

Ce_{1-x}Sr_xO_{2-δ} solid solution support cobalt-based catalysts for hydrogen production via auto-thermal reforming of acetic acid

Chenghong Shu^{a,d,#}, Chenyu Ding^{a,#}, Yan Liu^a, Wenjing Sun^c, Jia Huang^a, Fuxia Liao^a, Lihong Huang^{a,d,*}, Ning Wang^{b,*}

^a Department of Chemical and Pharmaceutical Engineering, Chengdu University of Technology, Chengdu 610059, China

^b Faculty of Environment and Life, Beijing University of Technology, Beijing 100124, China

^c China-America Cancer Research Institute, Key Laboratory for Medical Molecular Diagnostics of Guangdong Province, Guangdong Medical University, Dongguan, Guangdong 523808, China

^d State Key Laboratory of Geohazard Prevention and Geoenvironment Protection, Chengdu University of Technology, Chengdu 610059, China

These authors contributed equally to this work.

* Corresponding author at: Department of Chemical Engineering, Chengdu University of Technology, Chengdu 610059, China

E-mail address: ning.wang.1@bjut.edu.cn (N. Wang), huanglihong06@cdut.cn (L. Huang)

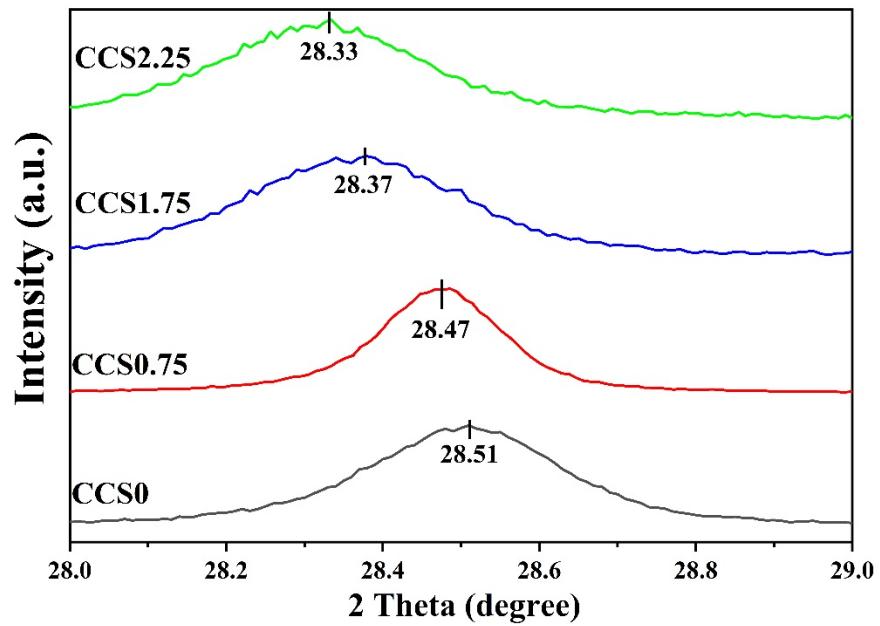


Fig. S1. Enlarged XRD patterns from 28° to 29°

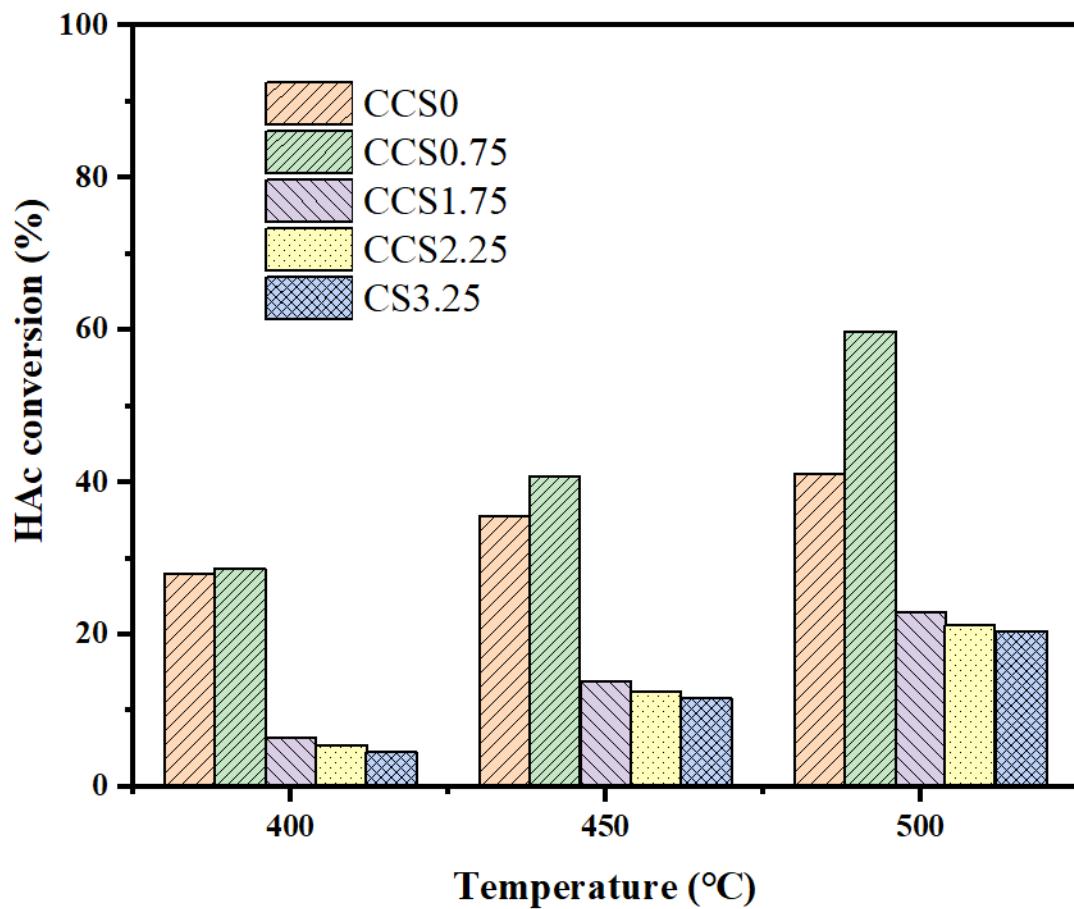


Fig. S2. Effect of temperature on the HAc conversion of the CCS_x catalysts at $\text{GHSV} = 50000 \text{ mL}\cdot\text{g}_{\text{catal}}^{-1}\cdot\text{h}^{-1}$ in ATR

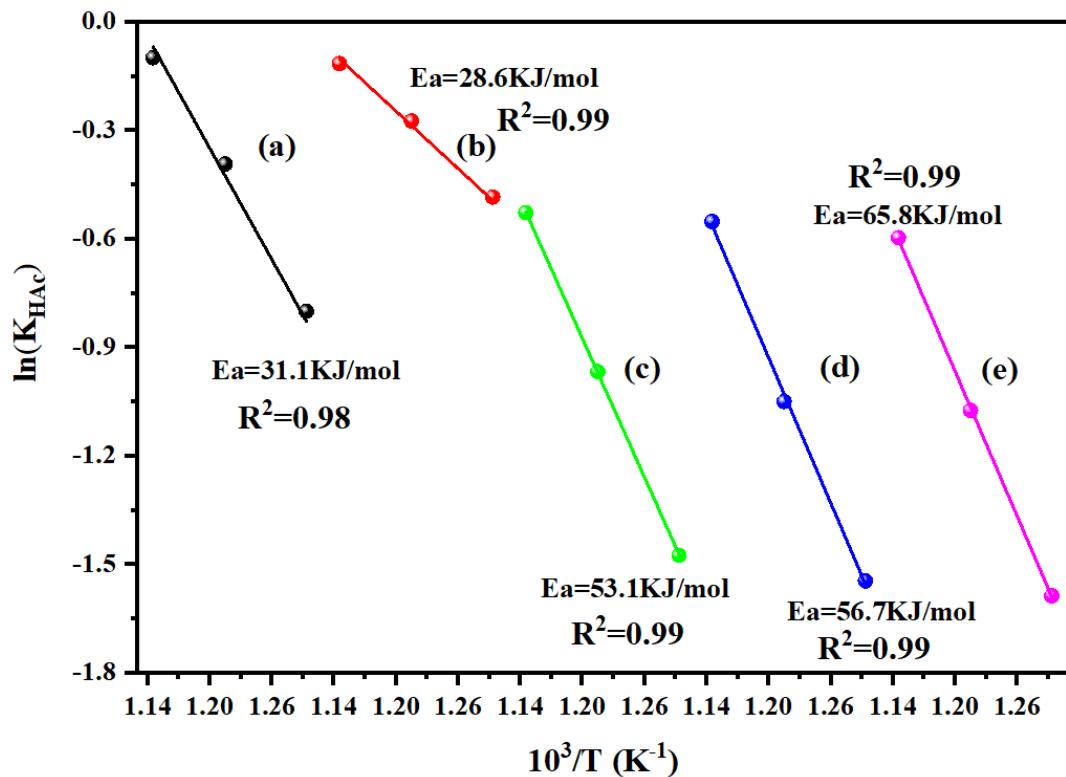


Fig. S3. Arrhenius plots of CCS_x catalyst: (a) CCS0, (b) CCS0.75, (c) CCS1.75, (d) CCS2.25 (e) CS3.25

Table S1. Cell parameters of CCS_x catalysts.

Catalysts	Main Phase composition	Space group	Cell parameters (Å)		
			a	b	c
CCS0	CeO ₂	Fm-3m	5.411	5.411	5.411
CCS0.75	Ce _{1-x} Sr _x O _{2-δ}	Fm-3m	5.423	5.423	5.423
CCS1.75	Ce _{1-x} Sr _x O _{2-δ}	Fm-3m	5.430	5.430	5.430
CCS2.25	Ce _{1-x} Sr _x O _{2-δ}	Fm-3m	5.425	5.425	5.425
CS3.25	SrCO ₃	Pm-cn	5.107	8.421	6.028

Table S2. Hydrogen uptake and Co⁰ reducibility from H₂-TPR

Catalysts	Hydrogen consumption (mmol/g)		Co ⁰
	Peak 1	Peak 2	Reducibility (%)
CCS0	0.93	1.39	10.5
CCS0.75	1.03	2.01	15.4
CCS1.75	0.45	0.77	8.5
CCS2.25	0.37	0.35	7.2
CS3.25	0.11	0.23	4.3

Table S3. The Co⁰ dispersion, hydrogen production rate, TOF-H₂ and E_a of CCS_x catalysts

Catalysts	Co ⁰ dispersion ^a	Hydrogen production rate ($\mu\text{mol}\cdot\text{H}_2\cdot\text{s}^{-1}\cdot\text{gcat}^{-1}$) ^b	TOF of H ₂ (10^{-2} s^{-1}) ^c	Activation energy (E _a) kJ*mol ⁻¹
CCS0	0.066	7.57	12.8	31.1
CCS0.75	0.074	9.77	14.8	28.6
CCS1.75	0.046	0.58	1.5	53.1
CCS2.25	0.027	0.33	1.4	56.7
CS3.25	0.015	0.06	0.5	65.8

^a Obtained from H₂-TPD by assuming H_{ad}/Co⁰_{surf}=1^b Obtained from Eq. (14)^c Obtained from Eq. (15)

Table S4. The distances between Ce/Sr atom and its nearest O atoms.

	Ce-O1	Ce-O2	Ce-O3	Ce-O4	Ce-O5	Ce-O6
d(Å)	2.35	2.37	2.37	2.37	2.37	2.37
	Sr-O1	Sr-O2	Sr-O3	Sr-O4	Sr-O5	Sr-O6
d(Å)	2.59	2.57	2.60	2.58	2.60	2.57

Table S5. The calculated E_{vac} (in eV) for the $Ce_{1-x}Sr_xO_{2-\delta}$ (111) surface with one and two O vacancies. For the CeO_2 (111) surface, the surface and subsurface O vacancy formation energies were 2.58 and 2.50 eV, respectively. $V_{OI}-V_{OIII}$ were the surface vacancies and $V_{OIV}-V_{OV}$ were the subsurface vacancies for the $Ce_{1-x}Sr_xO_{2-\delta}$ (111) surface; $V_{OIV-1}-V_{OIV-2}$ were the surface vacancies and $V_{OIV-3}-V_{OIV-4}$ were the subsurface vacancies.

$Ce_{1-x}Sr_xO_{2-\delta}$ ($Ce_{47}Sr_1O_{95}$)	V_{OI}	V_{OII}	$V_{OIII=OV}$	V_{OIV}	V_{OVI}
E_{vac} (eV)	-0.705	-0.704	-0.776	-0.804	-0.778
$Ce_{1-x}Sr_xO_{2-\delta}$ ($Ce_{47}Sr_1O_{94}$)	V_{OIV-1}	V_{OIV-2}	V_{OIV-3}	V_{OIV-4}	
E_{vac} (eV)	1.22	0.92	1.05	1.96	

^a The unique structure of Sr-CeO₂ with one O vacancy

^b The unique structure of Sr-CeO₂ with two O vacancy (based on O_{IV} structure by removing of the second structurally unique oxygen atoms)