

Selective Ion Transport through Three-Dimensionally Interconnected Nanopores of Quaternized Block Copolymer Membranes for Energy Harvesting Application

Ja-Min Koo^{†a}, Chul Ho Park^{†b}, Seungmin Yoo^c, Gyeong Won Lee^d, Seung Yun Yang^d, Joo Hyun Kim^a,
and Seong Il Yoo^{a*}

^aDepartment of Polymer Engineering, Pukyong National University, Busan, 48547, Republic of Korea
Email: siyoo@pknu.ac.kr

^b Jeju Global Research Center (JGRC), Korea Institute of Energy Research (KIER), Jeju Specific Self-Governing Province, 63357, Republic of Korea

^c Department of Chemical Engineering, Ulsan College, Ulsan 44610, Republic of Korea

^d Department of Biomaterials Science (BK21 Four Program), College of Natural Resources & Life Science, Pusan National University, Miryang 50463, Republic of Korea

[†]These authors contributed equally to this work.

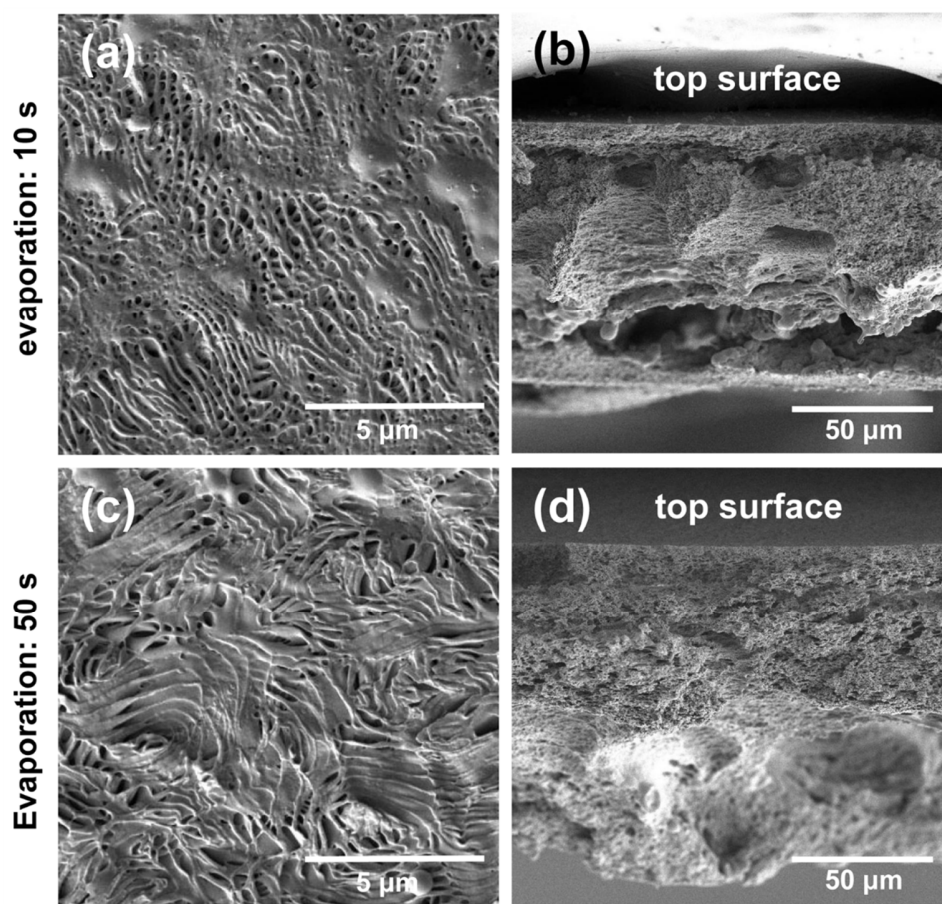


Figure S1. Plan-view (a, c) and cross-sectional (b, d) FE-SEM images of PS-P2VP membranes prepared by NIPS method with different evaporation time at room temperature. (a, b) 10 s; (c, d) 50 s.

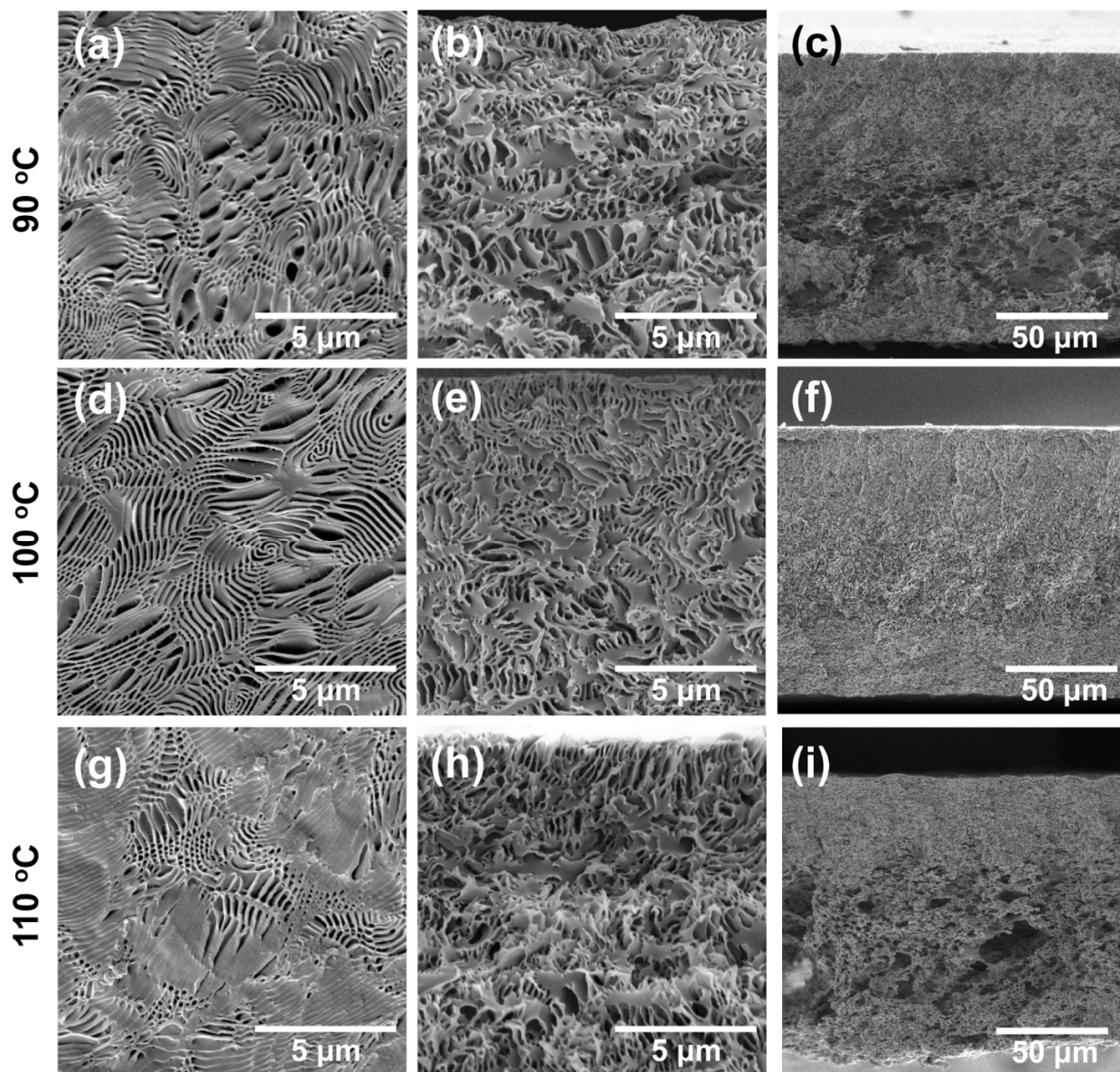


Figure S2. Plan-view and cross-sectional FE-SEM images of PS-P2VP membranes prepared by NIPS method with different evaporation temperature for 20 s. (a - c) 90 °C; (d - f) 100 °C; (g - i) 110 °C.

To confirm the interconnectivity of nanopores in the PS-P2VP membrane, permeation tests with a deionized (DI) water were performed at different working pressure in a stirred cell module (Amicon 8010, Millipore). As shown in Figure S3, the PS-P2VP membrane exhibited a water flux of $17 \text{ L m}^{-2} \text{ h}^{-1}$ at a pressure of 0.1 bar and a linear increase in water flux with working pressure, indicating good dimensional stability of the PS-P2VP membrane.

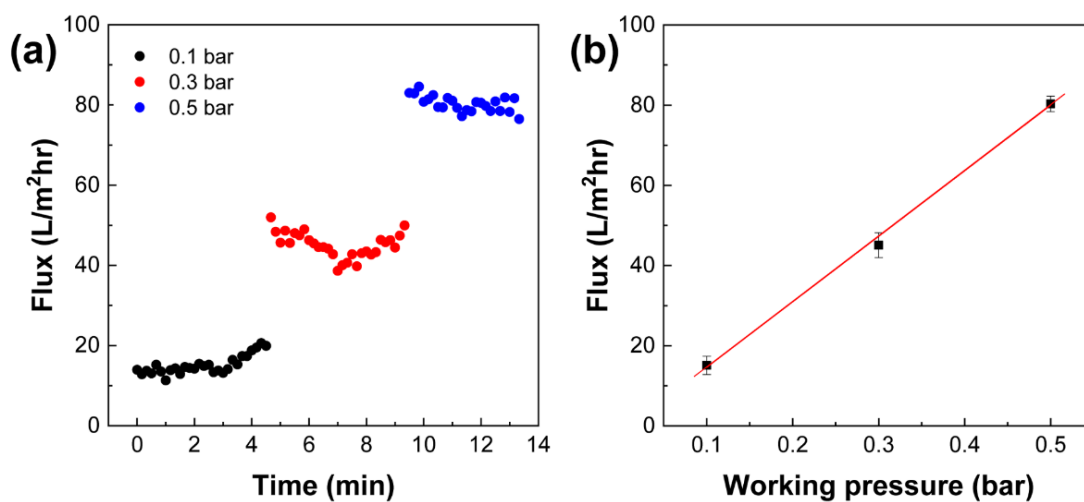


Figure S3. Flux data of deionized water using the PS-P2VP membrane from the evaporation condition of 100 °C and 20 s. (a) Flux change with increasing working pressure in permeability test and (b) plot of water flux as a function of working pressure.

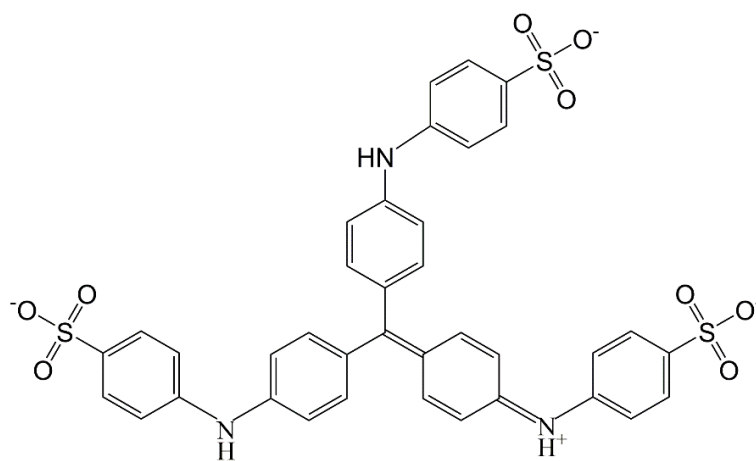


Figure S4. Molecular structure of methyl blue (CAS number: 28983-56-4).

Calculation of ion transport number

To calculate ion transport number, the diffusion potential (E_{diff}), which is generated by ionic diffusion across the membrane, needs to be determined by $E_{\text{diff}} = V_{\text{OC}} - E_{\text{redox}}$.^{1,2} In this equation, the redox potential (E_{redox}) is arose from the different potential drops at the electrode-solution interfaces in the two KCl reservoirs. We measured E_{redox} (18.5 mV) by inserting Ag/AgCl electrodes in the two KCl solutions (0.01M and 1M) that were connected by a salt bridge. From the diffusion potential, ion transport number (t) can be further determined by^{1,2}

$$t = \frac{1}{2} \left[1 + \frac{F}{RT} \frac{E_{\text{diff}}}{\ln(a_{\text{H}}/a_{\text{L}})} \right] \dots\dots\dots (1)$$

where F is the Faraday constant, R is the ideal gas constant, T is the temperature, and a_{H} (or a_{L}) is the activity of KCl in the solution at high (or low) concentration. From the equation (1), ion transport numbers were evaluated as 0.43, 0.57, 0.87, 0.87, and 0.68 for PS-QP2VP membranes with 0, 6, 12, 18, 24 h of quaternization, respectively.

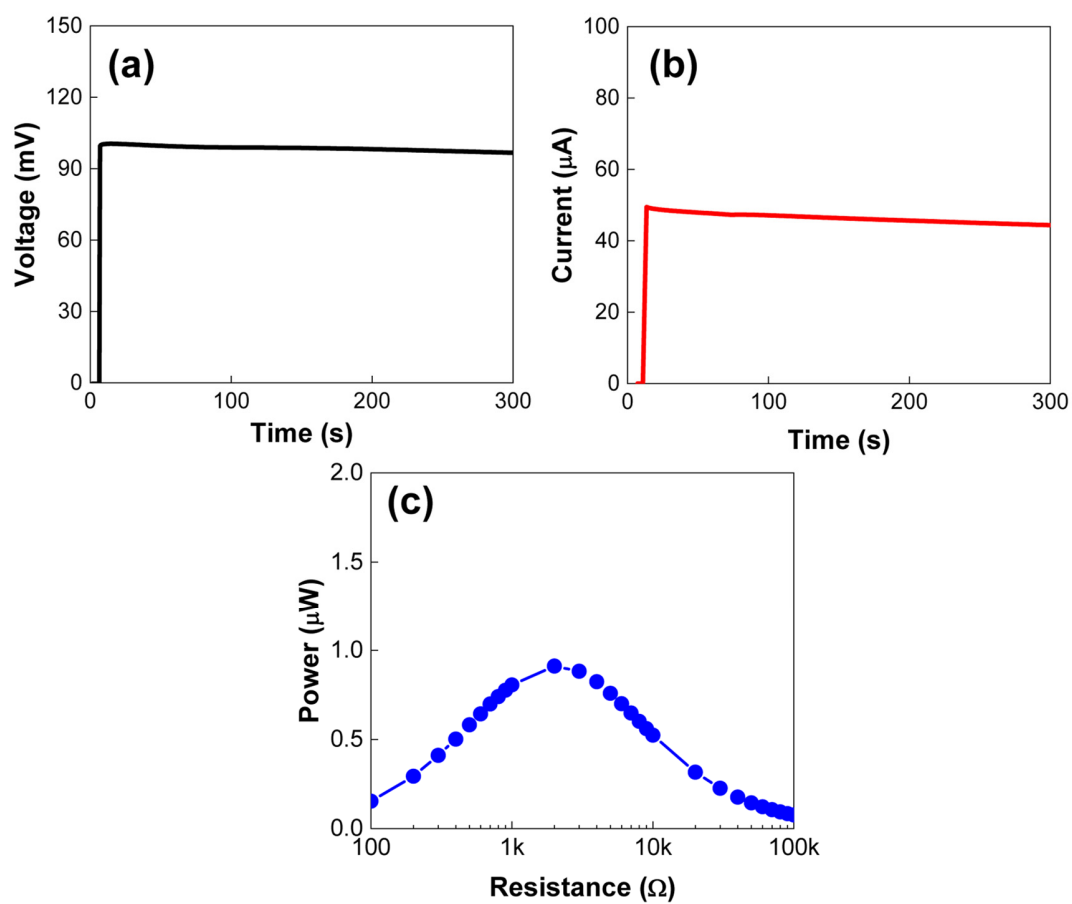


Figure S5. (a) Open-circuit voltage, (b) short-circuit current and (c) output power of concentration-gradient cells with commercial anionic-exchange membrane (Fujifilm) under the same experimentals with Figure 3 (main text).

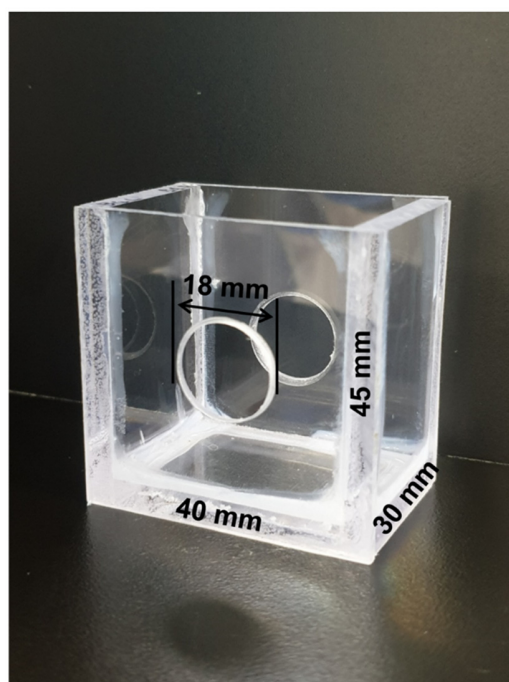


Figure S6. Photograph of polycarbonate containers utilized for the connection of concentration-gradient cells.

References

- 1 F. Yan, L. Yao, K. Chen, Q. Yang, B. Su, *J. Mater. Chem. A*, 2019, **7**, 2385.
- 2 D.-K. Kim, C. Duan, Y.-F. Chen, A. Majumdar, *Microfluid. Nanofluid.*, 2010, **9**, 1215.