# Supporting Information

Micropores-induced high-performance Fe-Nx/C electrocatalysts

towards the oxygen reduction reaction

Micropores-induced high-performance  $Fe-N_x/C$  electrocatalysts towards the oxygen reduction reaction

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#### 1. Experimental

#### Materials

Hydrochloric acid (HCl), isopropanol, ethanol, methanol and tetrahydrofuran (THF) were purchased from Sinopharm. High purity argon, oxygen and nitrogen gas were bought from Beijing AP BAIF Gases Industry Co. Ltd. Iron (II) phthalocyanine (FePc), commercial Pt/C (20 wt.%), Nafion solution (5 wt.%) were purchased from TCI, Johnson Matthey and DuPont, respectively. Commercial carbon black (Vulcan), and high specific surface area microporous carbon (MC) were purchased from Cabot, and Shaanxi Coal and Chemical Industry Group Co., Ltd respectively. Ultrapure water (18.2 M $\Omega$  cm) obtained from a water purification system (TTL-6B) without further purity.

#### Characterization and electrochemical testing

Powder X-ray diffraction (XRD) patterns were profiled on an X-ray diffractometer (D/max-2500, Rigaku, Japan) with Cu K $\alpha$  radiation ( $\lambda$  = 1.54056 Å) source. Scanning electron microscopy (SEM) and high-resolution transmission electron microscopy (HR-TEM) images were taken on the FE-JSM-6701F (JEOL, Japan) and JSM-2100 (JEOL, Japan) microscopes, respectively. The Brunauer-Emmett-Teller (BET) specific surface area and pore size distribution were determined by nitrogen adsorption-desorption measurements with a Quantachrome AUTOSORB-SI instrument. Raman spectra were recorded with a Horiba Jobin Yvon LabRam HR800 confocal microscope using a laser of 632.8 nm. The X-ray photoelectron spectroscopy (XPS) was performed with the Thermo Fisher Scientific ESCALAB 250 spectrometer using the C 1s peak (285 eV) as the reference for binding energy calibration. The FT-IR analysis was performed to determine the functional groups using Nicolet 8700/Continuum XL and the ultraviolet (UV) absorption spectroscopy was carried out using a Shimadzu UV-2450 with wavelength from 300 to 900 nm.

All the electrochemical measurements were conducted with an RRDE-3A electrochemical workstation (ALS/DY2323 Bi-potentiostat) using a standard three-electrode system at room temperature. A glassy carbon rotating disk electrode (RDE) or rotating ring disk electrode (RRDE) coated with electrocatalyst was used as the working electrode, a Pt wire and a saturated calomel electrode as the counter and reference electrodes, respectively. All potentials reported in this work were in reference to the reversible hydrogen electrode (RHE). In a typical preparation of working electrode, 10 mg of electrocatalyst was ultrasonically blending with 2.0 mL of ethanol and 20  $\mu$ L of Nafion (5 wt. %, Dupont) for 0.5 h to form a homogeneous electrocatalyst ink, 10  $\mu$ L of which was transferred onto the polished RDE or RRDE, leading to a geometric loading of 0.394 mg cm<sup>-2</sup>. The commercial Pt/C (20 wt. % of Pt, Johnson Matthey) working electrode was also used as a reference with the Pt loading of 20  $\mu$ g cm<sup>-2</sup>.

All the potentials were calibrated to the potentials vs. RHE (Potentials vs. RHE = potential vs. SCE + 0.241+0.0591\*pH V). The ORR experiments were carried out in 0.1 M KOH solution at the ambient temperature after being purged with O<sub>2</sub> or N<sub>2</sub> gas for 20 min. The glassy carbon rotating disk electrode is 4 mm in diameter. Koutecky–Levich (K-L) plots reflecting the relation of current density ( $J^{-1}$ ) versus rotation rate ( $\omega^{-1/2}$ ) were constructed according to:  $J^{-1} = J_{k}^{-1} + (0.2nFC_{O_2}D_{O_2}^{2/3}\gamma^{-1/6})^{-1}\omega^{-1/2}$ 

where  $J_k$  is the kinetic-limiting current, *n* is the number of electrons transferred per oxygen molecule, *F* is the Faraday constant (96,485 C mol<sup>-1</sup>),  $C_{O2}$ ,  $D_{O2}$  and  $\gamma$  are the concentration, the diffusion coefficient of oxygen and the kinematic viscosity, respectively, in 0.1 M KOH. For the Tafel plots, the kinetic current  $(J_k)$  was calculated from the mass-transport correction of RDE by:

$$J_k = \frac{J \times J_d}{J_d - J}$$

where  $J_d$  is the diffusion limited current density.

The percentage of hydrogen peroxide yield (%  $HO_2^-$ ) and the corresponding electron transfer number (*n*) was calculated by RRDE data from:

% HO<sub>2</sub> = 200 × 
$$\frac{I_r/N}{I_d + I_r/N}$$

$$n = 4 \times \frac{I_d}{I_d + I_r/N}$$

where  $I_d$  is disk current,  $I_r$  is ring current and N = 0.37 is the current collection efficiency of the Pt ring.

## 2. Supporting Results and Discussion.

sample	S <sub>BET</sub> (m <sup>2</sup> g <sup>-1</sup> )	S <sub>micro</sub> (m <sup>2</sup> g <sup>-1</sup> )	Porous volume (m <sup>3</sup> g <sup>-1</sup> )	microporous volume (m <sup>3</sup> g <sup>-1</sup> )
МС	3072	2305	1.613	1.011
Fe-N-MC	812	621	0.406	0.275
СВ	230	96	0.207	0.041
Fe–N–CB	65	0	0.107	0
CNT	22	0	0.030	0
Fe–N–CNT	21	0	0.027	0

Table S1. Pore characteristics of MC, Fe–N–MC, CB, Fe–N–CB, CNT, and Fe–N–CNT.

	Content of different N						Content of different	
Sample	C (at. %)	N (at. %)	species (at. %)		O (at.	Fe (at.	Fe species (at. %)	
			Pyrrole N /M-N	C-N	%)	%)	Fe(II)	Fe (Ш)
Fe–N–	92 51	4 41	2.22	2.00	10.02	1.25	0.42	0.92
MC	83.51	4.41-	2.33	2.08	10.83	1.25	0.42	0.83
Fe–N–	95 (9	( )7	1.11	5.20	7.24	0.62	0.28	0.34
СВ	85.68	85.68 6.37	1.11	5.26	7.34	0.02	0.28	0.34
Fe–N–	96.62	4.02	2.15	1.00	0.07	0.40	0.22	0.20
CNT	86.62	4.03	2.15	1.88	8.86	0.49	0.23	0.26
FePc	81.35	10.92	1.92	9.00	6.28	1.45	1.03	0.42

Table S2. The C-, N-, O- and Fe-content of Fe–N–MC, Fe–N–CB and Fe–N–CNT.

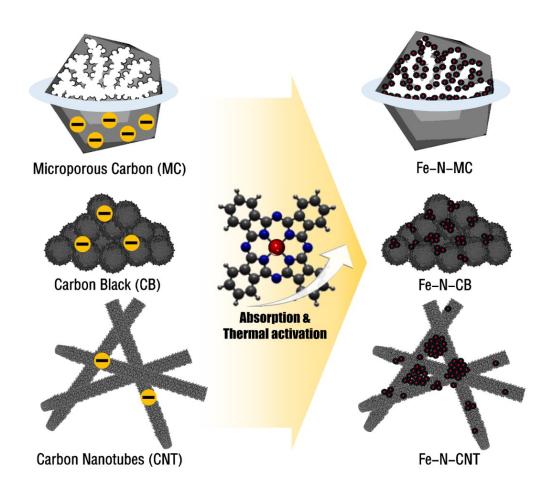
**Table S3.** Mössbauer parameters and assignment of the six components featured in thedeconvoluted Mössbauer spectrum of Fe–N–MC.

Fe species	IS / mm s <sup>-1</sup>	QS / mm s <sup>-1</sup>	Area (%)	assignment
D1	0.34113	0.7324	83.25	Fe <sup>II</sup> N <sub>4</sub>
D2	0.61689	2.1965	7.04	Fe <sup>II</sup> N <sub>2+2</sub>
D3	0.07068	1.8890	9.72	N-Fe <sup>(II/III)</sup> -N <sub>2+2</sub>

J<sub>d</sub> @ 0.1 V J<sub>k</sub> @ 0.9 V E<sub>1/2</sub> (V) Sample Eonset (V\*) (mA cm<sup>-2</sup>) (mA cm<sup>-2</sup>) Fe–N–MC 0.90 6.16 5.51 0.97 0.86 6.03 1.06 Fe-N-CB 0.95 0.90 0.80 Fe-N-CNT 5.75 0.15 Pt/C 0.97 0.84 6.10 1.25

**Table S4.** The electrochemical performance of Fe–N–MC, Fe–N–CB, Fe–N–CNT and 20% Pt/C in 0.1 M KOH

\*: versus reversible hydrogen electrode, vs. RHE, the same below



Scheme S1. The preparation process of Fe–N–MC, Fe–N–CB and Fe–N–CNT.

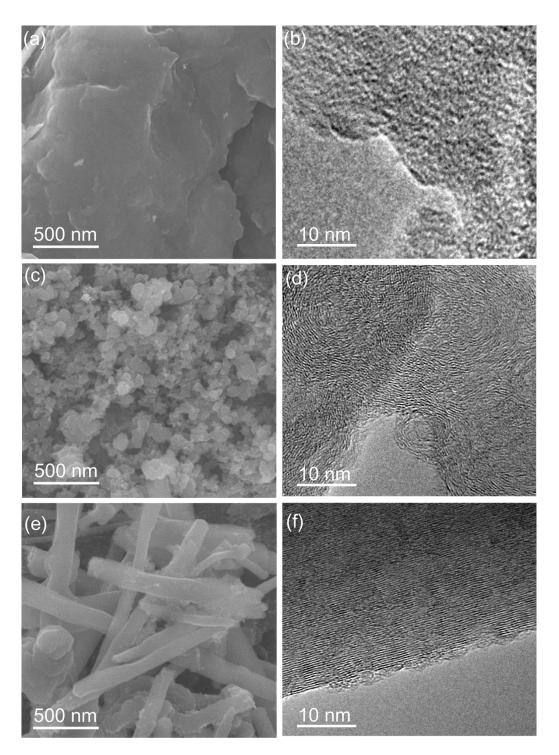


Fig. S1 Typical SEM and corresponding TEM images of (a, b) MC (c, d) CB and (e, f) CNT.

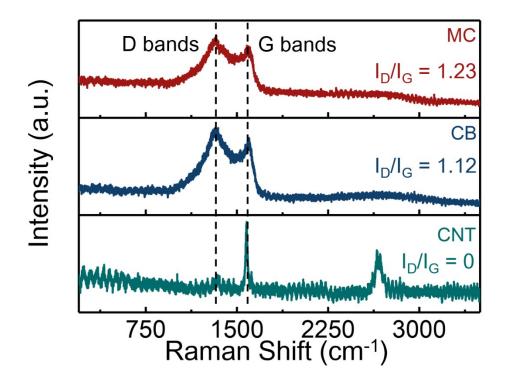


Fig. S2 Raman spectra of MC, CB and CNT carbon supports.

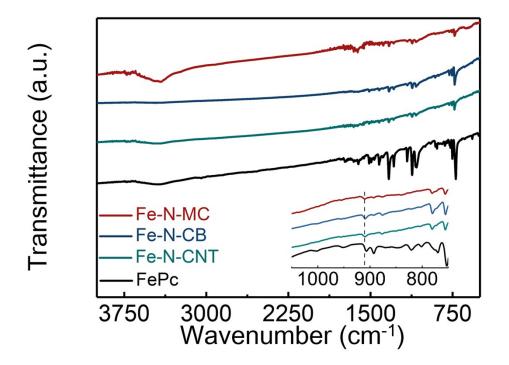
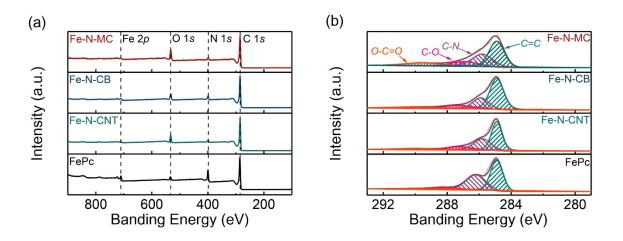


Fig. S3 FT-IR spectra of Fe–N–MC, Fe–N–CB, Fe–N–CNT and FePc supports.



**Fig. S4** (a) Survey XPS spectra and (b) High-resolution XPS spectra of C 1s for the Fe–N–MC, Fe–N–CB and Fe–N–CNT electrocatalysts.

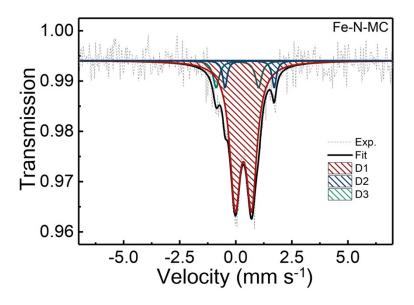


Fig. S5 <sup>57</sup>Fe Mössbauer spectroscopy of Fe–N–MC.

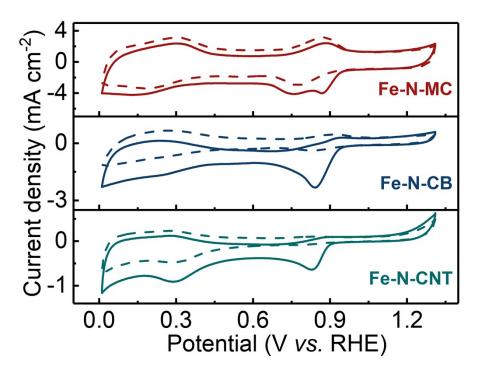


Fig. S6 CV curves for Fe–N–MC, Fe–N–CNT, Fe–N–CB in  $O_2$ -saturated (solid line) and  $N_2$ -saturated (dash line) 0.1 M KOH solution at a sweep rate of 50 mV s<sup>-1</sup>.

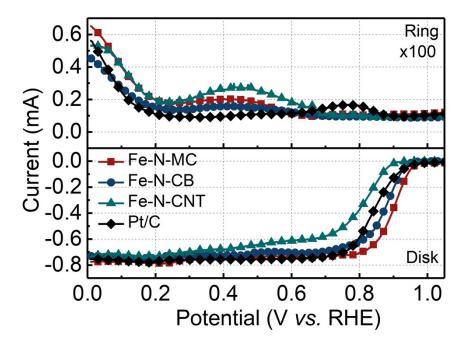
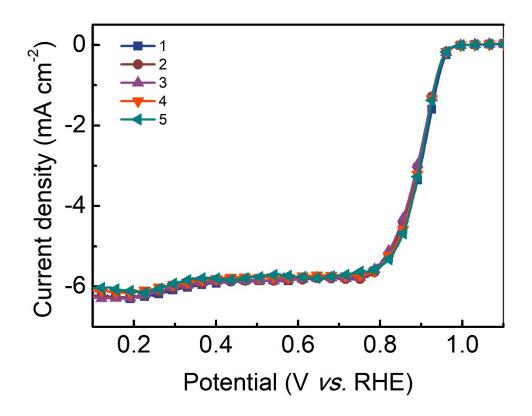


Fig. S7. The disk current (the lower half) and ring current (the upper half) in the RRDE tests of Fe–N–MC, Fe–N–CNT, Fe–N–CB and Pt/C in  $O_2$ -saturated 0.1 M KOH solution at a sweep rate of 5 mV s<sup>-1</sup> with a rotation rate of 1600 rpm.



**Fig. S8** The ORR performance of Fe–N–MC electrocatalysts which were prepared in large-scale from different areas of crucible.

Sample	Electrolyte	Eonset (V)	E <sub>1/2</sub> (V)	Ref.	
FePc/Ti <sub>3</sub> C <sub>2</sub> T <sub>x</sub>	0.1 M KOH	0.975 vs. RHE	0.886 vs. RHE	<b>S</b> 1	
FePc-Py-CNT	0.1 M KOH	0.990 vs. RHE	0.915 vs. RHE	S2	
NT-FePc-400	0.1 M KOH	0.94 vs. RHE	0.86 vs. RHE	S5	
RGO–FePc	0.1 M KOH	0.020 vs. Hg/HgO	-0.025 vs. Hg/HgO	96	
CNT-FePc	0.1 M KOH	0.018 vs. Hg/HgO	-0.024 vs. Hg/HgO	- S6	
DCI–Fe–700	0.1 M KOH	0.95 vs. RHE	0.88 vs. RHE	S8	
SA-Fe-HPC	0.1 M KOH	0.99 vs. RHE	0.89 vs. RHE	S9	
Fe–N–MC	0.1 M KOH	0.98 vs. RHE	0.90 vs. RHE	This work	

**Table S6.** Comparison of ORR performance in alkaline and acidic electrolyte for Fe–N–MC with the reported Fe–N–C (derived from FePc) catalysts.

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