

Supporting Information

Enhancing the anisole hydrodeoxygenation activity over Ni/Nb₂O_{5-x} by tuning the oxophilicity of the support

Hadi Ali^{1,2,3}, Tom Vandevyvere^{2,4}, Jeroen Lauwaert⁴, Sushil Kumar Kansal⁵, Maarten K. Sabbe^{2,4}, Shunmugavel Saravanamurugan^{1*}, Joris W. Thybaut^{2*}

¹Laboratory of bioproduct Chemistry, Center of Innovative and Applied Bioprocessing, Sector 81 (knowledge City), Mohali-140306, Punjab, India, Email:saravana@ciab.res.in

²Laboratory for Chemical Technology (LCT), Ghent University, Technologiepark 125, 9052, Ghent, Belgium. Email:joris.thybaut@ugent.be

³Energy Research Centre, Panjab University, Chandigarh 160014, India

⁴Industrial Catalysis and Adsorption Technology (INCAT), Valentin Vaerwyckweg 1, 9000, Ghent, Belgium

⁵Department of Chemical Engineering and Technology, Panjab University, Chandigarh 160014, India

Table S1. Structural properties of different Ni/Nb₂O₅-based catalysts

Catalyst	H ₂ adsorption (μmol/g) ^a				H ₂ -consumption (μmol/g) ^b
	<200 °C	200-300 °C	>300 °C	Total	
Ni/Nb ₂ O ₅ -C	3.6 (13%)	3.4 (12%)	20.3 (75%)	27.2	423
Ni/Nb ₂ O ₅ -P	1.8 (7%)	1.0 (4%)	24.2 (89%)	27.0	390
Ni/Nb ₂ O ₅ -HT	0.8 (3%)	4.2 (14%)	25.0 (83%)	30.0	442
Ni/Nb ₂ O ₅ -H	0.7 (3%)	5.5 (24%)	16.7 (73%)	23.0	452

^a Amount of H₂ adsorption derived from H₂-TPD, ^b H₂ consumption derived from H₂-TPR

Table S2. XPS results of the Nb 3d_{5/2} and O 1s of Ni/Nb₂O₅ catalysts

Catalysts ^a	Nb 3d _{5/2}		O 1s
	Nb ⁴⁺ /Nb ⁵⁺	Nb ⁴⁺ /Nb ⁴⁺⁺ Nb ⁵⁺	O _β / O _{total}
Ni/Nb ₂ O ₅ -C (Reduced)	0.92	0.4798	0.24
Ni/Nb ₂ O ₅ -H (Reduced)	1.01	0.504	0.35

^a Both the catalysts were reduced ex-situ with formier gas (5% H₂ in N₂) at 400 °C for 1 h prior to the XPS analysis.

Table S3. Catalytic activity of Ni/Nb₂O₅-H and previous studies related to Ni-based catalysts for HDO of anisole

Entry	Catalysts	Reaction conditions	Conv. (%)	Selec. DeO (%)	R _{HDO} ^a (mmol. g ⁻¹ _{Ni} . h ⁻¹)*10 ²	Reference
1	3wt% Ni/Nb₂O₅	240 °C, 20bar H₂, 1 h	90	91.0	5.45	This work
2	10wt% Ni/SiO ₂	300 °C, 50 bar H ₂ , 16 h	>99	80.4	0.23	[1]
3	10wt% Ni/Al ₂ O ₃	300 °C, 50 bar H ₂ , 16 h	>99	74	0.21	[1]
5	30wt% Ni/Al ₂ O ₃ -ZrO ₂	230 °C, 10 bar H ₂ , 3 h	100	77.6	0.97	[2]
6	10wt% Ni/SiO ₂	220 °C, 30 bar H ₂ , 4 h	>99	95	2.59	[3]
7	90wt% Ni/Nb ₂ O ₅	240 °C, 30bar H ₂ , 4h	>99	100	0.38	[4]
8	60wt% Ni 5wt%Cu 30wt%Si	320 °C, 60bar H ₂ , 2.5h	~85	100	2.59	[5]
9	5wt% Ni/TiO ₂ -ZrO ₂	300 °C, 40bar H ₂ , 4h	60	~87	5.19	[6]
10	90wt%Ni /SiO ₂	280 °C, 60bar H ₂ , 0.75h	100	40	0.12	[7]
11	16wt%Ni-2wt% Cu/Al ₂ O ₃	300°C, 10bar H ₂ , continuous-flow study	78.6	95.9	-	[8]
12	20wt%Ni/TiO ₂ 20wt%Ni/SBA-15	310°C, 15bar H ₂ , WHSV=20.4 ^{-h}	100	~90%	-	[9]
13	10wt%Ni/SBA-15	280°C, 35bar H ₂ , 6h	100	100	2.98	[10]
14	5wt%Ni/HSZ	200°C, 68bar H ₂ , 2.3 h	98	84	3.68	[11]

^aR_{HDO} = mol of the deoxygenated product (cyclohexane)/mass of Ni present in the catalyst * time(h)

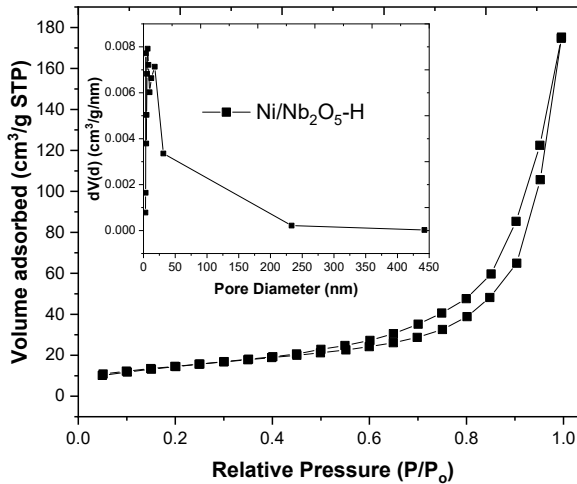
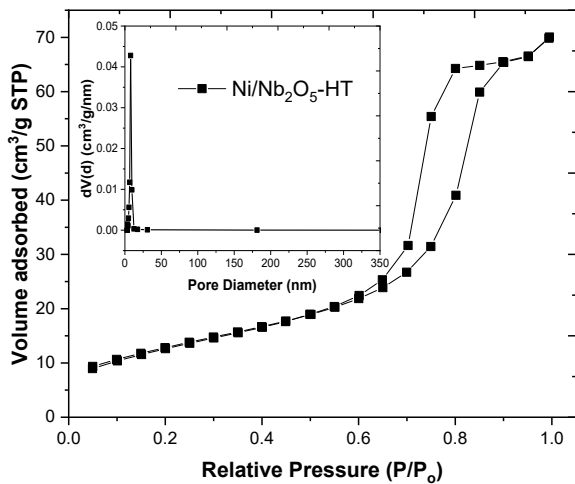
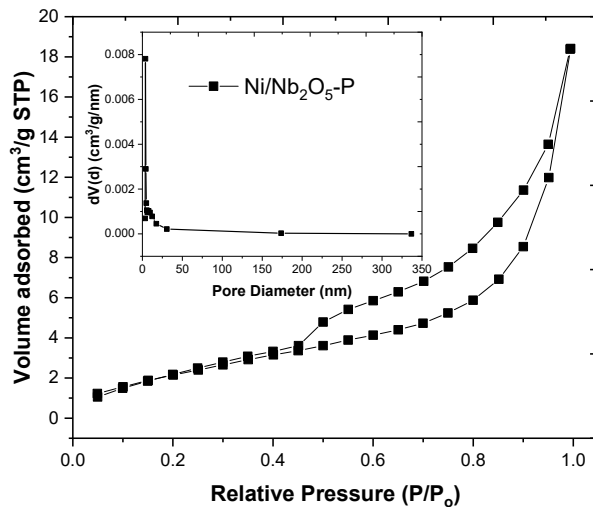
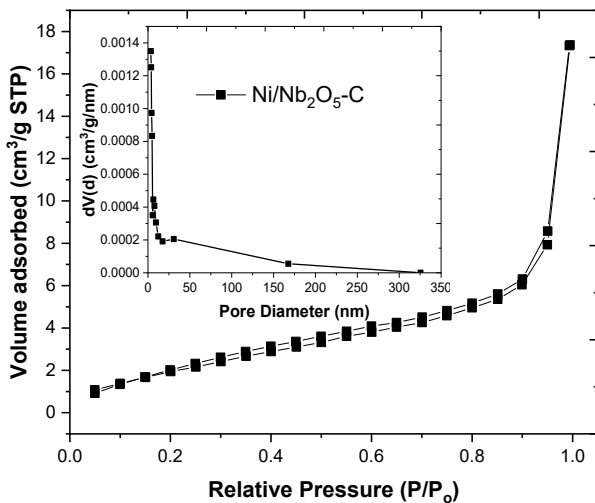


Figure S1. Physisorption isotherm of various Ni/Nb₂O₅ catalysts

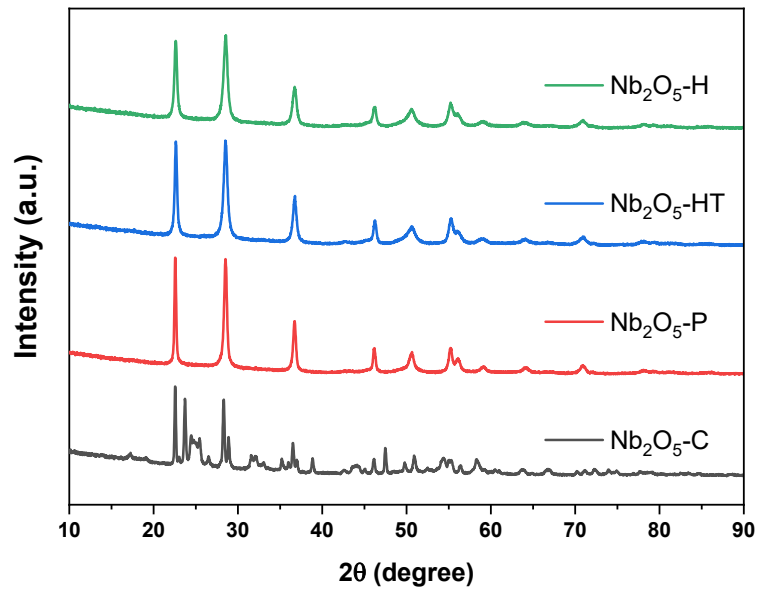


Figure S2. XRD patterns of Nb₂O₅ support

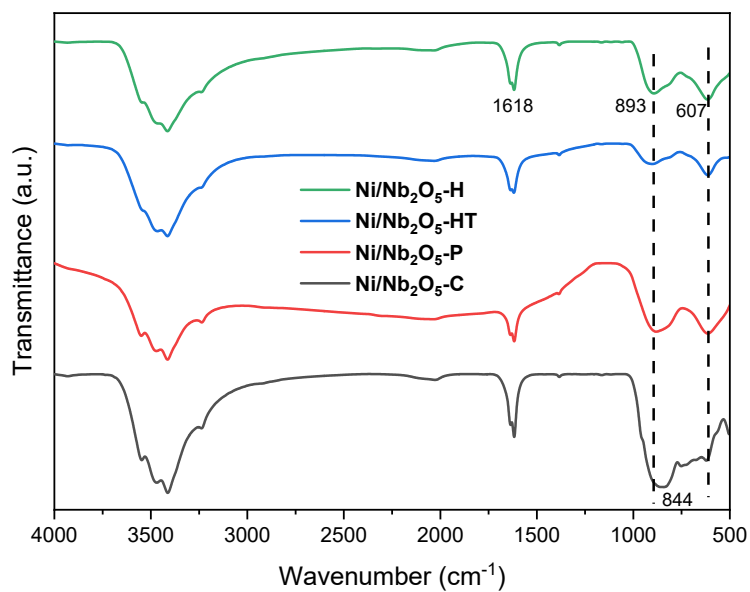


Figure S3. FTIR spectra of Ni/Nb₂O₅ catalysts

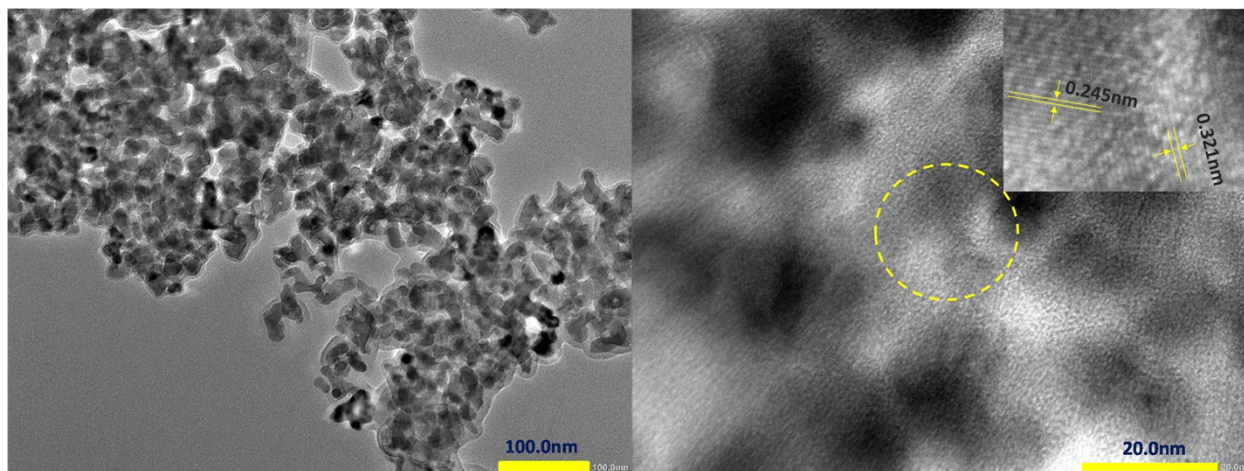


Figure S4. TEM (left) and HR-TEM (right) images of Ni/Nb₂O₅-H catalyst

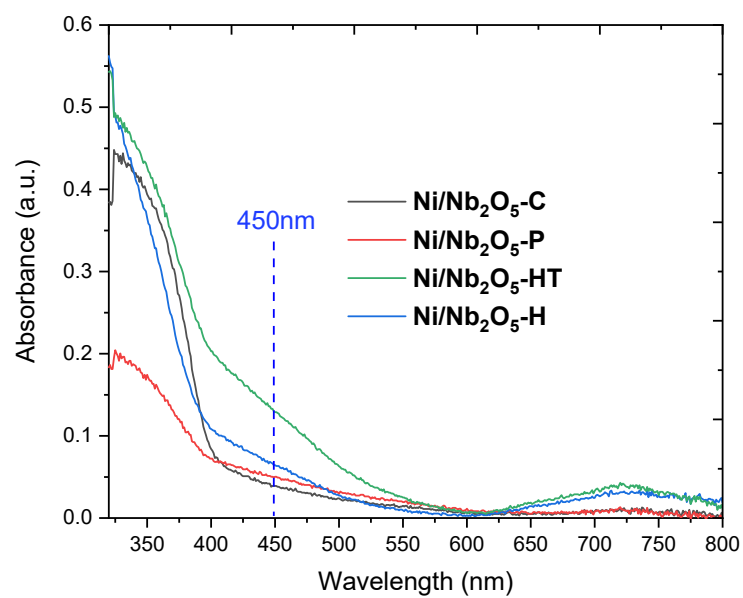


Figure S5. DRS-UV-Vis absorbance spectra of Ni/Nb₂O₅ catalysts

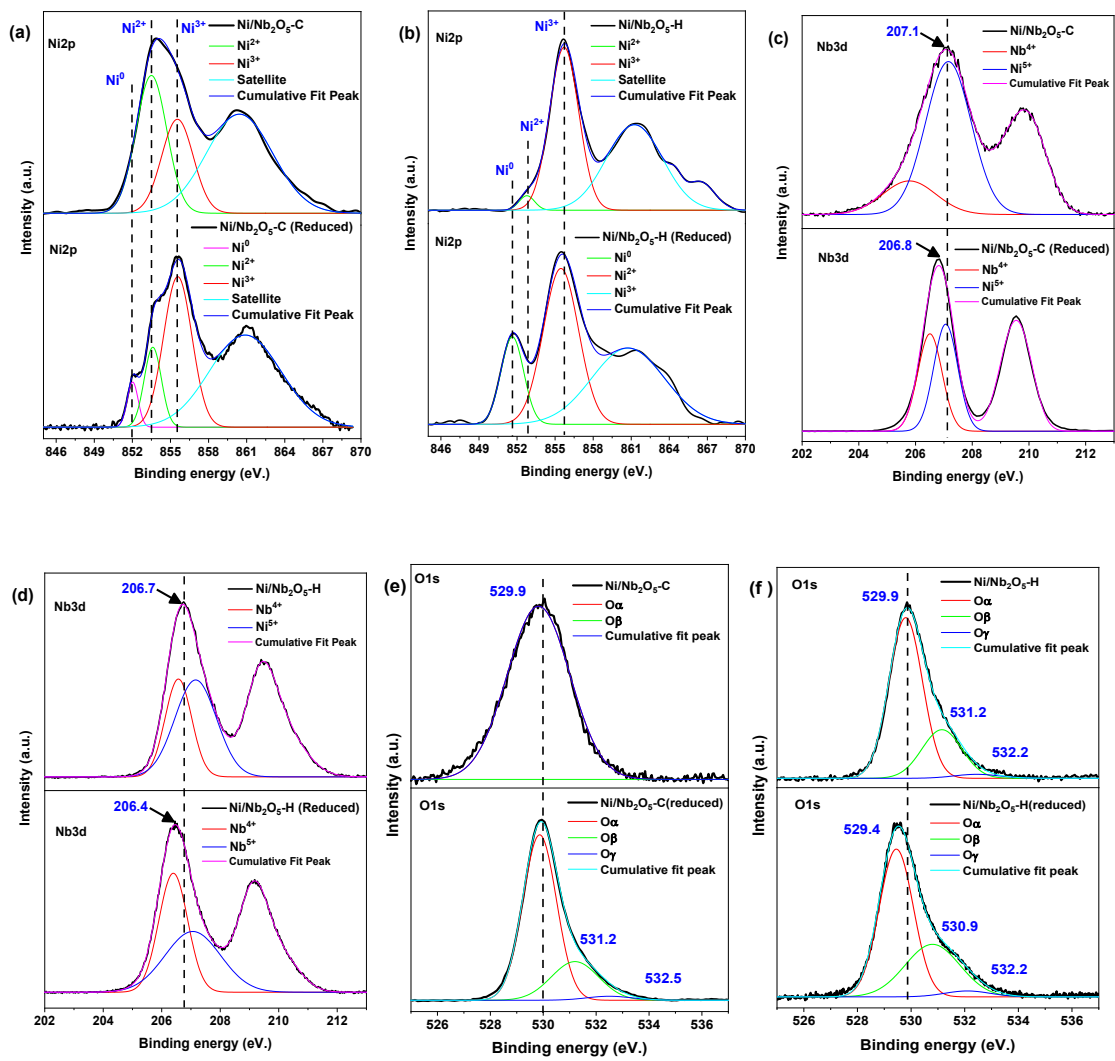


Figure S6. XPS spectra of (a) and (b) for Ni2p, (c) and (d) for Nb3d, (e) and (f) for O1s of Ni/Nb₂O₅-C and Ni/Nb₂O₅-H before and after reduction

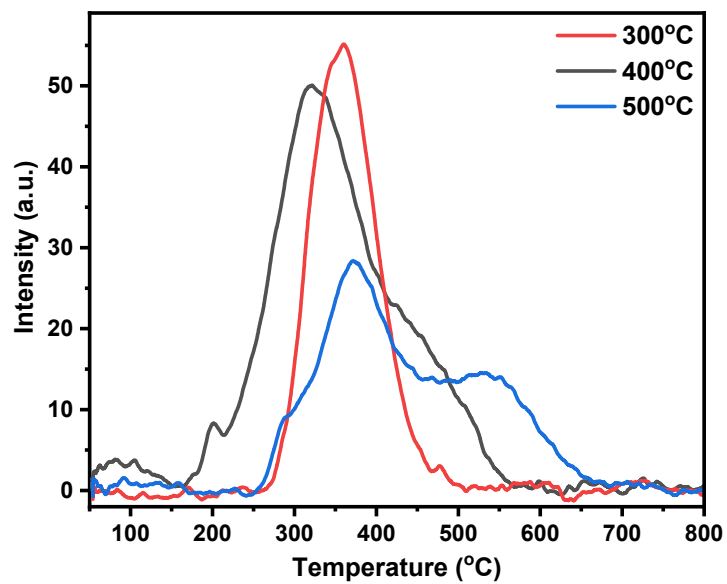


Figure S7. H₂-TPD of Ni/Nb₂O₅-H catalysts at a different reduction temperature

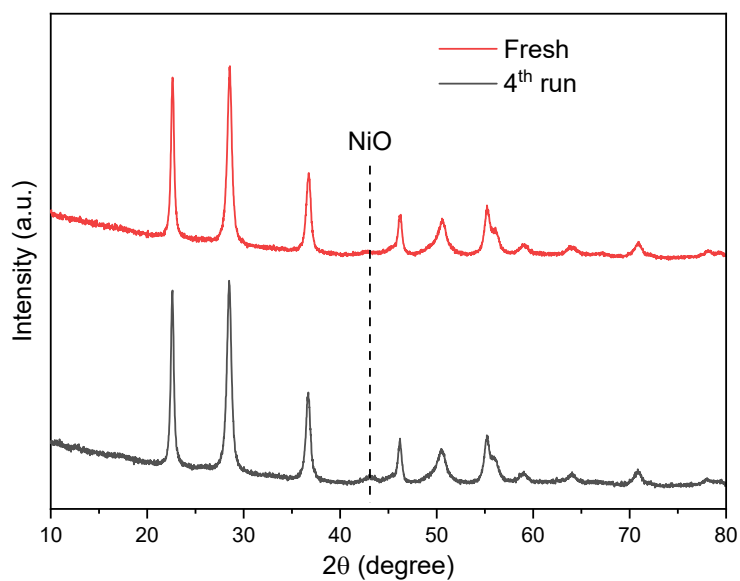


Figure S8. XRD pattern of fresh and spent Ni/Nb₂O₅-H

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