

## Enhanced performance of hydroxyl and cyano groups functionalized graphitic carbon nitride for efficient removal of crystal violet and methylene blue from wastewater

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### **Supporting Information**

**S1. Materials.** High purity 99.5%, 2,4,6-triazine and anhydrous potassium hydroxide (KOH, 99.95%) were provided by Sigma-Aldrich. Methylene blue (MB) and crystal violet (CV) were acquired from Thermo Fisher Co. (USA). All solutions were prepared using distilled water and all components were used without further purification.

**S2. Characterization.** The pristine g-C<sub>3</sub>N<sub>4</sub> and F/g-C<sub>3</sub>N<sub>4</sub> were characterized by x-ray Photoelectron Spectroscopy (XPS) using the Thermo Fisher ESCAlab 250, FT-IR spectroscopy using the Nicolet-Nexus 670 FTIR spectrometer (4 cm<sup>-1</sup> resolution and 32 scan), X-ray diffraction using an X'Pert Philips Materials Research Diffractometer, and SEM with a Hitachi SU-70 FE-SEM.

### **S3.**

The PFO model usually predicts the behavior at the initial stage of the adsorption process, while PSO model predicts the behavior at all stages of the adsorption process<sup>1</sup>.

Pseudo-first-order kinetic model:

$$\log(q_e - q_t) = \log q_e - \frac{K_1 t}{2.303} \quad (3)$$

Pseudo-second-order kinetic model:

$$\frac{t}{q_t} = \frac{1}{K_2 q_e^2} + \frac{t}{q_e} \quad (4)$$

Where  $k_1$  ( $\text{min}^{-1}$ ) and  $k_2$  ( $\text{g mol}^{-1} \text{ min}^{-1}$ ) are the rate constants.  $q_t$  and  $q_e$  are the adsorption uptake of heavy metal at time  $t$  (min) and at equilibrium. Where  $k_1$  ( $\text{min}^{-1}$ ) and  $k_2$  ( $\text{g mol}^{-1} \text{ min}^{-1}$ ) are the rate constants.  $q_t$  and  $q_e$  are the adsorption uptake of heavy metal at time  $t$  (min) and at equilibrium.

#### S4.

The Langmuir and Freundlich isotherm models are two extensively used mathematical models. The Langmuir model assumes a monolayer coverage and that all the adsorbent sorption sites are the same while the Freundlich isotherm model assumes that the coverage is multilayer and that all the adsorption sites are heterogenous. The Langmuir and Freundlich models are presented as Eq.(1) and Eq. [2], respectively, as follows:<sup>2-3</sup>

$$\ln q_e = \ln K_f + \frac{1}{n} \ln C_e \quad (1)$$

$$\frac{C_e}{q_e} = \frac{1}{b Q_0} + \frac{C_e}{Q_0} \quad (2)$$

Where  $q_e$ ,  $C_e$ ,  $b$ , and  $Q_0$  are the equilibrium adsorption capacity, the equilibrium concentration of the metal ions, the Langmuir constant, and the Langmuir monolayer adsorption capacity, respectively.  $1/n$  and  $K_f$  are the adsorption intensity and the Freundlich constant, respectively.

Moreover, the essential feature of the Langmuir isotherm can be defined as RL parameter given by Eq. (5).<sup>4</sup>

$$R_L = \frac{1}{1 + bc_0} \quad (5)$$

The separation factor ( $R_L$ ) can be used to indicate the shape of the adsorption behavior to be either irreversible ( $R_L = 0$ ), linear ( $R_L = 1$ ), unfavorable ( $R_L > 1$ ), or favorable ( $0 < R_L < 1$ ).<sup>5</sup>

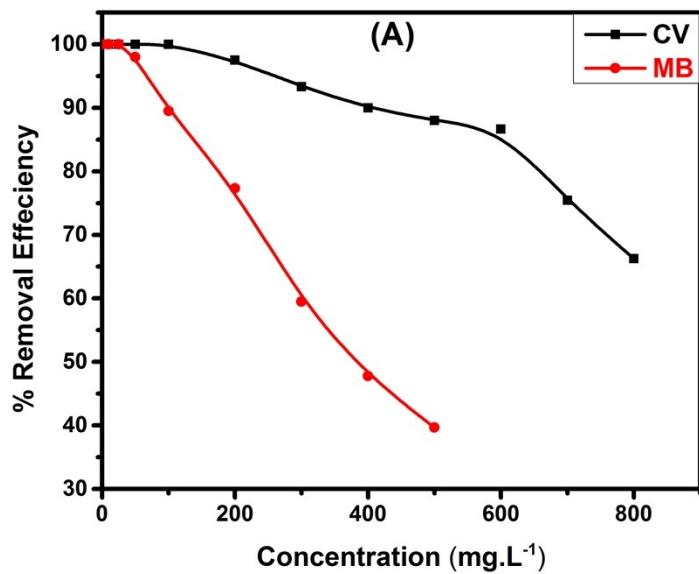


Figure S1: Dependence of the removal efficiency of CV and MB onto f/g-CN on the initial concentration. [Conditions:  $C_o = 0.5\text{-}800 \text{ mg/L}$  (CV),  $0.5\text{-}600 \text{ mg/L}$  (MB) ; pH = 8; Adsorbent dosage = 0.01 g/ 10 ml; T= 298 K].

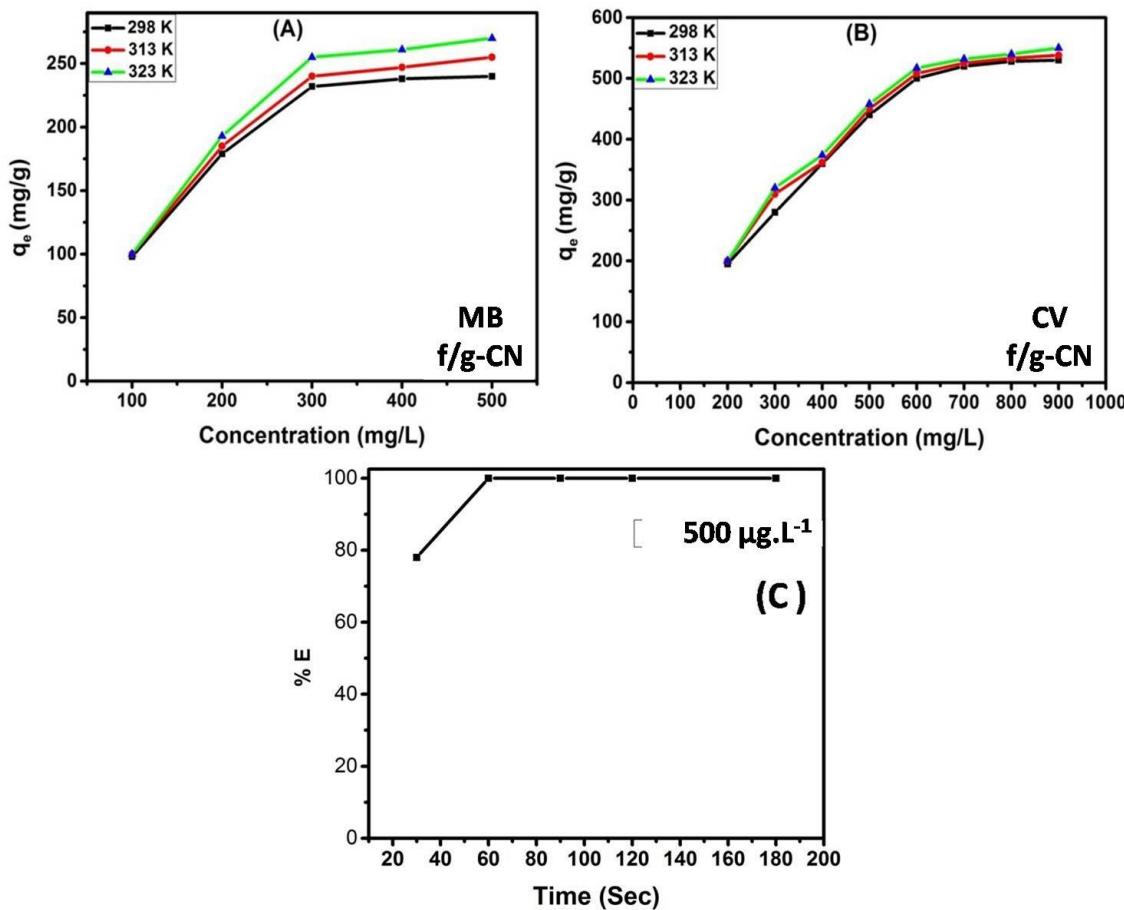


Figure S2: Effect of temperature on MB and CV adsorption onto f/g-CN (A, and B); Effect of contact time on the removal of 500  $\mu\text{g.L}^{-1}$  CV onto f/g-CN (C).

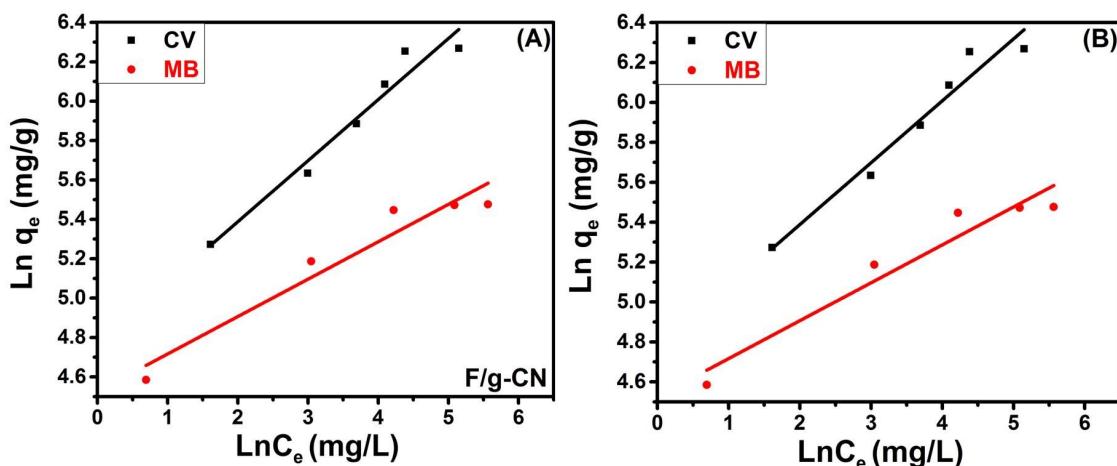


Figure S3: (A) PFO kinetic model and (B) Freundlich adsorption isotherm model.

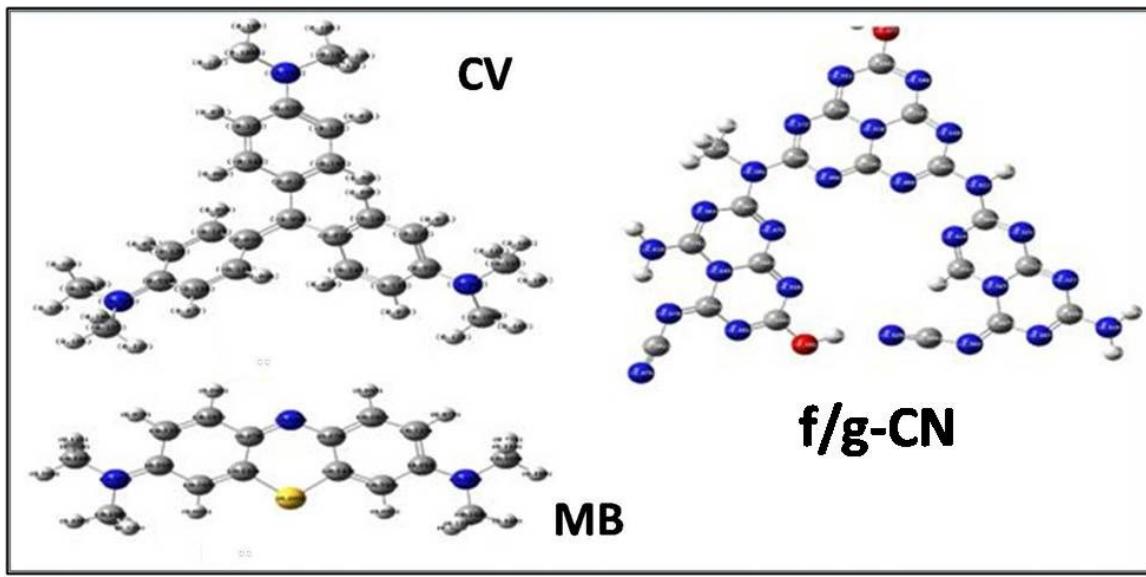


Figure S4: Electron density charge distribution of the MB, CV and f/g-CN.

**Table S1.** The elemental composition of g-CN and f/g-CN from XPS analysis.

Sample	C (%)	O (%)	N (%)
g-CN	45.98	2.62	51.4
f/g-CN	58.23	11.55	30.22

**Table S2.** The comparison of adsorption capacities of MB and CV through various adsorbents.

Dye	Adsorbent	Adsorption capacity (mg/g)	Reference
MB	NbO/g-C <sub>3</sub> N <sub>4</sub>	373.1	6
	g-C <sub>3</sub> N <sub>4</sub> /AFP	221.85	7
	GO/g-C <sub>3</sub> N <sub>4</sub> -Fe <sub>3</sub> O <sub>4</sub>	187.36	8
	CMC/PAA/GO	138	9
	CMC/Chitosan/GO	122.0	10
	C-C <sub>3</sub> N <sub>4</sub> -20	57.87	11
	Chitosan modified zeolite	37.04	12
	g-C <sub>3</sub> N <sub>4</sub> @NiCoLDH	25.16	13
	g-CN	28.9	This study
	f/g-CN	239.0	This study
	Biogenic β-CD functionalized	454.5	<sup>14</sup>

Fe° NPs			
CV	Fe <sub>3</sub> O <sub>4</sub> coated biochar	349.4	15
	Carboxylate-functionalized cellulose nanocrystals	348.9	16
	BAB-AT	280.0	17
	Alginate/pectin nanocomposite	251.4	18
	Magnetic nanoparticle-modified kaolin	247.7	19
	Surfactant modified magnetic nanoadsorbent	166.7	20
	Polydopamine/montmorillonite-embedded pullulan hydrogels	112.45	21
	AC-Fe <sub>2</sub> O <sub>3</sub> NPLs	16.5	22
	AA-AMP copolymer adsorbent	9.8	23
	g-CN	163.0	This study
	f/g-CN	532.0	This study

**Table S3.** Electronegativity and electrophilicity of MB, CV, and f/g-CN.

Component	MB	CV	f/g-CN
Electronegativity ( $\chi$ )	1.874	1.680	4.716
Electrophilicity ( $\omega$ )	0.981	0.960	7.011

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