

## **Selective catalytic reduction of NO over W-Zr-Ox/TiO<sub>2</sub>:**

### **Performance study of hierarchical pore structure**

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## Characterization

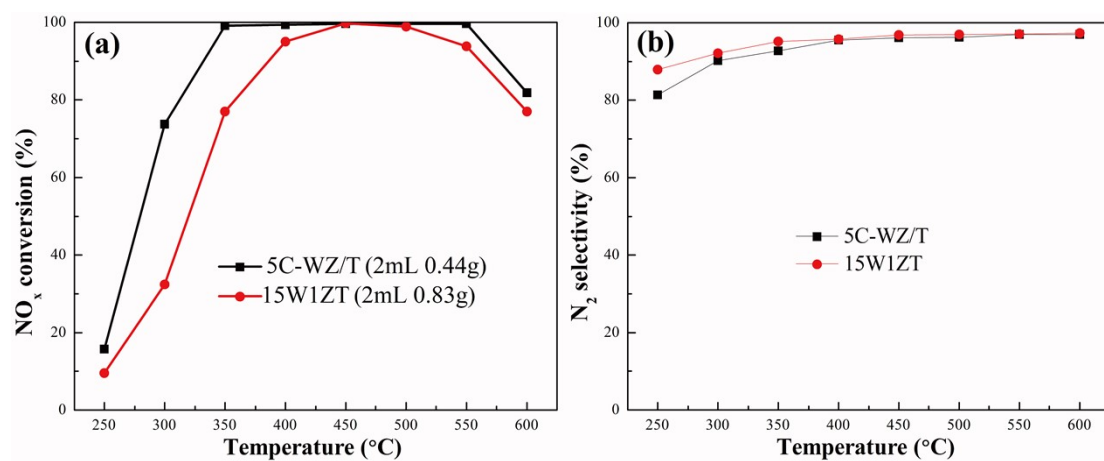
X-ray diffraction (XRD) patterns were obtained from an X-ray diffractometer (Smartlab TM 3 kW, Rigaku, Japan). The scan speed was  $10^\circ \cdot \text{min}^{-1}$  and the  $2\theta$  scans covered  $10\sim 85^\circ$ . The microstructural natures and element mapping of the catalysts have been investigated using a field emission scanning electron microscope (Carl Zeiss, Ultra 55) and transmission electron microscopy (JEOL, JEM-2010UHR). X-ray photoelectron spectroscopy (XPS) patterns were acquired by an AXIS ULTRA DLD instrument (Al-K $\alpha$  radiation, 1486.6 eV), and the vacuum degree was maintained at  $10^{-7}$  Pa. The samples were dried at  $100^\circ\text{C}$  for 24 h to remove moisture and then were tested without surface treatment. The curve fitting was performed by using XPSPEAK 4.1 with a Shirley-type background.

The temperature programmed desorption of ammonia (NH<sub>3</sub>-TPD) was conducted on the CHEMBET-3000 (Quantachrome) to obtain the surface acid properties. All the catalysts were preheated at  $400^\circ\text{C}$  under a helium stream for 1 h, and then cooled to  $50^\circ\text{C}$  for the ammonia adsorption. Afterwards, ammonia was desorbed from  $50^\circ\text{C}$  to  $550^\circ\text{C}$  at a heating rate of  $10^\circ\text{C} \cdot \text{min}^{-1}$ . The Semiautomatic Micromeritics TPD/TPR 2900 instrument was used for the temperature programmed reduction of hydrogen (H<sub>2</sub>-TPR). All the catalyst carriers were preheated to  $400^\circ\text{C}$  under an argon stream for 1 h, and cooled to  $50^\circ\text{C}$ . Then 5% H<sub>2</sub>/Ar flow was switched, and the temperature increased from  $50^\circ\text{C}$  to  $700^\circ\text{C}$  at a  $10^\circ\text{C} \cdot \text{min}^{-1}$  heating rate. The data were collected throughout the whole temperature range. The specific surface area and average pore diameter (BET method) of the samples were measured by N<sub>2</sub> adsorption/desorption isotherms at  $-196^\circ\text{C}$  using a surface-area analyzer (Micromeritics, 2020M V3.00H). All of the samples were degassed at  $350^\circ\text{C}$  under vacuum for 3 h prior to the adsorption experiments.

*In situ* Diffuse Reflectance Infrared Fourier Transform Spectra (*in situ* DRIFTS) were also collected by a Nicolet IS50 spectrometer. For NH<sub>3</sub>-SCR: 500 ppm NH<sub>3</sub> was pumped into the system for 10 min when the temperature was  $300^\circ\text{C}$ . Then the flow of NH<sub>3</sub> was stopped and 500 ppm NO + 10% O<sub>2</sub> was pumped into the system for 10

min. After that, 500 ppm NH<sub>3</sub> + 500 ppm NO + 10% O<sub>2</sub> was pumped into the system for 10 min. At last, the temperature increased to 450 °C and 600 °C at the mixed flow of NH<sub>3</sub>, NO and O<sub>2</sub>, and stayed at each temperature point for 10 min.

**Figure S1**

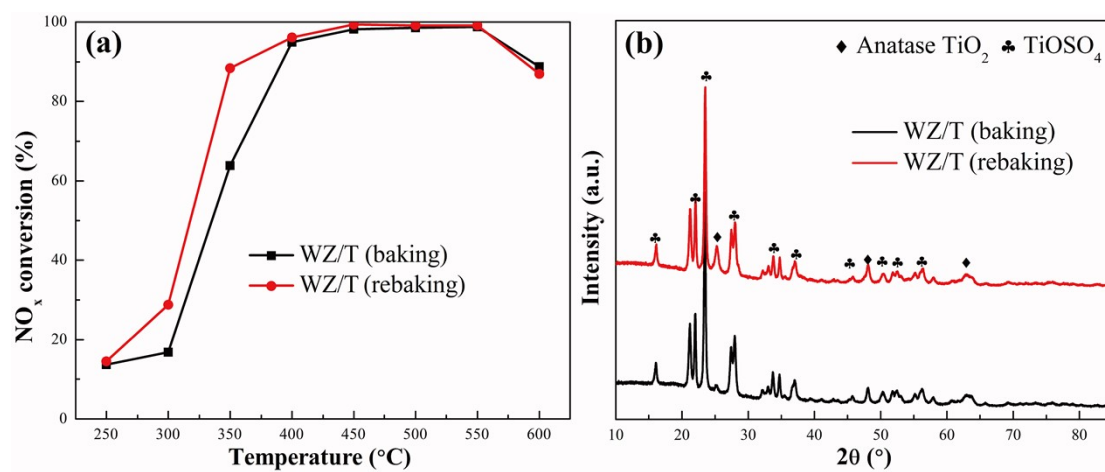


**Fig.S1** (a) NO conversion and (b) N<sub>2</sub> selectivity of 5C-WZ/T and 15W1ZT catalysts.

Reaction condition: 500 ppm NO, 500 ppm NH<sub>3</sub>, 10% O<sub>2</sub>, GSHV of 15000 h<sup>-1</sup> and N<sub>2</sub>

balance gas.

**Figure S2**



**Fig.S2** (a) NO conversion and (b) XRD patterns of different catalysts.

Figure S3

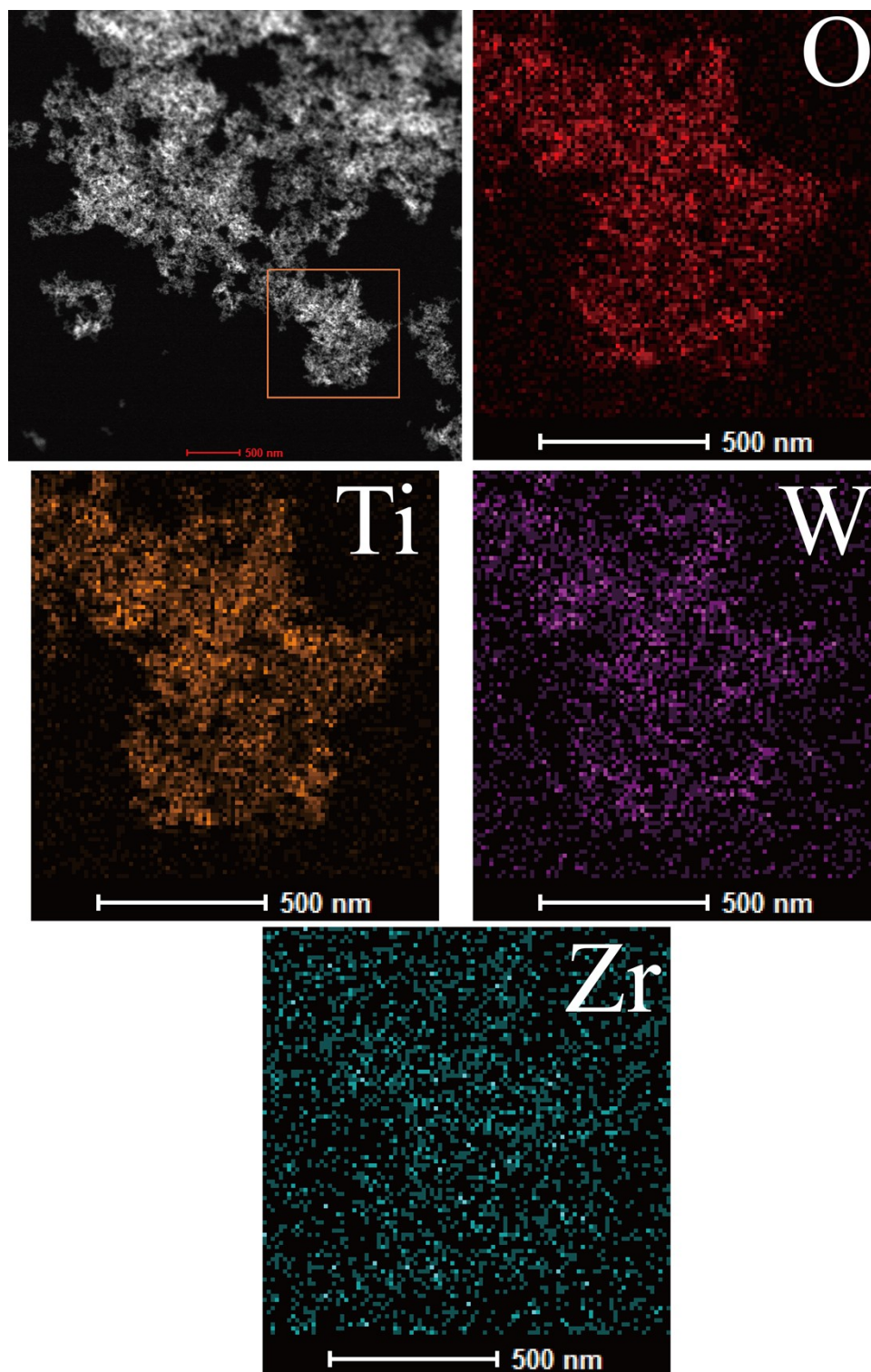


Fig.S3 Element mapping of 5C-WZ/T catalyst.

Figure S4

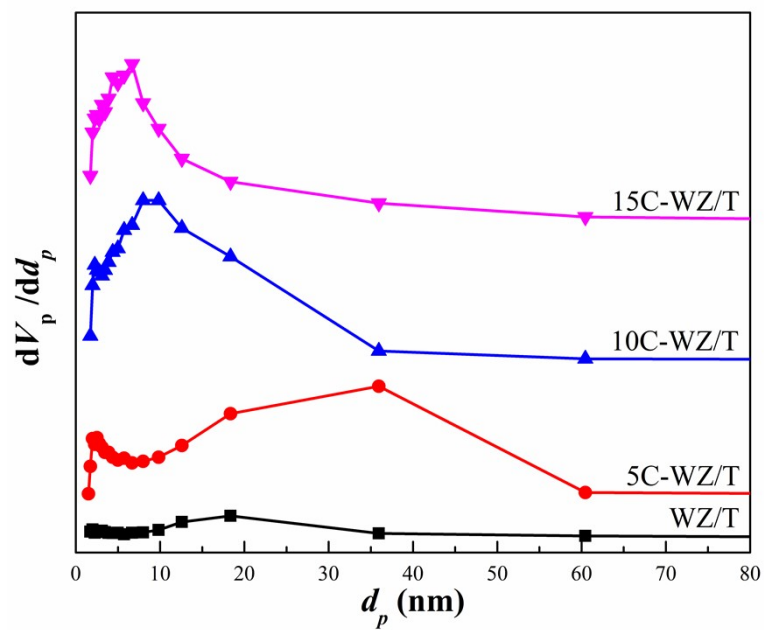
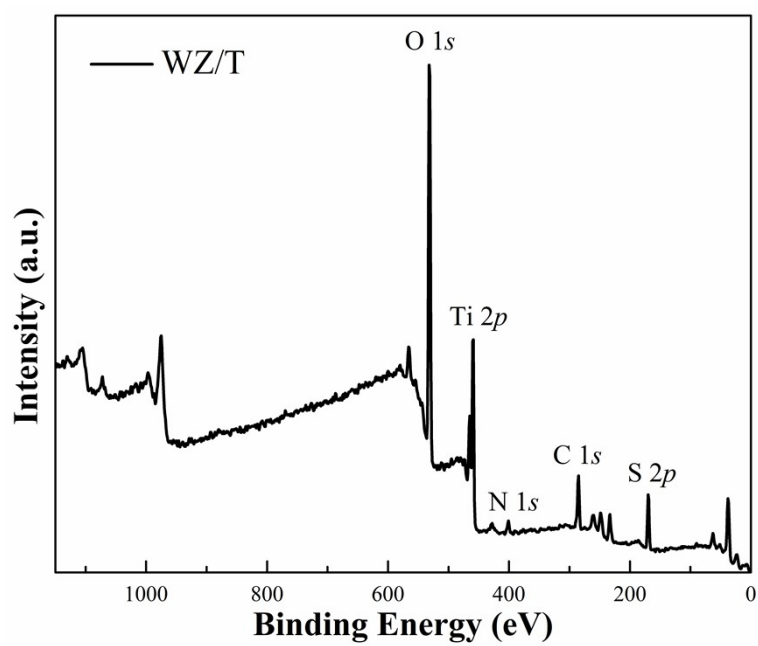


Fig.S4 Pore size distribution of different catalysts.

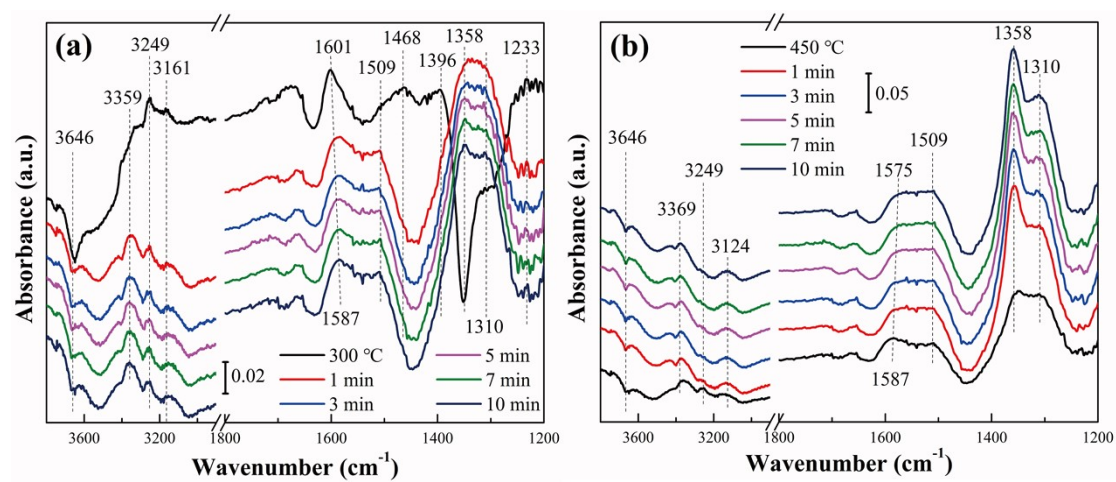
**Figure S5**



**Fig.S5** SurveyXPS high-resolution scans spectra of WZ/T catalyst.



**Figure S6**



**Fig.S6** *In-situ* diffuse reflection infrared spectrum of 5C-WZ/T catalyst: (a)  $\text{NO} + \text{O}_2$  reacted with  $\text{NH}_3$  at 450 °C, (d)  $\text{NO} + \text{O}_2$  reacted with  $\text{NH}_3$  at 600 °C.