## Supplementary Information for

## Anti-poisoning defective catalyst without metal active sites for NH<sub>3</sub>-SCR via in-situ stabilization

Ge Li<sup>1,†</sup>, Baodong Wang<sup>1,2,\*,†</sup>, Ziran Ma<sup>1,\*</sup>, Jing Ma<sup>1</sup>, Hongyan Wang<sup>1</sup>, Jiali Zhou<sup>1</sup>, Shengpan Peng<sup>1</sup>, Jessica Jein White<sup>3</sup>, Yonglong Li<sup>1</sup>, Jingyun Chen<sup>1</sup>, Zhihua Han<sup>1</sup>, Hui Wei<sup>1</sup>, Chuang Peng<sup>4</sup>, Yujie Xiong<sup>5,\*</sup>, Yun Wang<sup>3,\*</sup>

1National Institute of Clean-and-Low-Carbon Energy; Beijing 102211, China

2 NICE Europe Research GmbH, Stockholmer Platz 1, Stuttgart 70173, Germany

3Centre for Catalysis and Clean Energy, School of Environment and Science, Gold Coast Campus, Griffith University; Queensland 4222, Australia

4School of Resource and Environmental Sciences and Hubei International Scientific and Technological Cooperation Base of Sustainable Resource and Energy, Wuhan University; Wuhan 430072, China

5School of Chemistry and Materials Science, University of Science and Technology of China; Hefei, Anhui 230026, China This PDF file includes:

Figs. S1 to S25

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Fig.S1. N2 selectivity of hydrogenated TiO2-x catalysts

The selectively for N<sub>2</sub> was essentially unchanged after hydrogenation, remaining above 87.5%.



Fig.S2. HRTEM images of hydrogenated TiO<sub>2-x</sub> nano-powders.

The H-TiO<sub>2-x</sub> nanoparticles were found to have an anatase crystalline/disordered core–shell structure with a 1.75-2.63 nm thick disordered surface layer. The interplanar lattice spacing of hydrogenated TiO<sub>2</sub> was about 0.35 nm, which corresponded to that of the (101) plane of anatase (0.325 nm).

Chemical composition analysis results of the synthesized pristine titanium dioxide and hydrogenated  $TiO_{2-x}$  are listed in Table S1.



Fig. S3. XRD patterns of hydrogenated TiO<sub>2-x</sub> catalyst and pristine TiO<sub>2</sub>.

The phase composition of the pristine TiO<sub>2</sub> was primarily anatase and 6.84% rutile. However, after hydrogenation, the rutile diffraction peaks disappeared with only the anatase phase remaining. Rutile is much easier to reduce to hydrogenated TiO<sub>2-x</sub> compared with anatase. As the Ti–O distances (0.1949 and 0.1980 nm) in rutile are greater than those in anatase (0.1934 and 0.1980 nm), O is easier to separate from the TiO<sub>2</sub> crystal in rutile. The anatase diffraction peaks were also clearly broadened and less intense, indicating that the size and structure of the crystal had changed significantly. The average crystal size of the H-TiO<sub>2-x</sub> was estimated to be 17.34 nm using the Scherrer equation. This was due to trivalent Ti and O vacancies being produced during the hydrogenation reduction process.



Fig. S4. Raman spectra of hydrogenated TiO<sub>2-x</sub> catalyst and pristine TiO<sub>2</sub>.

Raman spectra of pristine TiO<sub>2</sub> and hydrogenated TiO<sub>2-x</sub> nanoparticles are shown in Fig. S4. Raman active modes located at ~143cm<sup>-1</sup> (E<sub>g</sub>), 395cm<sup>-1</sup> (B<sub>1g</sub>), 520cm<sup>-1</sup> (A<sub>1g</sub>), and 641 cm<sup>-1</sup> (E<sub>g</sub>) were detected for all samples, indicating that all samples were mainly composed of anatase phase. However, the scattering peaks of hydrogenated TiO<sub>2</sub> were broadened and shifted toward higher wavenumbers. The presence of defects was somewhat responsible for the blue-shift and broadening of the peaks.



Fig. S5. EPR spectra of hydrogenated TiO<sub>2-x</sub> catalyst and pristine TiO<sub>2</sub>.

Figure S5 shows the EPR spectra of hydrogenated  $TiO_{2-x}$  catalyst and pristine  $TiO_2$  measured at 293 K and ambient pressure. The reported g values for  $Ti^{3+}$  on the surface or in the bulk of  $TiO_2$  are 2.02–2.03 and 1.978, 1.959, respectively. In the hydrogenated  $TiO_{2-x}$ , the peak at g<2 was attributed to oxygen vacancy ( $V_0^*$ )  $Ti^{3+}$ . According to the chemical equilibrium, one  $Ti^{3+}$  and two  $Ti^{2+}$  are generated by the generation of oxygen vacancies. As shown in Fig. S5, more ( $V_0^*$ )  $Ti^{3+}$  peaks were present after hydrogenation, indicating that additional oxygen vacancies were generated on the surface of the material, which is more conducive to oxygen conduction in the denitrification reaction.



Fig. S6. <sup>1</sup>H NMR spectra of hydrogenated TiO<sub>2-x</sub> catalyst and pristine TiO<sub>2</sub>.

Figure S6 shows the <sup>1</sup>H NMR spectra of pristine  $TiO_2$  and hydrogenated  $TiO_{2-x}$ . The chemical shift at 5–7 ppm was attributed to surface-adsorbed water, while that at 2 ppm was attributed to H–O<sub>3C</sub> functional groups on the  $TiO_2$  surface. The content of surface-adsorbed water was significantly reduced, while that of H–O<sub>3C</sub> functional groups on the surface was significantly increased, after hydrogenation, which was due to the presence of hydrogen in the disordered surface layer resulting from hydrogenation.



Fig. S7. Photoluminescence spectra of hydrogenated TiO<sub>2-x</sub> catalyst and pristine TiO<sub>2</sub>.

Oxygen vacancies can adsorb  $O_2$  in the gas phase to form superoxide ions, which are good for the formation of nitro and nitrate groups to promote SCR activity. The oxygen vacancies of catalysts can be determined using PL spectra. Many studies have shown that a larger oxygen vacancy content results in a weaker PL signal. Figure S7 show the PL spectra of pristine TiO<sub>2</sub> and hydrogenated TiO<sub>2-x</sub>. The oxygen vacancy content of hydrogenated TiO<sub>2-x</sub> was higher than that of pristine TiO<sub>2</sub>. Oxygen vacancies benefit the recombination of photogenerated electron–hole pairs, suggesting a higher separation efficiency of charge carriers and, accordingly, superior catalytic activity for hydrogenated TiO<sub>2-x</sub>.



Fig. S8. O<sub>2</sub>-TPD profiles of hydrogenated TiO<sub>2-x</sub> catalyst and pristine TiO<sub>2</sub>.

Figure S8 shows O<sub>2</sub>-TPD spectra for the pristine TiO<sub>2</sub> and hydrogenated TiO<sub>2-x</sub> materials. Pristine TiO<sub>2</sub> and hydrogenated TiO<sub>2-x</sub> featured a strong oxygen adsorption capacity, with a clear oxygen desorption peak ( $\alpha$  peak) below 200 °C. As the temperature was increased, oxygen desorbed from the materials, but the peak shape was unclear. At approximately 600 °C, a second desorption peak ( $\beta$  peak) appeared for hydrogenated TiO<sub>2-x</sub>, while a third desorption peak ( $\gamma$  peak) appeared for hydrogenated TiO<sub>2-x</sub>, while a third desorption peak ( $\gamma$  peak) appeared for pristine TiO<sub>2</sub> at temperatures above 800 °C. The first desorption peak temperature of pristine TiO<sub>2</sub> was lower than that of hydrogenated TiO<sub>2-x</sub>, as shown in Fig. S8, which might correspond to physically adsorbed oxygen or weakly chemisorbed O<sub>2</sub> species. As the temperature increased, the slow desorption process of weakly chemisorbed oxygen occurred. The O<sub>α</sub> desorption peak occurred at a higher temperature, corresponding to strongly chemisorbed O<sup>-</sup> and O<sub>2</sub><sup>2</sup><sup>-</sup>, while the third desorption peak corresponded to chemically stable lattice oxygen. Considering the desorption temperatures, strongly chemisorbed O<sup>2-</sup>, namely, oxygen species from the second desorption peak, was likely to play a major role in the catalytic process. During the reaction, the improved desorption properties of chemisorbed  $O^{2-}$  on the catalyst contributed to more favorable catalytic reactivity. Catalysts with strong oxygen storage capacity and good oxygen desorption performance might be expected to show high catalytic activity. The chemically stable lattice oxygen sites are mainly derived from TiO<sub>2</sub> and O<sub>2</sub>. Chemisorbed O<sup>2-</sup> arises from interactions between O<sub>2</sub> and TiO<sub>2</sub>, with more oxygen defects resulting in more chemically adsorbed oxygen. Therefore, the oxygen deficiency can induce the catalyst surface to more easily desorb chemisorption O<sup>2-</sup>, which enhances the catalytic reaction efficiency. Therefore, regarding O<sub>β</sub>, the hydrogenated TiO<sub>2-x</sub> catalyst had more chemically adsorbed oxygen compared with pristine TiO<sub>2</sub>.



Fig. S9. H<sub>2</sub>-TPR profiles of hydrogenated TiO<sub>2-x</sub> catalyst and pristine TiO<sub>2</sub>.

Figure S9 shows the H<sub>2</sub>-TPR profiles of pristine TiO<sub>2</sub> and hydrogenated TiO<sub>2-x</sub>. Pristine TiO<sub>2</sub> exhibited a large H<sub>2</sub> reduction peak at 450–500 °C, which corresponded to the H<sub>2</sub> reduction temperature. This was consistent with our experimental TiO<sub>2</sub> hydrogenation temperature. As shown in Fig. S9, the redox performance of the catalyst increased significantly in the low-temperature zone after hydrogenation. The reduction peaks at 200–300 °C were attributed to the reduction of surface Ti<sup>4+</sup> ions. Mutual conversion between Ti<sup>3+</sup> and Ti<sup>4+</sup> endowed TiO<sub>2</sub> with redox performance, which was another reason for the denitrification performance of hydrogenated TiO<sub>2</sub> being significantly improved.



**Fig. S10.** In-situ XPS spectra of hydrogenated TiO<sub>2-x</sub> catalyst and pristine TiO<sub>2</sub>: O 1s

For better quantitative analysis, changes in the surface chemical bonding of  $TiO_2$  nanocrystals induced by hydrogenation were investigated using in-situ XPS. Figure S10-S12 show the O 1s, Ti 2p, and valence band spectra of pristine  $TiO_2$  and hydrogenated  $TiO_{2-x}$ . The O 1s XPS spectra of pristine and hydrogenated  $TiO_{2-x}$  showed large differences. The O 1s peaks were resolved into two peaks at about 529.7-530.8 eV and 531.0-531.6 eV for pristine  $TiO_2$  and hydrogenated  $TiO_{2-x}$ , respectively. The broader peak at 531.0-531.6 eV was attributed to oxygen adsorbed on the  $TiO_2$  surface. The narrow peak at 529.7-530.8 eV was attributed to Ti-O bonds in the  $TiO_2$  lattice. According to the peak fitting results, the ratio of adsorbed oxygen to lattice oxygen increased from 31.14% in the pristine  $TiO_2$  to 53.46% in the hydrogenated  $TiO_{2-x}$ . This variation was primarily the result of the loss of lattice oxygen during the hydrogenation process to

form oxygen vacancies, which subsequently adsorbed ambient water vapor to generate surface hydroxyl groups. This process increased the percentage of adsorbed oxygen in the material.



Fig. S11. In-situ XPS spectra of hydrogenated TiO<sub>2-x</sub> catalyst and pristine TiO<sub>2</sub>: Ti 2p

The Ti 2p spectrum of the H-TiO<sub>2-x</sub> shows a shift in the Ti<sup>4+</sup> 2p3/2 peak by 1.1 eV toward a higher binding energy, indicating that the Ti in this material gained electrons. This could have been a consequence of electron transfer to surrounding  $Ti^{4+}$  during the oxygen vacancy generation process, with the simultaneous formation of  $Ti^{3+}$ . After peak fitting, the  $Ti^{3+}/Ti^{4+}$  ratio was determined to be 6.15%.



Fig. S12. In-situ XPS spectra of hydrogenated TiO<sub>2-x</sub> catalyst and pristine TiO<sub>2</sub>: valence bands

As shown in Fig. S12, the bottom of the valence band in pristine  $TiO_2$  was positioned at 2.31 eV, and oxidation was weak. After hydrogenation, the bottom of the valence band of hydrogenated  $TiO_{2-x}$  was shifted to a higher binding energy of 3.37 eV, indicating that more defects were generated and that oxidation was significantly stronger.



Fig. S13 In-situ XPS spectra of hydrogenated TiO<sub>2-x</sub> in the NH<sub>3</sub>-SCR process at 150–400 °C: survey spectra.

As shown in Fig. S13, the XPS survey spectra acquired from the  $H-TiO_{2-x}$  catalyst during the denitrification process at 150-400 °C all contained a N 1s peak near 400 eV. This peak indicates that either nitrogen doping, or the adsorption of N-containing compounds occurred during the denitrification process.



Fig. S14. In-situ XPS spectra of hydrogenated TiO<sub>2-x</sub> in the NH<sub>3</sub>-SCR process at 150–400 °C: Ti 2p.

Fig. S14 presents the Ti 2p spectrum of the H-TiO<sub>2-x</sub> in the NH<sub>3</sub>-SCR process. During the deNOx process of hydrogenated TiO<sub>2-x</sub> at 150–400 °C, the Ti valence state did not change. The Ti spectrum of hydrogenated TiO<sub>2-x</sub> mainly showed that Ti in hydrogenated TiO<sub>2-x</sub> mainly existed in the form of Ti<sup>4+</sup> during the NH<sub>3</sub>-SCR process. Compared with freshly hydrogenated TiO<sub>2-x</sub> catalyst, Ti<sup>3+</sup> was observed to disappear during the reaction, which might be due to nitrogen doping.



Fig. S15. In-situ XPS spectra of hydrogenated TiO<sub>2-x</sub> in the NH<sub>3</sub>-SCR process at 150–400 °C: O 1s.

Fig. S15 provides the O 1s spectrum. The  $O_{\alpha}$  peak of  $O^{2^-}$  in the TiO<sub>2</sub> lattice appeared around 529–530 eV at 150–300 °C, the  $O_{\beta}$  peak of oxygen adsorbed on TiO<sub>2</sub> appeared around 530–532 eV, and the  $O_{\gamma}$  peak of surface hydroxyl groups (–OH) on TiO<sub>2</sub> appeared around 532–533 eV. As shown in Table S2, with increasing temperature, the  $O_{\beta}$ +  $O_{\gamma}$ /total O ratio continuously increased from 250 to 400 °C, indicating continuous adsorption of oxygen to supplement the continuous consumption of lattice oxygen by the hydrogenated TiO<sub>2-x</sub> catalyst. In the NH<sub>3</sub>-SCR process, not only adsorbed oxygen on the catalyst surface, but also oxygen in the catalyst body phase, participated in the catalytic reaction. The presence of oxygen defects accelerated the circulation of gaseous oxygen and lattice oxygen on the surface and in the bulk of the catalyst. Oxygen on the catalyst surface was oxidized to active oxygen, many oxygen vacancies were left on the catalyst surface, which were conducive to oxygen adsorption from the gas phase. Electrons were continuously exchanged through interactions between adsorbed oxygen and metal ions in the active surface components. This exchange maintained the balance of reactive oxygen species involved in the reaction on the catalyst surface.



**Fig. S16.** XPS spectra of the hydrogenated TiO<sub>2-x</sub> sample. (A) NH<sub>3</sub> atmosphere at 350°C, and (B) NO+O<sub>2</sub> atmosphere at 350°C.

Figure S16 demonstrates that nitrogen doping of the H-TiO<sub>2-x</sub> catalyst surface occurred under both conditions. Previous studies have shown that the nitrogen doping of TiO<sub>2</sub> can proceed under an NH<sub>3</sub> atmosphere at 500 °C as N from NH<sub>3</sub> partially replaces lattice oxygen of TiO<sub>2</sub>, forming O-Ti-N and oxygen vacancies<sup>1, 2</sup>.



Fig. S17 DRIFT spectra of hydrogenated TiO<sub>2-x</sub> catalyst. a Exposed to NO and O<sub>2</sub> for various times. b Preabsorbed with NO + O<sub>2</sub> and then treated with NH<sub>3</sub>. c Exposed to NH<sub>3</sub> for various times. d Preabsorbed with NH<sub>3</sub> and then treated with NO + O<sub>2</sub>. e Exposed to NH<sub>3</sub> + NO + O<sub>2</sub> for 30 min. f With a temperature gradient in NH<sub>3</sub> + NO + O<sub>2</sub> atmosphere



Fig. S18 NH<sub>3</sub>-TPD profiles of pristine TiO<sub>2</sub>, hydrogenated TiO<sub>2-x</sub> catalyst and N doped hydrogenated TiO<sub>2-x</sub>

The results obtained from NH<sub>3</sub>-temperature programmed desorption show that the pristine TiO<sub>2</sub> was somewhat acidic and was also able to adsorb NH<sub>3</sub>.We used the NH<sub>3</sub>-TPD curve peak fitting process to calculate the amount of NH<sub>3</sub> desorbed for each catalyst, and the results are listed in Table S4. It can be seen from Table S4 that according to the integrated area of the NH<sub>3</sub>-TPD spectrum, the total acid content is reduced after nitrogen doping, indicating that nitrogen doping reduces the acidity of the hydrogenated TiO<sub>2-x</sub> catalyst. This may be related to the N doping filling up part of the oxygen vacancies, resulting in a decrease in oxygen vacancies and a decrease in acidity.



Fig. S19 Py-IR spectra of pristine  $TiO_2$ , hydrogenated  $TiO_{2-x}$  catalyst and N doped hydrogenated  $TiO_{2-x}$ 

The results obtained from pyridine adsorption infrared spectroscopy show that the pristine TiO<sub>2</sub> was somewhat acidic and was also able to adsorb NH<sub>3</sub>. The peaks at wave numbers of 1608 cm<sup>-1</sup>, 1573 cm<sup>-1</sup>, 1493 cm<sup>-1</sup>, and 1446 cm<sup>-1</sup> are the peaks of L acid sites, and the peaks at 1541 cm<sup>-1</sup> maybe the peaks of B acid sites or the noise peak. Table S5 shows the pyridine infrared curve fitting results of pristine TiO<sub>2</sub>, hydrogenated TiO<sub>2-x</sub> and N-TiO<sub>2-x</sub> catalysts. It can be seen from Figure S19 and TableS5 that the acidic and the acid strength is obviously weakened after hydrogenation and nitrogen doping. The acidity of pristine TiO<sub>2</sub> may be caused by the small amount of impurities such as S and P (Table S1). The content of S and P in hydrogenated TiO<sub>2-x</sub> is greatly reduced (Table S1). The L acid is mainly caused by oxygen vacancies caused by surface defects of the sample. After the hydrogenated TiO<sub>2-x</sub> is doped with nitrogen, the L acid is reduced, indicating that the nitrogen doping has filled part of the oxygen vacancies, which is consistent with the results of NH<sub>3</sub>-TPD. It can be seen that the total acidity of the catalyst.

wt %	SiO <sub>2</sub>	P <sub>2</sub> O <sub>5</sub>	SO <sub>3</sub>	Cl	CaO	TiO <sub>2</sub>	ZrO <sub>2</sub>	Nb <sub>2</sub> O <sub>5</sub>
Pristine TiO <sub>2</sub>	0.022	0.181	1.775	0.016	0.031	97.921	0.017	0.037
Hydrogenated TiO <sub>2-x</sub>	0.939	0.187	0.288	0.027	0.159	98.019	0.018	0.040

Table S1 Chemical composition analysis results of pristine titanium dioxide and hydrogenated TiO<sub>2-x</sub>.

The pristine  $TiO_2$  powder is primarily composed of  $TiO_2$  with traces of SO<sub>3</sub>,  $P_2O_5$  and Cl. Hydrogenation drastically reduces SO<sub>3</sub> but does not affect the other impurities.

samples	Bing Energy (eV) and surface atomic concentrations (%)									
			01	S		N 1s				
	Oα/eV	Oβ/eV	Oγ/eV	(Οβ+ Ογ )/Ο	Surface concentration (%)	Ti-O- N/eV	N- H/eV	N- O/eV	Ti-O-N / N	Surface concentration (%)
150°C	529.7	530.42	532.22	21.36%	63.72	399.40	400.90	406.76	45.11%	0.23
200°C	529.93	530.99	532.55	28.77%	63.89	399.67	401.36	406.89	53.67%	0.28
250°C	529.98	531.12	532.61	12.33%	64.01	398.92	400.50	406.06	58.24%	0.31
300°C	530.09	531.1	532.42	13.40%	63.55	398.95		406.09	75.75%	0.38
350°C	529.99	531.07	532.25	15.35%	64.67	401.35		408.38	78.54%	0.45
400°C	532.01	532.89	534.34	21.60%	64.49	402.61			100%	0.44

Table S2 Binding energies and surface atomic concentrations of N and O in hydrogenated  $\rm TiO_{2-x}$ 

catalysts at 150-400 °C.

Sample	Shell	N <sup>a</sup>	$R(\text{\AA})^b$	$\sigma^2 \times 10^3 (\text{\AA}^2)^c$	$\Delta E_0  (\mathrm{eV})^d$	R factor
TiO <sub>2</sub>	Ti-O	6*	1.96±0.02	6.3±2.3	-1.8±2.6	0.008
Hydrogenated	Ti-O	5.9±0.8	$1.92 \pm 0.01$	3.4±2.7	-2.5±0.7	
TiO <sub>2-x</sub> catalyst	Ti-Ti	5.5±1.5	3.23±0.02	44.2±6.2		0.002
N-	Ti-O	6.1±1.2	$1.91 \pm 0.01$	6.5±3.5	-3.7±1.0	
Hydrogenated TiO <sub>2-x</sub>	Ti-Ti	7.7±3.6	3.23±0.03	72.3±12.8		0.004

**Table S3** EXAFS fitting parameters at the Ti K-edge for various samples (S02 = 0.73).

catalyst <sup>*a*</sup>N, coordination number; <sup>*b*</sup>R, bond distance; <sup>*c*</sup> $\sigma^2$ , Debye-Waller factor; <sup>*d*</sup> $\Delta E_0$ , inner potential correction; *R* factor, goodness of fit.

Samples	Weak ad	sorption NH <sub>3</sub>	Strong ac	Total NH <sub>3</sub>	
	Temperature peak (°C)	NH <sub>3</sub> desorption amount(mmol/g)	Temperature peak (°C)	NH <sub>3</sub> desorption amount(mmol/g)	amount(mmol/g)
Pristine TiO <sub>2</sub>	135.4	0.37231	311.2	0.25778	0.63009
H-TiO <sub>2-x</sub>	138.9	0.38470	295.9	0.18007	0.56477
N-H-TiO <sub>2-x</sub>	132.3	0.31102	295.0	0.20632	0.51734

Table S4 NH<sub>3</sub> desorption amount of pristine TiO<sub>2</sub>, H-TiO<sub>2-x</sub> and N-H-TiO<sub>2-x</sub>

Samples	Lewis acid	Bronsted acid	Total acid amount	
	Acidity amount(mmol/g)	Acidity amount(mmol/g)		
Pristine TiO <sub>2</sub>	5.163		5.163	
H-TiO <sub>2-x</sub>	2.527		2.527	
N-H-TiO <sub>2-x</sub>	2.183	0.249/——	2.432	

Table S5 Pyridine infrared adsorption amount of pristine TiO<sub>2</sub>,H-TiO<sub>2-x</sub> and N-H-TiO<sub>2-x</sub>

## References

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