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Supporting Information for

Construction of Nitrogen-Doped Porous Carbon Nanosheets Decorated with Fe-N4 and Iron Oxides by A Biomass Coordination Strategy for Efficient Oxygen Reduction Reaction

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1. Experimental section

1.1 Chemicals

Iron (III) chloride hexahydrate (FeCl₃•6H₂O), urea, sodium hydroxide (NaOH), and ethanol (99.7%) were purchased from Sinopharm Chemical Reagent Co., Ltd. 20% platinum (HiSPECTM 3000, Pt 20 wt% on carbon black, Johnson Matthey), Nafion solution (5 wt%, DuPont) and polytetrafluoroethylene (PTFE, 60 wt%) were purchased from Hesen Co. Ltd.All of the other chemicals used in this work were analytically pure and were used without further purification. Ultrapure water (resistivity > 18 M Ω cm) was used throughout the experiments.

1.2 Catalysts preparation

The synthesis process of the catalysts is shown in **Figure 1(a)**. Typically, a solution of 0.2 g FeCl3·6H2O dissolved in 10 mL of ultrapure water was dropwise added into 30 mg fresh egg white under moderate stirring. After stirring for 3 hours, $Fe³⁺$ coordinated with the egg white, and yellow colloid was formed. Then, the obtained colloid was sieved through a 0.5 mm mesh and freeze-dried under -50 °C on a freeze-drier (Beijing Leading Technology Co., Ltd, FD-1A-50), followed by ground with urea (the mass ratio of colloid to urea is 1:5) using a mortar and pestle for more than half an hour. Finally, the obtained mixture was placed in a quartz boat with 20 cm in length at the center of a 50-mm-diameter quartz tube in a horizontal tube furnace (Tianjin Zhonghuan Lab Furnace Co., Ltd, SK-G018123K) and heated at 800 °C, 900 °C, or 1000 °C for 2 hours with a ramp speed of 5 \degree C min⁻¹ under a constant N₂ flow. The as-synthesized samples are denoted as $Fe₂O₃@C/FeNC-X$, where X represents the heat treatment temperature. For comparison, the electrocatalysts derived from the egg white at 900 $^{\circ}$ C without artificial iron doping was prepared and denoted as NC-900.

1.3 Materials characterization

The morphology and structure of the as-synthesized catalysts were characterized using scanning electron microscopy (SEM) on a Hitachi S-4800 microscope and transmission electron microscopy (TEM) on FEI Tecnai G2 F30 microscope operated at an accelerated voltage of 200 kV. Powder X-ray diffraction (XRD) patterns were collected using a Bruker D8-Advance X-ray diffractometer with Cu Kα radiation (0.1542 nm) at an operating voltage of 40 kV (scan speed 2 and increment 0.02). X-ray photoelectron spectroscopy (XPS) was conducted on a K-Alpha X-ray photoelectron spectrometer (Thermo Fisher Scientific) with Al-Kα micro focused monochromated X-ray source. Raman spectrum was recorded at ambient temperature on a DXR Raman Microscope with 532 nm excitation length. Atomic force microscopy (Multimode 8, AFM) with PFT-QNM mode was carried out to characterize the surface morphology. Nitrogen adsorption/desorption isotherm was obtained on a Micromeritics ASAP 2020 instrument at 77 K. Before each measurement, the sample was evacuated under a vacuum for 3 hours at 150 $^{\circ}$ C. The specific surface area was calculated with the Brunauer-Emmett-Teller (BET) method and the pore size distribution (PSD) was calculated from the adsorption branch with the density functional theory (DFT) method. The final Fe content in the best forming catalyst was determined by the inductively coupled plasma optical emission spectrometry (Agilent, ICP-OES730).

X-ray absorption fine structure (XAFS) measurements at Fe K-edge and references were performed at the BL1W1B station in Beijing Synchrotron Radiation Facility (BSRF). XAFS data were collected using a fixed exit double-crystal Si (111) monochromator. The fluorescence signal was collected using a Lytle detector and the energy was calibrated using Fe foil. The acquired EXAFS data were processed using the Athena program in the IFEFFIT software package, and the data fitting was done by the Artemis program in IFEFFIT.

1.4 Electrode preparation and electrochemical measurements

The electrochemical tests were carried out in a three-electrode system on an electrochemical workstation (CHI760E). A rotating ring-disk electrode (RRDE) with a glassy carbon disk (4 mm diameter) and a Pt ring (5.0 mm inner-diameter and 7.0 mm outer-diameter) served as the substrate for the working electrode for evaluating the ORR performance, while platinum foil was utilized as the counter electrode. The potential was recorded using an Ag/AgCl electrode in saturated KCl as the reference electrode. All of the potentials were calibrated to the reversible hydrogen electrode (RHE) according to the Nernst equation as follow [1]:

$$
E (vs. RHE) = E (vs. Ag/AgCl) + 0.198 + 0.0592 \times pH
$$
 (1)

To prepare the working electrode, 10 mg catalysts mixed with 40μl Nafion solution (Sigma Aldrich, 5 wt%) were dispersed in 1 ml of ethanol solution by sonicating for at least two hours to form a homogeneous ink. A certain volume of catalyst ink was then drop-casted onto the glassy carbon electrode with a 400 μ g cm⁻² loading for the as-synthesized single-atom Fe catalysts and 100 μ g cm⁻² loading for commercial Pt/C, respectively.

RRDE measurements were conducted by linear sweep voltammetry (LSV) from 1.1 V to 0.2 V vs. RHE at a scan rate of 10 mV s⁻¹ at a rotation rate of 1600 rpm in 0.1 M KOH and 0.1 M HClO₄ media saturated with O₂, respectively. The background currents of these electrocatalysts in N2-saturated electrolyte have been deducted. The ring electrode was held at 1.45 V vs. RHE and the H₂O₂ collection coefficient at the ring in RRDE experiments was 0.37. The following equations were used to calculate n (the apparent number of electrons transferred during ORR) and H_2O_2 (%) (the percentage of H_2O_2 released during ORR) [2].

$$
n = 4 \times \frac{I_d}{I_d + I_r/N} \tag{2}
$$

$$
H_2O_2\% = 200 \times \frac{\frac{l_r}{N}}{l_d + \frac{l_r}{N}}
$$
 (3)

where I_d is the faradaic current at the disk, I_r is the faradaic current at the ring and N is the H_2O_2 collection coefficient at the ring.

The kinetic current densities (J_k) involved during the ORR process were determined by analyzing Koutecky-Levich (K-L) equation [3]:

$$
\frac{1}{J} = \frac{1}{J_L} + \frac{1}{J_k} = \frac{1}{B\omega^{1/2}} + \frac{1}{J_k}
$$
 (4)

$$
B = 0.62nF C_0 D_0^{2/3} v^{-1/6}
$$
 (5)

where *J* is the measured current density, J_k and J_l are the kinetic and diffusion limiting current densities, ω is the angular velocity of the rotating electrode ($\omega = 2\pi N$, N is the linear rotation speed). N is the electron transfer number, F is the Faraday constant $(96485 \text{ C mol}^{-1})$, C_o is the bulk concentration of oxygen $(1.2\times10^{-6} \text{ mol cm}^{-3})$, Do is the diffusion coefficient of oxygen in 0.1 M KOH and 0.1 M HClO₄ (1.9×10⁻⁵ cm² s⁻¹), and v is the kinematic viscosity of the electrolyte (0.01 $\text{cm}^2 \text{ s}^{-1}$ for both the 0.1 M HClO₄ solution and 0.1 M KOH solution).

To investigate the catalysts' durability, the chronoamperometry was conducted at 0.67 V for 40000s in O2-saturated 0.1 M KOH at a rotation speed of 1600 rpm.

Zinc-Air Battery Tests

A home-made zinc-air battery device has been employed for battery performance and stability measurements. The electrolyte used for the rechargeable zinc-air battery was 6 M KOH and 0.2 M Zn(Ac)2 solution. Typically, 5 mg single-atom Fe catalysts mixed with 20 μL Nafion solution (Sigma Aldrich, 5 wt%) were dispersed in 1 ml of ethanol solution by sonicating for two hours to form a homogeneous ink, a certain volume of catalyst ink was then brushed onto a 1.0 cm⁻² carbon paper

with a catalyst loading of 1 mg cm⁻². A polished zinc plate was used as the anode. As a reference material, 20 wt% Pt/C catalysts were prepared as the same procedure and the Pt/C loading on the carbon was 1.0 mg cm⁻². Discharge polarization and power density curves were measured on CHI 760E electrochemical workstation (CHI Instruments, Inc., Shanghai). The galvanostatic charge-discharge cycling curves were measured by a LAND multichannel battery testing system.

Figure S1. Thermal gravimetric curve of egg-white at a heating rate of 10 $^{\circ}$ C min⁻¹.

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Figure S2. Typical low-magnification TEM images of Fe₂O₃@C/FeNC-900.

Figure S3. HRTEM images of iron oxides nanoparticles in Fe₂O₃@C/FeNC-900.

Figure S4. HAADF STEM image of Fe₂O₃@C/FeNC-900 (a) and elemental mapping of (b) C, (c) N, (d) Fe and (e) O.

Figure S5. Wide-range XPS spectra of the as-synthesized catalysts pyrolyzed at different temperatures.

Element	$Fe2O3@C/FeNC-800$	$Fe2O3@C/FeNC-900$	$Fe2O3@C/FeNC-1000$
C	71.33	84.05	91.23
N	13.78	3.19	2.77
Fe	0.51	0.49	0.34
O	13.97	11.73	5.48

Table S1. The contents of C, N, Fe, O (according to XPS analysis) in the as-synthesized electrocatalysts in this work (at %).

Figure S6. High-resolution N 1s XPS spectra of (a) $Fe₂O₃@C/FeNC-800$ and (b) Fe2O3@C/FeNC-1000.

	Total nitrogen	Pyridinic-N	Pyrrolic-N	Graphitic-N	$Oxide-N$
Catalysts	(at. %)	(at. %)	(at, %)	$(at.\%)$	$(at.\%)$
$Fe2O3@C/FeNC-800$	5.14	44.73	17.79	31.76	5.72
$Fe2O3@C/FeNC-900$	3.19	31.19	16.53	43.71	8.57
$Fe2O3@C/FeNC-1000$	2.77	18.04	20.35	45.36	17.99

Table S2. Comparison of nitrogen contents in the as-synthesized catalysts.

*Nitrogen content (at.%) evaluated by XPS.

Figure S7. The high-resolution spectrum of Fe 2p of Fe₂O₃@C/FeNC-800.

Figure S8. The high-resolution spectrum of Fe 2p of Fe₂O₃@C/FeNC-1000.

Figure S9. The high-resolution spectra of C 1s of Fe₂O₃@C/FeNC-800, Fe₂O₃@C/FeNC-900 and Fe₂O₃@C/FeNC-1000.

Table S3. Fe K-edge EXAFS curves Fitting Parameters for various samples.

CN is the coordination number; R is interatomic distance (the bond length between central atoms and surrounding coordination atoms); σ^2 is Debye-Waller factor (a measure of thermal and static disorder in absorber-scatter distances); ΔE_0 is edge-energy shift (the difference between the zero kinetic energy value of the sample and that of the theoretical model). R factor is used to value the goodness of the fitting.

 $So²$ is the amplitude reduction factor and was set as 0.85 for Fe-N, which was obtained from the experimental EXAFS fit of FePc reference by fixing CN as the known crystallographic value and was fixed to all the samples.

Figure S10. The corresponding EXAFS k-space fitting results of Fe₂O₃@C/FeNC-900

Figure S11. (a) LSV curves of Fe₂O₃@C/FeNC-900 in O₂-saturated 0.1 M KOH at various rotation speeds. (b) K-L plots of Fe₂O₃@C/FeNC-900 at virous potentials.

Figure S12. (a) LSV curves of NC-900 in O₂-saturated 0.1 M KOH at rotation speed of 1600 rpm. (b) The i-t chronoamperometric responses of NC-900 and JM Pt/C in O₂-saturated 0.1 M KOH.

	E _{onset} (V)	$E_{1/2} (V)$	JL (mA cm ⁻²)	Tafel slop	Reference
Catalyst				$(mV dec-1)$	
Fe/N/CNT@PCF	0.87	0.77	4.1	65.8	$[4]$
SA-Fe/NHPC		0.87	5.0	52.0	$[5]$
NiFe@N-CFs	0.94	0.82	5.8	58.0	[6]
NPAC _{Co}	0.87	0.78	5.0	$\qquad \qquad -$	$[7]$
NBSCP	0.95	0.836	5.1	81.7	[8]
Fe-N-CNTs	0.94	0.811	4.9		[9]
Co ₃ O ₄ /NCMTs-800	0.91	0.78	4.5	42.9	$[10]$
FeNC-900		0.85	5.6	$\overline{}$	$[11]$
Fe-ISA/NC	1.0	0.89	6.2	59.3	$[12]$
Fe ₂ O ₃ @C/FeNC-900	1.0	0.89	6.1	49.0	This work

Table S4. Comparison of the ORR catalytic activities of some leading nonprecious metal catalysts derived from biomass precursors reported previously and our Fe₂O₃@C/FeNC-900 (as measured in 0.1 M KOH saturated with O2, electrode rotation speed: 1600 rpm).

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