

Electronic Supplementary Information

Synergistic catalysis in Ni/ZrO_x for hydrogen production from hydrolysis of ammonia borane

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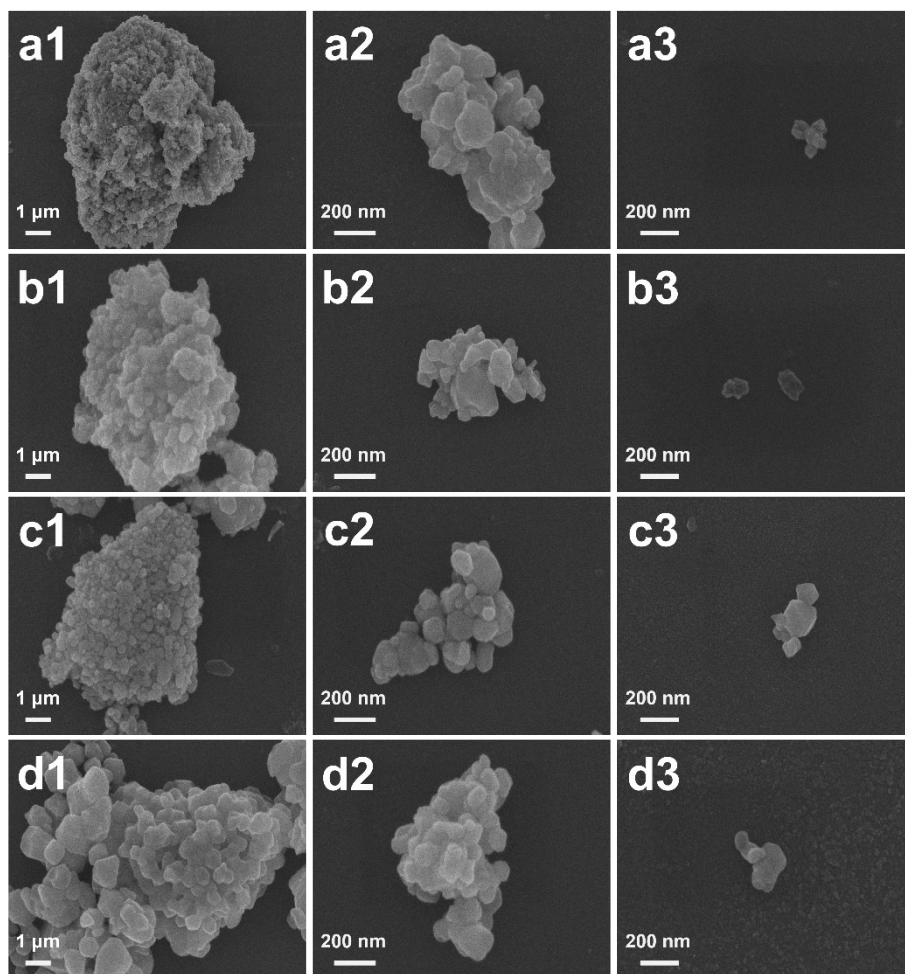


Fig. S1. SEM images of the as-synthesized ZrO_x-T samples: (a1–a3) ZrO_x-300, (b1–b3) ZrO_x-400, (c1–c3) ZrO_x-500 and (d1–d3) ZrO_x-600, respectively.

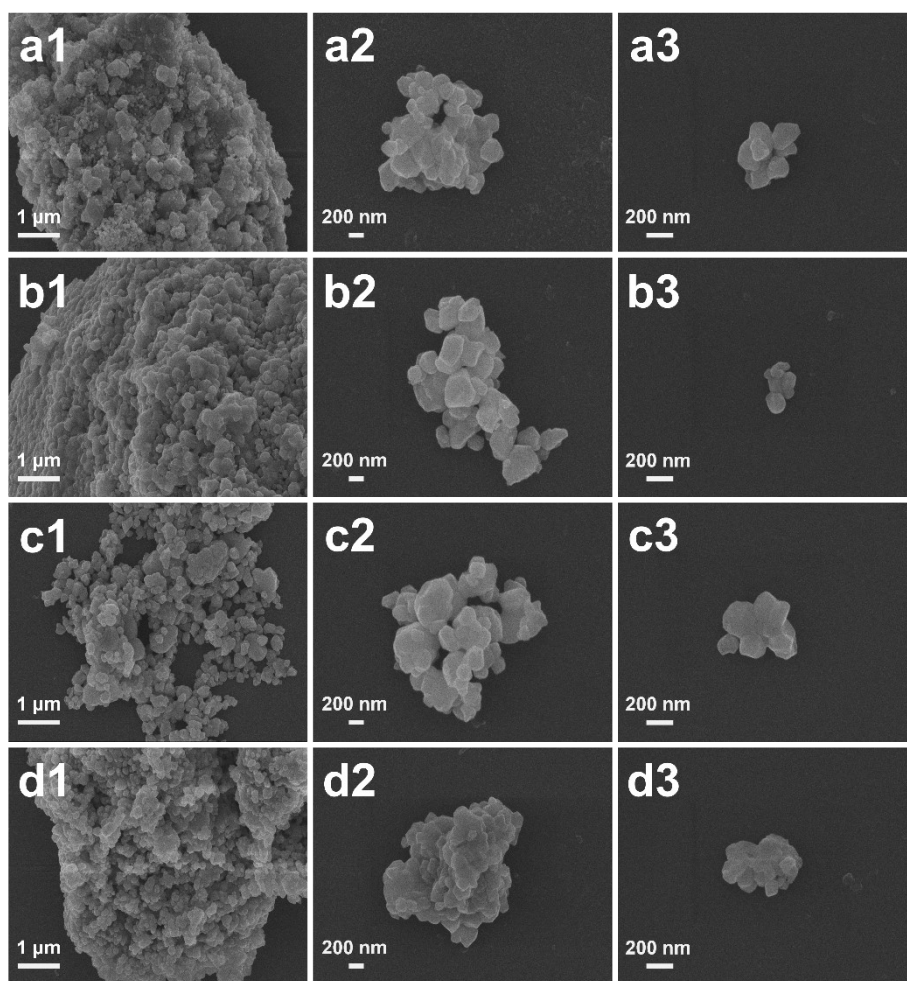


Fig. S2. SEM images of the as-synthesized Ni/ZrO_x-T samples: (a1–a3) Ni/ZrO_x-300, (b1–b3) Ni/ZrO_x-400, (c1–c3) Ni/ZrO_x-500 and (d1–d3) Ni/ZrO_x-600, respectively.

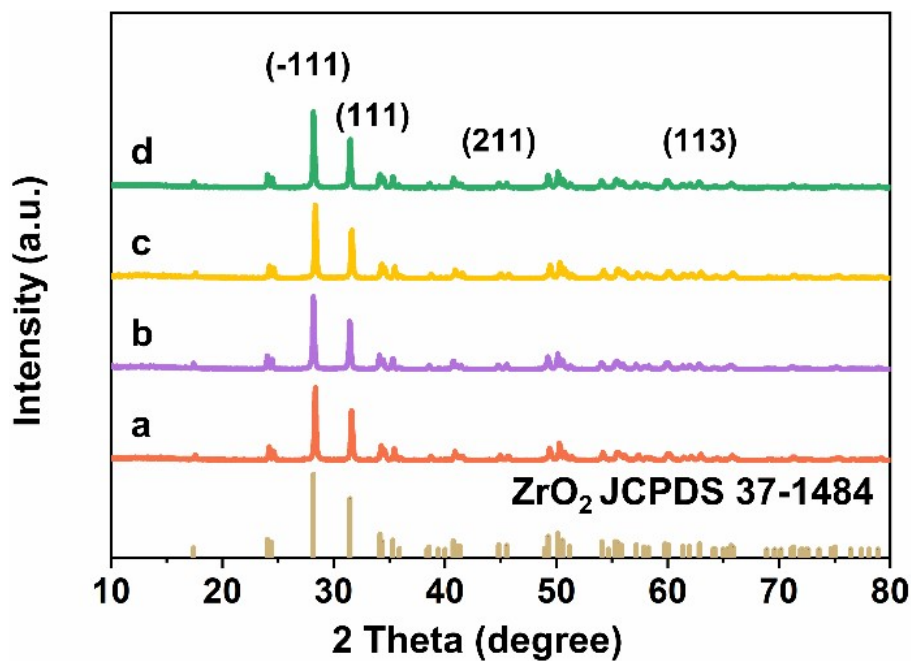


Fig. S3. XRD patterns of the as-synthesized ZrO_x-T samples: (a) ZrO_x-300, (b) ZrO_x-400, (c) ZrO_x-500 and (d) ZrO_x-600. XRD standard card for ZrO₂ is shown in the lower part of panel: ZrO₂-PDF#37-1484.

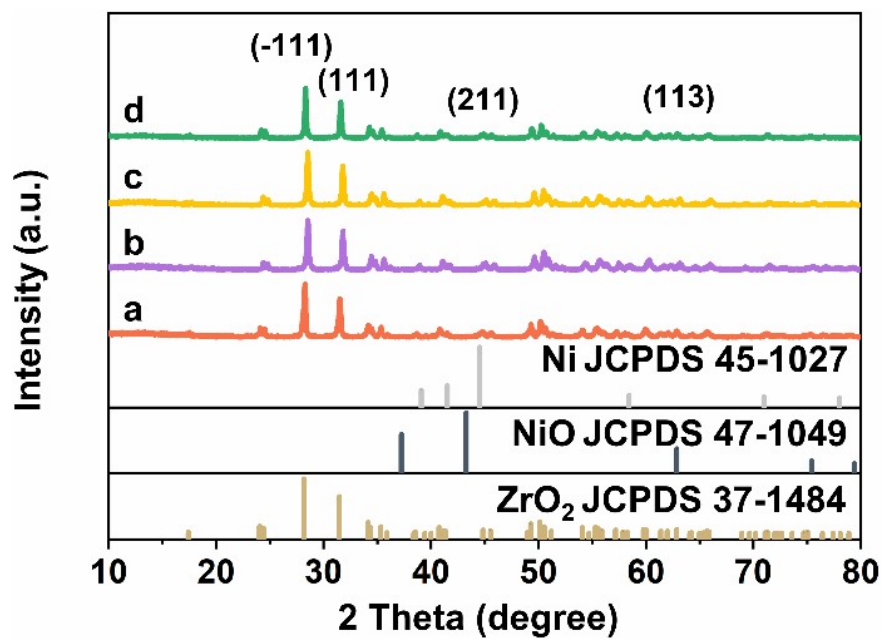


Fig. S4. XRD patterns of the as-synthesized Ni/ZrO_x-T samples: (a) Ni/ZrO_x-300, (b) Ni/ZrO_x-400, (c) Ni/ZrO_x-500 and (d) Ni/ZrO_x-600. XRD standard cards for Ni, NiO and ZrO₂ are shown in the lower part of the panel: Ni-PDF#45-1027, NiO-PDF#47-1049 and ZrO₂-PDF#37-1484.

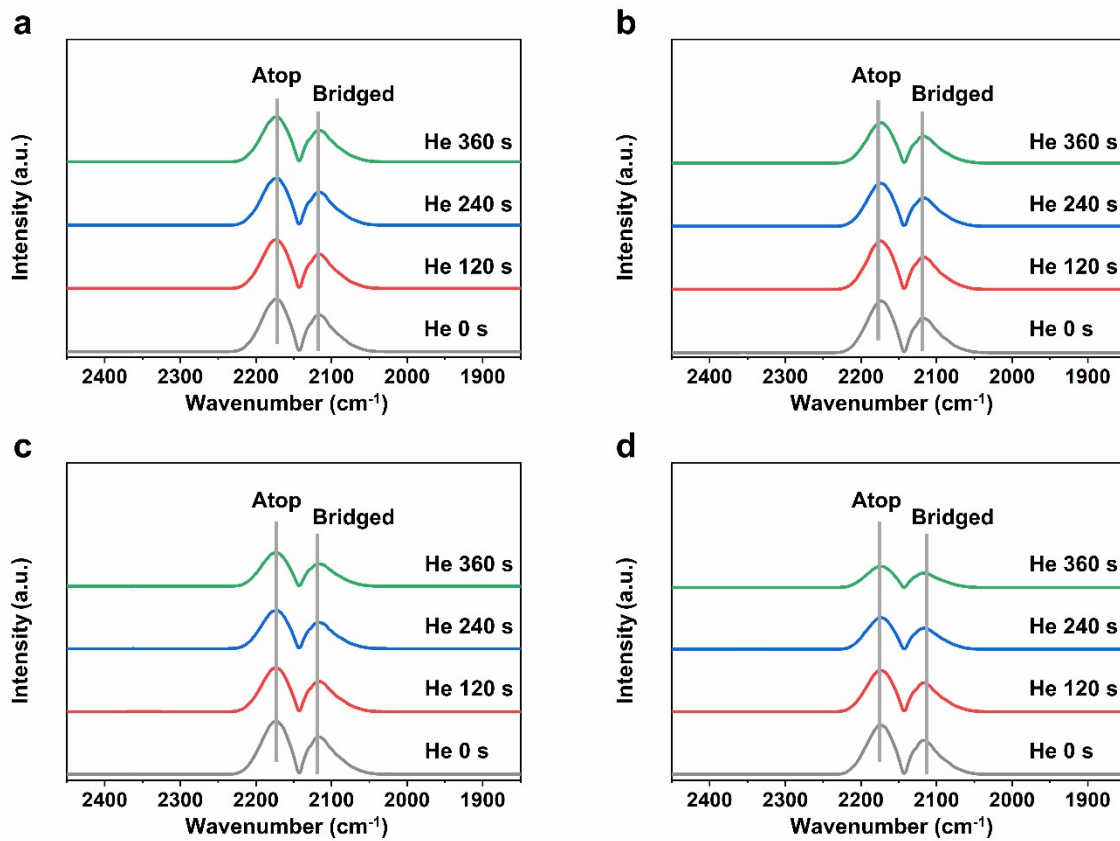


Fig. S5. *In situ* FT-IR spectra of CO chemisorption on (a) Ni/ZrO_x-300, (b) Ni/ZrO_x-400, (c) Ni/ZrO_x-500 and (d) Ni/ZrO_x-600 by flowing He as a purge gas after 0, 120, 240 and 360 s, respectively.

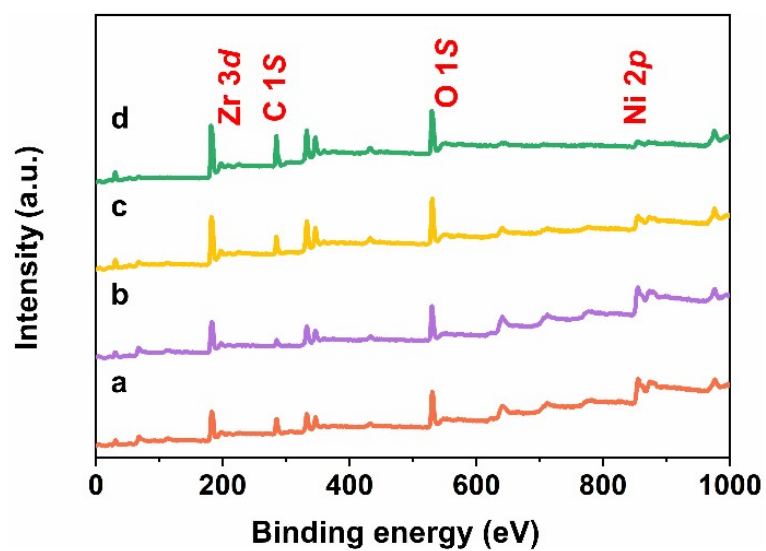


Fig. S6. XPS spectra of (a) Ni/ZrO_x-300, (b) Ni/ZrO_x-400, (c) Ni/ZrO_x-500 and (d) Ni/ZrO_x-600, respectively.

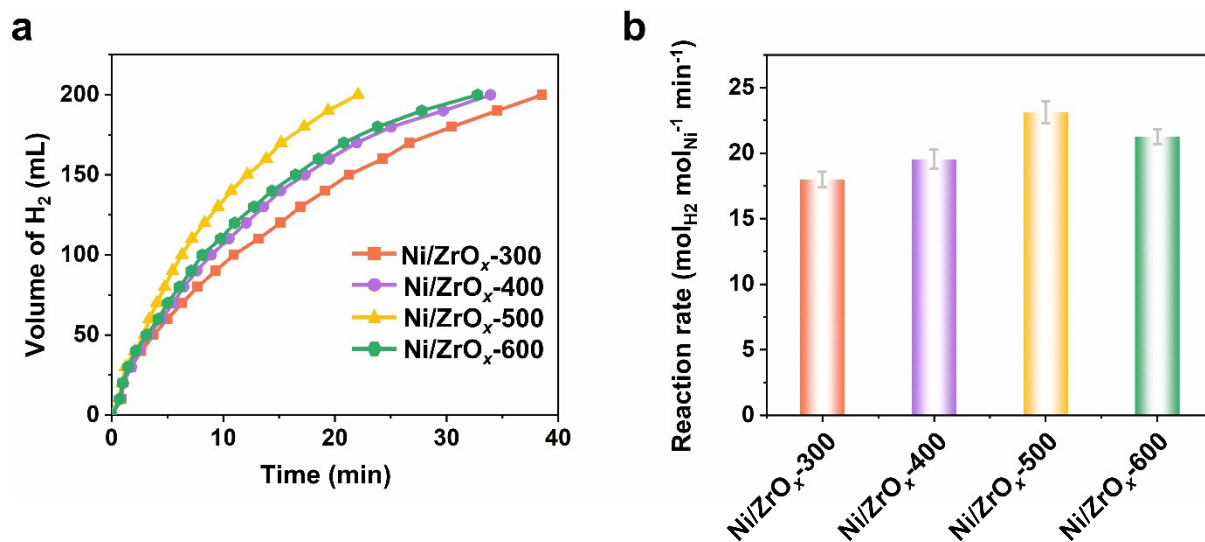


Fig. S7. (a) Plot of volume of H₂ vs. reaction time without NaOH for Ni/ZrO_x-T samples, and (b) the corresponding reaction rate values. Reaction conditions: (a) AB: 3.0 mmol, NaOH: 0 mmol, H₂O: 10 mL, catalyst: 40.0 mg, temperature: 25 °C.

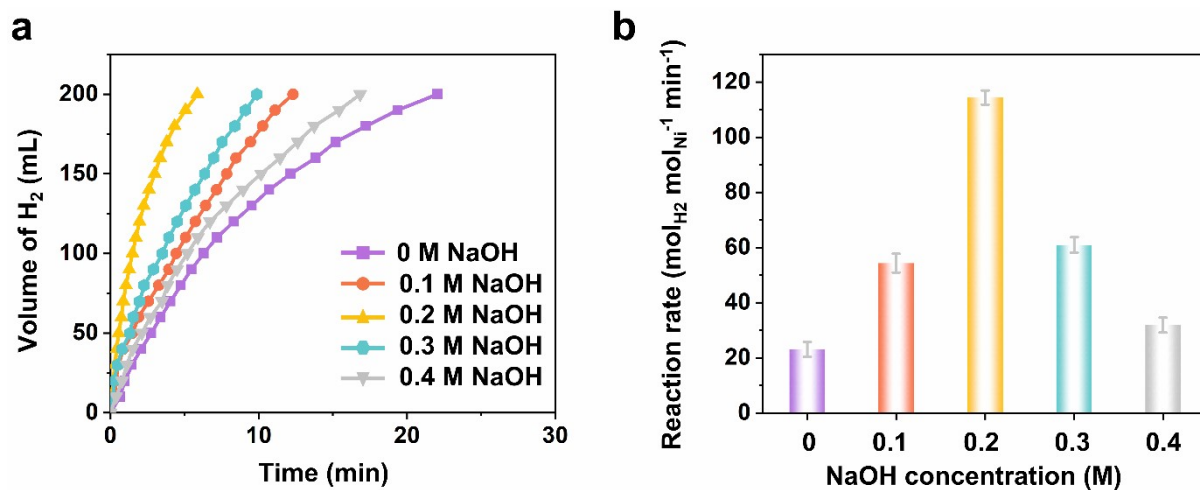


Fig. S8. (a) Plot of volume of H₂ vs. reaction time for Ni/ZrO_x-500 with different NaOH concentrations (0–4 M). (b) Effect of NaOH concentration on the reaction rate for Ni/ZrO_x-500. Reaction conditions: (a) AB: 3.0 mmol, NaOH: 0–40 mmol, H₂O: 10 mL, catalyst: 40.0 mg, temperature: 25 °C.

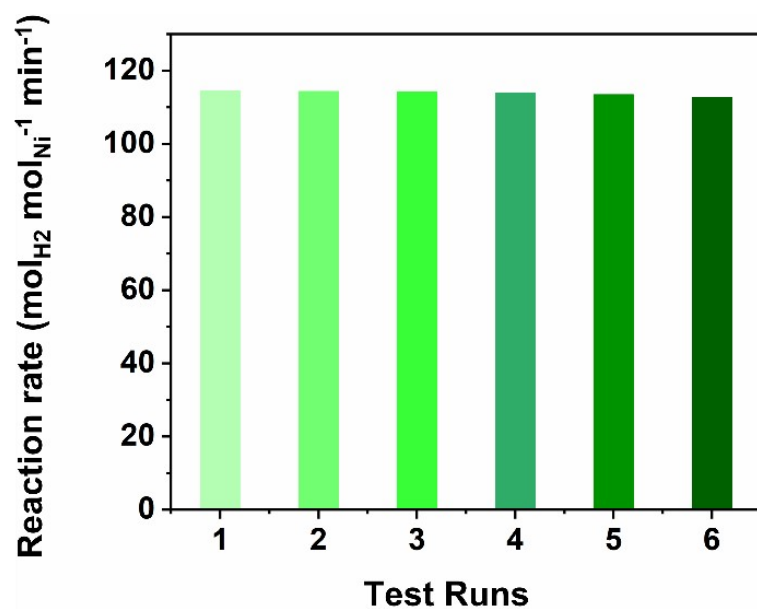


Fig. S9. Reaction rate of AB hydrolysis vs. recycling times over Ni/ZrO_x-500.

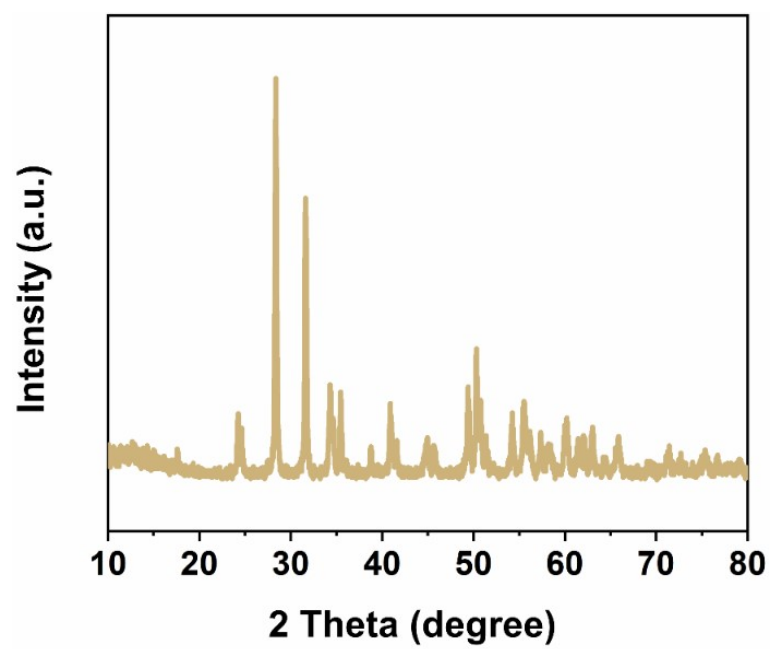


Fig. S10. XRD pattern of the used Ni/ZrO_x-500 sample.

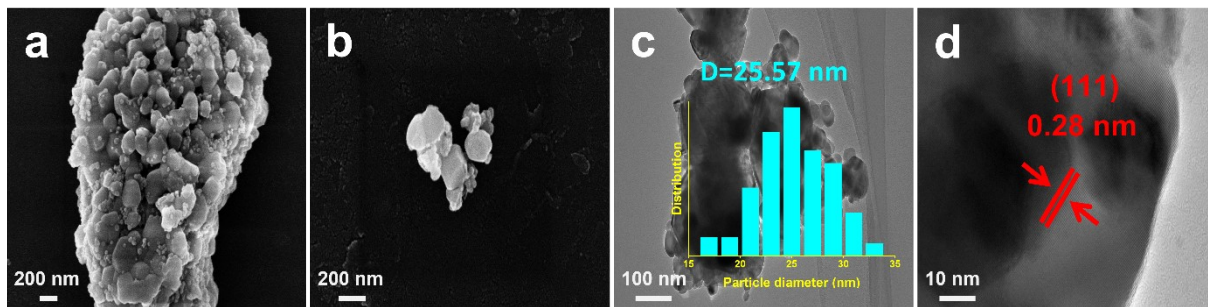


Fig. S11. (a–b) SEM images and (c–d) HR-TEM images of the used Ni/ZrO_x-500 sample with corresponding HR-TEM lattice fringe images.

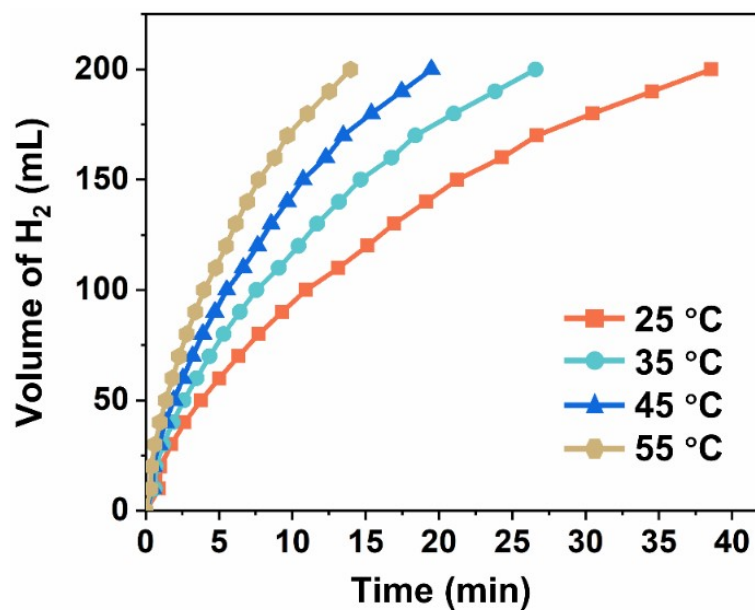


Fig. S12. Plot of volume of H₂ vs. reaction time for Ni/ZrO_x-300 under different reaction temperature (25–55 °C).

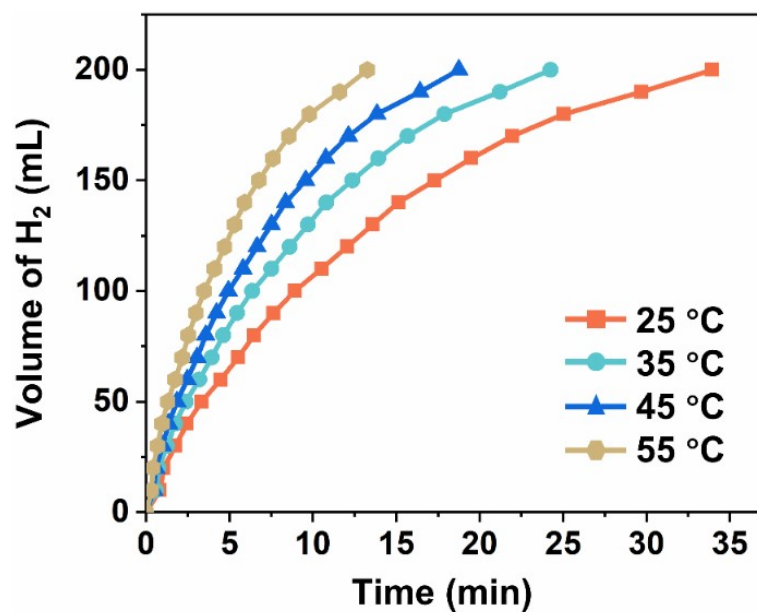


Fig. S13. Plot of volume of H₂ vs. reaction time for Ni/ZrO_x-400 under different reaction temperature (25–55 °C).

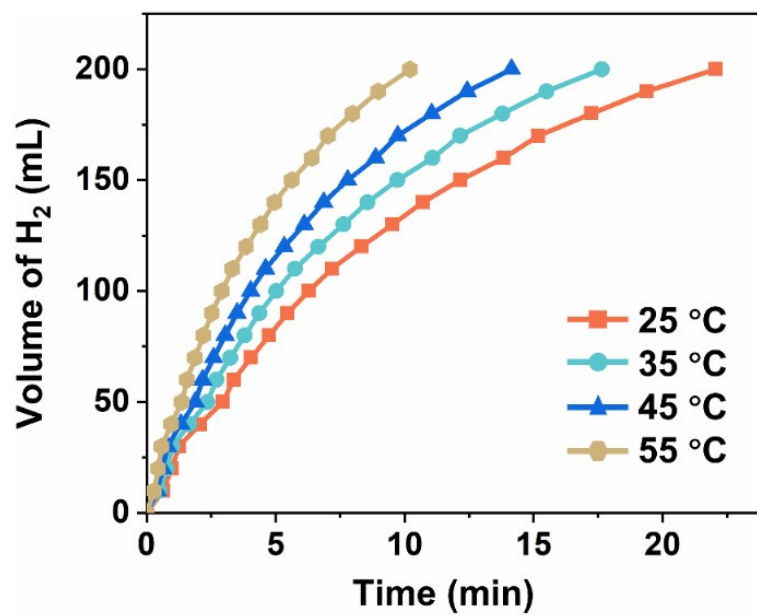


Fig. S14. Plot of volume of H₂ vs. reaction time for Ni/ZrO_x-500 under different reaction temperature (25–55 °C).

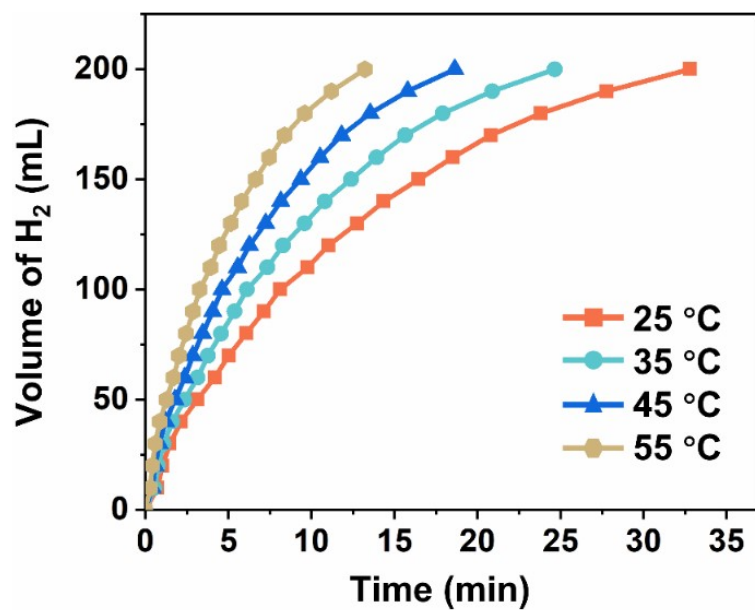


Fig. S15. Plot of volume of H₂ vs. reaction time for Ni/ZrO_x-600 under different reaction temperature (25–55 °C).

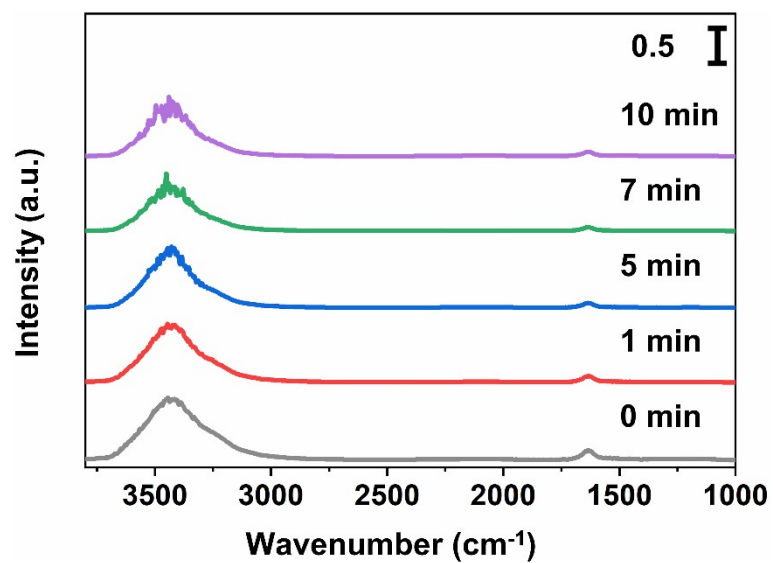


Fig. S16. *In situ* FT-IR spectra of AB hydrolysis reaction on ZrO_x-500 sample recorded in 3800–1000 cm⁻¹ by flowing AB solution as a reaction gas and He as a purge gas after 0, 1, 5, 7 and 10 min, respectively.

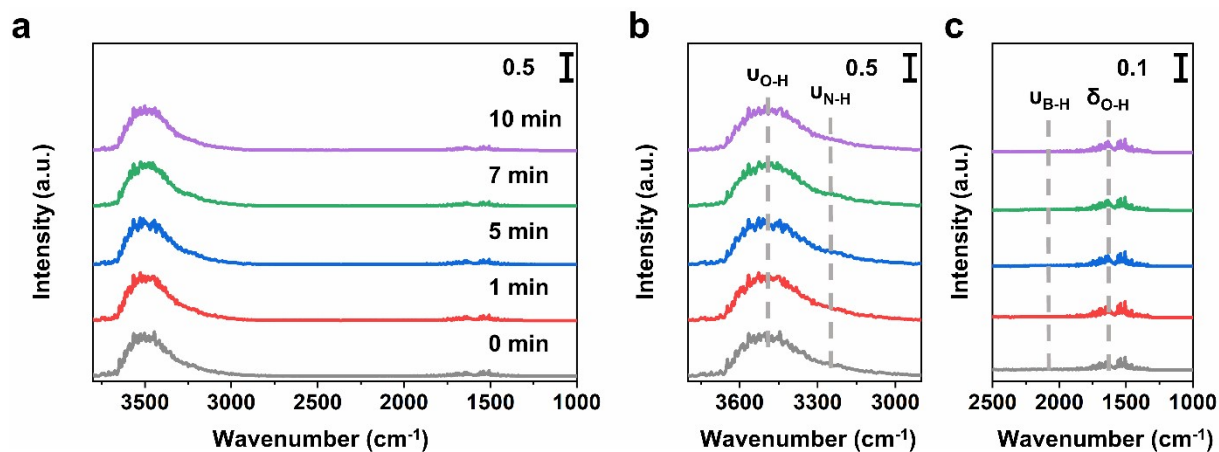


Fig. S17. *In situ* FT-IR spectra of AB hydrolysis reaction on KBr sample recorded in (a) 3800–1000 cm⁻¹, (b) 3800–2900 cm⁻¹ and (c) 2500–1000 cm⁻¹ by flowing AB solution as a reaction gas and He as a purge gas after 0, 1, 5, 7 and 10 min, respectively.

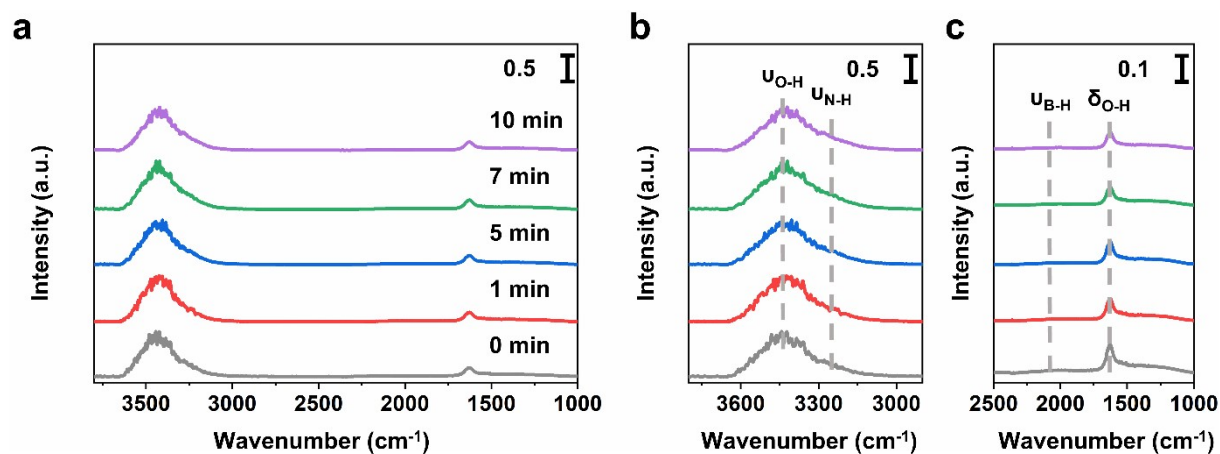


Fig. S18. *In situ* FT-IR spectra of AB hydrolysis reaction on Ni/ZrO_x-300 sample recorded in (a) 3800–1000 cm⁻¹, (b) 3800–2900 cm⁻¹ and (c) 2500–1000 cm⁻¹ by flowing AB solution as a reaction gas and He as a purge gas after 0, 1, 5, 7 and 10 min, respectively.

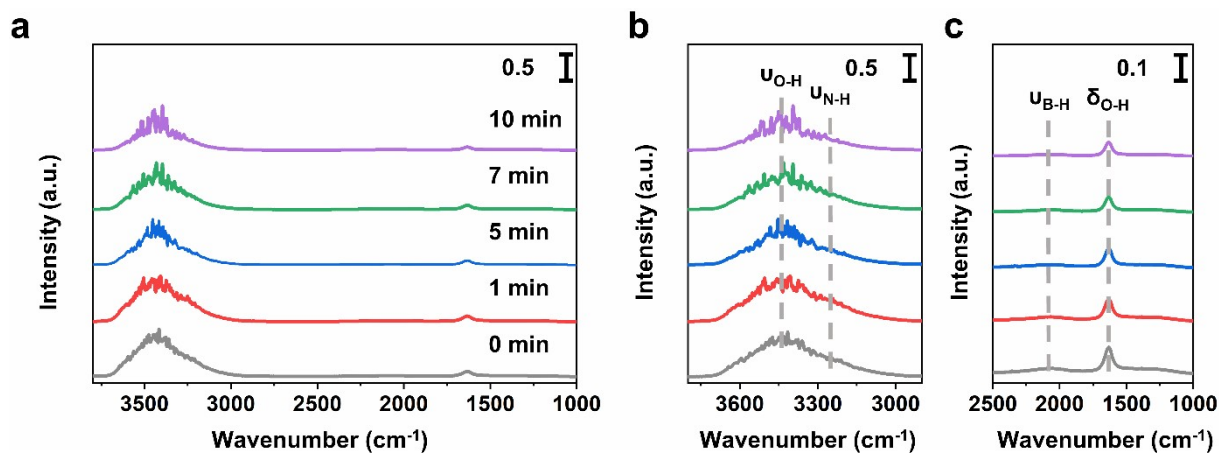


Fig. S19. *In situ* FT-IR spectra of AB hydrolysis reaction on Ni/ZrO_x-400 sample recorded in (a) 3800–1000 cm⁻¹, (b) 3800–2900 cm⁻¹ and (c) 2500–1000 cm⁻¹ by flowing AB solution as a reaction gas and He as a purge gas after 0, 1, 5, 7 and 10 min, respectively.

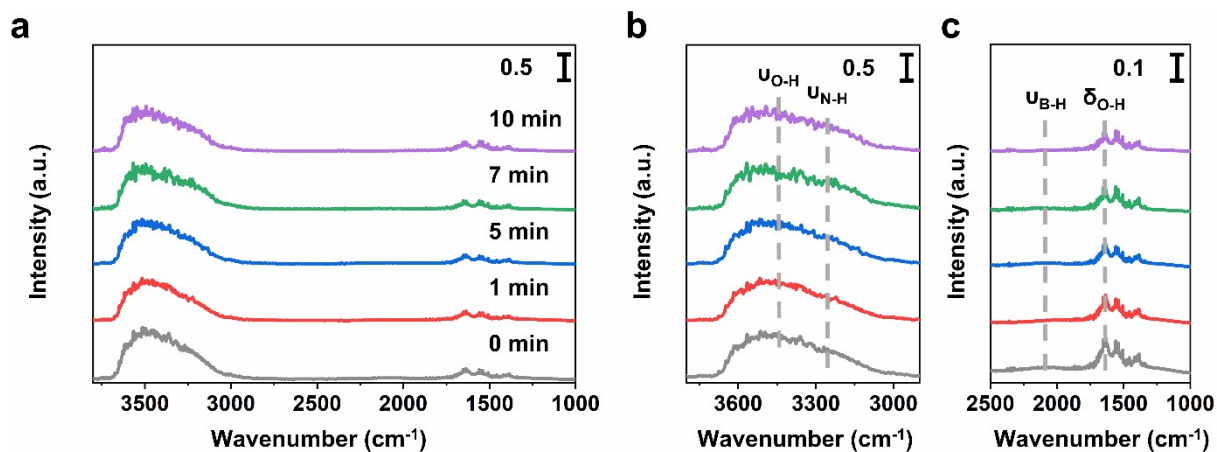


Fig. S20. *In situ* FT-IR spectra of AB hydrolysis reaction on Ni/ZrO_x-600 sample recorded in (a) 3800–1000 cm⁻¹, (b) 3800–2900 cm⁻¹ and (c) 2500–1000 cm⁻¹ by flowing AB solution as a reaction gas and He as a purge gas after 0, 1, 5, 7 and 10 min, respectively.

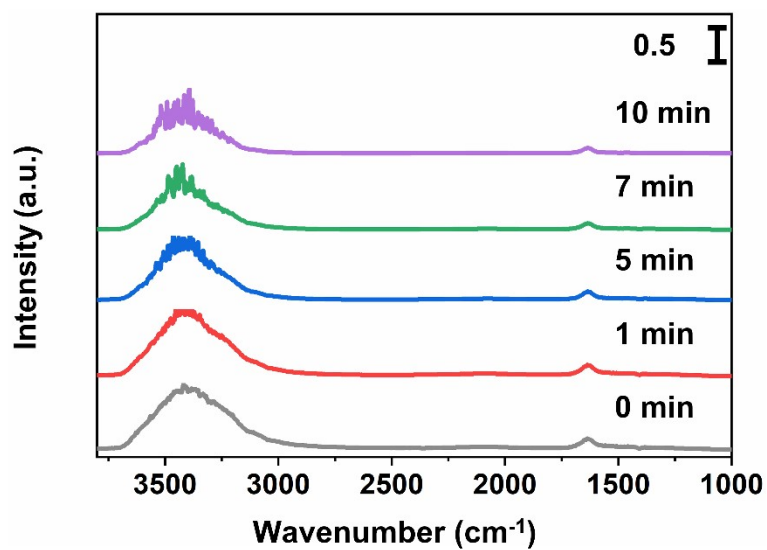


Fig. S21. *In situ* FT-IR spectra of AB hydrolysis reaction on Ni/ZrO_x-500 sample recorded in 3800–1000 cm⁻¹ by flowing AB solution as a reaction gas and He as a purge gas after 0, 1, 5, 7 and 10 min, respectively.

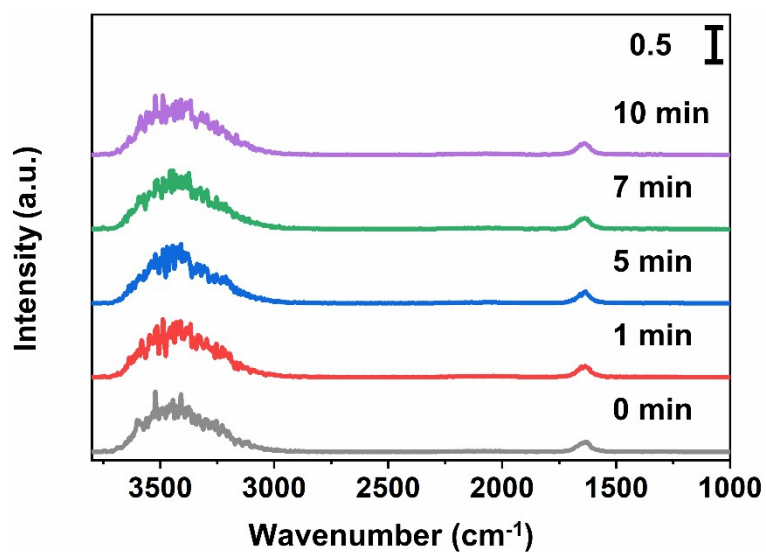


Fig. S22. *In situ* FT-IR spectra of ZrO_x-500 sample recorded in 3800–1000 cm⁻¹ by flowing pure H₂O with He as a purge gas after 0, 1, 5, 7 and 10 min, respectively.

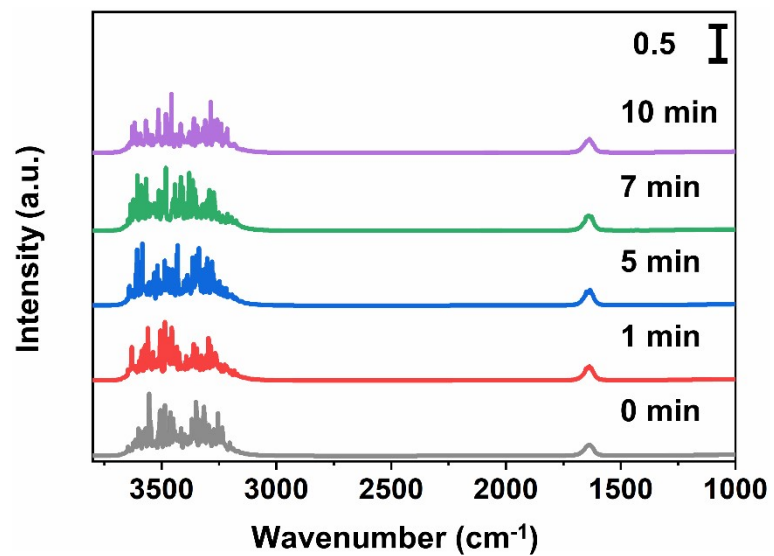


Fig. S23. *In situ* FT-IR spectra of Ni/ZrO_x-500 sample recorded in 3800–1000 cm⁻¹ by flowing pure H₂O with He as a purge gas after 0, 1, 5, 7 and 10 min, respectively.

Table S1. Physicochemical properties of Ni/ZrO_x-T samples

Entry	Catalyst	Ni content (wt. %) ^a	Ni content in the filtration liquid (wt. %) ^a	Zr content in the filtration liquid (wt. %) ^a	Mean particle size of Ni (nm) ^b	Theoretical dispersion degree of Ni ^c
1	Ni/ZrO _x -300	4.579	/	/	22.27	2.28%
2	Ni/ZrO _x -400	4.667	/	/	22.35	2.27%
3	Ni/ZrO _x -500	4.453	/	/	23.20	2.19%
4	Ni/ZrO _x -600	4.516	/	/	28.33	1.79%

^a Content of Ni and Zr species was determined by inductively coupled plasma-atomic emission spectroscopy (ICP-AES).

^b Mean particle size of Ni was determined by HR-TEM analysis over 100 particles for each sample.

^c Theoretical dispersion of Ni was calculated based on the result of HR-TEM.

Table S2. Compositional properties of Ni/ZrO_x-T samples

Entry	Catalyst	Ni ²⁺ /(Ni ⁰ +Ni ²⁺) ratio ^a	Zr ³⁺ /(Zr ³⁺ +Zr ⁴⁺) ratio ^b	O _v /(O _v +O _l +O _s) ratio ^c
1	Ni/ZrO _x -300	42.10%	32.96%	19.88%
2	Ni/ZrO _x -400	47.28%	60.42%	26.91%
3	Ni/ZrO _x -500	58.13%	84.64%	38.01%
4	Ni/ZrO _x -600	50.41%	75.55%	34.89%

^a Ni²⁺/(Ni⁰+Ni²⁺) ratio was calculated from Ni 2*p* XPS spectra.

^b Zr³⁺/(Zr³⁺+Zr⁴⁺) ratio was calculated from Zr 3*d* XPS spectra.

^c O_v/(O_v+O_l+O_s) ratio was calculated from O 1*s* XPS spectra.

Table S3. Reaction rates for AB hydrolysis over Ni/ZrO_x-T and ZrO_x-T catalysts

Entry	Sample ^a	Reaction condition	Reaction rate (mol _{H₂} mol _{Ni} ⁻¹ min ⁻¹)
1	Ni/ZrO _x -300	0 M NaOH	17.99±0.60
2	Ni/ZrO _x -400	0 M NaOH	19.53±0.73
3	Ni/ZrO _x -500	0 M NaOH	23.13±0.83
4	Ni/ZrO _x -600	0 M NaOH	21.26±0.58
5	Ni/ZrO _x -500	0.1 M NaOH	54.38±3.41
6	Ni/ZrO _x -500	0.2 M NaOH	114.41±2.58
7	Ni/ZrO _x -500	0.3 M NaOH	60.93±2.77
8	Ni/ZrO _x -500	0.4 M NaOH	31.90±2.70
9	/	0.2 M NaOH	0±0
10	Ni/ZrO _x -300	0.2 M NaOH	38.68±3.64
11	Ni/ZrO _x -400	0.2 M NaOH	71.42±2.15
12	Ni/ZrO _x -600	0.2 M NaOH	85.89±3.92
13	ZrO _x -300	0.2 M NaOH	0±0
14	ZrO _x -400	0.2 M NaOH	0±0
15	ZrO _x -500	0.2 M NaOH	0±0
16	ZrO _x -600	0.2 M NaOH	0±0

^a Reaction conditions: AB: 3.0 mmol, H₂O: 10 mL, catalyst: 40.0 mg, temperature: 25 °C.

Table S4. Catalytic performance for AB hydrolysis over previously reported heterogeneous catalysts and this work

Entry	Catalyst	Temperature (K)	NaOH Concentration (M)	TOF (min ⁻¹)	<i>E_a</i> (kJ mol ⁻¹)	Ref.
1	Ni/ZrO _x -300	298	0.2	38.68±3.64 ^a 91.86±2.68 ^b	38.24	This work
2	Ni/ZrO _x -400	298	0.2	71.42±2.15 ^a 151.03±3.41 ^b	31.97	This work
3	Ni/ZrO _x -500	298	0.2	114.41±2.58 ^a 196.82±2.58 ^b	21.26	This work
4	Ni/ZrO _x -600	298	0.2	85.89±3.92 ^a 170.39±2.77 ^b	26.80	This work
5	CoNi/α-MoC	298	0.5	321.1 ^b	/	1
6	10Ni30Mo _x C/γ-Al ₂ O ₃	298	1	75.1 ^a	33.12	2
7	hcp-CuNi/C	300	1	22.64 ^a	29.92	3
8	Ni/KB	298	0	7.47 ^a	/	4
9	Ni/CeO ₂	298	0	1.7 ^a	25	5
10	Ni/CNTs	298	0	26.2 ^a	32.3	6
11	NiNPs/ZIF-8	298	0.3	85.7 ^a	42.70	7
12	Ni/Ti ₃ C ₂ Tx-4	298	0	161.0 ^a	59.3	8
13	rGO/CoNi-N	298	0	126 ^a	32.8	9
14	Ni-CeOx/Graphene	298	0	68.2 ^a	28.9	10
15	Ni NPs@3D-(N)GFs	303	0	41.7 ^a	/	11
16	Ni/SiO ₂	303	0	13.2 ^a	34.0	12

^a the initial TOF value was calculated based on the following equation: TOF (h⁻¹) = (converted substrate (mmol))/(total metal amount (mmol))(reaction time (h)).

^b the initial TOF value was calculated based on the following equation: TOF (h⁻¹) = (converted substrate (mmol))/(surface atoms of active metal (mmol))(reaction time (h)).

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