

## Supplementary information

### **Enhancement of pore confinement caused by mosaic structure on Ru nanoparticles for pH-universal hydrogen evolution reaction**

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#### **1 Some supplementary information during the experiment**

The turnover frequency (TOF) values of the catalysts for the HER were calculated through the following equation:

$$\text{TOF (s}^{-1}\text{)} = (j \times A) / (2 \times F \times n).$$

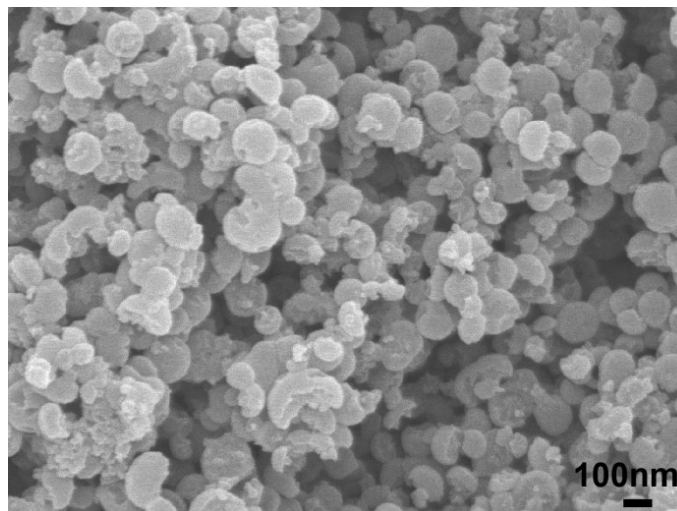
In the formula,  $j$  ( $\text{A} \cdot \text{cm}^{-2}$ ) is the current density at an overpotential of -100 mV,  $A = 0.07065 \text{ cm}^2$  is the geometric surface area of the glassy carbon electrode,  $F = 96,500 \text{ C} \cdot \text{mol}^{-1}$  is the Faraday constant, and  $n$  (mol) is the molar number of Ru loaded on the working electrode, which was calculated according to the result of ICP-OES.

The Faraday efficiency (FE) of the HER is determined using  $\text{FE} = n / (Q/2F)$ , where  $F$  is the Faraday constant,  $n$  is the total amount of  $\text{H}_2$ , and  $Q$  is the total amount of charge obtained from the  $i$ - $t$  curve.

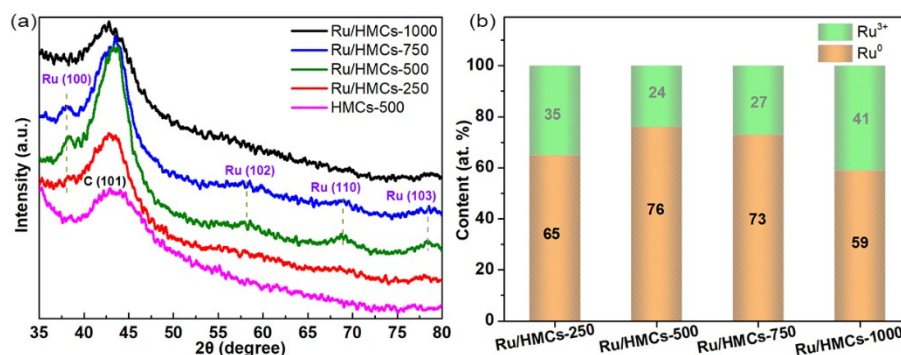
#### **2 Characterization techniques and other Supplements**

Fig. S5 present the cyclic voltammetry (CV) curves of the Ru/HMCs- $x$  recorded in the potential range of 0.346-0.446 V, 1.024-1.124 V and 0.611-0.711 V in 0.5 M  $\text{H}_2\text{SO}_4$ , 1 M KOH, and 0.5 M PBS with different scanning rates (e.g., 20, 40, 60, 80, 100, 120, 140, 160, 180 and 200  $\text{mV} \cdot \text{s}^{-1}$ ), respectively. According to the slope of the current density, which linearly changes with the increase in the scanning speed, the  $C_{dl}$  values of the corresponding catalyst can be calculated.<sup>1</sup> After extracting the  $C_{dl}$

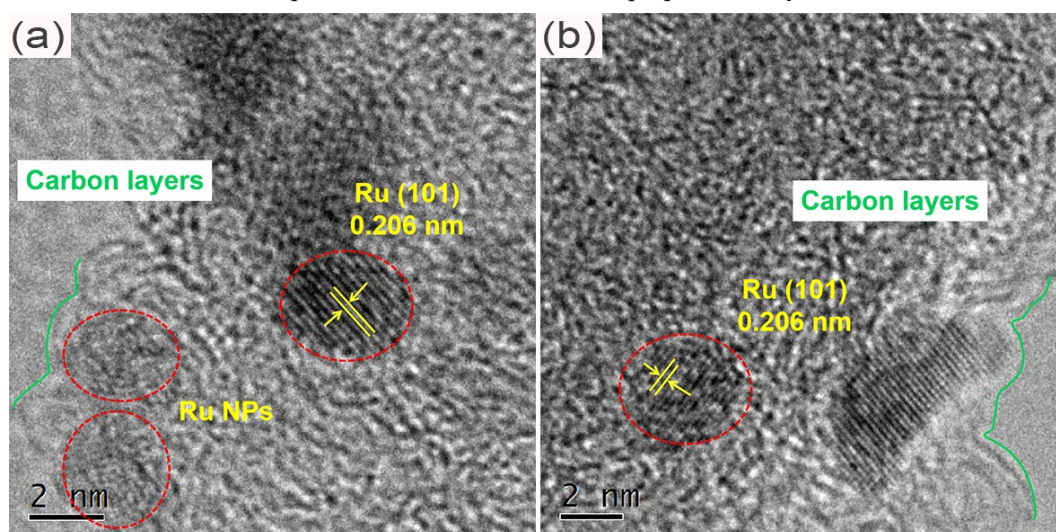
from the fitted linear regressions, we can calculate the electrochemically active surface area (ECSA) from the equation of  $ECSA = C_{dl}/C_s$ , where  $C_s$  are assumed to be same for all electrodes.<sup>2</sup>



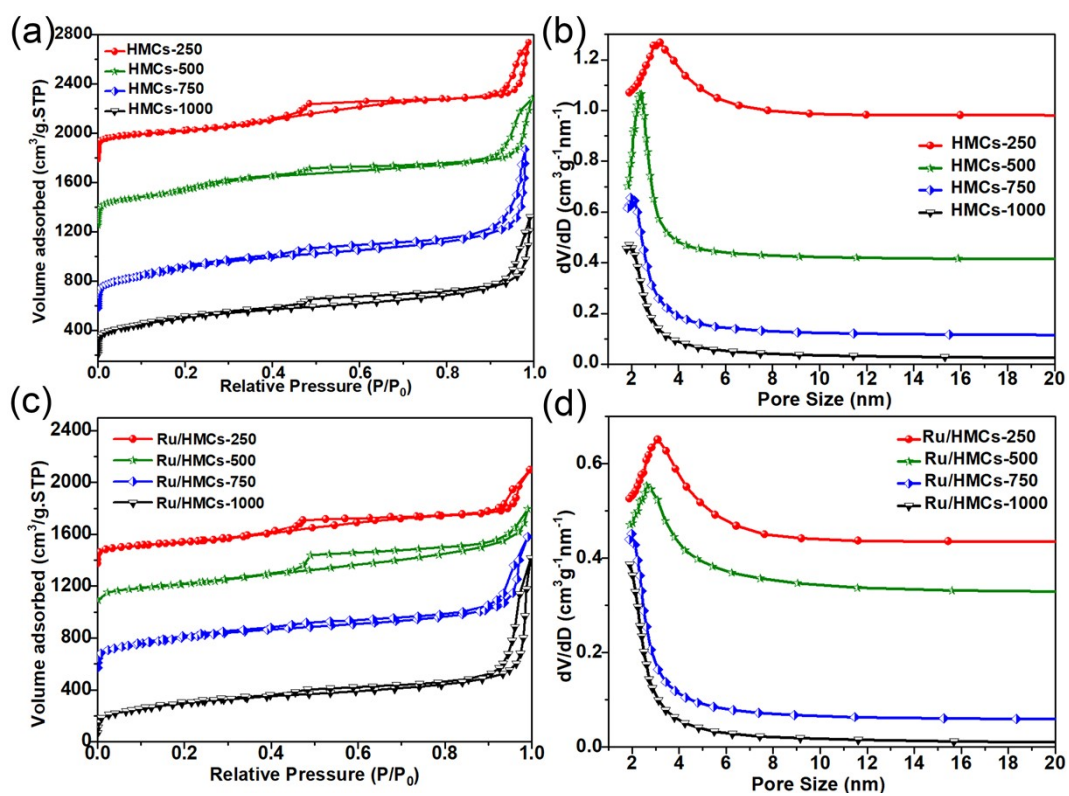
**Fig. S1** SEM images of hollow mesoporous carbon spheres was prepared by adjusting PH= 11.5 with sodium hydroxide.



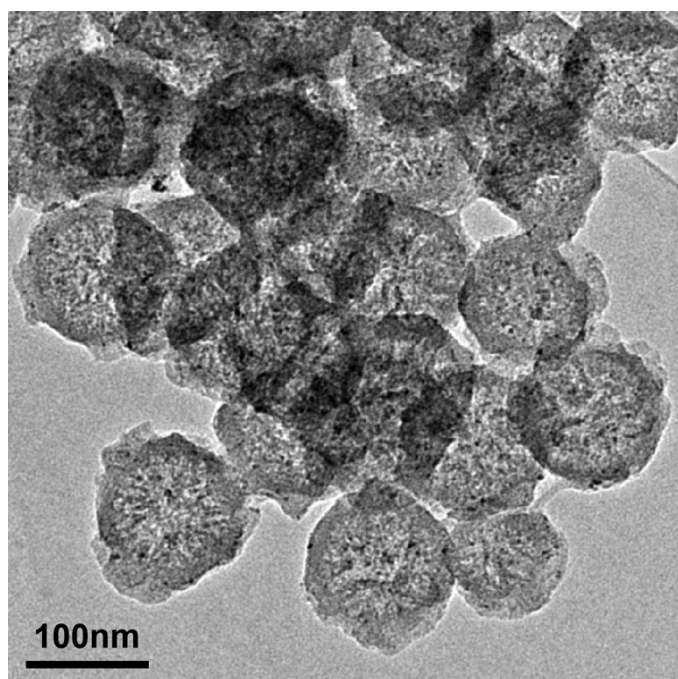
**Fig. S2** (a) Local enlarged XRD images of Ru/HMCs-x and HMCs-500. (b) Relative contents comparison of Ru<sup>0</sup> and Ru<sup>3+</sup> in as-prepared catalysts.



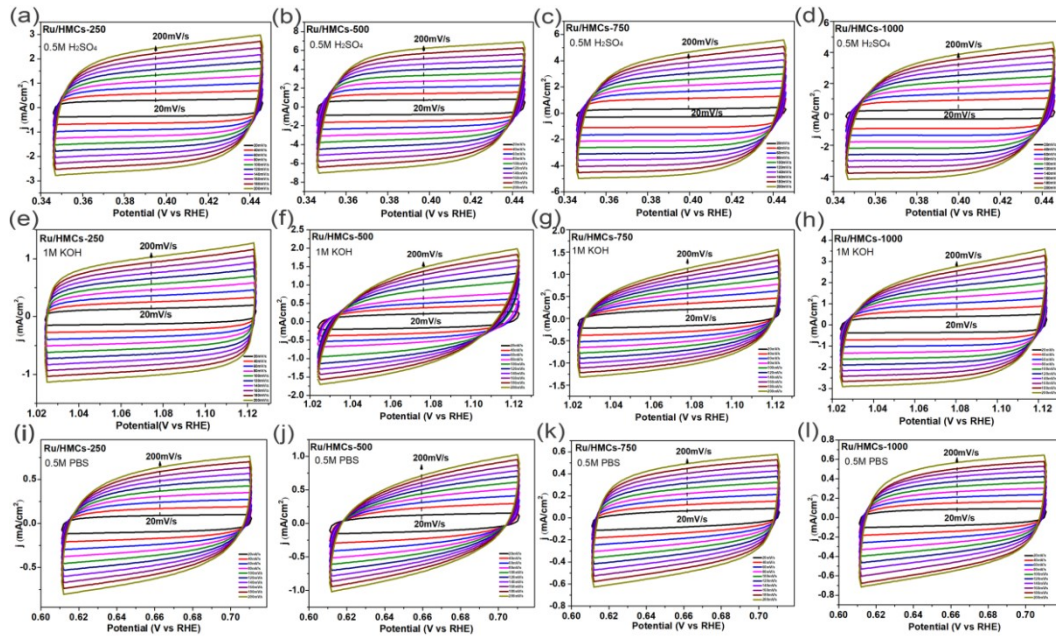
**Fig. S3** HRTEM images of Ru/HMCs-500.



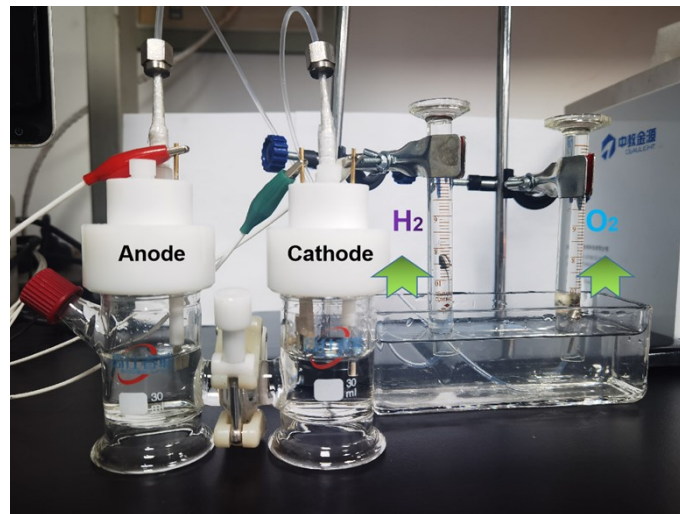
**Fig. S4** N<sub>2</sub> adsorption and desorption isotherms of (a) HMCs-x and (c) Ru/HMCs-x. Pore size distribution of (b) HMCs-x and (d) Ru/HMCs-x.



**Fig. S5** TEM images of Ru/HMCs-500.



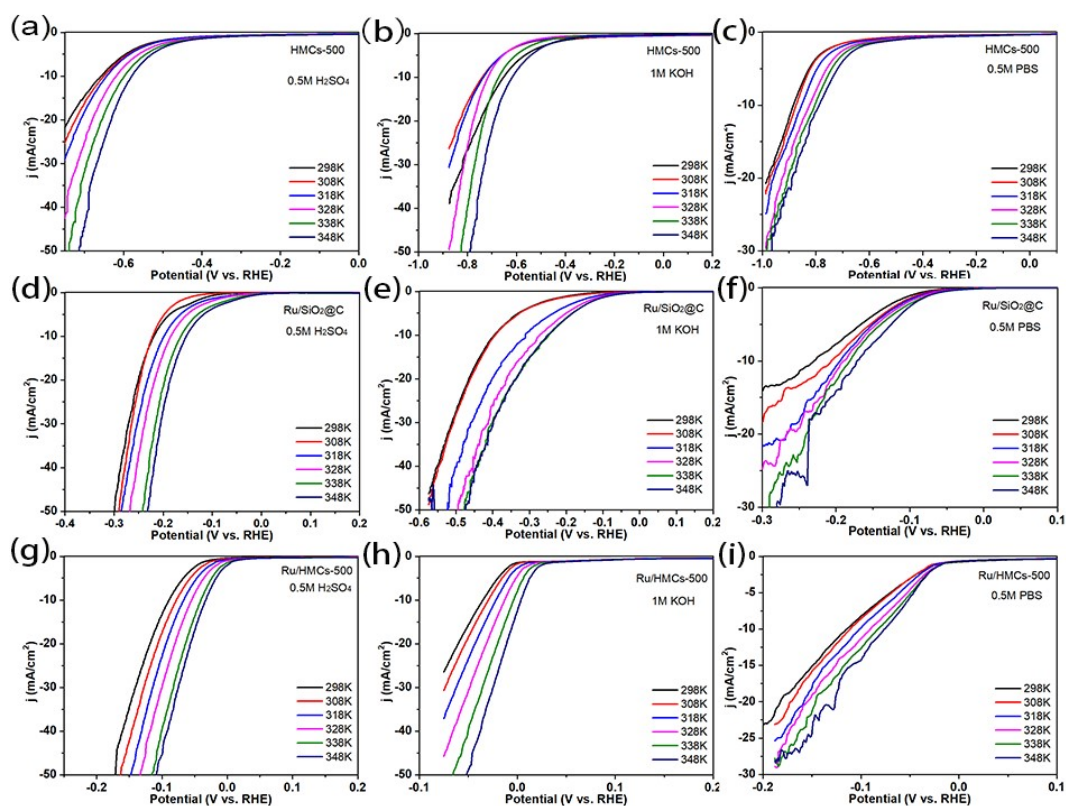
**Fig. S6** Cyclic voltammetry curves of Ru/HMCs-x at scan rates from 20 to 200  $\text{mV s}^{-1}$  in 0.5 M  $\text{H}_2\text{SO}_4$ , 1 M KOH, 0.5 M PBS, respectively. The differences in current density variation ( $\Delta J = J_a - J_c$ ) at overpotential of 0.396 V, 1.074 V, and 0.661 V in acidic, alkaline, and neutral solutions plotted against the scan rate fitted to a linear regression enables the estimation of  $C_{dl}$ .



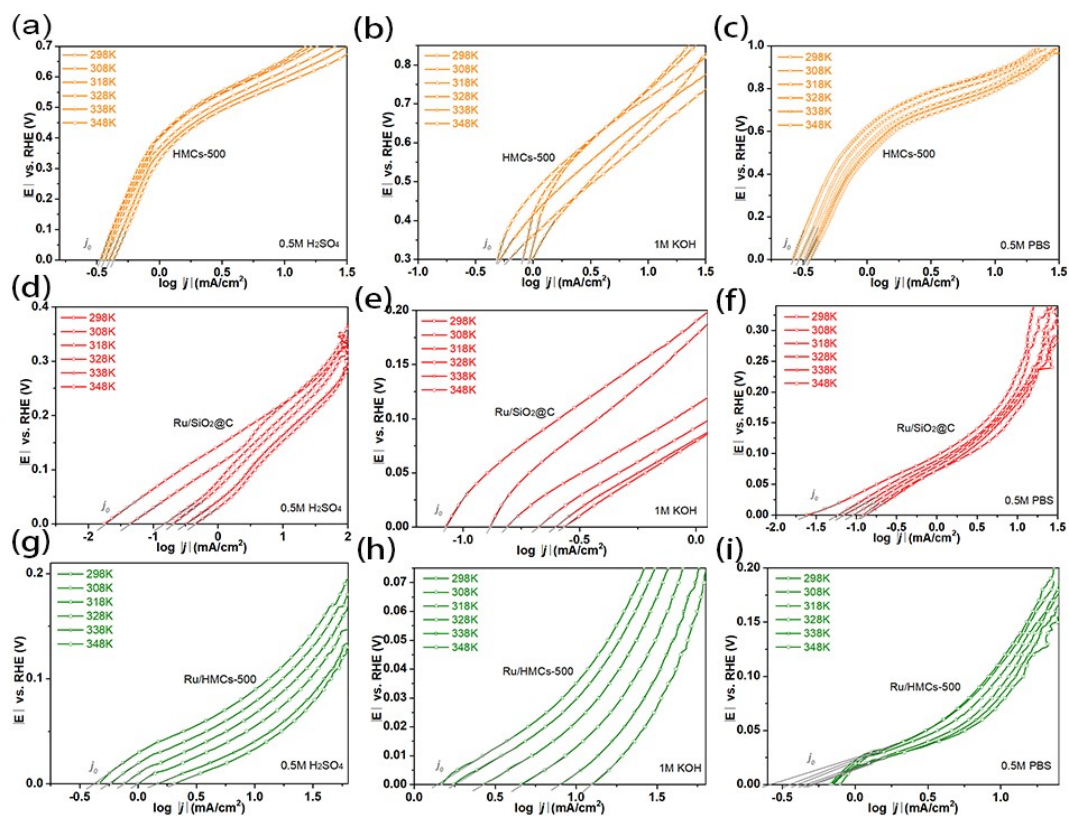
**Fig. S7** Diagram of the device for collecting hydrogen and oxygen using the drainage gas collection method.

The two compartments of the airtight H-type electrolytic cell were separated by Nafion membrane, one of which was a catalyst-decorated carbon paper working electrode (geometric area  $1 \text{ cm}^2$ , catalyst loading  $0.34 \text{ mg}\cdot\text{cm}^{-2}$ ) and Ag/AgCl reference electrode, the other chamber is the Pt sheet counter electrode. Under acidic and neutral conditions, the overpotential of 300 mV were tested for 10 min, and the released  $\text{H}_2$  was collected by the drainage gas-gathering method (Fig. S6). Under

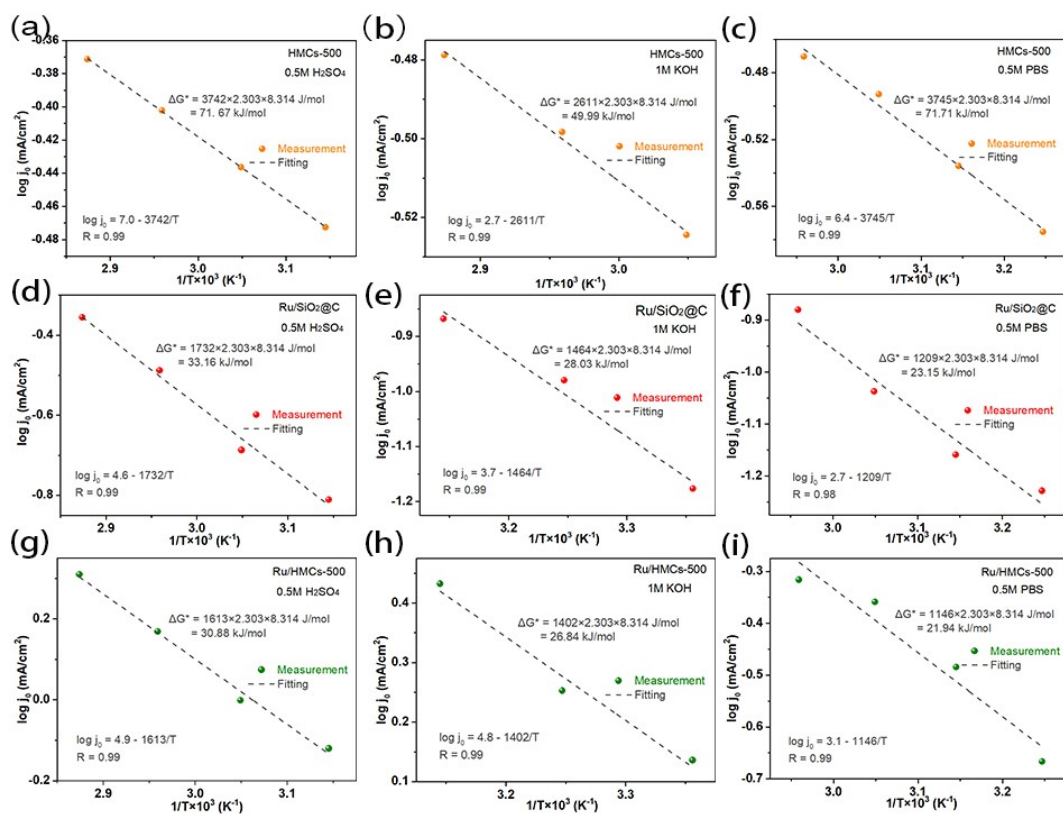
alkaline conditions, due to the rapid hydrogen production, the overpotential was selected at 100 mV, and the amount of H<sub>2</sub> in the reaction for 10 min was collected.



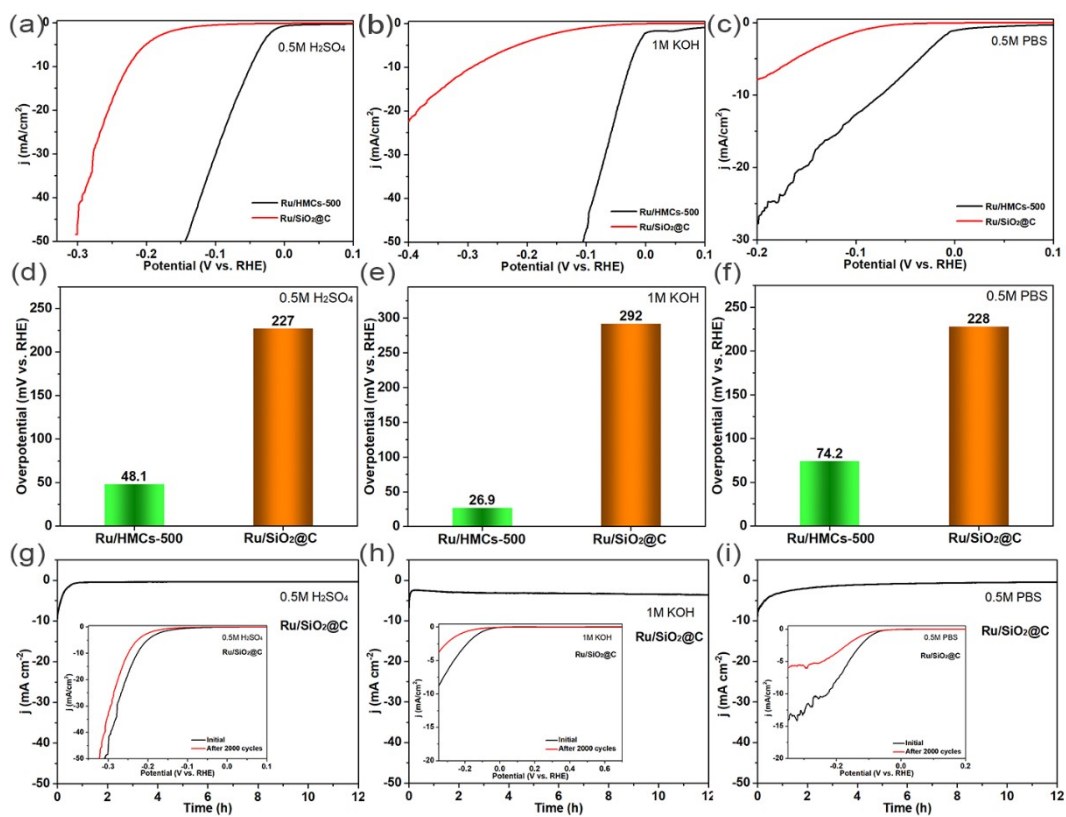
**Fig.S8** Linear sweep voltammetry (LSV) curves of the catalysts in different electrolytes at temperatures from 25 to 75 °C for the hydrogen evolution reaction (HER). (a-c) HMCs-500, (d-f) Ru/SiO<sub>2</sub>@C and (g-i) Ru/HMCs-500.



**Fig. S9** Tafel curves of (a-c) HMCs-500, (d-f) Ru/SiO<sub>2</sub>@C and (g-i) Ru/HMCs-500 catalysts in different electrolytes at different temperatures ranging from 298 to 348 K. The exchange current density ( $j_0$ ) was calculated by extending the linear part of Tafel plots.

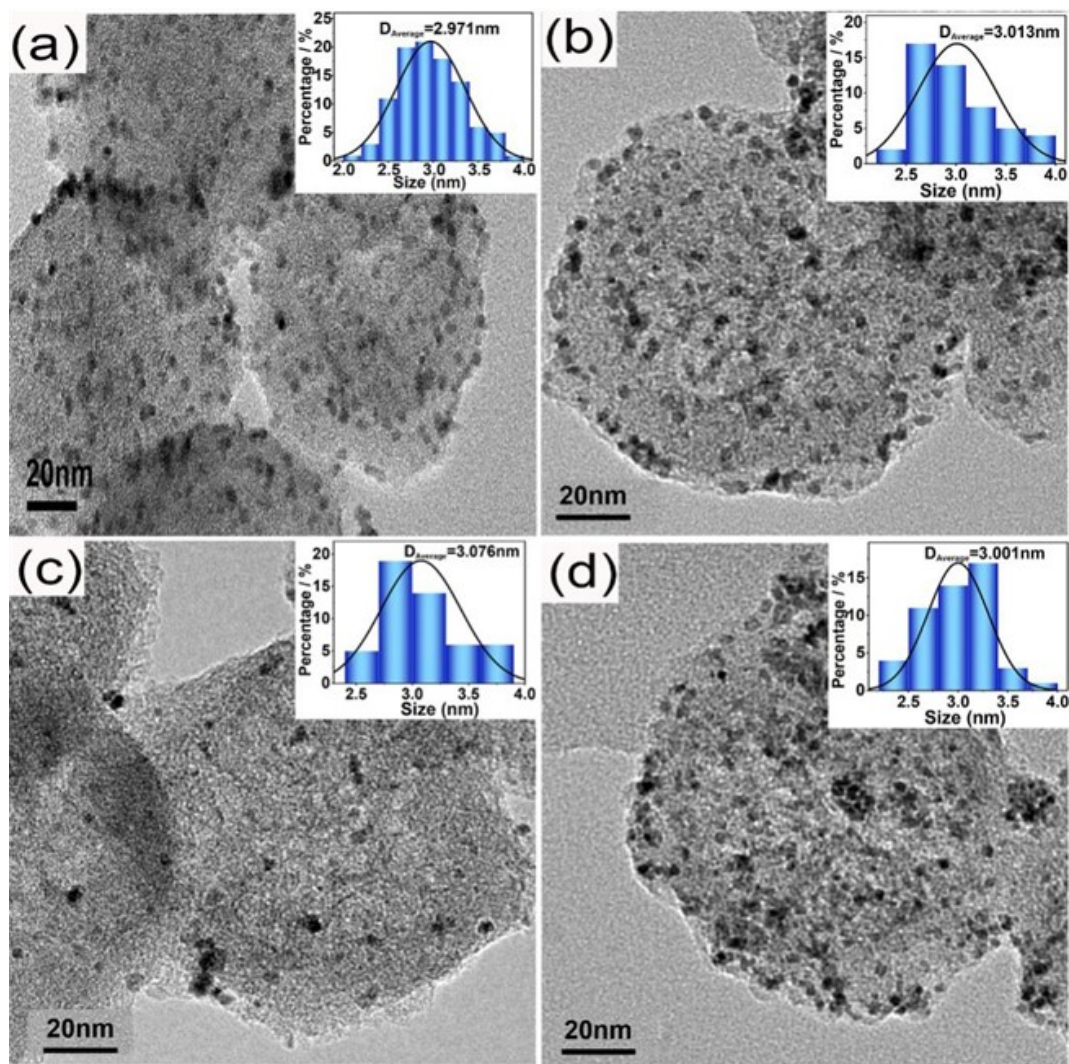


**Fig. S10** Typical Arrhenius plots for the (a-c) HMCs-500, (d-f) Ru/SiO<sub>2</sub>@C and (g-i) Ru/HMCs-500 catalysts in different electrolyte solutions. The calculation of the  $\Delta G^*$  is based on the Arrhenius equation:  $\log j_0 = \log(FKc) - \Delta G^*/2.303RT$ .



**Fig. S11** (a-c) Comparison of HER performance of Ru/SiO<sub>2</sub>@C and Ru/HMCs-500. (d-f) Histograms comparing overpotentials of Ru/HMCs-500 and Ru/SiO<sub>2</sub>@C at 10 mA·cm<sup>-2</sup> in different electrolytes. (g-i) The time-dependent current density curve of Ru/SiO<sub>2</sub>@C. (inset: LSV curves of the Ru/SiO<sub>2</sub>@C before and after 2000 CV cycles.)





**Fig. S12** TEM comparison of Ru/HMCs-500 before and after LSV test. (a) TEM image of Ru/HMCs-500 before testing. (b) TEM image after testing in 0.5 M H<sub>2</sub>SO<sub>4</sub> solution, (c) in 1 M KOH solution and (d) in 0.5 M PBS solution. (Inset: Ru NPs size distribution images)

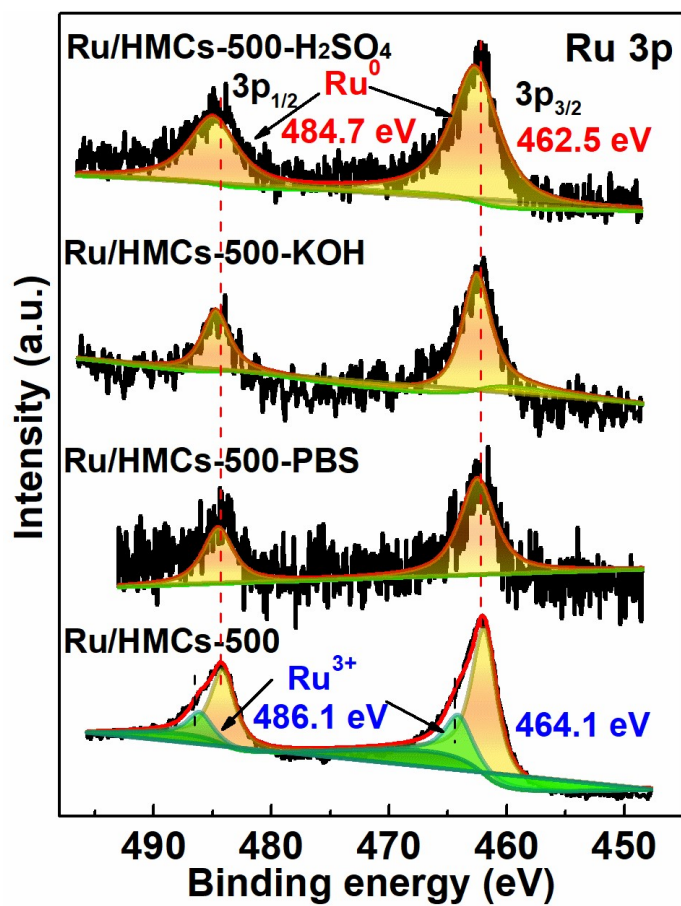


Fig. S13 Comparison of Ru 3p XPS peaks of Ru/HMCs-500 before and after LSV testing.

**Table S1** EDS and ICP-OES data of Ru/HMCs-x samples.

Sample		Ru/HMCs-250	Ru/HMCs-500	Ru/HMCs-750	Ru/HMCs-1000
EDS	Ru wt.%	3.67	1.82	1.99	4.22
ICP-OES	Ru wt.%	4.26	3.75	4.34	4.65

**Table S2** Textural Parameters of the Samples of HMCs-x and Ru/HMCs-x.

Sample	Average particle size (nm)	BET surface area (m <sup>2</sup> g <sup>-1</sup> )	Pore volume (cm <sup>3</sup> g <sup>-1</sup> )	Pore size (nm)
HMCs-250	121.3	861.4	1.51	3.21
HMCs-500	121.1	1177.1	1.71	2.42
HMCs-750	97.63	1260.6	2.04	1.96
HMCs-1000	98.31	1121.6	1.75	1.90
Ru/HMCs-250	131.2	680.9	1.19	3.09
Ru/HMCs-500	128.7	784.3	1.27	2.62
Ru/HMCs-750	110.2	984.7	1.61	1.97
Ru/HMCs-1000	100.3	947.5	2.08	1.90

**Table S3** Comparison of HER performance in 1 M KOH for Ru/HMCs-500 with other HER electrocatalysts.

Reaction medium	Catalyst	$\eta_{10}/\text{mV}$	Tafel slope (mV dec <sup>-1</sup> )	Ref.
1 M KOH	Ru/HMCs-500	26.9	45.7	This work
	MoP-Ru <sub>2</sub> P/NPC	47	36.9	[3]
	Ru-FeP	62	45	[4]
	Ru@Co/N-CNTs	48	45	[5]
	Co-Ru-MoS <sub>2</sub>	52	55	[6]
	Ni <sub>5</sub> P <sub>4</sub> -Ru	54	52	[7]

**Table S4** Comparison of HER performance in 0.5 M H<sub>2</sub>SO<sub>4</sub> for Ru/HMCs-500 with other HER electrocatalysts.

Reaction medium	Catalyst	$\eta_{10}/\text{mV}$	Tafel slope (mV dec <sup>-1</sup> )	Ref.
0.5 M H <sub>2</sub> SO <sub>4</sub>	<b>Ru/HMCs-500</b>	<b>48.09</b>	<b>38.99</b>	<b>This work</b>
	Ru <sub>x</sub> Fe <sub>y</sub> -NCs /CNF	66	43.44	[1]
	MoP-Ru <sub>2</sub> P/NPC	82	64.99	[3]
	Ru@Co/N-CNTs	92	73	[5]
	ECM@Ru	63	47	[8]
	Ni@Ni <sub>2</sub> P-Ru HNRs	51	35	[9]
	Ru@WNO-C	172	—	[10]
	RuTe <sub>2</sub> /Gr	72	33	[11]

**Table S5** Comparison of HER performance in 1 M PBS for Ru/HMCs-500 with other HER electrocatalysts.

Reaction medium	Catalyst	$\eta_{10}/\text{mV}$	Tafel slope (mV dec <sup>-1</sup> )	Ref.
	<b>Ru/HMCs-500</b>	<b>71.1</b>	<b>53.0</b>	<b>This work</b>
	MoP-Ru <sub>2</sub> P/NPC	126	70.89	[3]
	RuP-475	47	45	[12]
1 M PBS	s-RuS <sub>2</sub> /S-rGO	93	41	[13]
	RuP <sub>2</sub> @NPC	57	87	[14]
	Ru/C-2	188	109	[15]
	RuP@NPC	110	59	[16]

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