# Boosting ammonia synthesis over MoO<sub>2</sub> by Li intercalation

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#### **Materials and Methods**

#### 1. Materials.

Molybdenum oxide (MoO<sub>2</sub>) was purchased from Alfa Aesar Co, Ltd. Iron(III) chloride (FeCl<sub>3</sub>), lithium hydride (LiH), magnesium oxide (MgO), chloroplatinic acid hexahydrate (H<sub>2</sub>PtCl<sub>6</sub>·6H<sub>2</sub>O), ruthenium(III) chloride hydrate (RuCl<sub>3</sub>·xH<sub>2</sub>O), and tetrahydrofuran (THF) were purchased from Aladdin. Cobalt(II) chloride hexahydrate (CoCl<sub>2</sub>·6H<sub>2</sub>O), nickel(II) chloride hexahydrate (NiCl<sub>2</sub>·6H<sub>2</sub>O), absolute ethanol (AR grade), and concentrated hydrochloric acid (HCl) were purchased from Sinopharm Chemical Reagent Co, Ltd. The purities of H<sub>2</sub>, N<sub>2</sub>, and Ar gases are all 99.9995%.

### 2. General Characterization

The powder X-ray diffraction (XRD) patterns were performed on a Rigaku D/Max 2500/PV X-ray diffractometer with monochromator Cu K $\alpha$  radiation ( $\lambda$ =1.5418 Å) from 10° to 80° with the scanning rate of 6°/min. Transmission electron microscopy (TEM) images, mapping images, were measured using a Tecnai G2 S-Twin F20 at the acceleration voltage of 200 kV. Scanning electron microscopy (SEM) and energy dispersive X-ray spectroscopy (EDS) analysis were collected using a Helios NanoLab 600I from FEI Company. X-ray photoelectron spectroscopy (XPS) was recorded on a Thermo ESCALAB 250 X-ray photoelectron spectrometer with a monochromated X-ray source (Al K $\alpha$  *hv*=1486.6 eV). The energy scale of the spectrometer was calibrated using Au4f<sub>7/2</sub>, Cu2p<sub>3/2</sub>, and Ag3d<sub>5/2</sub> peak positions. The standard deviation for the binding energy (BE) values was 0.1 eV. Argon ion etch for one minute. Ultraviolet photoelectron spectroscopy (UPS) measurements were carried out by a Prevac spectrometer with a VG

Scienta R3000 hemispherical electron energy analyzer. Photons with energy of 21.22 eV generated by helium I were used for UPS spectra. The electron paramagnetic resonance spectra were obtained on a JES-FA 200 EPR spectrometer. The details of the instrumental parameters were as follows: scanning frequency: 9.45 GHz; scanning width: 800 mT; scanning power: 0.998 mW; scanning temperature: 293 K. Fourier transform infrared (FTIR) spectroscopy was performed on a Bruker VERTEX 80 V spectrometer. The Brunauer-Emmett-Teller (BET) surface areas of the samples were measured from the adsorption of N2 at 77 K by using a Micromeritics ASAP 2020M system. Ferromagnetism was measured with a superconducting quantum interference device (SQUID, Quantum Design Inc.). Inductively coupled plasma (ICP) analyses were carried out on an iCAP 7600 ICP-OES instrument. The temperatureprogrammed desorption was performed on an Autochem II 2920 apparatus (Micromeritics, USA). Quantitative samples were usually loaded and pre-treated in an inert gas flow at 500 °C for 1 h. The samples were saturated with a flow of 25 mL min<sup>-1</sup> 10% N<sub>2</sub> (or H<sub>2</sub>)/He for 60 min. After being purged with inert gas for 1 h, the samples were heated from 50 °C to 500 °C with a heating rate of 10 °C/min under inert gas atmosphere, and the desorbed NH<sub>3</sub> (N<sub>2</sub>, H<sub>2</sub>) was determined using a thermal conductivity detector. Catalytic reactions were carried out over the WFSM-3060 catalyst evaluation system from Tianjin Xianquan Industry and Trade Development Ltd. Ammonia concentration was measured by ion chromatography (IC) on a PIC-10 produced by Qingdao Puren Instrument Ltd.

#### 3. Kinetic calculations

If assuming the dissociation of  $N_2 (N_2^* \rightarrow 2N^*)$  as the rate-determining step:

$$r = \frac{\stackrel{\rightarrow K_2 P_{N_2}}{\prod_{k_4} \left(1 + K_1 P_{H_2} + K_2 P_{N_2} + \sqrt{K_1 K_3 P_{H_2}}\right)^2} \tag{1}$$

If assuming the formation of NH (N\* + H\*  $\rightarrow$  NH\*) as the rate-determining step:

$$r = \frac{\overrightarrow{K_1 K_2 K_3 K_4} \sqrt{P_{H_2} P_{N_2}}}{\left(1 + K_1 P_{H_2} + K_2 P_{N_2} + \sqrt{K_1 K_3 P_{H_2}} + \sqrt{K_2 K_4 P_{N_2}}\right)^2}$$
(2)

Where  $\vec{ki}$  is the rate constant of the forward reaction and Ki is the equilibrium constant in step *i*.

#### 4. Density Functional Theory (DFT) Calculations

The DFT calculations were performed by using the Vienna Ab Initio Simulation Package (VASP)<sup>[1,2]</sup> based on density functional theory (DFT)<sup>[3,4]</sup>. The exchange-correlation interaction adopted the generalized gradient approximation (GGA) with Perdew-Burke-Ernzerhof (PBE) functional<sup>[5]</sup>. The projector augmented wave (PAW) method<sup>[6,7]</sup> were used to describe the ion-electron interactions.

The energy cutoff of the plane-wave basis was set to 400 eV. The convergence criteria of the residual force and energy during the structure relaxation are set to 0.01 eV Å<sup>-1</sup> and 10<sup>-4</sup> eV, respectively. We chose  $4 \times 2 \times 1$  Gemma k-points in the first Brillouin zone for geometric optimization and electronic structure calculation. The structure of bulk molybdenum(IV) oxide including four MoO<sub>2</sub> units was composed of a periodic supercell<sup>[8]</sup>, which is used to construct the periodic plate of (011) surface calculations. The (011) surfaces were modeled by a three-layer plate containing Mo<sub>8</sub>O<sub>16</sub> each layer. Three models of MoO<sub>2-x</sub>, Li-MoO<sub>2-x</sub> and Fe@Li-MoO<sub>2-x</sub> (the concentration of both oxygen vacancy and iron were set to be 1.408 %, and the concentration of lithium was evenly mixed at 16.901% were constructed. In order to avoid the interaction between two adjacent layers, a 15-Å-thick vacuum region was added along the z-axis. During

the optimization, the bottom two layers remained fixed, and the top layer and the adsorbent were completely relaxed.

The adsorption energies  $(E_{ad})$  of molecule were defined as Equation (3):

$$E_{ad} = E_{total} - E_{surf} - E_{mole} \quad (3)$$

where  $E_{total}$ ,  $E_{surf}$ , and  $E_{mole}$  are the energies of adsorption configurations, slab models, and free gas molecules.

The formation Gibbs free energy ( $\Delta G$ ) in the reaction coordinate is calculated as Equation <sup>[9]</sup>(4):  $\Delta G = \Delta E + \Delta ZPE - T\Delta S$  (4)

where  $\Delta E$  is the adsorption energy,  $\Delta ZPE$  is the correction of zero-point energy and  $T\Delta S$  is the entropy difference between the gas phase and adsorbed state. The zero-point energies and entropies of the reactive species are calculated from the vibrational frequencies at 673 K and 10 bar and the vibrational frequencies and entropies of molecules in the gas phase are taken from the NIST database [http://cccbdb.nist.gov/].

Differential Charge Density (DCD) was adopted to qualitatively evaluate the charge density difference  $\Delta \rho(r)$ , which can be defined as Equation (5):

$$\Delta \rho(r) = \rho_{Li - MoO_{2 - x}}(r) - \rho_{MoO_{2 - x}}(r) - \rho_{Li}(r) \quad (5)$$

where  ${}^{\rho_{Li-MoO_{2}-x}(r)}$  represents the total charge density of the fully relaxed configuration of Li-MoO\_{2-x} surface.  ${}^{\rho_{MoO_{2}-x}(r)}$  and  ${}^{\rho_{Li}(r)}$  represent the total electronic charge densities of the separated MoO\_{2-x} surface and doped lithium, respectively, which maintain the same geometrical structures as the relaxed configuration of Li-MoO\_{2-x} surface.

All the transition states were determined using the climbing image-nudged elastic band (CI-NEB) method<sup>[10,11]</sup>. Four images were set in the elastic band between the initial and final states to calculate the

transition state (TS) configuration at the saddle point. The convergence criterion for energy is  $10^{-7}$  eV and for force is 0.01 eV Å<sup>-1</sup>.



Fig. S1. Powder XRD patterns of  $MoO_2$  and  $MoO_{2-x}/Li$ .



Fig. S2. XPS spectra of Li 1s for  $MoO_2$  and  $MoO_{2-x}/Li$ .



Fig. S3. SEM (left) and TEM (right) images of the  $MoO_2$  sample.



Fig. S4. SEM (left) and TEM (right) images of the  $MoO_{2-x}/Li$  sample.



Fig. S5. SEM images of (a)  $MoO_2$  and (b)  $MoO_{2-x}/Li$ . The insets show the corresponding HRTEM images.



Fig. S6. XPS spectra of Cl 2p for  $MoO_2$ ,  $FeCl_3$ - $MoO_2$  and  $Fe@MoO_{2-x}/Li$ .



Fig. S7. HRTEM image of the multiple layers of the Fe@MoO<sub>2-x</sub>/Li nanosheets.



Fig. S8. TEM images of  $Ru@MoO_{2\text{-}x}/Li$  and  $Ni@MoO_{2\text{-}x}/Li.$ 



Fig. S9. UPS spectra of  $MoO_2$ ,  $MoO_{2-x}/Li$  and  $Fe@MoO_{2-x}/Li$ .



Fig. S10. Schematic diagram of the whole catalytic system.



Fig. S11. The calibration curve of  $NH_4^+$  using the ion chromatograph method.



Fig. S12. Ammonia synthesis rate of Fe@MoO<sub>2-x</sub>/Li with different amount of Fe loadings.



Fig. S13. Powder XRD patterns of a mixture of Fe@MoO<sub>2-x</sub>/Li (30 mg) and quartz sand (500 mg) before and after the reaction.



Fig. S14. TEM image of Fe@ $MoO_{2-x}/Li$  after the reaction. The inset histogram shows the diameter distributions of Fe nanoparticles.



Fig. S15. XPS spectra of Li 1s for Fe@MoO<sub>2-x</sub>/Li before and after the reaction.



Fig. S16. FTIR spectra of Fe@MoO $_{2\text{-}x}/\text{Li}$  before and after the reaction.



Fig. S17. XPS spectra of Mo 3d and O 1s for Li-free MoO<sub>2-x</sub>.



Fig. S18. <sup>1</sup>H NMR spectra (400 MHz) of both  ${}^{15}NH_4{}^+$  and  ${}^{14}NH_4{}^+$  produced from the reactions using  ${}^{15}N_2$  or  ${}^{14}N_2$  as the N<sub>2</sub> source.



Fig. S19. Elementary steps for ammonia synthesis based on Langmuir-Hinshelwood mechanism.



Fig. S20. XPS spectra of Mo 3d for Fe@MoO<sub>2-x</sub>/Li before and after the acid leaching treatment.



**Fig. S21.** Magnetization versus magnetic field (M-H) plots of Fe@ MoO<sub>2-x</sub>/Li before and after the acid leaching treatment.



Fig. S22. Dependences of ammonia synthesis on the partial pressures of  $H_2$ 



Fig. S23. H<sub>2</sub>-TPD profiles of  $MoO_{2-x}/Li$  and Fe@  $MoO_{2-x}/Li$  (after leaching).



**Fig. S24.** (a) Two possible positions for oxygen vacancy. (b) The optimization model of optimal oxygen vacancy. Note: We choose the surface of Li-MoO<sub>2</sub> to model the two oxygen vacancies separately to find the best oxygen vacancy position. It is calculated that the slab energy of the model that forms oxygen vacancies at VO<sub>2</sub> position is -655.18 eV. The configuration that forms oxygen vacancies at VO<sub>1</sub> shows the lowest energy -656.06 eV, which has been applied in the further calculations.



Fig. S25. The optimized configurations of  $N_2$  adsorption on the models of  $MoO_{2-x}$ ,  $MoO_{2-x}/Li$  and  $Fe@MoO_{2-x}/Li$  (after leaching).



Fig. S26. The optimization model of  $MoO_{2-x}$  and the optimized configuration of N\*, N\*+H\* and NH\* adsorption on the model of  $MoO_{2-x}$ .



Fig. S27. The optimization model of  $MoO_{2-x}/Li$  and the optimized configuration of N\*, N\*+H\* and NH\* adsorption on the model of  $MoO_{2-x}/Li$ .



Fig. S28. The optimization model of  $Fe@MoO_{2-x}/Li$  (after leaching) and the optimized configuration of N\*, N\*+H\* and NH\* adsorption on the model of  $Fe@MoO_{2-x}/Li$  (after leaching).



Fig. S29 The optimized configurations of transition states on the models of  $MoO_{2-x}$ ,  $MoO_{2-x}/Li$  and  $Fe@MoO_{2-x}/Li$  (after leaching).

| Catalysts  | Temperature (°C) | Pressure<br>(MPa) | flow rate $(m1 min^{-1})$ | $\frac{\text{RNH}_3}{(\text{mmol } g^{-1} h^{-1})}$ | Ref.      |
|--|------------------|-------------------|---------------------------|---|-----------|
| Fe(1%)@MoO <sub>2-x</sub> /Li                            | 400              | 1.0               | 60                        | 4.57  | This work |
| Fe(0.1%)@MoO <sub>2-x</sub> /Li<br>(after acid leaching) | 400              | 1.0               | 60                        | 4.71  | This work |
| Ni <sub>2</sub> Mo <sub>3</sub> N                        | 400              | 0.1               | 60                        | 0.39  | 12        |
| Co <sub>3</sub> Mo <sub>3</sub> N                        | 400              | 0.1               | 60                        | 0.65  | 12        |
| Fe-Mo-N  | 400              | 0.1               | 60                        | 0.14  | 12        |
| Fe-LiH   | 350              | 1.0               | 30                        | 10.5  | 13        |
| LaCoSi   | 400              | 0.1               | 60                        | 1.25  | 14        |
| LaCoSi   | 400              | 0.9               | 60                        | 5.00  | 14        |
| Ni-LaN bulk  | 400              | 0.1               | 60                        | 2.40  | 15        |
| Ni-LaN NPs   | 400              | 0.1               | 60                        | 5.54  | 15        |
| Cs-Ru (1%)/MgO   | 400              | 5.0               | 60                        | 2.70  | 16        |
| Ru(1%)/CeO <sub>2</sub> -H                               | 400              | 1.0               | 60                        | 3.98  | 17        |
| Ru(0.1%)/C12A7:e <sup>-</sup>                            | 400              | 1.0               | 60                        | 0.99  | 18        |
| Ru(1.2%)/C12A7:e <sup>-</sup>                            | 400              | 1.0               | 60                        | 8.245   | 18        |
| LaRuSi   | 400              | 0.1               | 60                        | 1.76  | 19        |
| Ru (12%)/CaFH  | 340              | 0.1               | 60                        | 15  | 20        |
| Cs-Ru (10%)/MgO  | 340              | 0.1               | 60                        | 8.32  | 20        |

Table S1. Ammonia synthesis over recently developed catalysts

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