## Deep desulfurization upon inverse-micellar polyoxometalates and oxygen

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# **Supplementary captions**

S1. Materials and Physical measurements

S2. Catalytic oxidative desulfurization for model oil and or diesel and gasoline

Fig. S1 The IR spectrum of (CTA)PMo<sub>4</sub>V<sub>8</sub>, CTAB and (NH<sub>4</sub>)<sub>5</sub>H<sub>6</sub>PMo<sub>4</sub>V<sub>8</sub>

Fig. S2 The DR-UV-Vis spectra of PMoV and (CTAB)<sub>5</sub>PMoV

Fig. S3 The SEM image of (CTA)PMo<sub>4</sub> $V_8$ 

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Fig. S5 Arrhenius activation energies for sulfur-containing compound oxidation with Anderson catalyst (CTA)PMo<sub>4</sub>V<sub>8</sub> using dioxygen as the oxidant. Conditions: (CTA)PMo<sub>4</sub>V<sub>8</sub> (0.05 mmol), sulfur-containing compound (S: 500 ppm) in 6 mL decalin, reaction temperature 80, 85, 90 and 100 °C, oxidant O<sub>2</sub>

Fig. S6 GC-MS spectrum of the reaction product (dibenzothiophene sulfone)

Fig. S7 The influence of DBT concentrations on the catalytic activity. Reaction conditions: DBT (500 ppm, 6 mL decalin) (CTA)PMo<sub>4</sub>V<sub>8</sub> (0.05 mmol) at 100 °C with  $O_2$ , 5 h

Fig. S8 The crystal of the catalytic product DBTO<sub>2</sub>

Fig. S9 The stability of (CTA)PMo<sub>4</sub> $V_8$  was determined by IR(a), XPS(b) and SEM(c)

Table S1 The comparison between various catalysts under aerobic conditions

#### S1. Materials and Physical measurements

All chemicals and solvents used were AR grade or better without further purification. Dibenzothiophene (DBT, M = 184.26, 640 mg) was dissolved in decalin (250 mL) at room temperature as simulated diesel whose sulfur content was 500 ppm. A decalin solution with a series of DBT gradients was configured as the model oil. For oxidation desulfurization, thiophene, DBT, BT and 4, 6-DMDBT were prepared from the stock solution.  $(NH_4)_5H_6PV_8Mo_4O_{40}$  and  $(CTA)PMo_4V_8$  were prepared according to Ref. [1,2] Characterization of  $(CTA)PMo_4V_8$  was given in Supporting Information.

The model and manufacturer of physical measurements used were detailed in the Supplementary Information. The reaction product was determined by GC-MS. The S-content of diesel and gasoline were determined build ICP-AES (ICP 6300). IR spectra (4000 - 400 cm<sup>-1</sup>) were recorded in discs on a Nicolet Magna 560 IR spectrometer. <sup>31</sup>P MAS NMR measurements were obtained using a Bruker AVANCE III 400MB spectrometer at 202.5 MHz. XRD patterns of the samples were collected on a Japan Rigaku Dmax 2000 VPC X-ray diffractometer with Cu Ka radiation ( $\lambda = 0.154178$  nm). UV-vis spectra (200 - 800 nm) were recorded on a Cary 500 UV-Vis-NIR spectrophotometer. XPS patterns of the samples were collected on a micro-focused monochromatic Al Ka X-ray source XPS (Thermo Scientific). A SU8010 scanning electron microscope determined SEM images. Using JEM-2100 instrument to record TEM micrographs. The analysis of the recovered solutions was performed using high-performance liquid chromatography (HPLC) and samples were detected by RID detector.

### S2. Catalytic oxidative desulfurization for model oil and or diesel and gasoline

Catalytic oxidative desulfurization for model oil or diesel and gasoline was done according to our previous report. The oxidation of DBT-containing model oil was conducted in a glass reactor with an oxygen bubbling device like cold trap. 0.03 mmol of catalyst and 6 mL of DBT-containing model oil were added into the reactor and heated up to the desired temperature and stirred at 500 rpm. Then molecular oxygen was bubbled through the reaction solution for 10 mL·min<sup>-1</sup>. After designated reaction time, the mixture was centrifuged in 8000 rpm for 20 min to separate the insoluble catalyst and let the mixture stand for one night to precipitate needle crystals-DBTO<sub>2</sub>. The insoluble catalyst was washed with alcohol to remove the decalin off the surface of the catalyst. Then the solid catalyst was reused without further treatment. The content of DBT in decalin was analyzed immediately by GC.

The oxidation of diesel and gasoline was conducted as follows: 6 mL of diesel (with 1282 ppm sulfur content) or gasoline (with 996 ppm) was mixed 0 0.05 mmol of catalyst in a three-necked bottle which placed in oil bath for 8 h with stirring (500 rpm) at 100 °C with flowing molecular oxygen at 10 mL/min. The oxidized oil was cooled to room temperature and centrifuged in 8000 rpm for 20 min to separate the insoluble catalyst. The separated liquid was filtered using Bochner funnel containing 0.3 g column-layer chromatographic silica gel to adsorb oxidative products.



Fig. S1 The IR spectrum of (CTA)PMo $_4V_8$ , CTAB and (NH<sub>4</sub>) $_5H_6PMo_4V_8$ 



Fig. S2 The DR-UV-Vis spectra of PMoV and (CTAB)<sub>5</sub>PMoV



Fig. S3 The SEM image of (CTA)PMo<sub>4</sub> $V_8$ .



Fig. S4 The TEM images of (CTA)PMo $_4V_8$ 



**Fig. S5** Arrhenius activation energies for sulfur-containing compound oxidation with Anderson catalyst (CTA)PMo<sub>4</sub>V<sub>8</sub> using dioxygen as the oxidant. Conditions: (CTA)PMo<sub>4</sub>V<sub>8</sub> (0.05 mmol), sulfur-containing compound (S: 500 ppm) in 6 mL decalin, reaction temperature 80, 85, 90 and 100 °C, oxidant O<sub>2</sub>.



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Fig. S7 The influence of DBT concentrations on the catalytic activity. Reaction conditions: DBT (500 ppm, 6 mL decalin) (CTA)PMo<sub>4</sub>V<sub>8</sub> (0.05 mmol) at 100 °C with  $O_2$ , 5 h



Fig. S8 The crystal of the catalytic product  $DBTO_2$ 







Fig. S9 The stability of (CTA)PMo $_4V_8$  was determined by IR(a), XPS(b) and SEM(c)

Catalyst	Usage	Substrate	Temperature	Reaction time	conversion	Ref.
	(mg)		(°C)	(h)	(%)	
$[C_{18}H_{37}N(CH_3)_3]_5PV_2Mo_{10}O_{40}$	33	DBT	60	4	100	3
$[C_8H_{17}N(CH_3)_3]_3H_3V_{10}O_{28}$	40	DBT	90	7	100	4
$[(C_{18}H_{37})_2N(CH_3)_2]_5[IMo_6O_{24}]$	39	DBT, BT, 4, 6-DMDBT	80	8, 12, 8	92, 100, 92	5
$[(C_{18}H_{37})_2N(CH_3)_2]_3Co(OH)_6Mo_6O_{18}$	11	DBT, 4, 6-DMDBT, BT	80	5, 7, 12	100, 100, 65	6
$[C_8H_{17}N(CH_3)_3]_3HIV_9O_{28}$	40	DBT, 4, 6-DMDBT	90	6, 7	100	7
$[C_{16}H_{33}N(CH_3)_3]_5[PMo_{10}V_2O_{38}(O_2)_2]$	191	DBT	70	4	98	8
$[C_{18}H_{37}N(CH_3)_3]_7PW_{10}Ti_2O_{38}(O_2)_2$	242	DBT	90	6	100	9
[Cu <sub>2</sub> (BTC) <sub>4/3</sub> (H <sub>2</sub> O) <sub>2</sub> ] <sub>6</sub> [H <sub>5</sub> PV <sub>2</sub> Mo <sub>10</sub> O <sub>40</sub> ]	44	DBT	80	1.5	100	10
(NH <sub>4</sub> ) <sub>3</sub> Co(OH) <sub>6</sub> Mo <sub>6</sub> O <sub>18</sub>	20	DBT	60	1	99	11
H <sub>8</sub> PV <sub>5</sub> Mo <sub>7</sub> O <sub>40</sub>	910	BT	120	6	99	12
Na <sub>3</sub> H <sub>6</sub> CrMo <sub>6</sub> O <sub>24</sub>	20	DBT, 4, 6-DMDBT, BT	60	2, 3, 4	100, 100, 90	13
Na <sub>3</sub> H <sub>6</sub> FeMo <sub>6</sub> O <sub>24</sub>	20	DBT, 4, 6-DMDBT, BT	60	3, 3, 4	99, 99, 95	14
(NH <sub>4</sub> ) <sub>5</sub> H <sub>6</sub> PV <sub>8</sub> Mo <sub>4</sub> O <sub>40</sub>	20	DBT, 4, 6-DMDBT,	100	6, 6, 11, 12	100, 100, 100, 97	15
DOM@MOE 100@L7SM 5(DM7)	150		60	2	100 ~90	16
POWI@MOF-199@LZSWI-3(PMZ)	200		00	2	100, <80	10
$PMO_6 W_6 O_{40} @MOF-199 @MCM-41$	200	DRI	83	3	98.5	1 /

Table S1 The desulfurization upon various POMs using oxygen or air as oxidant

SRL-POM@MOF-199@MCM-41	150	DBT	60	2	100	18
Metal-POM@MOF-199@MCM-41	200	DBT	80	3	99.1	19
S/D/C-POM@MOF@MCM-41	150	DBT, 4, 6-DMDBT, BT	50	1.5	100, 70, 92	20
Cs-POM@MOF-199@MCM-41	200	DBT	80	5	99.6	21
PV8M04O40@iPAF-1	12	DBT, 4, 6-DMDBT	80	5	100, 100	22
[C <sub>8</sub> mim] <sub>3</sub> H <sub>3</sub> V <sub>10</sub> O <sub>28</sub> /g-BN*	80	DBT, 4-MDBT, 4, 6-	120	4, 5, 5	99.8, 99.5, 95.3	23
		DMDBT				
CNTs@PDDA@Mo <sub>16</sub> V <sub>2</sub>	100	DBT	60	3	99.4	24
CNC@PIL@POM*	20	DBT, 4, 6-DMDBT, BT	100	6, 7, 9	100	25
[(C <sub>8</sub> H <sub>17</sub> ) <sub>3</sub> NCH <sub>3</sub> ] <sub>3</sub> PMo <sub>12</sub> O <sub>40</sub> /γ-MMS*	25	DBT, 4-MDBT	120	5, 7	100	26
H <sub>4</sub> PMo <sub>11</sub> V <sub>1</sub> O <sub>40</sub>	12	DBT	100	6	17.3	This work

## Reference

- 1. H. Lü, Y. Zhang, Z. Jiang, C. Li, Green Chemistry, 12 (2010) 1954.
- S.-y. Fujibayashi, K. Nakayama, M. Hamamoto, S. Sakaguchi, Y. Nishiyama, Y. Ishii, Journal of Molecular Catalysis A: Chemical, 110 (1996) 105-117.
- 3. H. Lu, J. Gao, Z. Jiang, Y. Yang, B. Song and C. Li, *Chemical Communications*, 2006, **2**, 150-152.
- N. Tang, Y. Zhang, F. Ling, H. Lu, Z. Jiang and C. Li, *Chemical Communications*, 2012, 48, 11647-11649.
- 5. H., Zhang, Y., Jiang, Z. and C., *Green Chemistry*, 2010, **12**: 1954.
- L. Hongying, W. Ren, W. Liao, C. Wei, L. Yang and Z. Suo, *Applied Catalysis B Environmental*, 2013, s 138–139, 79-83.
- 7. N. Tang, Z. Jiang and C. Li, *Green Chemistry*, 2015, 17: 817-820.
- 8. M. Tao, H. Zheng, J. Shi, S. Wang, X. Wang and G. Huang, *Catalysis Surveys from Asia*, 2015, **19**: 257-264.
- 9. C. Jiang, J. Wang, S. Wang, H. Y. Guan, X. Wang and M. Huo, *Applied Catalysis B Environmental*, 2011, **106**, 343-349.
- Y. Liu, S. Liu, S. Liu, D. Liang, S. Li, Q. Tang, X. Wang, J. Miao, Z. Shi and Z. Zheng, *ChemCatChem*, 2013, 5, 3086-3091.
- L. Sun, T. Su, J. Xu, D. Hao, W. Liao, Y. Zhao, W. Ren, C. Deng and H. Lü, *Green Chemistry*, 2019, 21: 2629-2634.
- B. Bertleff, J. Claußnitzer, W. Korth, P. Wasserschei, A. Jess and J. Alber, Acs Sustainable Chemistry & Engineering, 2017, 5: 4110-4118.
- 13. M. Chi, Z. Zhu, L. Sun, T. Su and H. Lü, *Applied Catalysis B Environmental*, 2019, **259**, 118089.
- 14. J. X. A, Z. Z. A, T. S. A, W. L. A, C. D. A, D. H. A. B, Y. Z. A. C, W. R. C and H. L. A, *Chinese Journal of Catalysis*, 2020, **41**, 868-876.
- 15. S. Meng, Z. Dan, Y. Xia, Y. Li and Y. Wu, *Fuel Process Technol*, 2017, 160, 136-142.
- 16. Si-Wen, Li, Rui-Min, Gao, Wei, Zhang, Yuan, Zhang and Jian-she, Fuel, 2018, 221: 1-11.
- 17. S. W. Li, R. M. Gao, R. L. Zhang and J. S. Zhao, *Fuel*, 2016, **184**, 18-27.
- 18. S. W. Li, Z. Yang, R. M. Gao, G. Zhang and J. S. Zhao, *Applied Catalysis B Environmental*, 2018, **221**: 574-583.
- S.-W. Li, J.-R. Li, Y. Gao, L.-L. Liang, R.-L. Zhang and J.-s. Zhao, *Fuel*, 2017, 197, 551-561.
- 20. S. Li, R. Gao and J. Zhao, Acs Sustainable Chemistry & Engineering, 2018, 6: 15858-15866.
- S. W. Li, J. R. Li, Q. P. Jin, Z. Yang, R. L. Zhang, R. M. Gao and J. S. Zhao, *Journal of Hazardous Materials*, 2017, 337: 208-216.
- 22. J. Song, Y. Li, P. Cao, X. Jing and G. Zhu, Advanced Materials, 2019, 31: 1902444.
- 23. C. Wang, Z. Chen, X. Yao, Y. Chao, S. Xun, J. Xiong, L. Fan, W. Zhu and H. Li, *Fuel*, 2018, **230**, 104-112.
- 24. G. Yan, R. Gao, Z. Gai, Z. Ying and J. Zhao, Fuel, 2018, 224, 261-270.
- 25. H. Yang, Q. Zhang, J. Zhang, L. Yang and H. Chen, Journal of Colloid & Interface

Science, 2019, **554**: 572-579.

26. S. X. A, W. J. B, T. G. B, M. H. B, R. M. B, M. Z. B, W. Z. B and H. L. B, *Journal of Colloid and Interface Science*, 2019, **534**, 239-247.