### *Electronic Supplementary Information*

# **Efficient**  $C_2H_2$ -selective separation in a microporous  $Zn(II)$ -based **metal-organic framework via the dual-ligand strategy**

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## <span id="page-1-0"></span>Content



#### <span id="page-2-0"></span>**S1. Materials and General Methods**

All reagents and materials were obtained commercially and used as received without further purification. Elemental analyses of carbon, hydrogen and nitrogen were performed on a PerkinElmer 2400C elemental analyzer. Powder X-ray diffraction (PXRD) data were collected on a Bruker D8 ADVANCE X-ray powder diffractometer (Cu Kα,  $\lambda = 1.5418$  Å) with 2θ (5-50°). Thermogravimetric analyses (TGA) were measured under a nitrogen stream employing the NETZSCH STA 449C microanalyzer thermal analyzer at a heating rate of 5 °C min<sup>-1</sup>. The gas sorption isotherms were measured on Micrometrics ASAP 2020M sorption equipment. Breakthrough experiments were performed on a Quantachrome dynaSorb BT equipment.

#### <span id="page-2-1"></span>**S2. Experiment Section and Characterization**

#### <span id="page-2-2"></span>**S2-1. Synthesis of 1**

A mixture of Zn(NO3)<sup>2</sup> 6H2O (29.9 mg, 0.1 mmol), H4L1 (22.5 mg, 0.05 mmol), Adenine(6.7 mg, 0.05 mmol) N,N-dimethylformamide (DMF, 4.0 mL),  $H_2O$  (2.0 mL), and CH<sub>3</sub>CH<sub>2</sub>OH (1.0 mL) was placed in a 15 mL bomb and heated at 105 ˚C for 72 h. The yellow block crystals (Fig. S1 and S2) were collected after cooling it to room temperature at a rate of 10 °C h<sup>-1</sup>(48% yield based on H<sub>4</sub>L1). After three days of the solvent exchange with acetone, adsorbent **1a** was obtained by activating at 373 K under vacuum for 6 h to remove the guest solvents. Anal. Calcd. (found) (%) for  $[(Me)_2NH_2][Zn_{2.5}(L1)(Ade)(HCOO)](DMF)_2(H_2O)_3$ : C, 41.78 (41.53); H, 3.49 (3.65); N, 11.47 (11.62).



**Fig. S1** Microscopy photograph of crystal morphology for MOF **1**.



**Fig. S2** SEM image of MOF **1**.

#### <span id="page-3-0"></span>**S2-2. Crystallographic Data Collection and Refinement**

The single crystal structure of **1** was measured by single crystal X-ray diffraction (SCXRD) on Bruker SMART APEX II CCD diffractometer equipped with graphite monochromated Mo K $\alpha$ radiation ( $\lambda$  = 0.710 73 Å) via  $\phi/\omega$  scan method. The diffraction data were corrected for Lorentz and polarization effects for empirical absorption based on multiscan. The structures were solved by the direct methods and refined by full-matrix least-squares refinements based on *F<sup>2</sup>* . Anisotropic thermal parameters were applied to all non-hydrogen atoms. All hydrogen atoms of ligands were calculated and added at ideal positions. The disordered lattice molecules were refined by the SQUEEZE program. and this result is consistent to the results of TGA. Crystallographic calculations were performed using *Olex* 2 with 'XL' plug-ins.





$\rho$ [g·cm <sup>-3</sup> ]	1.027			
$\mu$ [mm <sup>-1</sup> ]	1.233			
F[000]	763			
$\theta$ [°]	1.733 - 25.976			
Reflections collected / unique	13347 / 9553			
Goodness-of-fit on $F^2$	0.975			
Final R indices $[I>2\sigma(I)]$	$R_1^a = 0.0587$ , $wR_2^b = 0.1540$			
R indices (all data)	$R_1^a = 0.0931$ , $wR_2^b = 0.1710$			
${}^{a}R_{1} = \sum   F_{o} - F_{c}  /\sum  F_{o} $ ; ${}^{b}wR_{2} = [\sum w(F_{o}^{2}-F_{c}^{2})^{2}/\sum w(F_{o}^{2})^{2}]^{1/2}$				

**Table S2.** Selected bond lengths [Å] and angles [°] for **1**.





Symmetry codes:#1 -x+1,-y+1,-z+1; #2 x,y-1,z; #3 -x+1,-y,-z; #4 x+1,y+1,z; #5 -x+2,-y+1,-z; #6 x+1,-y+1,-z; #7 x+1,y,z; #8 x-1,y-1,z; #9 x,y+1,z; #10 x-1,y,z.



Fig. S3 Coordination environment of  $Zn^{2+}$  ions in 1. Symmetric code: a 1-x, 1-y, 1-z; b 1-x, -y, -z; c 2-x, 1-y, -z; d 1+x, 1+y, z; e 1-x, 1-y, -z; f 1+x, y, z.



**Fig. S4** Coordination mode of L1and ancillary ligand Ade in **1**.



**Fig. S5** 3D porous network viewed along the [101] direction and the Zn-Ade linear chain.



**Fig. S6** Topological net viewed along the [121] direction.



**Fig. S7** PXRD patterns of simulated **1**, as-synthesized **1**, tested **1a** after adsorption, and **1** in different solvents for 12 h.



**Fig. S8** TGA curve of as-synthesized **1** and adsorbent **1a**.



Fig. S9 (a)  $N_2$  adsorption isotherms at 77 K of 1a. (b) The BET surface area plot for 1a.



**Fig. S10** The pore size distribution of **1a** (mainly at 5.8 and 7.3 Å), as calculated by Original Density Functional Theory.

#### <span id="page-8-0"></span>**S3. Gas Adsorption**

Table S3. Comparison of C<sub>2</sub>H<sub>2</sub> uptake amount and storage density of some MOF adsorbents for  $C_2H_2/CO_2$  separation at 1 bar.

	<b>Uptake amount</b>	<b>Storage density</b>		
Adsorbent	$(cm3 g-1)$	$(g \text{ cm}^{-3})$	Reference	
$ZJU-50a$	192	0.24	S <sub>2</sub>	
MIL-160	191	0.25	S <sub>3</sub>	
Ni3-bdc-tpt	162.1	0.2	S <sub>4</sub>	
$UPC-200(Al)$ -F-BIM	144.5	0.11	S <sub>5</sub>	
<b>SNNU-45</b>	134.0	0.13	S <sub>6</sub>	
UTSA-74a	104	0.16	S7	
1a	100.8	0.12	This work	
SIFSIX-21-Ni	90.7	0.14	S8	
$CAU-10-H$	89.8	$\overline{\phantom{a}}$	S <sub>9</sub>	
ZJU-74a	85.7	0.13	S10	
$ZNU-1$	76.3	0.1	S11	
<b>SNNU-313-Cl</b>	76.2	0.13	S12	
$JCM-1$	75.0	0.12	S13	
ZU-610	72.8	0.13	S14	
UTSA-300a	69.5	0.13	S15	
$JNU-1$	60.0	0.10	S16	
ZrT-1-tetrazol	57.7	$\overline{\phantom{0}}$	S17	
$Ni3(pzdc)2(7Hade)2$	52.9	0.12	S18	
$CuI(\omega)UiO-66-(COOH)2$	47.9	0.11	S19	
$CPL-1-NH2$	41.2	0.09	S20	

#### <span id="page-8-1"></span>**S3-1. Isosteric Heat of Adsorption**

The adsorbate molecules (CO<sub>2</sub>, CH<sub>4</sub>, C<sub>2</sub>H<sub>2</sub>, C<sub>2</sub>H<sub>4</sub> and C<sub>2</sub>H<sub>6</sub>) and the adsorbent lattice atoms is reflected in the isosteric heat of adsorption  $(Q_{st})$  using Virial 2 model, which define as:

$$
lnP = lnN + 1/T \sum_{i=0}^{m} a_i N^i + \sum_{i=0}^{n} b_i N^i \quad (1)
$$

$$
Q_{st} = -R \sum_{i=0}^{m} a_i N^i \quad (2)
$$

Here, *Q*st is the coverage-dependent enthalpy of adsorption, *P* is the pressure (mmHg), *N* is the adsorbed amount (mg/g), *T* is the temperature (K), *a<sup>i</sup>* and *b<sup>i</sup>* are virial coefficients, and *m* and *N* represent the number of coefficients used to describe the isotherms.  $Q_{st}$  is the coverage–dependent

enthalpy of adsorption and *R* is the universal gas constant. A virial-type equation (**1**) was used to fit adsorption data at 273 K and 298 K, and then the values of *ɑ<sup>0</sup>* through *ɑ<sup>m</sup>* were used to calculate the isosteric heat of adsorption using equation (**2**).



Model	$Q_{\rm st}$ (User)				
Equation	$y=ln(x)+1/K*(a0+a1*x+a2*x^2+a3*x^3+a4*x^4+a5*x^5)+(b0)$				
Plot	$C_2H_2-298K$	$CO2$ -298K	$C_2H_6$ -298K	$C_2H_4-298K$	$CH4-298K$
a <sub>0</sub>	-3952.70986	-3489.14808	-3633.91412	$-3608.9671$	$-2125.6155$
a1	$-9.8061$	6.42307	2.99682	10.98306	$-364.03645$
a2	0.15103	$-0.0061$	0.66592	0.81971	158.88258
a <sub>3</sub>	$-0.0016$	$1.49673*10^{-4}$	$-0.0148$	$-0.01677$	$-28.32673$
a <sub>4</sub>	$1.64845*10^{-5}$	$-2.59128*10^{-7}$	$2.21869*10^{-4}$	$2.51057*10^{-4}$	2.23417
b <sub>0</sub>	13.74304	$-1.06893*10-9$	$-1.25616*10^{-6}$	$-1.40382*10-6$	12.23594
b <sub>1</sub>	0.038	13.13678	12.76962	12.67893	
Reduced Chi-Sqr	$1.26434*10^{-4}$	$1.25635*10^{-4}$	$1.1543*10^{-4}$	$1.40661*10^{-4}$	0.18227
R-Square (COD)	0.99997	0.99996	0.99997	0.99996	0.98538
Adj. R-Square	0.99995	0.99995	0.99997	0.99995	0.93463

Fig. S11 Virial fitting of  $C_2H_2$ ,  $CO_2$ ,  $C_2H_4$ ,  $C_2H_6$ , and CH<sub>4</sub> adsorption isotherms (points) for  $Q_{st}$ calculation on **1a**.

#### <span id="page-10-0"></span>**S3-2. Ideal Adsorbed Solution Theory (IAST)**

The experimental measured loadings for pure  $CO_2$ ,  $CH_4$ ,  $C_2H_2$ ,  $C_2H_4$  and  $C_2H_6$  (measured at 273 and 298 K) in samples were fitted with a dual Langmuir-Freundlich (L-F) model (equation **3**):

$$
q = \frac{a_1 * b_1 * p^{c_1}}{1 + b_1 * p^{c_1}} + \frac{a_2 * b_2 * p^{c_2}}{1 + b_2 * p^{c_2}}
$$
 (3)

Where *q* and *p* are adsorbed amounts per mass of adsorbent (mmol/g) and pressures of component *i* (kPa), respectively.

IAST calculations of adsorption selectivity for binary mixtures defined by equation **4**:

$$
S_{ijj} = \frac{x_i * y_j}{x_j * y_i} \qquad (4)
$$

Where  $x_i$  and  $x_j$  are the molar loadings in the adsorbed phase in equilibrium with the bulk gas phase with partial pressures  $y_i$ , and  $y_j$ . We calculate the values of  $x_i$  and  $x_j$  using IAST of Myers and Prausnitz.



Model	$LF$ (User)				
Equation	$Al * bl * x^c l/(1 + bl * x^c l)$				
Plot	$C_2H_6-298K$	$C_2H_4-298K$	$C_2H_2-298K$	$CO2$ -298K	$CH4-298K$
A <sub>1</sub>	$3.1593 \pm$ 0.03513	$3.69706 \pm$ 0.05025	$6.23973 \pm$ 0.06375	5.86577 $\pm$ 0.08138	$4.43214 \pm$ 0.44792
b1	$0.05671 \pm$ 0.0012	$0.0324 \pm$	$0.04029 \pm$ $6.08126*10^{-4}$ 7.93605*10 <sup>-4</sup>	$0.00886 \pm$ $5.33928*10-5$	$0.00198 \pm$ $1.40198*10^{-4}$
c <sub>1</sub>	$0.86242 \pm$ 0.01183	$0.89557 \pm$ 0.01108	$0.91443 \pm$ 0.01064	$0.94839 \pm$ 0.00488	$0.99325 \pm$ 0.01101
Reduced Chi-Sqr	$1.60115*10-4$	$1.17711*10^{-4}$	$4.07429*10^{-4}$	$1.46286*10^{-5}$	4.84442*10-6
R-Square (COD)	0.99975	0.99984	0.99985	0.99998	0.99991
Adj. R-Square	0.99974	0.99983	0.99984	0.99998	0.99991

Fig. S12 Single-site Langmuir-Freundlich fitting (red lines) of  $C_2H_2$ ,  $CO_2$ ,  $C_2H_4$ ,  $C_2H_6$ , and  $CH_4$ adsorption isotherms (black points) on **1a** at 298 K.

#### <span id="page-10-1"></span>**S3-3. Dynamic Gas Breakthrough Experiments**

The mixed-gas breakthrough separation experiment was measured at 296 K using a lab scale fix-bed reactor. The as-synthesized sample 0.985 g of **1**a (985 mg) was degasified in-situ in the column through vacuuming at 333 K for 6 h before the measurement. A helium flow (10 mL/min) was used after the activation process to purge the adsorbent. The flow of He was then turned off, while a gas mixture of 50%  $C_2H_2$ , 50%  $CO_2$  at 1 mL/min was allowed to flow into the column. The outlet composition was continuously monitored by gas chromatograph until complete breakthrough was achieved. On the basis of the gas balance, the gas adsorption capacities can be determined as follows:

$$
q_{i} = \frac{C_{i}V}{22.4 \times m} \times \int_{0}^{t} (1 - \frac{F}{F_{0}})dt
$$
 (5)

Where *qi* is the equilibrium adsorption capacity of gas *i* (mmol/g), *Ci* is the feed gas concentration, *V* is the volumetric feed flow rate (cm<sup>3</sup>/min), *t* is the adsorption time (min),  $F_0$  and  $F$ are the inlet and outlet gas molar flow rates, respectively, and m is the mass of the adsorbent (g).

The separation factor  $(α)$  of the breakthrough experiment is determined as:

$$
\alpha = \frac{q_1 y_2}{q_2 y_1} \quad (6)
$$

In which  $y_i$  is the molar fraction of gas *i* in the gas mixture.

#### <span id="page-11-0"></span>**S3-4. GCMC Computational Details**

Grand canonical Monte Carlo (GCMC) simulations were modeled for the gas adsorption by using RASPA.<sup>1</sup> The 2×2×2 unit cell of framework with rigid structure was employed, and the *Q*eq method was used to fit the partial charges of all atoms in the framework. The interaction energies between the gas molecules and framework were computed through the Coulomb and Lennard-Jones (LJ) potentials. All parameters of the host-guest interaction behavior were modeled with the universal force field (UFF). A cutoff distance of 12 Å was used for LJ interactions, and Ewald summation was employed to compute the Coulombic interactions. The  $5\times10^6$  maximum loading steps and  $5\times10^6$  production steps were employed for each run.



**Fig.** S13 Optimum adsorption sites for  $C_2H_2$  (a) and  $CO_2$  (b) in 1a.



**Fig.** S14 Simulated probability density distribution profile of  $C_2H_2$  (a-c) and  $CO_2$  (d-f) in 1a by GCMC simulation at 100 kPa and 298 K. (Note:  $C_2H_2$  was more concentrated in the voids of the adsorbent than  $CO<sub>2</sub>$ , which was compatible with experimental results.)

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