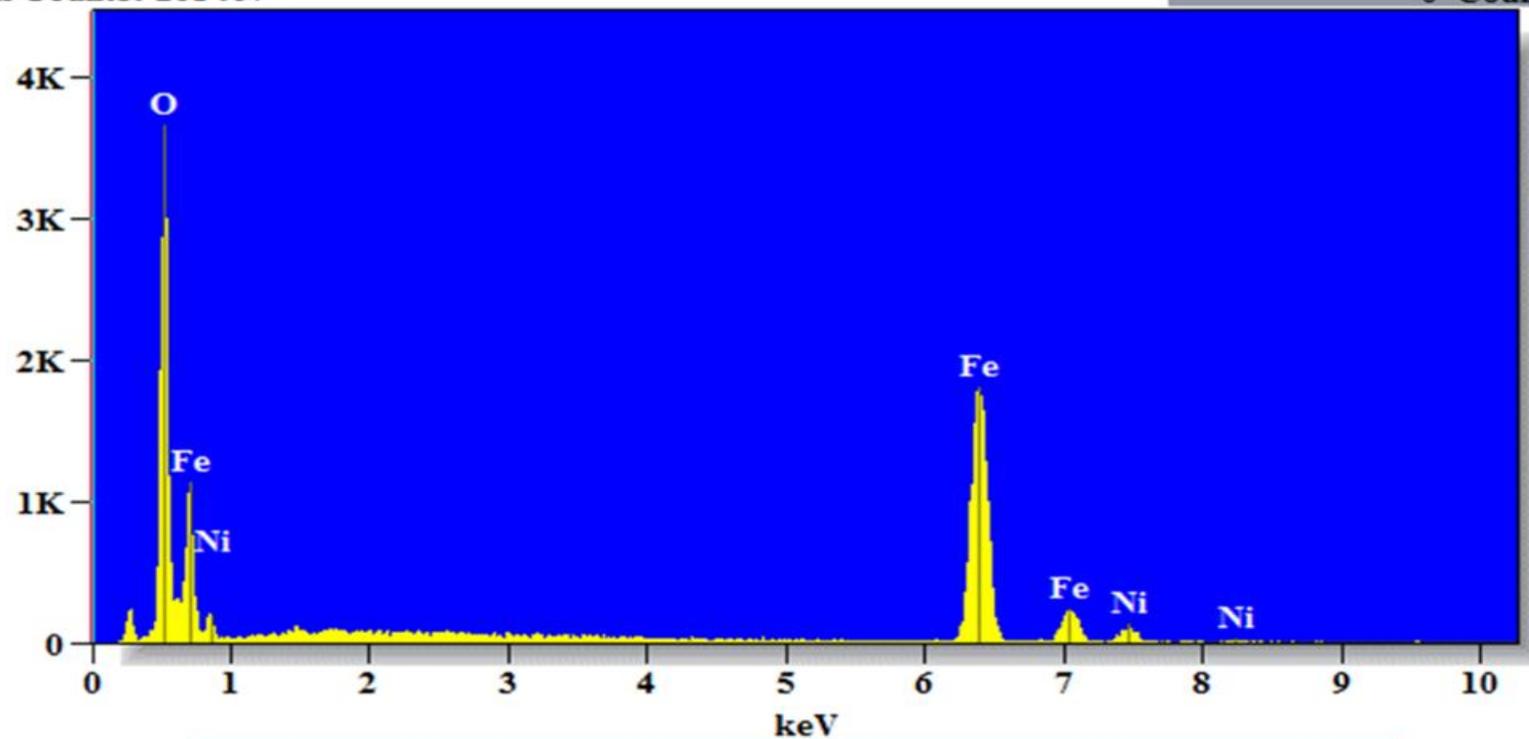


Integral Counts: 105407

Base(4)

Cursor: 0.000 keV  
0 Counts



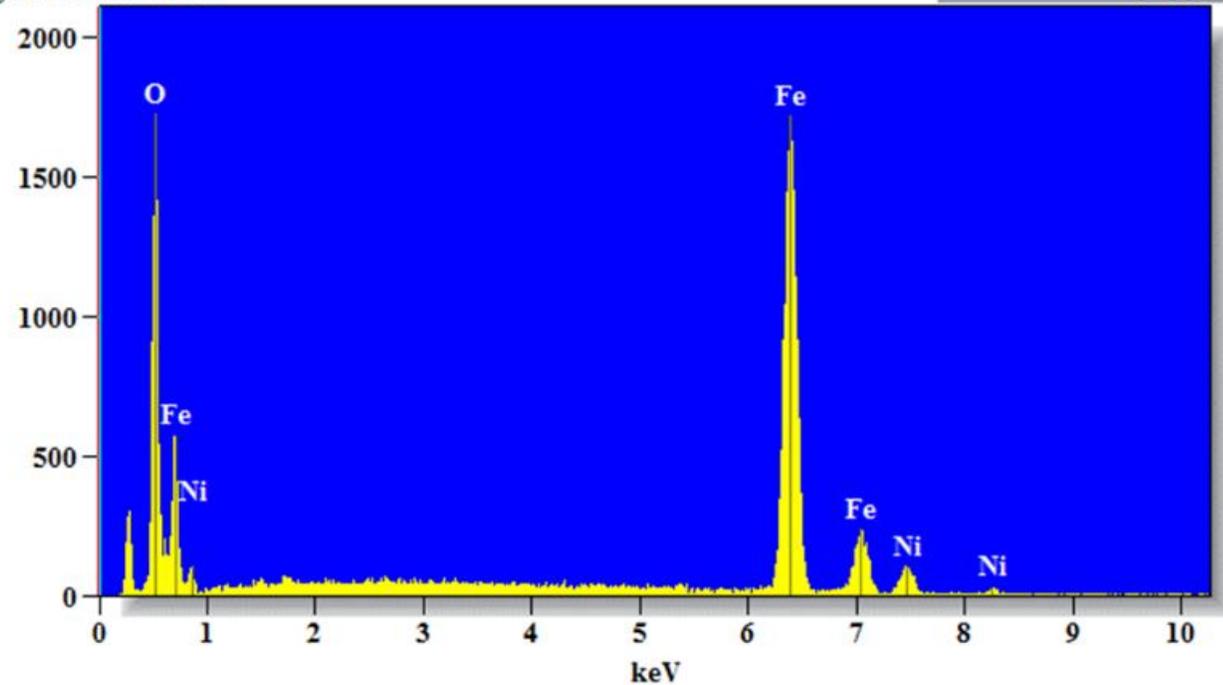
<i>Element</i>	<i>Net Counts</i>	<i>Int. Cps/nA</i>	<i>Weight %</i>	<i>Atom %</i>
<i>O</i>	19080	---	34.22	64.58
<i>Fe</i>	28336	---	60.57	32.74
<i>Fe</i>	9804	---	---	---
<i>Ni</i>	1645	---	5.21	2.68
<i>Ni</i>	1335	---	---	---
<i>Total</i>			100.00	100.00

Sup.Figure 1a Elemental composition for 5NF catalyst obtained using EDS

Full scale counts: 1727  
Integral Counts: 76042

Base(3)

Cursor: 0.000 keV  
0 Counts



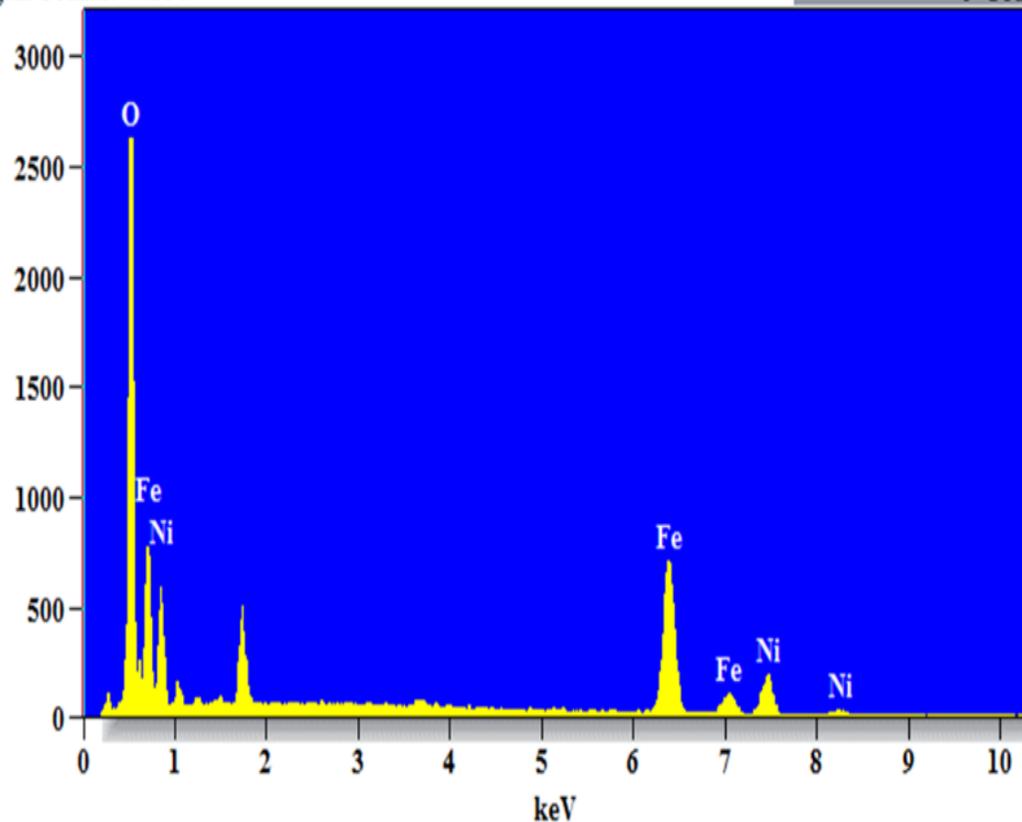
<i>Element</i>	<i>Net Counts</i>	<i>Int. Cps/nA</i>	<i>Weight %</i>	<i>Atom %</i>
<i>O</i>	8940	---	22.39	49.08
<i>Fe</i>	25985	---	67.31	45.84
<i>Fe</i>	5170	---	---	---
<i>Ni</i>	1545	---	10.3	5.08
<i>Ni</i>	719	---	---	---
<i>Total</i>			100.00	100.00

Sup.Figure 1b Elemental composition for 10NF catalyst obtained using EDS

Full scale counts: 2634  
Integral Counts: 74504

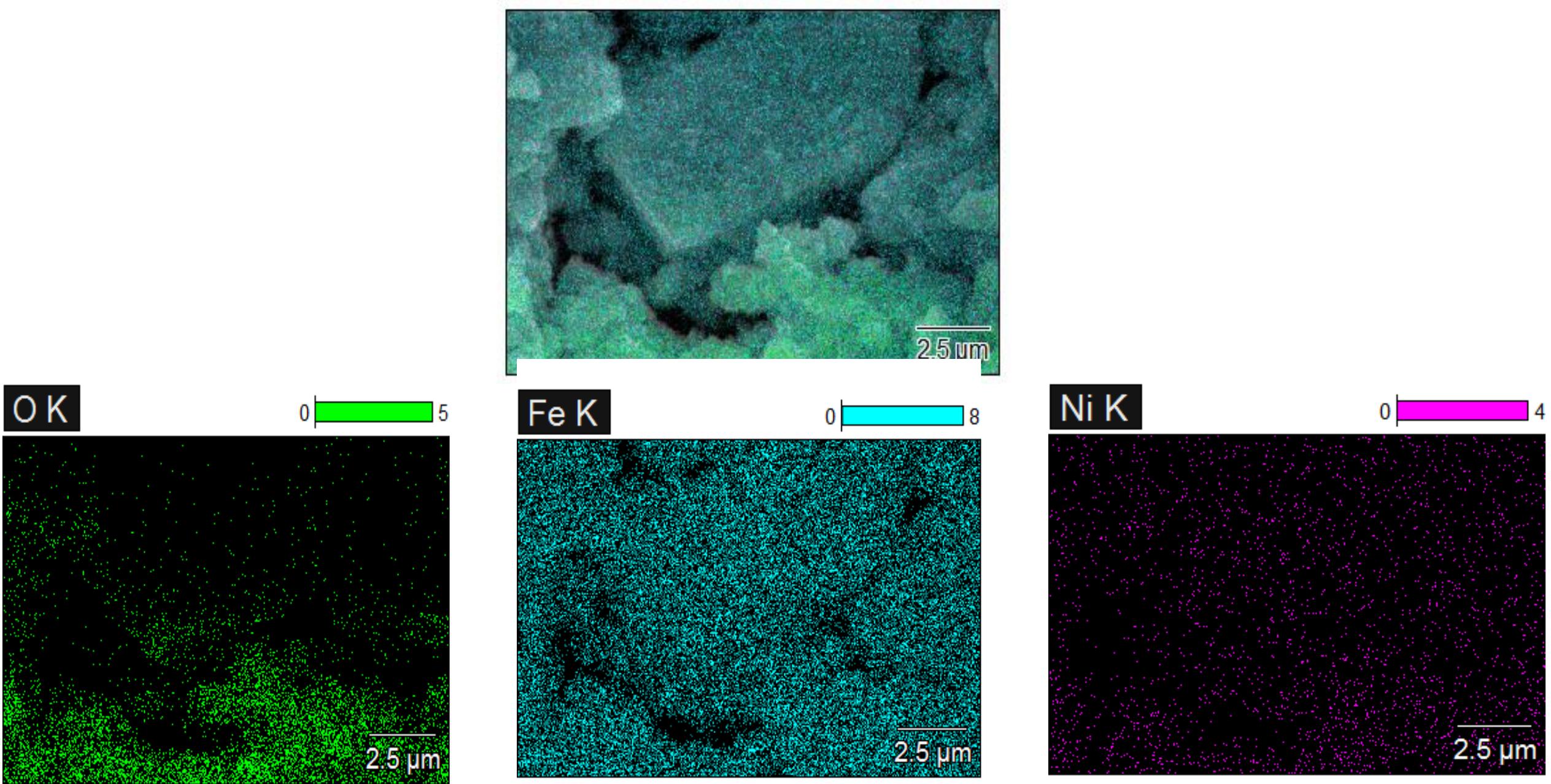
Base(11)

Cursor: 0.000 keV  
0 Counts

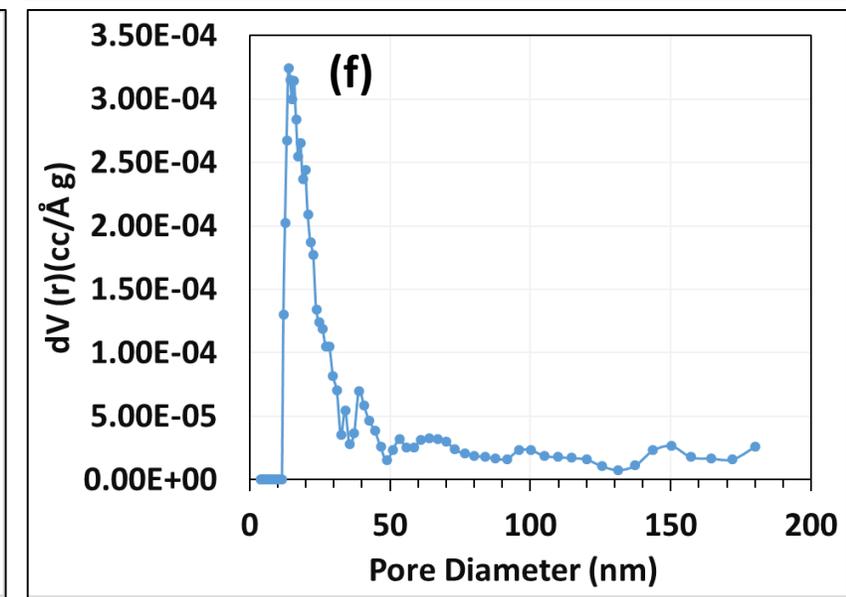
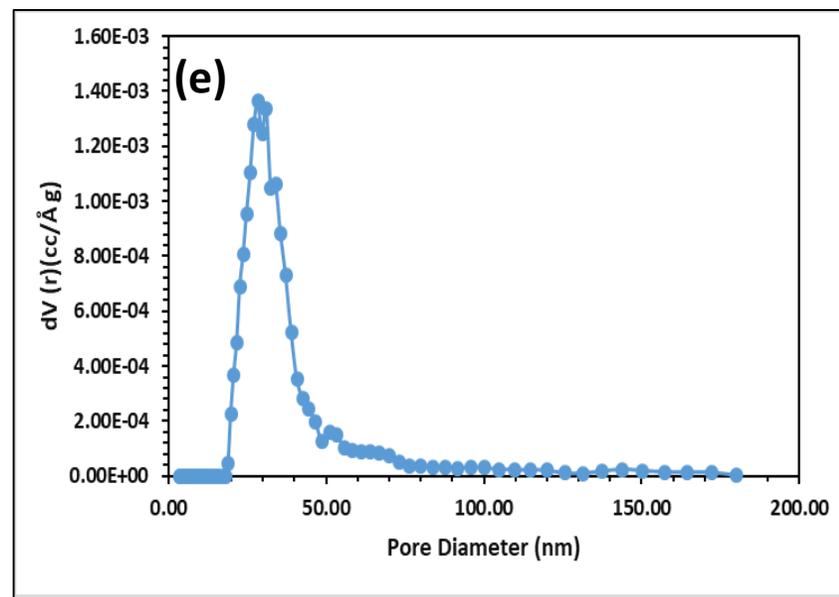
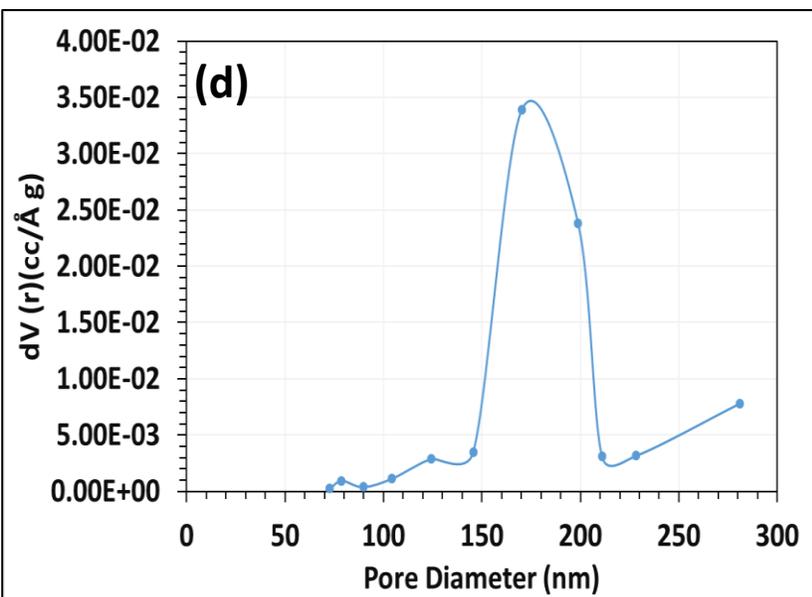
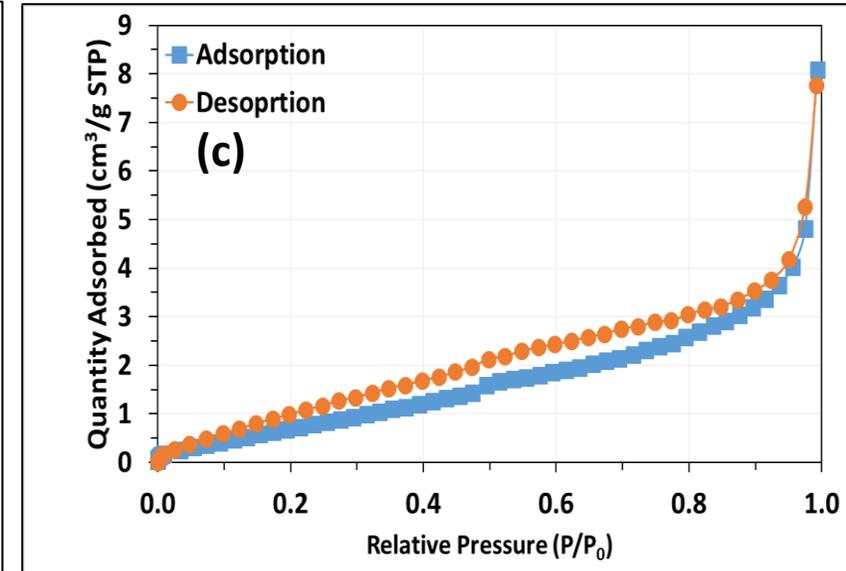
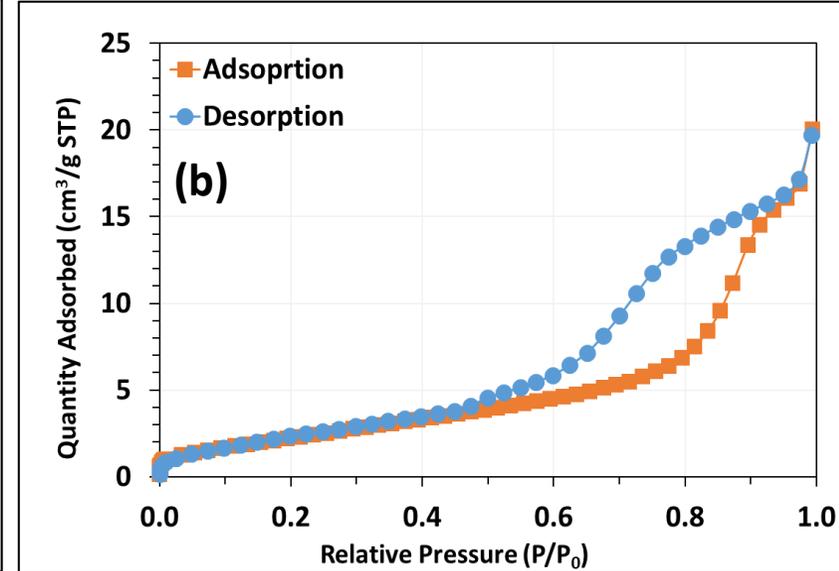
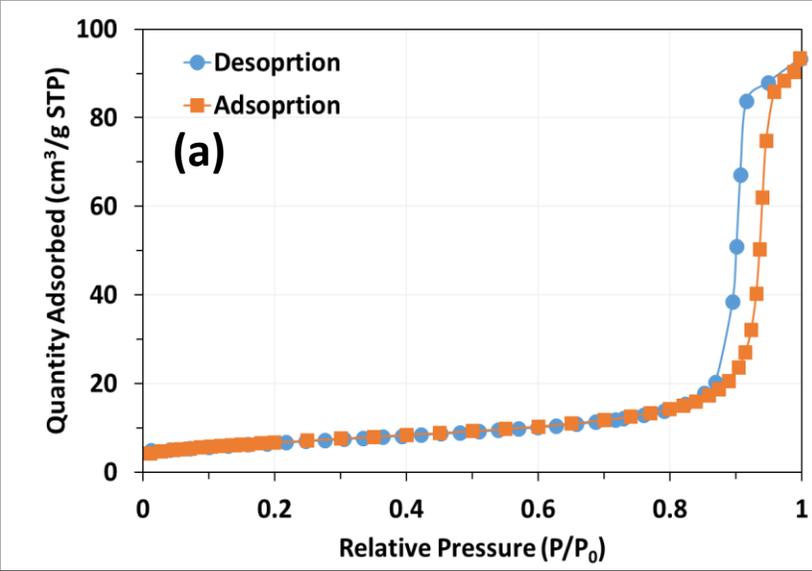


<i>Element</i>	<i>Net Counts</i>	<i>Int. Cps/nA</i>	<i>Weight %</i>	<i>Atom %</i>
<i>O</i>	14123	---	26.67	56.30
<i>Fe</i>	10899	---	58.03	36.27
<i>Fe</i>	5439	---	---	---
<i>Ni</i>	2732	---	15.3	7.43
<i>Ni</i>	3089	---	---	---
<i>Total</i>			100.00	100.00

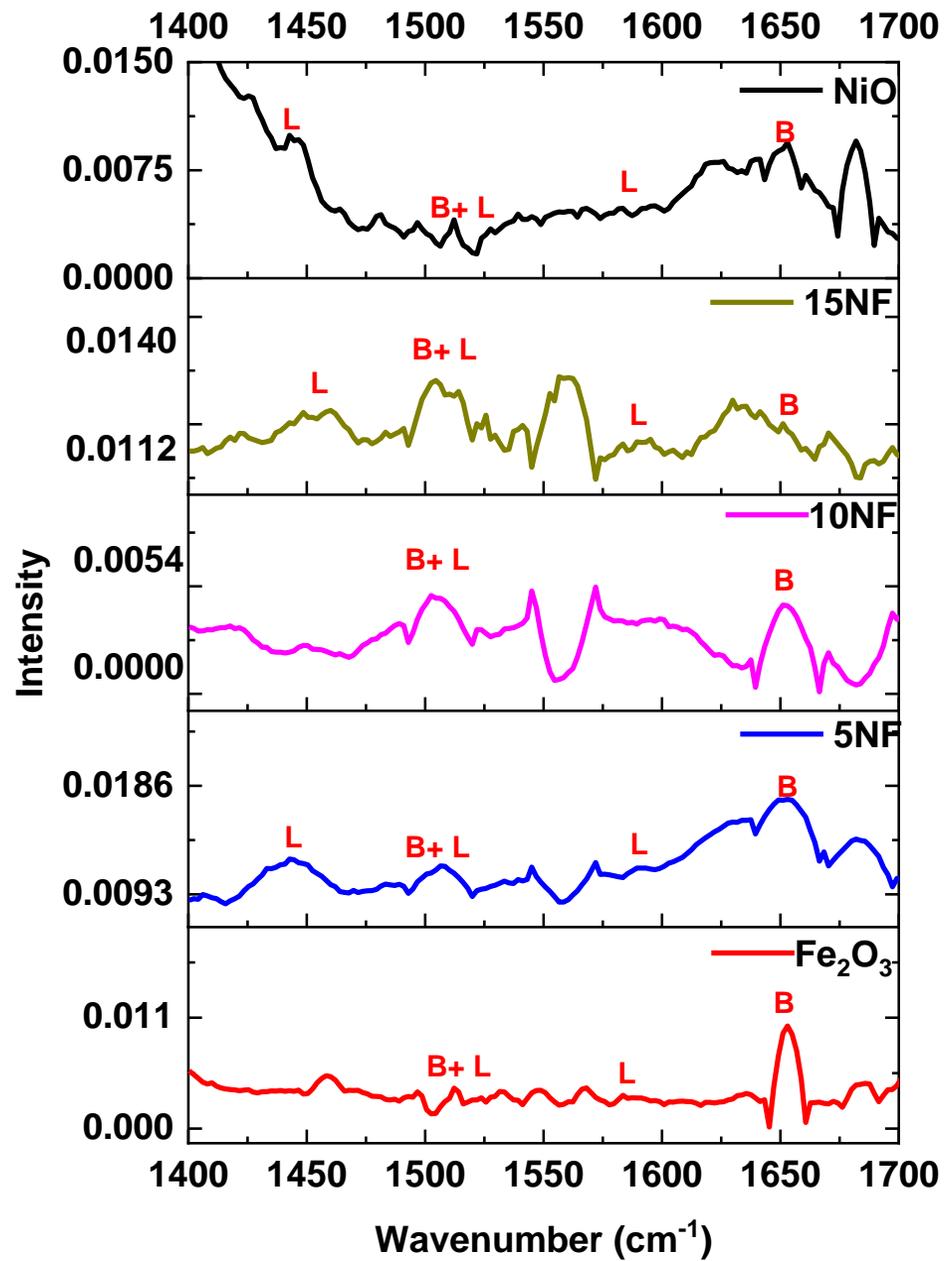
Sup.Figure 1c Elemental composition for 15NF catalyst obtained using EDS



Sup.Figure 1d Elemental mapping for 10NF catalyst obtained using FESEM



Sup. Figure 2 Adsorption-Desorption isotherm of catalysts (a) 5 NF, (b) 10 NF, (c) 15 NF, (d)  $dV(r)$  vs pore diameter for 5 NF, (e)  $dV(r)$  vs pore diameter for 10 NF, (f)  $dV(r)$  vs pore diameter for 15 NF.



Sup.Figure 3 Pyridine adsorbed -FTIR spectra of prepared catalysts.

$$\text{CO}_2 \text{ conversion (\%)} = \frac{[\text{CO}_2(\text{in}) - \text{CO}_2(\text{out})]}{[\text{CO}_2(\text{in})]} \times 100$$

Sup. Equation 1

$$\text{CO selectivity (\%)} = \frac{[\text{CO}]}{[\text{CO}_2(\text{in}) - \text{CO}_2(\text{out})]} \times 100$$

Sup. Equation 2

$$\text{CH}_4 \text{ selectivity (\%)} = \frac{[\text{CH}_4]}{[\text{CO}_2(\text{in}) - \text{CO}_2(\text{out})]} \times 100$$

Sup. Equation 3

$$\text{CH}_3\text{OH selectivity of (\%)} = \frac{[\text{CH}_3\text{OH}]}{[\text{CO}_2(\text{in}) - \text{CO}_2(\text{out})]} \times 100$$

Sup. Equation 4

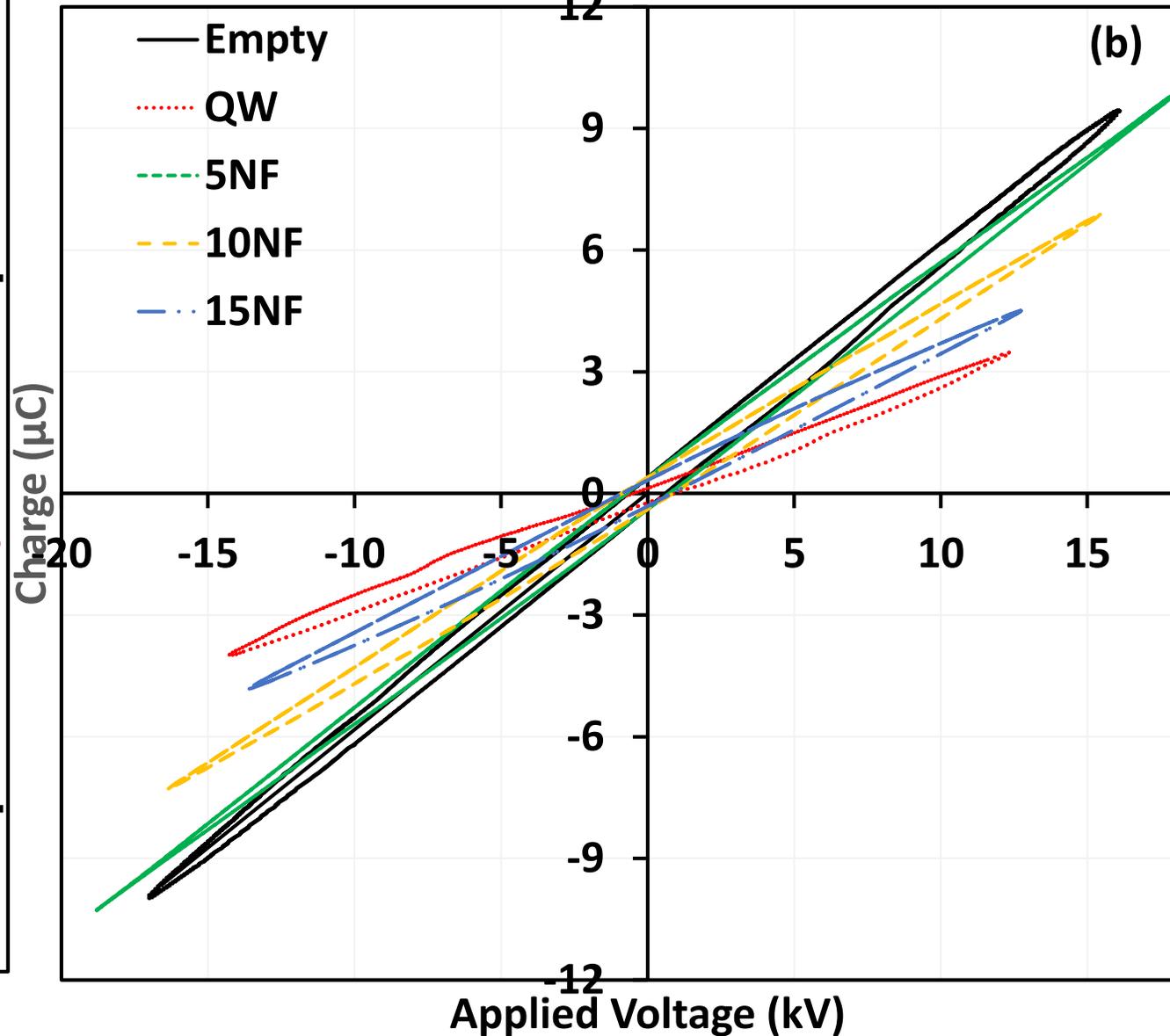
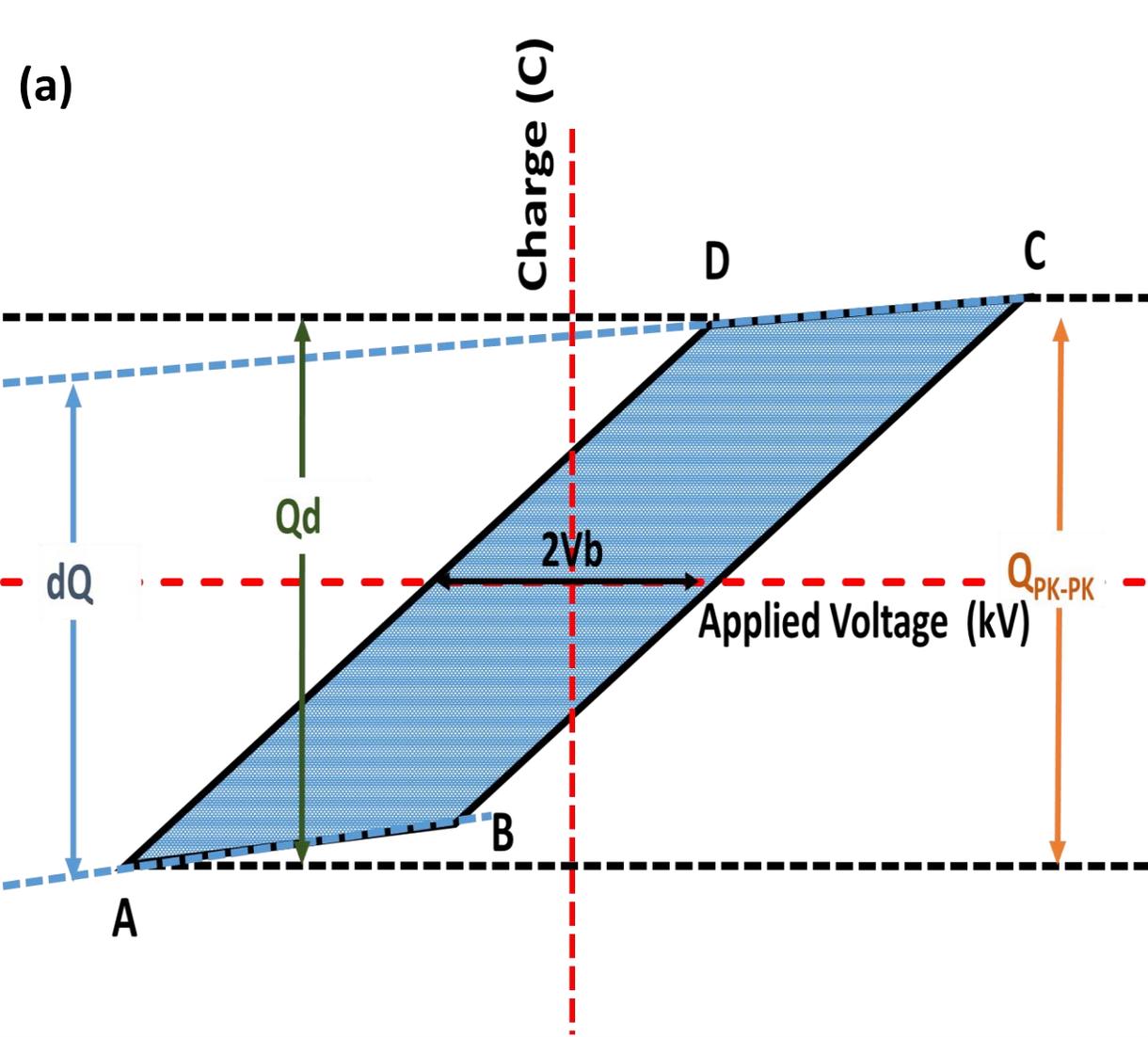
$$\text{Yield}(\text{CH}_3\text{OH}(\%), \text{CO}(\%), \text{CH}_4(\%)) = \frac{[(S_{\text{CH}_3\text{OH}}(\%), S_{\text{CO}}(\%), S_{\text{CH}_4}(\%)) \times X_{\text{CO}_2}(\%)]}{100}$$

Sup. Equation 5

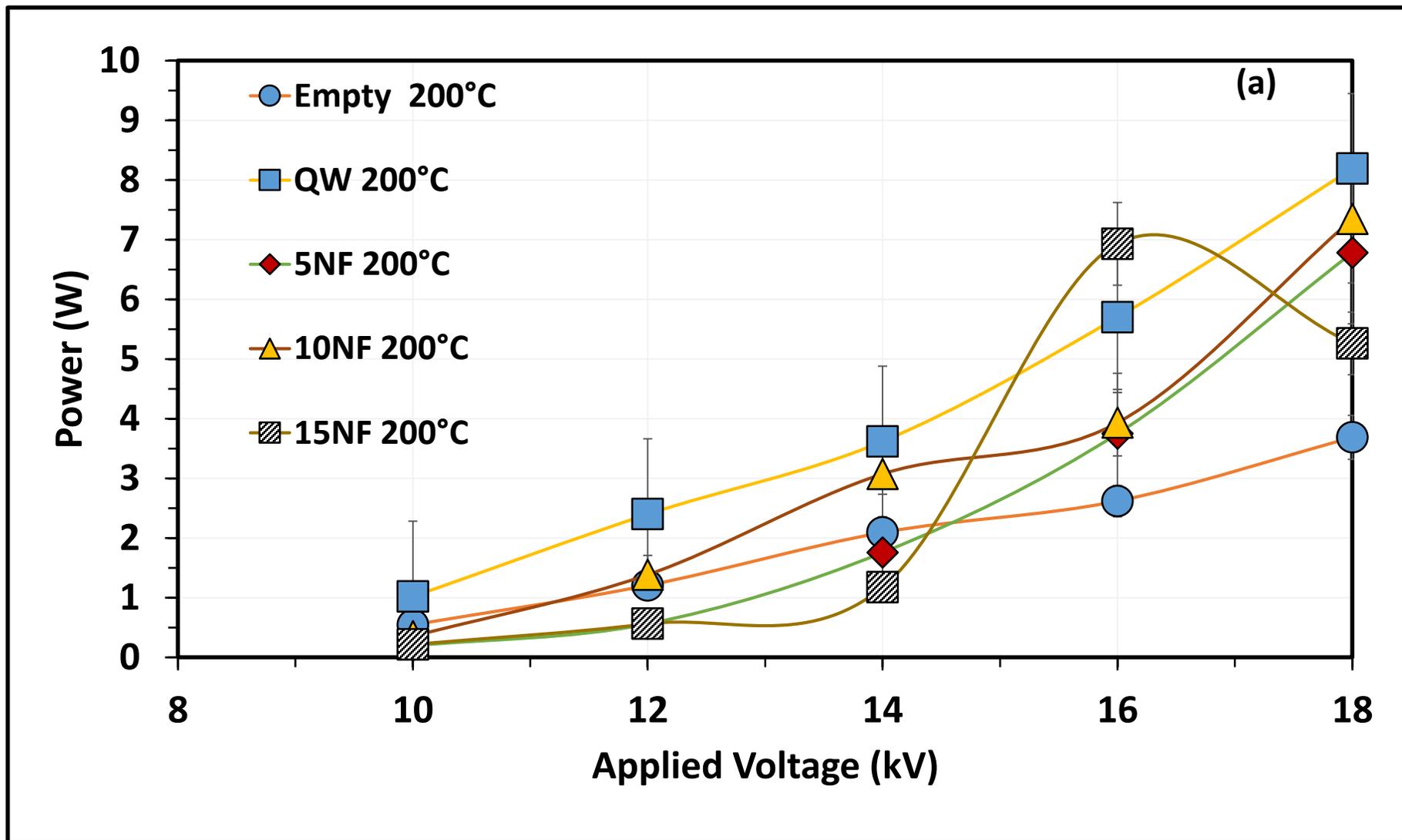
$$\text{Specific input energy (SIE J/L)} = \frac{\text{Power injected into the reactor (W)}}{\text{Feed flow rate } \left(\frac{\text{L}}{\text{S}}\right)}$$

Sup. Equation 6

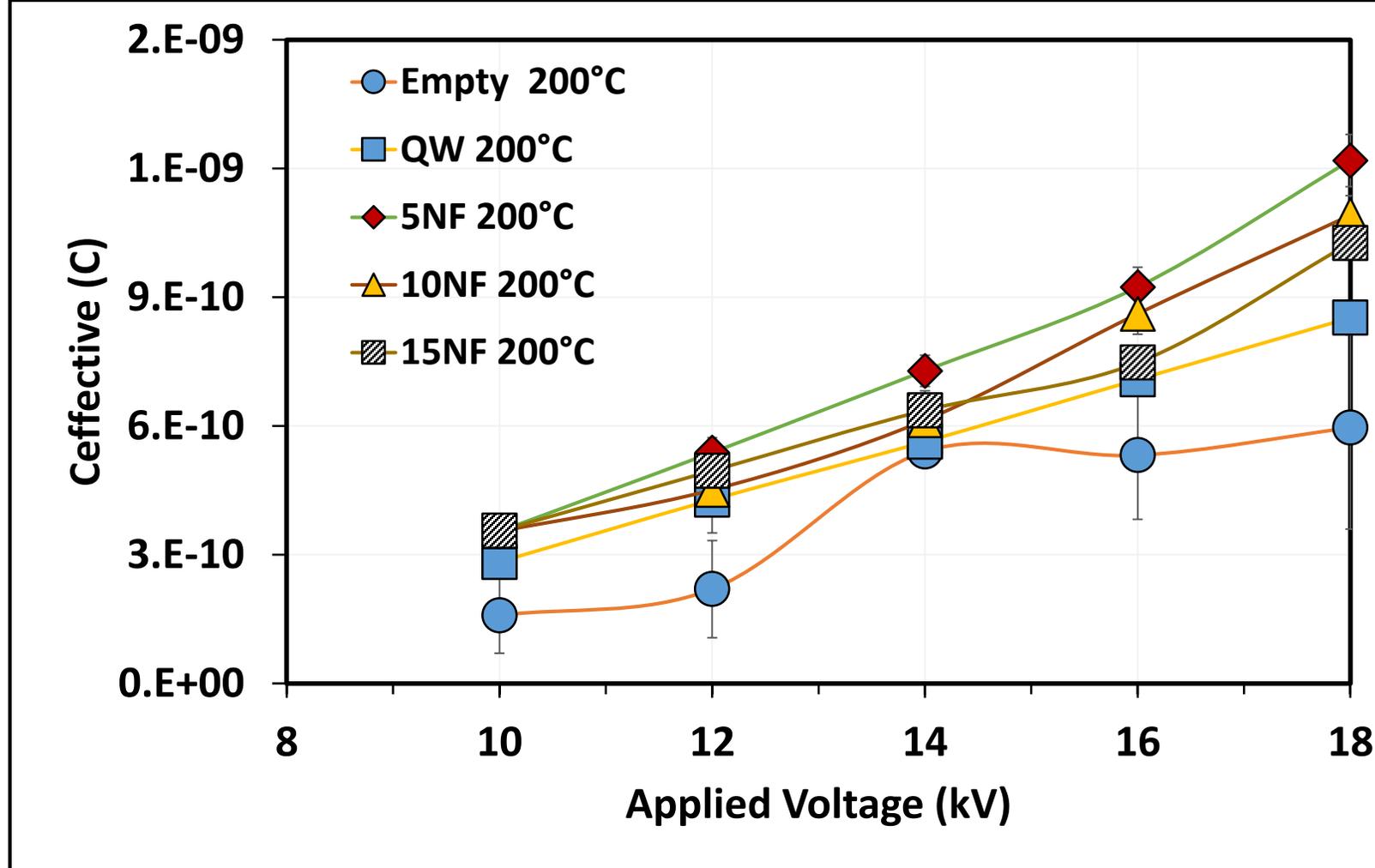
Where  $S_{\text{CH}_3\text{OH}}$  and  $X_{\text{CO}_2}$  are  $\text{CH}_3\text{OH}$  selectivity and  $\text{CO}_2$  conversion, respectively.



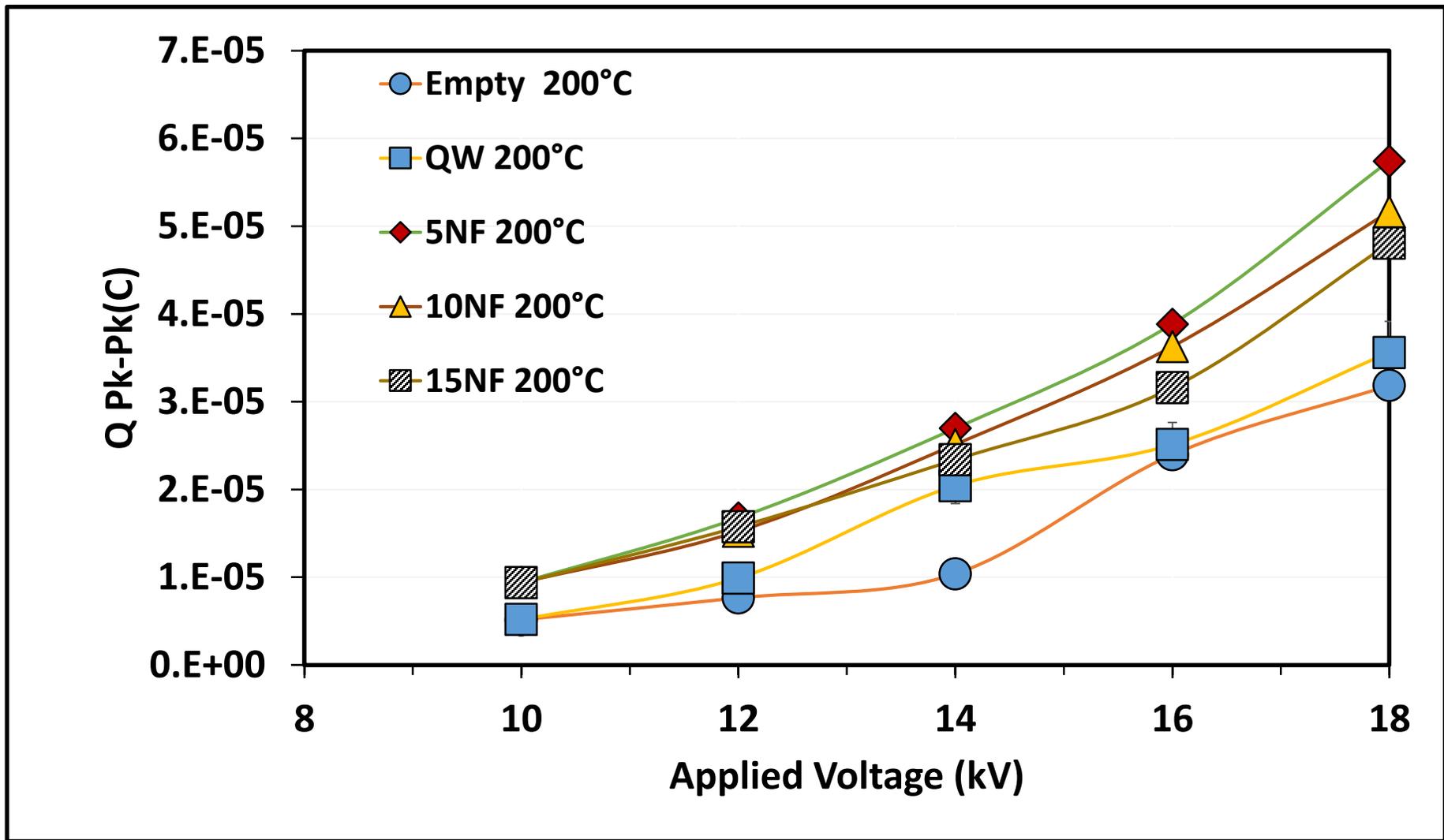
Sup. Figure 4 a) Typical schematic of Lissajous Figure, b) Discharge characteristics of reactor Lissajous figure at 14 kV for different packing materials (feed flow rate 100 ml/min,  $\text{CO}_2:\text{H}_2=1:3$ , frequency 50 Hz.)



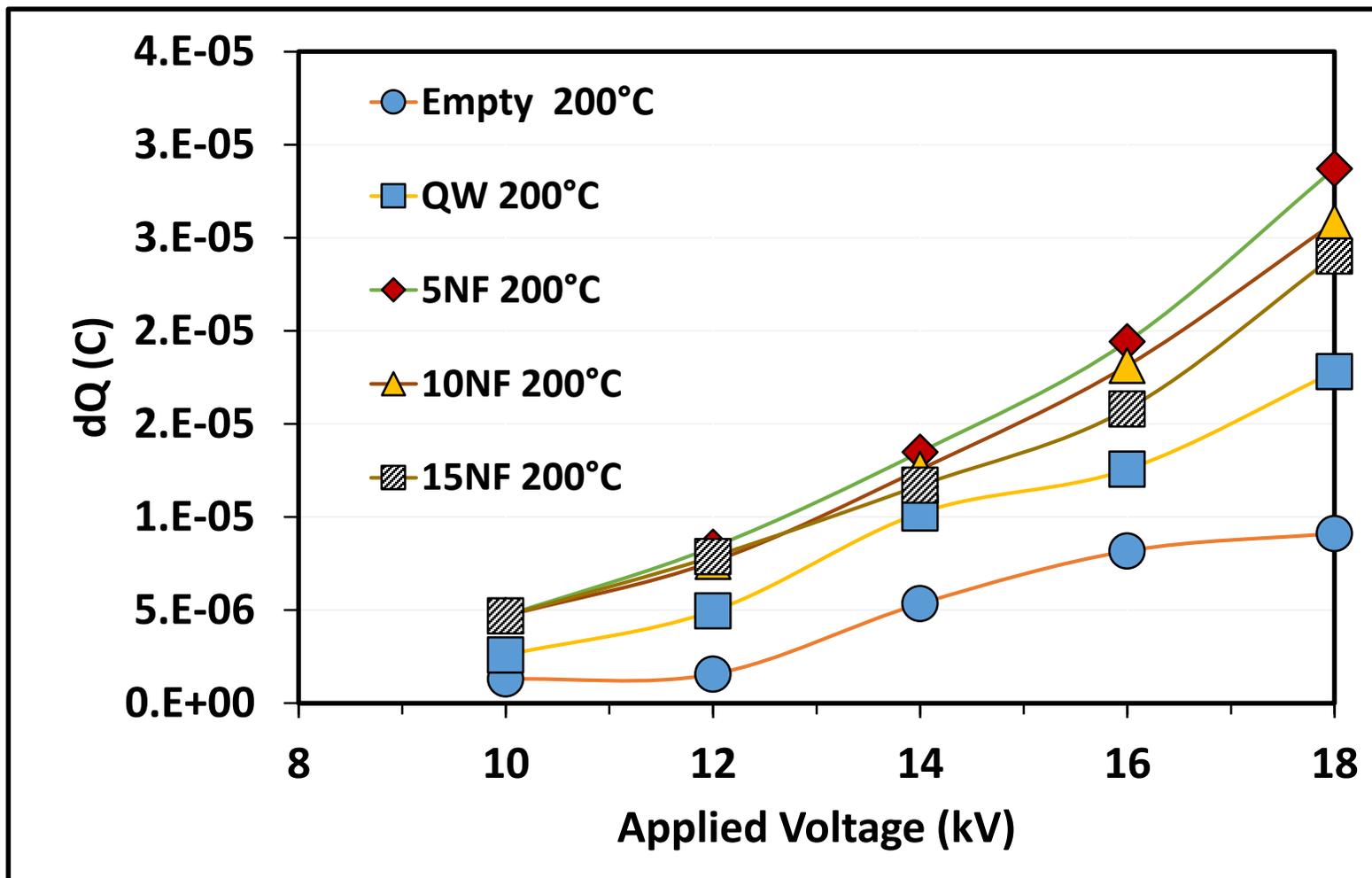
Sup.Figure 5 Discharge characteristics for various reactors: (a) impact of applied voltage on power injected into reactor ,(fee flow rate 100 ml/min, CO<sub>2</sub>:H<sub>2</sub>=1:3, frequency 50 hz.)



Sup.Figure 6 Discharge characteristics for various reactors: variation in effective capacitance with applied voltage, (feed flow rate 100 ml/min, CO<sub>2</sub>:H<sub>2</sub>=1:3, frequency 50 hz.)



Sup.Figure 7 Discharge characteristics for various reactors: peak charge transfer as a function of applied voltage (feed flow rate 100 ml/min, CO<sub>2</sub>:H<sub>2</sub>=1:3, frequency 50 hz.)



Sup.Figure 8 Discharge characteristics for various reactors: charge transfer per half cycle (feed flow rate 100 ml/min, CO<sub>2</sub>:H<sub>2</sub>=1:3, frequency 50 hz.)