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Supplemental Information



Fig. S1. EDX spectra for the SCR catalyst.

Table S1. Experimental conditions TPSR measurements.

	Condi.	Step 1	Step 2	Step 3	Step 4	Step 5	Step 6	Step 7
GHSV / h ⁻¹	40000	40000	40000	40000	40000	40000	40000	40000
H ₂ O / vol.%	8	8	8	8	8	8	8	8
CO_2 / vol.%	0	0	6	6	6	6	0	0
O ₂ / vol.%	10	0	10	10	10	10	0	0
NH ₃ / ppm	0	750	750	750	750	750	0	0
NO _x / ppm	500	0	500	500	500	500	0	0
CH ₂ O / ppm	0	0	Var. 0, 100	Var. 0, 100	Var. 0, 100	Var. 0, 100	0	0
CO / ppm	0	0	Var. 0, 60	Var. 0, 60	Var. 0, 60	Var. 0, 60	0	0
DME / ppm	0	0	Var. 0, 12	Var. 0, 12	Var. 0, 12	Var. 0, 12	0	0
N ₂	Rest	Rest	Rest	Rest	Rest	Rest	Rest	Rest
Temp./ °C	550	200	200	200-550	550	550-200	200	200-550

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Temp. Gradient / K/min	0	0	0	5	0	-5	0	5	

Table S2. Experimental conditions NH ₃ -TPD measurements.							
	Conditioning	Step 1	Step 2	Step 3			
GHSV / h ⁻¹	40000	40000	40000	40000			
H ₂ O / vol.%	8	8	8	8			
CO ₂ / vol.%	0	0	0	0			
O ₂ / vol.%	10	10	0	0			
NH₃ / ppm	0	300	0	0			
NO _x /ppm	500	0	0	0			
CH ₂ O / ppm	0	Var. 0, 100	0	0			
CO / ppm		Var. 0, 60	0	0			
DME / ppm		Var. 0, 12	0	0			
N ₂	Rest	Rest	Rest	Rest			
Temperature / °C	550	Var. 150, 200, 250, 300, 350	Var. 150, 200, 250, 300, 350	Var. 150-550, 200-550, 250-550, 300-550, 350-550			
Temp. Gradient / K/min	0	0	0	5			

Table 35. Experimental com		uesorption investiga	ition measuremen	15.		
	Conditioning	Step 1	Step 2	Step 3	Step 4	Step 5
GHSV / h ⁻¹	40000	40000	40000	40000	40000	40000
H ₂ O / vol.%	8	8	8	8	8	8
CO ₂ / vol.%	0	0	0	0	0	0
O ₂ / vol.%	10	0	0	0	0	0
NH₃ / ppm	0	750	0	0	0	0
NO _x /ppm	500	0	0	0	0	0
CH ₂ O / ppm	0	Var. 0, 100	0	0	0	0
CO / ppm		Var. 0, 60	0	0	0	0
DME / ppm		Var. 0, 12	0	0	0	0
N ₂	Rest	Rest	Rest	Rest	Rest	Rest
Temperature / °C	550	Var. 150, 200	Var. 150, 200	Var. 150-100, 200- 100	100	100-550
Temp. Gradient / K/min	0	0	0	-5	0	5

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Fig. S2. Schematic representation of a performed TPSR experiment with CH_2O dosing at SGTB. The temperature ramps at the beginning and at the end show the performed conditioning of the catalyst before and after the experiment.



Fig. S4. Schematic representation of a performed modified NH_3 -TPD experiment with CH_2O dosing at SGTB. The temperature ramps at the beginning and at the end show the performed conditioning of the catalyst before and after the experiment.



Fig. S3. Schematic representation of a performed NH_3 -TPD experiment with CH_2O dosing at SGTB. The temperature ramps at the beginning and at the end show the performed conditioning of the catalyst before and after the experiment.

Coverage of surface hydroxyl groups by formaldehyde

In order to perform in-situ Diffuse Reflectance Infrared Fourier Transform Spectroscopy (DRIFTS) measurements to study the formaldehyde adsorption on the catalyst surface, the commercial formaldehyde solution was added into water, and dosed into gas mixture. A small amount of methanol was present in commercial formaldehyde solution as the stabilizer, which cannot be avoided in the gas flow. By exposing the catalyst to an atmosphere with/without formaldehyde (CH₂O) under SCR conditions at 300 °C (with only NO₂ present), the results were depicted in Figure S5. The spectrum without CH₂O showed weak bands at 3336 and 3277 cm⁻¹, which are attributed to the stretching modes of NH₃, which is adsorbed to Brønsted acid sites (Al-OH-Si).^{1,2} The negative band at 3656 cm⁻ ¹ is related to vibration modes of Cu-OH groups, which are coordinated by NH₃. Besides this, a very weak signal with negative intensity at 3612 cm⁻¹ is attributed to OH groups on Brønsted acid sites, as it is partially coordinated by NH₃.³ When CH₂O was added, it adsorbs on the surface OH groups, leading the bands at 3336 and 3277 cm⁻¹ to lose intensity and this finding indicates that the presence of CH_2O promotes the NO_x conversion by NH₃, i.e. that NH₃ adsorption is less likely under these reaction conditions. Unfortunately, the signal at 3612 cm⁻ ¹ is not distinct enough to judge, whether the corresponding site undergoes a similar effect.

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In addition, one would expect a change of the signal at 3656 cm⁻ 1 to positive intensity when $\mathsf{CH}_2\mathsf{O}$ was added, as NH_3 is consumed under these reaction condition, i.e. presence of NO₂, which would be consistent with our observation on the signal intensity at 3336 cm⁻¹ and 3277 cm⁻¹. However, we found that the respective signal just gets less negative, which we attribute to that the presence of CH₂O partially cover the Cu-OH sites.

Even, with Methanol present as a stabilizer, no indications in the spectra are found for the presence of methanol⁴, the signal at 3647 cm⁻¹ has to stem from another species. Hence, for the band appearing at 3647 cm⁻¹, which has been observed by Xue et al.³ as well, we tentatively assign it to water species on the zeolite surface.³



Fig. S5. The DRIFTS result of the catalyst under the NO₂ SCR condition with/without the presence of CH₂O at 300 °C

Nitrate formation

The catalytic material was subjected to a pretreatment procedure involving exposure to NO and NO₂ at a temperature of 400 °C with a 10% oxygen concentration. Subsequently, the catalyst was subjected to an exposure to 800 ppm of NH₃ in a nitrogen environment at 200 °C for 30 minutes before being switched to an atmosphere containing formaldehyde under Selective Catalytic Reduction (SCR) conditions. The accompanying Figure S6 presents the results of DRIFTS analysis carried out at temperatures ranging from 200 °C to 400 °C. Upon exposure to an atmosphere containing only NH₃, two distinct bands were observed in the spectra, with the primary band at 1444 cm⁻¹ attributed to the presence of NH₄⁺ species resulting from NH₃ adsorption onto Brønsted acid sites, and a weaker band at 1618 cm⁻¹ assigned to molecularly adsorbed NH₃ on Lewis acid sites.⁵ Upon introduction of the SCR atmosphere containing formaldehyde, additional spectral bands were identified, including one at 1626 cm⁻¹ commonly attributed to surface-bridging nitrates based on aluminum sites.5



200 °C

Ľ.

350 °C



Fig. S6. The DRIFTS result of the catalyst under the NH₃ SCR condition with the presence of CH₂O at 200 °C to 400 °C

Table S4. DRIFTS	Assignment.	
IR-Band	Assignment	References
1670 cm ⁻¹	Nitrites, NO ₂ -	6
1626 cm ⁻¹	Bridging nitrates on Al	7–9
1617-	NH ₃ coordinated on Lewis acid site	10
1621 cm ⁻¹		
1576 cm ⁻¹	Monodentate nitrates on Cu	8
1559 cm ⁻¹	Monodentates nitrate	11,12
1546-	Monodentates nitrate	13,14
1539 cm ⁻¹		
1507 cm ⁻¹	Nitrites, NO ₂ -	8
1489 cm ⁻¹	NH ₄ NO ₃	7
1455 cm ⁻¹	NH4 ⁺ on Brønsted acid	7
1457 cm ⁻¹	Nitrite	13
1445 cm ⁻¹	NH4 ⁺ from NH4NO3	7

Table S5. DRIFTS Assignment.

HCN formation

The accompanying figure displays the DRIFTS results for the investigation of the effect of CH_2O and the NO_2/NO_x ratio on SCR conditions at 200 °C. The presence of CH_2O and a NO_2/NO_x ratio of 0% is indicated by the C-H vibration bands at 2886 cm⁻¹ and 2955 cm⁻¹, which are assigned to HMT according to previous studies.^{15,16} This observation suggests the formation of HMT on the surface. Additionally, the IR band at 1313 cm⁻¹ suggests the presence of formamide, which can undergo dehydration to form HCN.



Fig. S7. DRIFTS spectra at 200 °C between 3800 and 600 cm⁻¹ after dosing NO, O_2 , H_2O and, in the lower measurement, additional CH₂O being dosed over the investigated SCR catalysts with preadsorbed NH₃ at 200 °C. Before preadsorbing NH₃, the catalyst was pretreated with NO and NO₂ at 400 °C with 10% O₂.



Fig. S8. DRIFTS spectra at 200 °C between 1700 and 950 cm⁻¹ after dosing NO, O_2 , H_2O and, in the lower measurement, additional CH₂O being dosed over the investigated SCR catalysts with preadsorbed NH₃ at 200 °C. Before preadsorbing NH₃, the catalyst was pretreated with NO and NO₂ at 400 °C with 10% O₂

Assignment	References
v(CH ₂) stretch	15,16
δ(C–H)	16,17
C=O	18
0C0	19
$v(CH_2)$ scissor (HMT)	15,16
$v(CH_2)$ wag (HMT)	15,16
CN	18
v(C-N)	17
v(CN) stretch (HMT)	15
	Assignment $v(CH_2)$ stretch $\delta(C-H)$ $C=O$ OCO $v(CH_2)$ scissor (HMT) $v(CH_2)$ wag (HMT) CN $v(C-N)$ $v(CN)$ stretch (HMT)

H₂O and formaldehyde influence under NO₂ SCR conditions

The TPSR experiments with and without CH₂O, described in the original draft, were repeated accordingly, but now with the absence of H₂O vapor, fed into the gas stream. Figure S9 displays the NO_x conversion efficiency of the NH₃ SCR with a NO_2 / NO_x ratio of 100% under the presence and absence of H₂O and CH_2O . The characteristic increase of NO_x conversion efficiency at low temperatures with CH₂O can be observed with and without H₂O added during the experiment. This shows that even without H₂O, no NH₄NO₃ was formed from the reaction of NH₃ and NO₂ and no deactivation of the catalyst occurs. At high temperatures of T > 370 °C a significant promoting effect of H_2O can be observed, while at temperatures of T < 320 °C a lesser deactivation effect of NH₄NO₃ occurred. Additionally, the overall selectivity to N₂O increased in the absence of H₂O, for both experiments with and without CH₂O. Displayed in Figure S10, with the absence of H₂O an increased N₂O peak from 108 ppm to 160 ppm can be seen for the experiment without CH_2O . In the presence of CH_2O no peak is detected, but the N_2O concentration is elevated with H₂O. These results go in line with the results, described by Han et al.²⁰, where H₂O hinders the NH₄NO₃ formation and increases the selectivity for decomposition to NO₂ instead of N₂O.



Fig. S9. NO_x conversion efficiency in % versus inlet temperature in °C for the investigated Cu-CHA SCR catalyst in the presence (100 ppm CH₂O) and the absence of formaldehyde and in the presence (8% H₂O) and the absence of H₂O vapor. The dotted line refers to the curves without formaldehyde; red: without H₂O vapor; blue: with H₂O vapor



Fig. S10. N₂O concentration versus inlet temperature in °C for the investigated Cu-CHA SCR catalyst in the presence (100 ppm CH₂O) and the absence of formaldehyde and in the presence (8% H₂O) and the absence of H₂O vapor. The dotted line refers to the curves without formaldehyde; red: without H₂O vapor; blue: with H₂O vapor

References

- 1 Z. Chen, C. Bian, Y. Guo, L. Pang and T. Li, Efficient Strategy to Regenerate Phosphorus-Poisoned Cu-SSZ-13 Catalysts for the NH 3 -SCR of NO x : The Deactivation and Promotion Mechanism of Phosphorus, *ACS Catal.*, 2021, **11**, 12963–12976.
- 2 W. Hu, U. Iacobone, F. Gramigni, Y. Zhang, X. Wang, S. Liu, C. Zheng, I. Nova, X. Gao and E. Tronconi, Unraveling the Hydrolysis of Z 2 Cu 2+ to ZCu 2+ (OH) and Its Consequences for the Low-Temperature Selective Catalytic Reduction of NO on Cu-CHA Catalysts, ACS Catal., 2021, **11**, 11616–11625.
- 3 H. Xue, X. Guo, T. Meng, Q. Guo, D. Mao and S. Wang, Cu-ZSM-5 Catalyst Impregnated with Mn–Co Oxide for the Selected

Catalytic Reduction of NO: Physicochemical Property–Catalytic Activity Relationship and In Situ DRIFTS Study for the Reaction Mechanism, *ACS Catal.*, 2021, **11**, 7702–7718.

- 4 G. Mirth, J. A. Lercher, M. W. Anderson and J. Klinowski, Adsorption complexes of methanol on zeolite ZSM-5, *Faraday Trans.*, 1990, **86**, 3039.
- 5 Di Wang, L. Zhang, K. Kamasamudram and W. S. Epling, In Situ-DRIFTS Study of Selective Catalytic Reduction of NO x by NH 3 over Cu-Exchanged SAPO-34, *ACS Catal.*, 2013, **3**, 871–881.
- 6 T. Zhang, F. Qiu, H. Chang, X. Li and J. Li, Identification of active sites and reaction mechanism on low-temperature SCR activity over Cu-SSZ-13 catalysts prepared by different methods, *Catal. Sci. Technol.*, 2016, **6**, 6294–6304.
- 7 D. Yao, B. Liu, F. Wu, Y. Li, X. Hu, W. Jin and X. Wang, N 2 O Formation Mechanism During Low-Temperature NH 3 -SCR over Cu-SSZ-13 Catalysts with Different Cu Loadings, *Ind. Eng. Chem. Res.*, 2021, **60**, 10083–10093.
- 8 Q. Liu, Z. Fu, L. Ma, H. Niu, C. Liu, J. Li and Z. Zhang, MnO -CeO2 supported on Cu-SSZ-13: A novel SCR catalyst in a wide temperature range, *Applied Catalysis A: General*, 2017, 547, 146–154.
- 9 L. Negahdar, N. E. Omori, M. G. Quesne, M. D. Frogley, F. Cacho-Nerin, W. Jones, S. W. T. Price, C. R. A. Catlow and A. M. Beale, Elucidating the Significance of Copper and Nitrate Speciation in Cu-SSZ-13 for N 2 O Formation during NH 3 -SCR, ACS Catal., 2021, 11, 13091–13101.
- 10 L. Xie, F. Liu, K. Liu, X. Shi and H. He, Inhibitory effect of NO2 on the selective catalytic reduction of NOx with NH3 over one-potsynthesized Cu–SSZ-13 catalyst, *Catal. Sci. Technol.*, 2014, **4**, 1104.
- 11 S. Yang, Y. Fu, Y. Liao, S. Xiong, Z. Qu, N. Yan and J. Li, Competition of selective catalytic reduction and non selective catalytic reduction over MnO x /TiO 2 for NO removal: the relationship between gaseous NO concentration and N 2 O selectivity, *Catal. Sci. Technol.*, 2014, **4**, 224–232.
- 12 Y. Ji, T. J. Toops, U. M. Graham, G. Jacobs and M. Crocker, A kinetic and DRIFTS study of supported Pt catalysts for NO oxidation, *Catal Lett*, 2006, **110**, 29–37.
- 13 C. Yu, L. Wang and B. Huang, In Situ DRIFTS Study of the Low Temperature Selective Catalytic Reduction of NO with NH3 over MnOx Supported on Multi-Walled Carbon Nanotubes Catalysts, *Aerosol Air Qual. Res.*, 2015, **15**, 1017–1027.
- 14 D. Yang, J. Li, M. Wen and C. Song, Enhanced activity of Cadoped Cu/ZrO2 for nitrogen oxides reduction with propylene in the presence of excess oxygen, *Catalysis Today*, 2008, **139**, 2–7.
- 15 D. M. Yufanyi, J. F. Tendo, A. M. Ondoh and J. K. Mbadcam, CdO Nanoparticles by Thermal Decomposition of a Cadmium-Hexamethylenetetramine Complex, *JMSR*, 2014, **3**. DOI: 10.5539/jmsr.v3n3p1.
- 16 J. E. Bertie and M. Solinas, Infrared and Raman spectra and the vibrational assignment of hexamethylenetetramine- h12 and d12, *The Journal of Chemical Physics*, 1974, **61**, 1666–1677.
- 17 A. B. Ngo, T. H. Vuong, H. Atia, U. Bentrup, V. A. Kondratenko, E. V. Kondratenko, J. Rabeah, U. Ambruster and A. Brückner, Effect of Formaldehyde in Selective Catalytic Reduction of NOx by Ammonia (NH3-SCR) on a Commercial V2O5-WO3/TiO2 Catalyst under Model Conditions, *Environmental science & technology*, 2020, 54, 11753–11761.

Journal Name

- 18 M. M. Dawley, A. M. Scott, F. C. Hill, J. Leszczynski and T. M. Orlando, Adsorption of Formamide on Kaolinite Surfaces: A Combined Infrared Experimental and Theoretical Study, *J. Phys. Chem. C*, 2012, **116**, 23981–23991.
- 19 Y. DENKWITZ, A. KARPENKO, V. PLZAK, R. LEPPELT, B. SCHUMACHER and R. BEHM, Influence of CO2 and H2 on the low-temperature water–gas shift reaction on Au/CeO2 catalysts in idealized and realistic reformate, *Journal of Catalysis*, 2007, 246, 74–90.
- 20 J. Han, A. Wang, G. Isapour, H. Härelind, M. Skoglundh, D. Creaser and L. Olsson, N 2 O Formation during NH 3 -SCR over Different Zeolite Frameworks: Effect of Framework Structure, Copper Species, and Water, *Ind. Eng. Chem. Res.*, 2021, **60**, 17826–17839.