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## Efficient dehydrogenation of high concentration formic acid over PdAu/AC-NH<sub>2</sub>

## catalyst without additives under ambient conditions

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 $\textbf{Fig. S1} \text{ TEM imagines of (a) Pd/AC-NH}_2\text{, (b) Pd}_4\text{Au}_1\text{/AC-NH}_2\text{, (c) Pd}_2\text{Au}_3\text{/AC-NH}_2\text{ and (d) Pd}_1\text{Au}_4\text{/AC-NH}_2\text{.}$ 



Fig. S2 Survey XPS characterization of  $Pd_3Au_2/AC-NH_2$ .



Fig. S3 TOF values' change with the concentration of FA at 303 K.



Fig. S4 TEM image of  $Pd_3Au_2/AC-NH_2$  after 3 cycles of 5 M FA dehydrogenation (a) and neat FA (b). XPS spectra of  $Pd_3Au_2/AC-NH_2$  before reaction and after 3 cycles of 5 M FA dehydrogenation and neat FA at 303 K.



Fig. S5 Mass spectrum (MS) of gas products over Pd<sub>3</sub>Au<sub>2</sub>/AC-NH<sub>2</sub> using He carrier gas (Neat FA, 1 mL, 303 K).



Fig. S6 Arrhenius plot (ln (TOF) vs. 1000\*1/T of Pd<sub>3</sub>Au<sub>2</sub>/AC-NH<sub>2</sub> catalyst.



Fig. S7 (a) The relationship between TOF values and Pd binding energy. (b) A trade-off relation between Pd bind energy

and surface energy as a function of Au content.

| Catalyst  | Pd / wt.% | Au / wt.% | Mole ratio of Pd/Au |
|---|-----------|-----------|---------------------|
| Pd/AC-NH <sub>2</sub>   | 3.39      | /         | /                   |
| Pd <sub>4</sub> Au <sub>1</sub> /AC-NH <sub>2</sub>                   | 2.95      | 1.26      | 4.35                |
| Pd <sub>3</sub> Au <sub>2</sub> /AC-NH <sub>2</sub>                   | 2.26      | 2.21      | 1.90                |
| Pd <sub>2</sub> Au <sub>3</sub> /AC-NH <sub>2</sub>                   | 1.57      | 4.22      | 0.69                |
| Pd <sub>1</sub> Au <sub>4</sub> /AC-NH <sub>2</sub>                   | 0.75      | 5.62      | 0.24                |
| Pd <sub>3</sub> Au <sub>2</sub> /AC                                   | 2.41      | 2.38      | 1.88                |
| Used Pd <sub>3</sub> Au <sub>2</sub> /AC-NH <sub>2</sub> <sup>a</sup> | 2.13      | 2.11      | 1.78                |

 Table S1 ICP results of the as prepared catalysts.

a ICP results of  $Pd_3Au_2/AC-NH_2$  after three cycles of neat FA dehydrogenation at 303 K.

 $\label{eq:stables} \textbf{Table S2} \ The \ textural \ properties \ of \ various \ samples \ measured \ by \ N_2 \ adsorption/desorption \ isotherms.$ 

| Different stages                                    | $S_{BET}/m^2g^{1}$ | Pore volume / $cm^{-3} g^{-1}$ | Pore size / nm |
|---|--------------------|--------------------------------|----------------|
| AC  | 939                | 0.66                           | 5.34           |
| Pd <sub>3</sub> Au <sub>2</sub> /AC                 | 877                | 0.63                           | 5.34           |
| AC-NH <sub>2</sub>                                  | 421                | 0.50                           | 5.22           |
| Pd <sub>3</sub> Au <sub>2</sub> /AC-NH <sub>2</sub> | 399                | 0.43                           | 5.75           |

| Samples   | C / wt.% | H / wt.% | $\mathrm{N}^a$ / wt.% | $\mathrm{N}^{b}$ / wt.% |
|---|----------|----------|-----------------------|-------------------------|
| Fresh Pd <sub>3</sub> Au <sub>2</sub> /AC-NH <sub>2</sub>             | 63.57    | 3.52     | 2.88                  | 5.23                    |
| Used Pd <sub>3</sub> Au <sub>2</sub> /AC-NH <sub>2</sub> <sup>c</sup> | 64.15    | 2.44     | 2.44                  | /                       |

Table S3 Elemental content analysis of Pd<sub>3</sub>Au<sub>2</sub>/AC-NH<sub>2</sub>.

a Determined by Element Analysis (EA). b Determined by survey XPS. c Elemental content analysis of Pd<sub>3</sub>Au<sub>2</sub>/AC-

 $\rm NH_2$  after three cycles of neat FA dehydrogenation at 303 K.

| Catalyst   | Temp. / K | Additives   | TOF / h <sup>-1</sup> | Ref.      |
|--|-----------|-------------|-----------------------|-----------|
| Pd <sub>3</sub> Au <sub>2</sub> /AC-NH <sub>2</sub>          | 293       | 5 M FA      | 1830 <sup>b</sup>     |           |
|  | 303       | 5 M FA      | 3300 <sup>b</sup>     |           |
|  | 313       | 5 M FA      | 5730 <sup>b</sup>     | 41        |
|  | 323       | 5 M FA      | 8710 <sup>b</sup>     | this work |
|  | 303       | 1 M FA      | 4355 <sup>a</sup>     |           |
|  | 303       | Neat FA     | 603 <sup>b</sup>      |           |
| $Pd_{0.85}Ir_{0.15}/SBA-15-NH_2$                             | 298       | 1 M FA      | 1500 <sup>b</sup>     | 34        |
| PdMn <sub>0.6</sub> @S-1                                     | 298       | 1 M FA      | 610 <sup>b</sup>      | 6         |
| Ni <sub>0.4</sub> Pd <sub>0.6</sub> /NH <sub>2</sub> -N-rGO  | 298       | 1 M FA      | 954 <sup>b</sup>      | 16        |
| Au <sub>1</sub> Pd <sub>1.5</sub> /MIL-101-NH <sub>2</sub>   | 298       | 1 M FA / SF | 526 <sup>b</sup>      | 33        |
| Pd <sub>1</sub> Au <sub>1</sub> /72-LA                       | 303       | 1 M FA / SF | 3583ª                 | 37        |
| Au <sub>2</sub> Pd <sub>3</sub> @(P)N-C                      | 303       | 1 M FA      | 358ª                  | 32        |
| Pd@SS-CNR  | 303       | 1 M FA / SF | 1878 <sup>b</sup>     | 30        |
| Pd/CZIF-8-950  | 303       | 1 M FA / SF | 1166 <sup>b</sup>     | 49        |
| $Pd@Bi_{0.11}/C$   | 313       | 1 M FA / SF | 4100 <sup>b</sup>     | 31        |
| Pd@CN900K  | 323       | 1 M FA / SF | 8000 <sup>a</sup>     | 14        |
| 0.8Pd-0.2Ni(OH)2@S-1   | 333       | 1 M FA / SF | 5803 <sup>b</sup>     | 39        |
| (Co <sub>6</sub> )Ag <sub>0.1</sub> Pd <sub>0.9</sub> /rGO   | 333       | 1 M FA / SF | 2739 <sup>b</sup>     | 15        |
| Pd <sub>0.6</sub> Ag <sub>0.4</sub> @ZrO <sub>2</sub> /C/rGO | 333       | 1 M FA / SF | 4300 <sup>b</sup>     | 38        |
| Au@SiO <sub>2</sub>  | 403       | 1 M FA      | 403 <sup>b</sup>      | 45        |
| Pd/C   | 293       | 6.6 M       | 87 <sup>b</sup>       | 29        |

| Table S4 Catalytic activities of reported catalysts for the dehydrogenation of formic acid. |
|---|
|---|

| CoAgPd/MIL-101  | 323 | 1.5 M FA / SF | 98 <sup>b</sup>   | 40 |
|---|-----|---------------|-------------------|----|
| AgPd/0.2CND/SBA-15  | 323 | 1.5 M FA / SF | 893 <sup>b</sup>  | 35 |
| Pd/XC-72R   | 333 | 2.6 M FA / SF | 7256 <sup>b</sup> | 30 |
| Au/m-ZrO <sub>2</sub>                                       | 353 | 10.5 M FA     | 660 <sup>b</sup>  | 46 |
| Au/SiO <sub>2</sub> -Schiff                                 | 323 | 10 M FA       | 4683 <sup>b</sup> | 47 |
| Pd <sub>60</sub> Au <sub>40</sub> /HPC-NH <sub>2</sub>      | 298 | 1 M FA        | 3763 <sup>b</sup> | 57 |
| Au <sub>0.5</sub> Pd <sub>0.5</sub> /NH <sub>2</sub> -N-rGO | 298 | 1 M FA        | 4446 <sup>b</sup> | 43 |
| Pd <sub>60</sub> Au <sub>40</sub> /ZrSBA-15-AP              | 298 | 2 M FA        | 1185 <sup>b</sup> | 41 |
| Au <sub>0.4</sub> Pd <sub>0.6</sub> /CBH-A                  | 298 | 1 M FA        | 5625 <sup>b</sup> | 42 |

a: TOF value was calculated based on the completion time of gas releasing.

b: Initial TOF was calculated based on the initial conversion of FA.

SF: Sodium Formate.