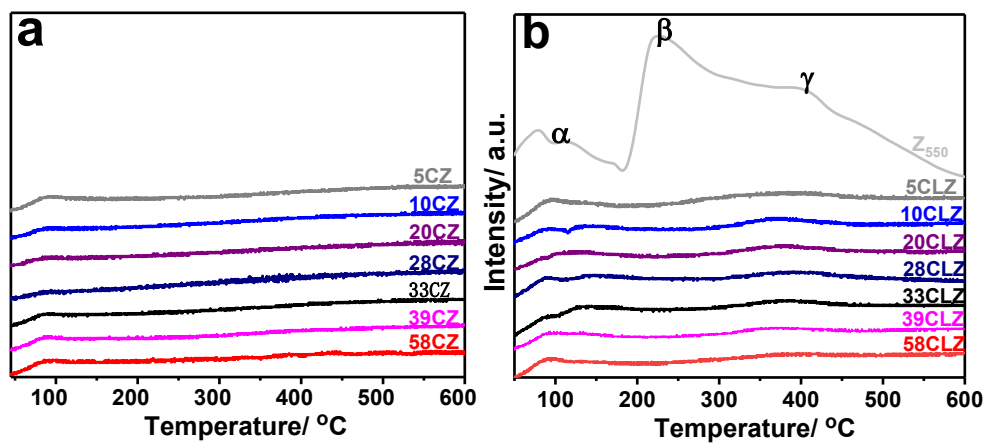


Figure S2. CO<sub>2</sub>-TPD profiles of as-prepared catalysts (a: wCZ; b: wCLZ and standard ZrO<sub>2</sub>).

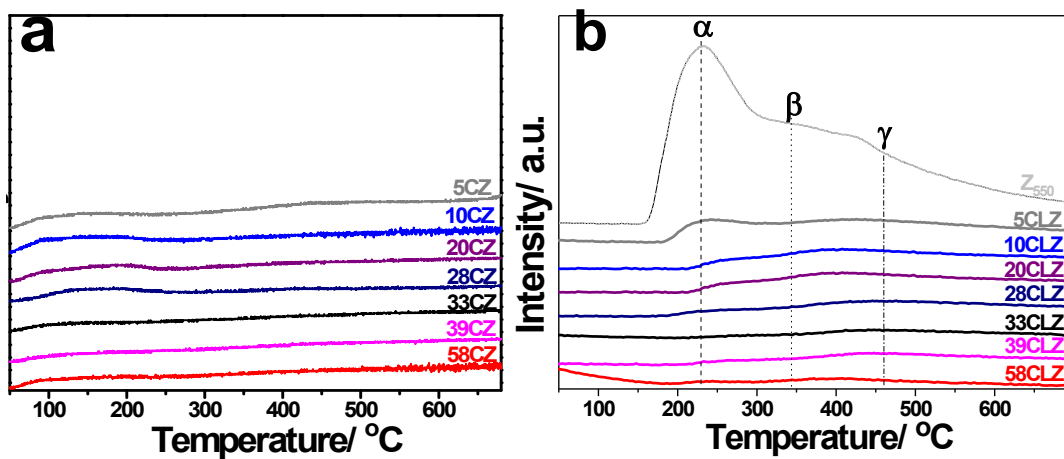
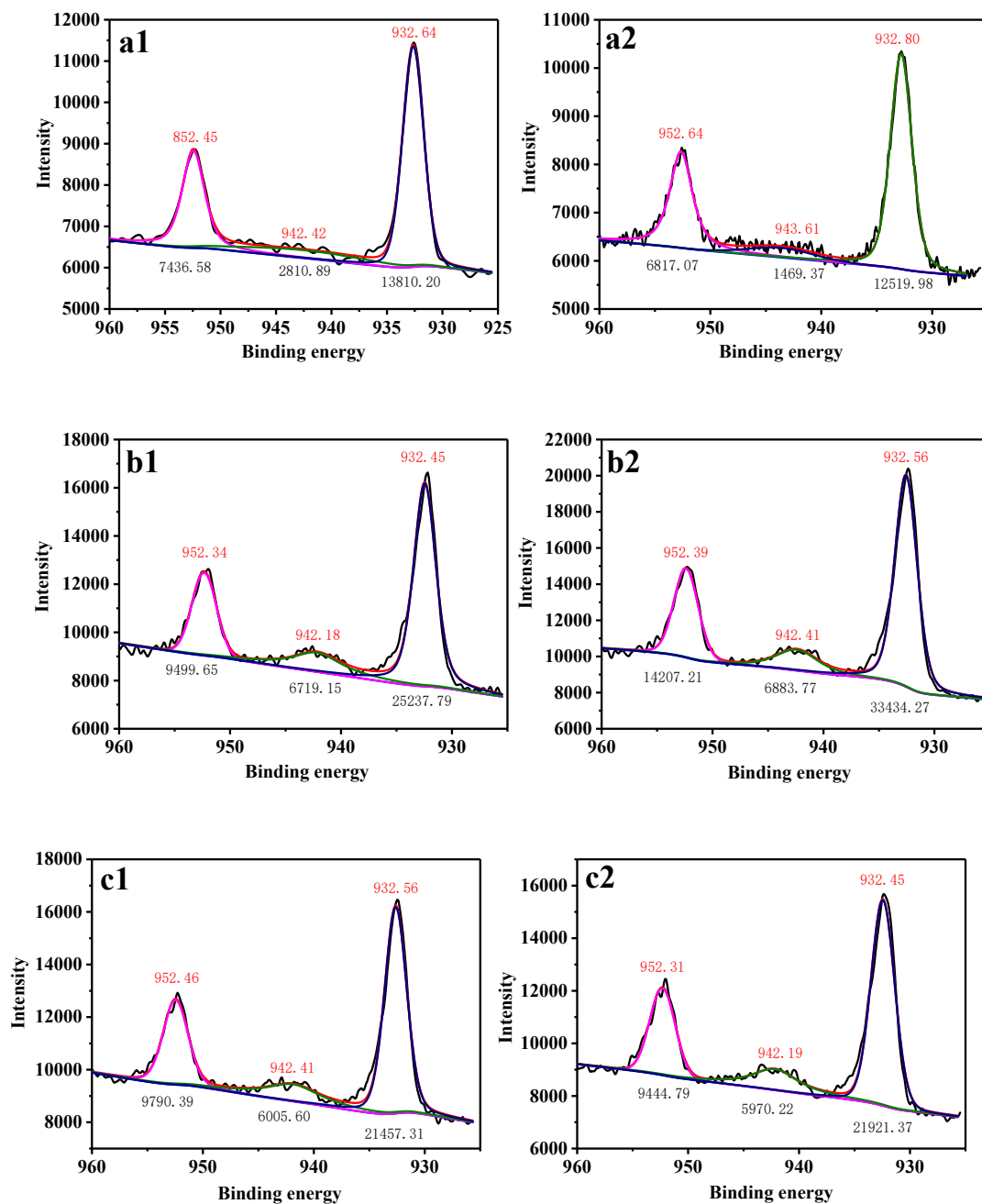
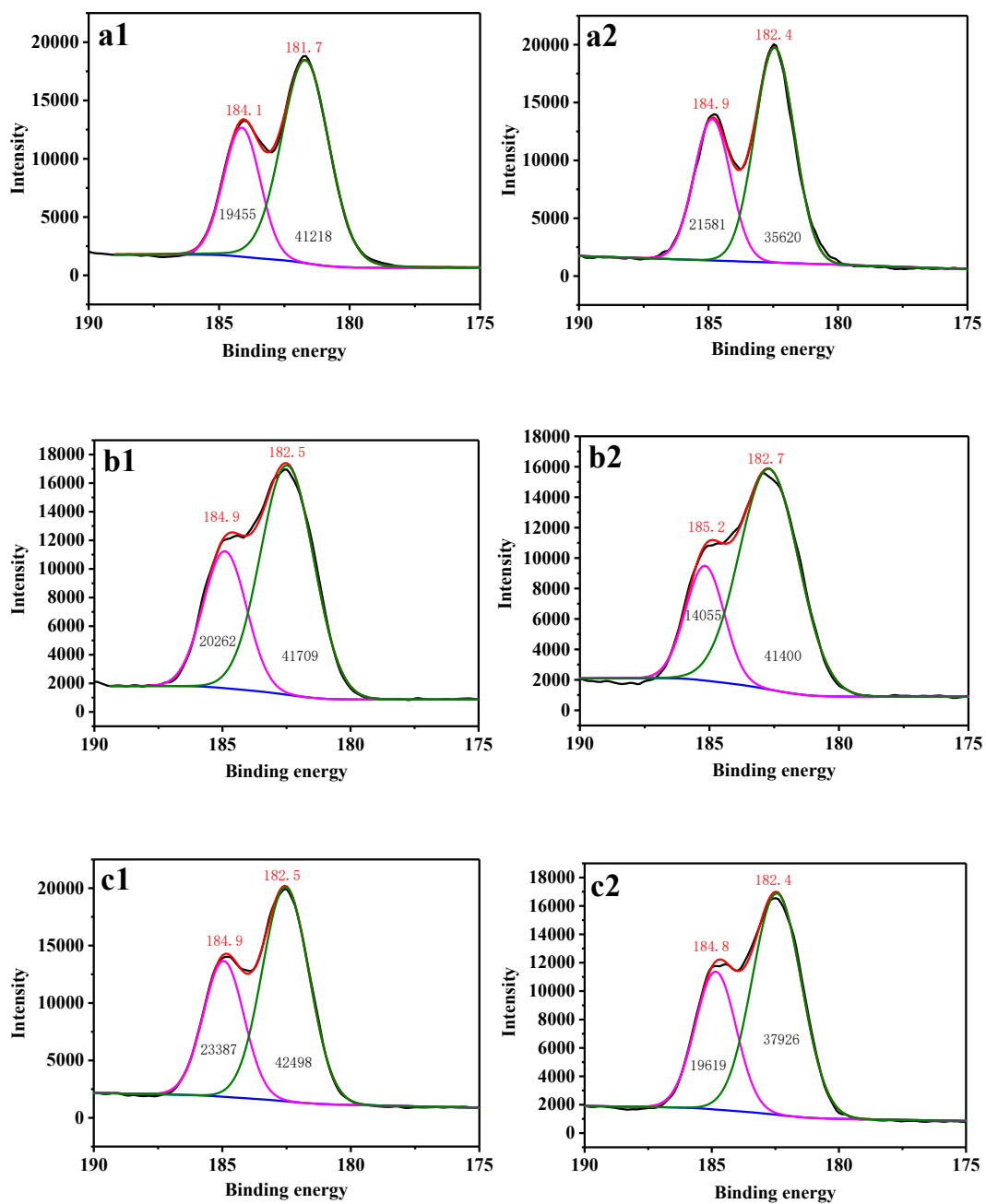


Figure S3. NH<sub>3</sub>-TPD profiles of as-prepared catalysts (a: wCZ; b: wCLZ and standard ZrO<sub>2</sub>).



**Figure S4.** Cu 2p spectra of reduced catalysts (a1: 5CZ; a2: 5CLZ; b1: 33CZ; b2: 33CLZ; c1: 39CZ; c2: 39CLZ).





**Figure S5.** Zr 3d spectra of reduced catalysts (a1: 5CZ; a2: 5CLZ; b1: 33CZ; b2: 33CLZ; c1: 39CZ; c2: 39CLZ).

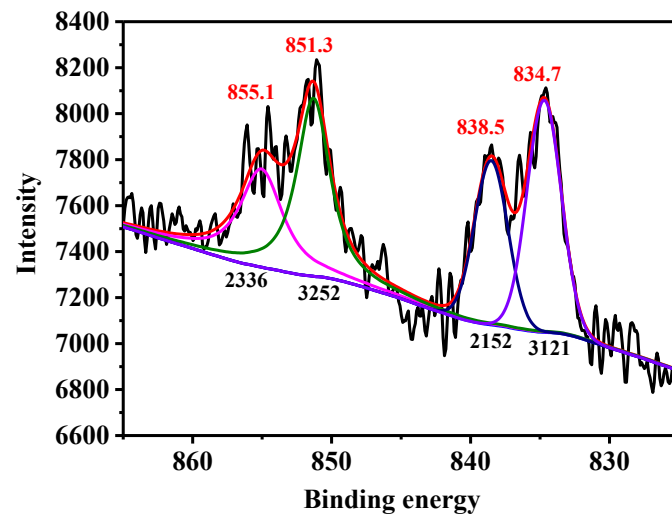


Figure S6. La 3d spectra of reduced 33CLZ catalysts.