Supporting Information

Favorably Adjusting the Pore Characteristics of Copper Sulfide by Template Regulation for Vapor-Phase Elemental Mercury Immobilization

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Kinetic Simulation

The pseudo-first order kinetic model was used to predict the Hg^0 adsorption capacity based on an ~80% breakthrough dataset. The Hg^0 adsorption rate was proportional to the difference between the equilibrium capacity and the adsorbed amount at any time, as described as follows:

$$\frac{\mathrm{d}Q_t}{\mathrm{d}t} = k_1(Q_e - Q_t) \tag{S1}$$

Equation (3) could be modified to the following equation based on the initial conditions of t=0, $Q_t=0$:

$$Q_{t} = Q_{e}(1 - e^{-k_{1}t})$$
(S2)

where the pseudo-first-order kinetic constant (k_1, \min^{-1}) can be determined by fitting the adsorption breakthrough curve.

Besides, the pseudo-second-order kinetic model was also adopted to simulate the Hg⁰ adsorption behavior, which could be described by equation (S3):

$$\frac{dQ_t}{dt} = k_2 (Q_e - Q_t)^2 \tag{S3}$$

Equation (S3) could be modified to the following equation based on the initial conditions of t=0, Q_t =0:

$$\frac{t}{Q_t} = \frac{1}{k_2 Q_e^2} + \frac{1}{Q_e} t$$
(S4)

where the pseudo-second-order kinetic constant $(k_2, mg g^{-1} min^{-1})$ can be determined by fitting the adsorption breakthrough curve.

Hg-TPD Test

First, the fresh sorbent was pretreated at its optimal reaction temperature (75 °C) under ~100 μ g m⁻³ carried by N₂ for a continuous 30 min. Subsequently, the inlet Hg⁰ was cut off, and the Hg-laden sorbent was purged by pure N₂ at a same temperature until the outlet Hg⁰ equaling to zero. Then, the temperature stepwise increased from 75 to 350 °C with the heating rate of 10 °C min⁻¹. During this process, the desorbed/decomposed mercury was continuously recorded by the on-line mercury analyzer (VM3000, Mercury Instrument, Inc.).

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Experiments	Materials	Carrier gas (1L min ⁻¹)	Temperature (°C)	
Set I	Cu-BTC CuS-BTCs Nano-CuS	Pure N ₂	75	
Set II	9CuS-BTC	Pure N ₂	25-100	
Set III	9CuS-BTC	Pure N ₂	75	
Set IV	9CuS-BTC	Pure N_2 $N_2 + 5\% O_2$ $N_2 + 5\% O_2 + 100 \text{ ppm SO}_2$ SFG	75	

Table S1. Experimental conditions

SFG: Simulated flue gas (5% $O_2,\,100$ ppm SO_2 and 8% H_2O carried by $N_2)$

Sorbents	Carrier gas	Inlet Hg ⁰ concentration (μg m ⁻³)	Optimal temperature (°C)	Hg ⁰ adsorption capacities (mg g ⁻¹)	Hg ⁰ adsorption rates (μg g ⁻¹ min ⁻¹)	Reference
CuS-BTC	N ₂	100	75	208.50	97.30	This work
FeWS _x /TiO ₂	N_2	4300	100	9.00	25.00	[S1]
[MoS ₄] ²⁻ /CoFe-LDH	$N_2 + 4\% O_2$	350	75	16.39	5.00	[S1]
Disordered MoS ₂	$N_2 + 6\% O_2 + 6\%$ SO_2	240	100	16.39	3.83	[S2]
Mn-SnS ₂	$N_2 + 5\% O_2$	300	150	0.57	9.45	[S1]
Fe-ZnS	Air	1600	20	8.65	4.82	[S1]
MoS_3/γ - Fe_2O_3	N_2	110	60	12.80	1.55	[S1]
Co ₉ S ₈ -PC	N_2	210	100	43.18	12.15	[S3]
MoS ₃ /TiO ₂	N_2	280	60	28.10	24.80	[S1]
Co _x Zn _{1-x} S	$N_2 + O_2$	1100	50	46.01	17.00	[S1]
ZnO@CuS	N_2	800	75	60.53	16.81	[S4]
Fe ₃ O ₄ @CuS	N_2	90	75	88.70	13.25	[S1]
nano-CuS	N_2	90	75	122.40	13.56	[S1]
Sulfurated Fe-Ti spinel	N_2	4300	60	48.60	43.30	[S1]
FeMoS _x /TiO ₂	N_2	4300	60	41.80	72.20	[S1]
Co_3S_4	N_2	1300	100	43.03	84.10	[S1]
Sulfureted MoO ₃ /Fe- Ti spinel	SFG	4300	60	66.30	93.30	[S1]

 Table S2. Performance comparison among benchmark metal sulfides

Simulated flue gas (SFG) contains N_2 , O_2 , SO_2 , and H_2O .

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Figure S1. XRD patterns of different samples



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24CuS-BTC



Figure S3. EDS line scanning of Cu-BTC, 9CuS-BTC, and 24CuS-BTC



Figure S4. EDS mappings of Cu-BTC, 9CuS-BTC, and 24CuS-BTC



Figure S5. The distribution of micropores in Cu-BTC



Figure S6. A diagrammatical illustration on the transformation of Cu-BTC to 24CuS-BTC





24CuS-BTC







Figure S7. Comparison between the high-resolution SEM images of 9CuS-BTC and 24CuS-BTC



Figure S8. The breakthrough curve of 9CuS-BTC



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