# **Electronic Supplementary Information (ESI)**

Facile Synthesis of Fe<sub>2</sub>P/Co Embedded Trifunctional Electrocatalyst for High-Performance Anion Exchange Membrane Fuel Cells, Rechargeable Zn-Air Batteries and Overall Water Splitting

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## **Experimental section**

#### Materials

All chemicals were from commercial and used without further purification. Zinc nitrate hexahydrate  $(Zn (NO_3)_2 \cdot 6H_2O, 98\%)$  and Pt/C catalysts (20 wt% Pt loading on an activated carbon support) were obtained from Alfa Aesar. IrO<sub>2</sub> and 2-methylimidazole (98%) were purchased from Aladdin. Cobalt nitrate hexahydrate (Co  $(NO_3)_2 \cdot 6H_2O, 99\%$ ) and 1, 1'-Bis (diphenylphosphino) ferrocene (97%) were purchased from Macklin.

#### Synthesis of DPPF@ZnCo-ZIF

Firstly, 0.6158 g 2-methylimidazole was dissolved in 15 mL methanol by ultrasonic treatment for 2 min to prepare a homogeneous solution A. Secondly, 0.4462 g Zn  $(NO_3)_2 \cdot 6H_2O$ , 0.3274 g  $Co(NO_3)_2 \cdot 6H_2O$  and 0.2079 g DPPF were dissolved in 30 mL methanol with well stirring for 60min to prepare solution B. Then, solution A was quickly added to solution B and stirred strongly for 1.5 h at room temperature. Next, the mixture solution was transferred to a 100 mL stainless steel autoclave and heated at 120 ° C for 4 h. The prepared products were collected through the centrifugal process and washed with methanol for several times. Finally, they were dried in vacuum at 70 °C for 12 h to obtain DPPF@ZnCo-ZIF. ZnCo-ZIF and DPPF@Zn-ZIF were also synthesized via similar procedure without adding DPPF or Co  $(NO_3)_2 \cdot 6H_2O$ , respectively.

### Synthesis of Fe<sub>2</sub>P/Co@NPC

The resulting powder DPPF@ZnCo-ZIF, ZnCo-ZIF and DPPF@Zn-ZIF were calcined under Ar at 950 °C (ramp rate: 5 °C min<sup>-1</sup>) for 3 h separately and then cooled to room temperature. The Fe<sub>2</sub>P/Co@NPC, Co@NC and Fe<sub>2</sub>P@NPC were collected without further treatment. To determine the optimum conditions for the formation of Fe<sub>2</sub>P/Co@NPC catalysts, different pyrolysis temperatures

(850, 950, 1050 °C) were also examined denoted as  $Fe_2P/Co@NPC -X$  (X =850,950,1050). The  $Fe_2P/Co@NPC$  mentioned below refers to the sample synthesized with the temperature at 950 °C in particular.

#### Structural characterization of the samples

SEM and TEM images of the samples were received by HITACHI S-4800 and TECNAI G2 F20 microscopes, respectively. PXRD were performed on a D8 ADVANCE X-ray diffractometer (Cu Kα radiation as source). The pore structure was investigated by N<sub>2</sub> adsorption-desorption measurements on an ASAP 2460 instrument. XPS measurements were conducted on the Thermo Fisher ESCALAB 250 with an A1 Kα X-ray source. In order to determine the element contents, ICP measurements were conducted on Inductively Coupled Plasma Optical Emission Spectrometer (ICP-OES). Raman spectra were recorded on a LabRam HR Evolution, using 514 nm as laser.

#### **Electrochemical measurements**

The Electrochemical performances of ORR, OER and HER were recorded by Electrochemical Workstation (CHI 760E, Shanghai Chenhua Instrument Corporation, China). All electrochemical measurements were made on a typical three-electrode system. Platinum mesh was used as counter electrode for ORR test, graphite rod for OER and HER test. The saturated calomel electrode is used as a reference electrode. All the potential is converted to a reversible hydrogen electrode. For ORR, the LSV curves were obtained in a 0.1 M KOH solution saturated with  $O_2$  at a scan rate of 5 mV·s<sup>-1</sup> and a rotation speed of 1600 rpm in the potential range of 0.1 to -1 V. The electron transfer number (n) and the yield of  $H_2O_2$  are obtained from the following equation through RRDE:

$$n = 4 \frac{I_D}{\frac{I_R}{N} + I_D}$$

$$H_2 O_2 \% = 200 \frac{I_R / N}{\frac{I_R}{N} + I_D}$$

where  $I_D$  is disk current,  $I_R$  is ring current, and N is the current collection efficiency of the Pt ring, N = 0.37.<sup>1</sup>

The electron transfer number (n) and kinetic current density  $(J_k)$  can also be calculated based on the Koutecky-Levich (K-L) equation:

$$\frac{1}{J} = \frac{1}{J_K} + \frac{1}{J_L} = \frac{1}{\frac{1}{B\omega^2}} + \frac{1}{J_K}$$
$$B = 0.62nFC_0 D_0^{\frac{2}{3}} V^{-\frac{1}{6}}$$

Where J is the measured current density,  $J_K$  and  $J_L$  are the kinetic and limiting current density respectively,  $\omega$  is the angular velocity of the disk, n is the number of electron transfers, F is the Faraday constant (96485 C·mol<sup>-1</sup>), and C<sub>0</sub> is the concentration of O<sub>2</sub>(1.2×10<sup>-6</sup> mol·cm<sup>-3</sup>), D<sub>0</sub> is the diffusion coefficient of O<sub>2</sub> in 0.1 M KOH (1.9×10<sup>-5</sup> cm<sup>2</sup>·s<sup>-1</sup>), and V is the kinematic viscosity of the electrolyte (0.01 cm<sup>2</sup>·s<sup>-1</sup>).<sup>2</sup> To eliminate the error, the oxygen reduction current (J) the oxygen reduction current is calculated as the current measured in saturated oxygen minus saturated nitrogen.

The 1 M KOH solution was used as the electrolyte for OER and HER tests. All LSV curves are obtained by IR compensation. The CV curves at different scan rates are also measured to determine the electrochemical double layer capacitance ( $C_{dl}$ ), and then ESCA can be calculated based on the  $C_{dl}$  value.

The synthesized Fe<sub>2</sub>P/Co@NPC were applied as the cathode catalyst with the loading of 1 mg cm<sup>-2</sup>. PtRu/C (40 wt% Pt and 20 wt% Ru on Vulcan XC-72, Johnson Matthey) was used as the anode catalyst with the loading of 0.4 mg<sub>PtRu</sub> cm<sup>-2</sup>. The catalyst ink was prepared by ultrasonically dispersing the catalysts and PAP-TP-100 (the hydroxide exchange membrane and ionomer, 5 wt% in ethanol) into water and isopropanol (1:25 v/v) for 2.0 h. Then the catalyst ink was sprayed onto both sides of PAP-TP-85 membrane (15  $\mu$ m) to fabricate a catalyst-coated membrane (CCM) with the electrode area of 5 cm<sup>-2</sup>. All CCMs were immersed into 3 M KOH solution for 4.0 h (exchange the solution every 2.0 h) and then rinsed thoroughly with deionized water until the pH of the residual water was neutral. The obtained CCM was assembled with a fluorinated ethylene propylene (FEP) gasket, a GDL (SGL 29 BC), a graphite bipolar plate with 5 cm<sup>2</sup> flow field (Electro Chem) and a metal current collector for each side to complete the full HEMFC. The H<sub>2</sub>-O<sub>2</sub> fuel cell were tested (Scribner 850e) under galvanic mode using humidified H<sub>2</sub> and O<sub>2</sub>. The cell temperature was set to 80 °C, and the flow rate of both H<sub>2</sub> and O<sub>2</sub> gas was 1.0 and 1.5 L min<sup>-1</sup> with 2.5 bar backpressure.

We assembled a self-made Zn-air battery, in which 6 M KOH and 0.2 M ZnO were served as electrolyte, zinc piece and Fe<sub>2</sub>P/Co@NPC-loaded carbon paper (1 mg cm<sup>-2</sup>) used as the anode and air cathode, respectively. The stability of Fe<sub>2</sub>P/Co@NPC was evaluated using a rechargeable zinc air battery at a current density of 5 mA cm<sup>-2</sup>. For comparison, a Zn-air battery based on Pt/C-IrO<sub>2</sub> was also assembled (using a mixture of Pt/C and IrO<sub>2</sub> as an electrocatalyst with a mass ratio of 1:1). In order to test the overall water-splitting activity, two identical Fe<sub>2</sub>P/Co@NPC electrodes coated on carbon paper were assembled into a full electrolyzer configuration. The catalyst loading was 1 mg·cm<sup>-2</sup> in 1M KOH solution.

## Working electrode preparations

In short, a 5mg sample was dispersed in a 1mL solution containing 600  $\mu$ L anhydrous ethanol, 400  $\mu$ L water, and 50  $\mu$ L Nafion (5 wt%) to prepare homogeneous catalytic ink and then treated with

ultrasound for 1 h. Then the obtained homogeneous catalyst inks 15  $\mu$ L were dropped onto RDE (0.19625 cm<sup>2</sup>) and then dried at room temperature to afford a mass loading of about 0.364 mg cm<sup>-2</sup>. Commercial platinum carbon (20 wt%) and IrO<sub>2</sub> catalyst inks were prepared using the same process for comparison.

#### DFT calculation details.

DFT calculations were performed through the projector augmented wave (PAW) method by using the Vienna ab initio simulation package (VASP). The Generalized gradient approximation (GGA) method with the Perdew-Burke-Ernzerhof (PBE) was adopted as the exchange-correlation functional. The kinetic cutoff energy was set to 450 eV. The k-mesh in Brillouin zones was determined based on Monkhorst-Pack kpoint grids. The calculation uses gamma-centered k-points 1×3×1 for Fe<sub>2</sub>P(111)-Co(111) heterojunction,  $6 \times 5 \times 1$  for Co(111),  $5 \times 5 \times 1$  for Fe<sub>2</sub>P(111), zero damping DFT-D3 method of Grimme, and the convergence tolerance for the residual force and energy on each atom during structure relaxation were set to 0.02 eVÅ<sup>-1</sup> and 10<sup>-5</sup> eV. The spin was constrained for all the systems with unpaired electrons. VASP-sol package<sup>3</sup> is used to simulate the solution environment, where the over dielectric constant (cr) is set to 80<sup>4, 5</sup>. The z-direction is set to 20 Å, which is to avoid steric hindrance and interaction due to periodicity. The optimization of the unit cell parameters is carried out by the method of fixing the lattice vector (modify constr cell relax.F file in VASP and recompile), the cell 30.000×6.758×20.000, a=b=c=90° for  $Fe_2P(111)$ -Co(111), parameters are obtained as 4.209×4.872×20.000, a=b=c=90 ° for Co(111), and 6.438×6.439×20.000, a=b=90 °, c=94.802 ° for  $Fe_2P$  (111). The free energy diagrams were estimated as follow to illustrate the activity of ORR <sup>6,7</sup>:  $\Delta G = \Delta E + \Delta Z P E - T \Delta S + \Delta G_{II} + \Delta G_{PH}$ 

$$\varphi = G_{abslab} - G_{slab}$$

Where  $\Delta E$  is the reaction energy of reactant and product molecules adsorbed on catalyst surface based on the DFT calculations;  $\Delta ZPE$  and  $\Delta S$  are the change of zero-point energy and entropy, T is the temperature (here, 298.15 K is selected). The bias effect on the free energy is taken into account by  $\Delta GU=-neU$ , where U is the electrode applied potential relative to RHE as mentioned above, e is the elementary charge transferred and n is the number of proton-electron pairs transferred.  $\Delta GPH$  is the correction of the H+ free energy and depends on the reaction. In our work, the U is considered as 0 V, PH is 0,  $\Delta ZPE$  and  $\Delta S$  are considered as G<sub>K</sub> (calculated by VASP-kit code <sup>8</sup>), T is 298.15K. So we can get the following formula.

$$\Delta G = \Delta E + G_K$$



Figure S1. a) SEM image, b) TEM image of DPPF@ZnCo-ZIF.



Figure S2. a) SEM image, b) TEM image of Co@NC.



Figure S3. a) SEM image, b) TEM image of Fe<sub>2</sub>P@NPC.



Figure S4. a-e) Elemental mapping of Fe<sub>2</sub>P/Co@NPC.



Figure S5. TEM image of Fe<sub>2</sub>P/Co@NPC.



Figure S6. XRD pattern of DPPF@ZnCo-ZIF and ZnCo-ZIF.



**Figure S7.** a) XPS survey spectrum (the inset table is surface atomic weight percentages). b) High-resolution XPS spectrum of C 1s of Fe<sub>2</sub>P/Co@NPC.



Figure S8. a) LSV curves of Fe<sub>2</sub>P/Co@NPC sample at different rotation speed. b) K-L plots of Fe<sub>2</sub>P/Co@NPC at different potentials. c) Tafel plot of Fe<sub>2</sub>P/Co@NPC, Co@NC, Fe<sub>2</sub>P@NPC and Pt/C.
d) Chronoamperometric response of Fe<sub>2</sub>P/Co@NPC and Pt/C with methanol added at 500 s.



Figure S9. a) Nyquist plots for  $Fe_2P/Co@NPC$ , Co@NC,  $Fe_2P@NPC$  and  $IrO_2$  during OER. b) Chronoamperometric responses of  $Fe_2P/Co@NPC$  in 1 M KOH at a current density of 10 mA cm<sup>-2</sup> in OER.



**Figure S10.** a) Comparison of the overpotential required at 10 mA cm<sup>-2</sup> among Fe<sub>2</sub>P/Co@NPC in HER. b) Nyquist plots for Fe<sub>2</sub>P/Co@NPC, Co@NC, Fe<sub>2</sub>P@NPC and Pt/C during HER.



Figure S11. CV curves of a) Fe<sub>2</sub>P/Co@NPC, b) Co@NC, c) Fe<sub>2</sub>P@NPC in 1 M KOH electrolyte for

HER. d) Current density versus scan rate for Fe<sub>2</sub>P/Co@NPC, Co@NC and Fe<sub>2</sub>P@NPC.



Figure S12. Raman spectra of Fe<sub>2</sub>P/Co@NPCs at different pyrolysis temperature.



**Figure S13.** a) High-resolution XPS spectrum of N 1s for Fe<sub>2</sub>P/Co@NPCs at different pyrolysis temperature. b) The contents of various doped N.



Figure S14. a) ORR polarization curves of Fe<sub>2</sub>P/Co@NPCs at different pyrolysis temperature and

Pt/C.



Figure S15. a) OER polarization curves, b) comparison of the overpotential required at 10 mA cm<sup>-2</sup>,
c) Nyquist plots, d) Tafel plot of Fe<sub>2</sub>P/Co@NPCs at different pyrolysis temperature and IrO<sub>2</sub> in 1 M KOH.



Figure S16. a) HER polarization curves, b) comparison of the overpotential required at 10 mA cm<sup>-2</sup>,
c) Nyquist plots, d) Tafel plot of Fe<sub>2</sub>P/Co@NPCs at different pyrolysis temperature and Pt/C in 1 M KOH.



**Figure S17.** CV curves of a) Fe<sub>2</sub>P/Co@NPC-850, b) Fe<sub>2</sub>P/Co@NPC-950, c) Fe<sub>2</sub>P/Co@NPC-1050 in 1 M KOH electrolyte for HER. d) Current density versus scan rate for Fe<sub>2</sub>P/Co@NPCs at different pyrolysis temperature.



Figure S18. LED powered by two Zn–air batteries with the Fe<sub>2</sub>P/Co@NPC as air-cathode connected in series.



**Figure S19.** a) Polarization curves for overall water splitting (inset shows the photograph of a water electrolyzer). b) Chronoamperometric response curves for the water splitting device.



Figure S20. SEM image of Fe<sub>2</sub>P/Co@NPC after 2000 cycles of CV test for ORR.



Figure S21. XRD patterns of Fe<sub>2</sub>P/Co@NPC after 2000 cycles of CV test for ORR.



Figure S22. a) P 2p; b) Fe 2p; c) N 1s; d) Co 2p for Fe<sub>2</sub>P/Co@NPC after 2000 cycles of CV test for ORR.



Figure S23. The three intermediates (OOH\*, O\*, OH\*) adsorption diagram for Fe<sub>2</sub>P(111) (a-c), Co(111) (d-f), Fe<sub>2</sub>P(111)-Co(111) (g-i).



**Figure S24.** The Charge transfer diagram 3d (a-b) and 2d (c) at the  $Fe_2P(111)$ -Co(111) heterojunction interface represented by charge density differential method, where yellow represents charge increase and blue represents charge decrease. It can be seen that the electrons around the P active site (at the interface) are greatly increased.

Sample	Fe	Со
Co@NC	/	10.10
Fe <sub>2</sub> P@NPC	4.95	/
Fe <sub>2</sub> P/Co@NPC-850	5.51	2.70
Fe <sub>2</sub> P/Co@NPC-950	6.13	5.42
Fe <sub>2</sub> P/Co@NPC-1050	5.58	2.75

 Table S1. Inductively coupled plasma (ICP) results of different electrocatalysts (wt %).

Catalysts	ORR	OER	HER	Reference
	E <sub>1/2</sub>	$\eta_{10}$	$\eta_{10}$	
	(V)	(mV)	(mV)	
Fe <sub>2</sub> P/Co@NPC	0.876	331	235	This work
FeCo/CO <sub>2</sub> P@NPCF	0.770	330	260	9
Fe-N <sub>4</sub> SAs/NPC	0.885	430	202	10
PPy/ FeTCPP/Co	0.860	340	240	11
Fe <sub>3</sub> C-Co/NC	0.885	340	238	12
Co-Co <sub>9</sub> S <sub>8</sub> @SN-CNTs-900	0.810	450	240	13
CoSA+Co <sub>9</sub> S <sub>8</sub> /HCNT	0.855	330	250	14
CO <sub>2</sub> P/CoNPC	0.843	326	208	15
Co/CNFs (1000)	0.896	320	190	16
Co@N-CNTF	0.810	350	220	17

**Table S2.**The comparison of ORR, OER and HER activity of Fe<sub>2</sub>P/Co@NPC with recently reported electrocatalysts.

Catalysts	Cathode loading	Anode loading Pmax		Reference
	(mg cm <sup>-2</sup> )	(mg cm <sup>-2</sup> )	(mW cm <sup>-2</sup> )	
Fe <sub>2</sub> P/Co@NPC	1.0	0.4 Pt-Ru	1250	This work
Ce/Fe-NCNW	1.0	0.75 Pt-Ru	496	18
Fe-N-MPC	2.0	0.8 Pt-Ru	473	19
Cu SAC	2.0	0.5 Pt	196	20
NFC@Fe/Fe <sub>3</sub> C-9	2.0	0.4 Pt	237	21
FeSiNC_50a	3.0	0.4 Pt-Ru	208	22
Fe-LC-900	2.0	0.8 Pt	50	23
NBSCP	3.0	0.4 Pt	172	24
Fe <sub>0.5</sub> –N-C	1.0	Pt-Ru	504	25
Co <sub>1.08</sub> Fe <sub>3.34</sub> @NGT	3.0	0.4 Pt	117	26

Table S3. Summary the performance of  $H_2/O_2$  AEMFCs for non-precious metal catalysts.

Catalysts	Open Voltage	Pmax	Reference
	(V)	(mW cm <sup>-2</sup> )	
Fe <sub>2</sub> P/Co@NPC	1.35	233.56	This work
Co-NDC	1.30	154.00	27
Co-N-CNTs	1.36	101.00	1
Fe-SCNS	1.47	163.00	28
PcCu-O <sub>8</sub> -Co/CNT	1.37	94.00	29
Fe-N/P-C-700	1.42	133.20	30
FeCo@C MS.	1.34	86.09	31
CO <sub>2</sub> FeO <sub>4</sub> /NCNTs	1.43	90.68	32
CoNi-SAs/NC	1.36	101.40	33

Table S4. Summary the performance of Zn-air battery with previously reported electrocatalysts.

**Table S5.** Free energy of each intermediate process, each value has been corrected for zero-point energy and entropy  $(G_K)$  to get  $\Delta G$ . Unit is eV.

Species	$\Delta G_{OH}$	$\Delta G_{0^*}$	$\Delta G_{OOH*}$
Co(111)	1.034	1.308	1.780
Fe <sub>2</sub> P(111)	-0.196	-0.312	3.352
Fe <sub>2</sub> P(111)-Co(111)	0.768	2.140	2.922

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