Supporting information

Regular Hexagonal CuBi Nanosheets Boost Highly Efficient CO²

Reduction to HCOOH in Solid-Electrolyte Cell

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Calculation of faradaic efficiency

The faradaic efficiency of products was calculated as follows:

$$
FE_{H_2 \text{ or } CO} \text{ (*)} = \frac{i_{H_2 \text{ or } CO}}{i_{Total}} \times 100\% = \frac{c_{H_2 \text{ or } CO} \times \nu \times \frac{2P_0 F}{RT}}{i_{Total}} \times 100\%
$$

 $i(A)$ is partial current of the H_2 and CO product.

c (ppm) is the volume concentrations of H_2 and CO analyzed by GC.

 v (ml min⁻¹) is gas flow rate.

 P_0 is the atmosphere pressure (1.013 bar).

T is the temperature (298 K).

R is the ideal gas constant (83.14 mL bar mol⁻¹ K⁻¹).

$$
FE_{HCOOH} (\%) = \frac{Q_{HCOOH}}{Q_{Total}} \times 100\% = \frac{C_{HCOOH} \times V \times N \times F}{Q_{Total}} \times 100\%
$$

C (mol L^{-1}) is concentration of formate in the electrolyte.

V (L) is the volume of the electrolyte.

N is number of electrons are needed to produce one formate molecule, whose value is two.

F is Faraday's constant whose value (96485 C mol⁻¹).

Q*Total* (C) is total charge during the experiment

Calculation of energy conversion efficiency

H-cell and flow-cell belong to the half cell and corresponding energy conversion efficiency (EE) was calculated in the cathode. The overpotential of oxygen evolution was assumed to be zero. The EE of formate can be calculated as follow:¹

$$
EE_{half-cell} = \frac{(1.23 + (-E_{foramte})) \times FE_{formate}}{(1.23 + (-E_{applied}))}
$$

Eformate is the thermodynamic potential (versus RHE) for CRR to formate, which is - 0.2 for acetate.

FEformate is the measured faradaic efficiency of formate.

Eapplied is the applied potential (versus RHE) in three electrode system.

Formate energy efficiency reported in others' work was also calculated in full cell (MEA system):

$$
EE_{full-cell} = \frac{(1.23 + (-E_{formate})) \times FE_{formate}}{-E_{full-cell applied}}
$$

EEfull-cell applied is the full-cell potential applied in the MEA system.

Figures and Tables

Figure S1 SEM images of (a) BiOON₄ and (b) BiO_x.

Figure S2 High-resolution XPS of N 1s.

Figure S3 Faradaic efficiencies of products in the H cell.

Figure S4 CV curves for (a) BiO_x, (b) BiOON₄ and (c) Cu-BiOON₄ performed in the

region of -0.30 \sim -0.38 V vs. Ag/AgCl at various scan rates in 0.1 M KHCO₃ solution.

Figure S5 The top view of (a) anode and cathode electrode. (b) The front view of the solid electrolyte layer, which contains a serpentine channel filled with styrenedivinylbenzene copolymer spheres. (c) The diagram of the working device of a solid electrolyte.

Figure S6 Potential- dependent in situ Raman spectra in 0.1 M KHCO₃ electrolyte for BiOON4.

Figure S7 (a) XRD pattern of Cu-BiOON₄ after 30 min reduction in CRR, noted as After-Cu-BiOON4. (b) SEM image, (c) high-resolution TEM image and (d) SAED pattern of After-Cu-BiOON4. (f) High-angle annular dark field STEM image of After-Cu-BiOON⁴ hexagonal nanosheet and (e) corresponding EDS element analysis graph. C and O both came from absorbed $HCO₃$ species in $KHCO₃$ electrolyte.

Figure S8 The optimized adsorption models of *OCHO intermediate on (a) 4Cu-Bi(012) and (b) 4Cu-Bi(104).

Figure S9 Chronoamperometric responses at different potentials with 1 M KOH electrolytes in the flow cell.

Figure S10 (a) Calibration cure between HCOOH concentration and relative peak area vs $H₂O$ using in the high-performance liquid chromatography (HPLC). The linear correlation coefficient is 0.99997. (b) The original chromatographic column curve of H2O sample. (c) The curve of catholyte detected by the inspection detector on HPLC was collected from the stability test of $Cu-BiOON₄$ at 2.35 V for 4h in the solid electrolyte device.

Table S1 Elemental content of samples obtained from XPS.

Electrocatalyst	N (at. %)	O (at. %)	Bi (at. $\%$)	Cu (at. $\%$)
$Cu-BiOON4$	10.0	67.5	19.1	3.4
BiOON ₄	5.5	69.6	24.9	$- -$
BiO _x	$\overline{}$	68.7	31.3	$- -$

Electrocatalyst	Electrolyte(pH)	FE^{a} (%)	$E^b(V)$	$E^d(V)$	ref
Bi nanostructure	$0.5M$ KHCO ₃	92	-0.9	-0.9	$\overline{2}$
Bi nanosheets	$0.5M$ NaHCO ₃	86	-1.1		\mathfrak{Z}
Bi dendrites	$0.5M$ NaHCO ₃	98	-0.82	-0.72 to -0.92	$\overline{4}$
Bismuthene NA	$0.5M$ KHCO ₃	95	-0.88	-0.75 to -0.95	5
$Bi2S3-Bi2O3$	$0.1M$ KHCO ₃	93.8	-1.1	-1.0 to -1.4	6
Bi-Cu	$0.5M$ KHCO ₃	95.8	-0.9	-0.9 to -1.0	$\boldsymbol{7}$
$In_{16}Bi_{84}$ NS	$0.5M$ NaHCO ₃	$\sim\!\!100$	-0.94	-0.84 to -1.54	$8\,$
CuBi ₂ O ₄	$0.5M$ NaHCO ₃	95	-0.93	-0.83 to -1.03	9
Bi ₂ CO ₃ NS	$0.1M$ KHCO ₃	92	-1.2	-1.1 to -1.2	10
CuBi ₇₅	$0.5M$ KHCO ₃	$\sim\!\!100$	-0.77	-0.57 to -1.47	11
Cu ₁ Sn ₁	$0.5M$ NaHCO ₃	95.4	-1.2	-1.2 to -1.3	12
BiCu/CF-0.1	0.5 M KHCO ₃	94.2	-0.8	-0.7 to -1.1	13
$Bi-Cu(2:1)$	$0.1M$ KHCO ₃	94.1	-1.0	-0.8 to -1.2	14
$Cu-BiOON4$	$0.1M$ KHCO ₃	~100	-0.6	-0.5 to -1.2	This work

Table S2 Comparison of formate production on various Me-Sn bimetallic catalysts under comparable conditions.

^aMaximum FE_{HCOOH} under the reported conditions. ^{*b*}Overpotential at which the maximum FE is achieved. *^c*Current density achieved at the listed overpotential. *^d*The potential window of faradaic efficiency (>90%) toward formate.

Table S3 Summary of Sn-based electrocatalyst performance for the reduction of CO₂

to formate in flow cell.

^aMaximum *FE*_{HCOOH} under the reported conditions. ^{*b*}Potential at which the maximum FE is achieved. *^c*Partial current density of formate achieved at the listed overpotential.

Table S4 Summary of the electrocatalyst performance for producing HCOOH in solid electrolyte devices.

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