

*Supplementary Information*

*for*

Asymmetric Nanoporous Membranes for  
ethanol/water Pervaporation Separation and Their  
Design

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## 1. Free Energy Calculation

The Helmholtz free energy profiles for ethanol molecules are calculated to shed light on the diffusion behavior of ethanol near the permeate-side surface. Provided that ethanol is a dominant phase in the system, their free energy profiles are computed directly from the concentration profiles along the z-axis. The calculation of free energy is based on Equation 1:

$$\Delta A = -k_b T \ln \frac{C_i(z)}{C_{i,ref}} \quad (1)$$

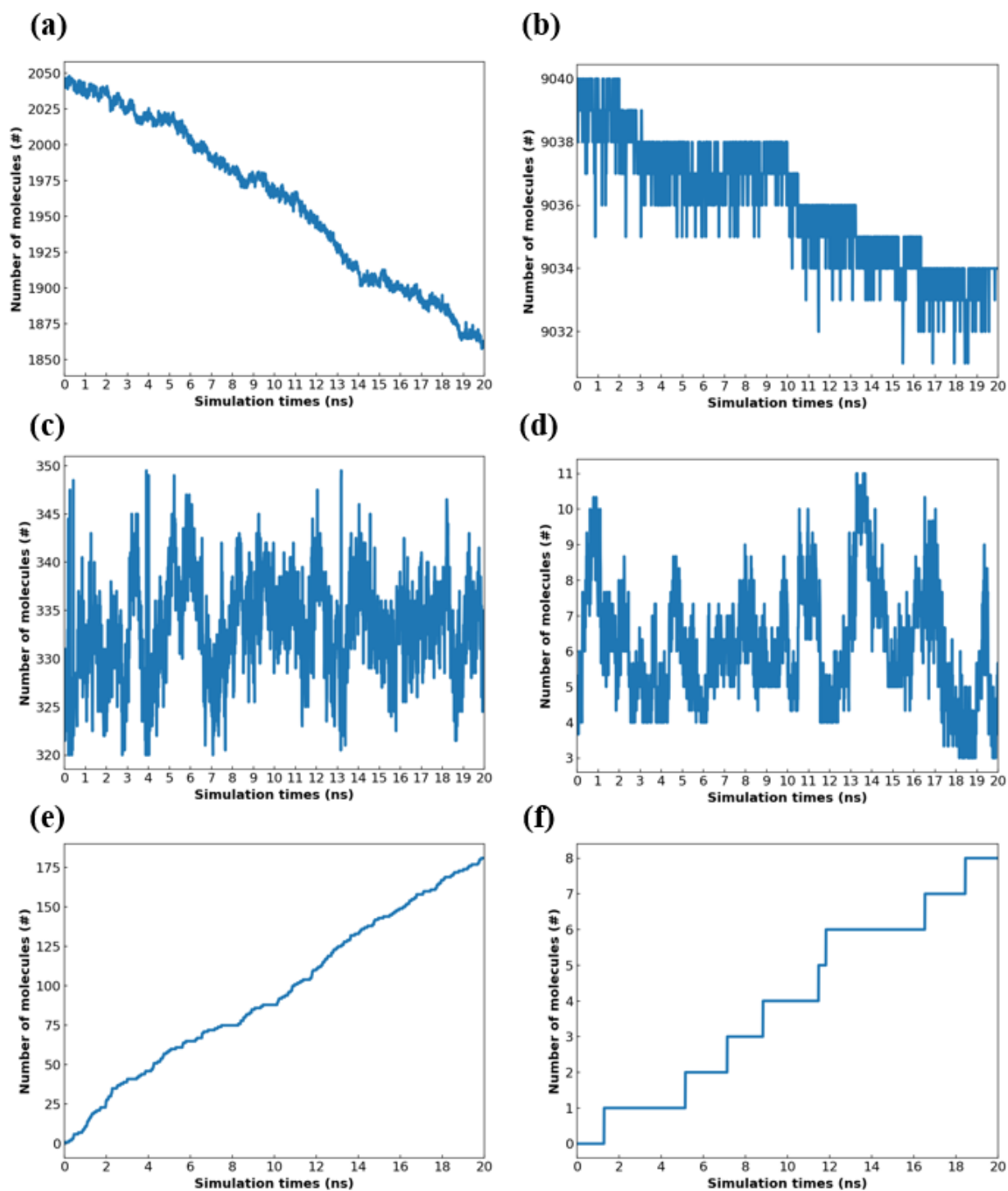
Where  $k_b$  is the Boltzmann constant, T is the temperature,  $C_i(z)$  is the ethanol concentration at a specific position, and  $C_{i,ref}$  denotes the maximum concentration of ethanol molecules along the z-axis.

**Table S1.** The results for the four types of membrane separation factor and thickness-normalized flux are presented per four independent calculations.

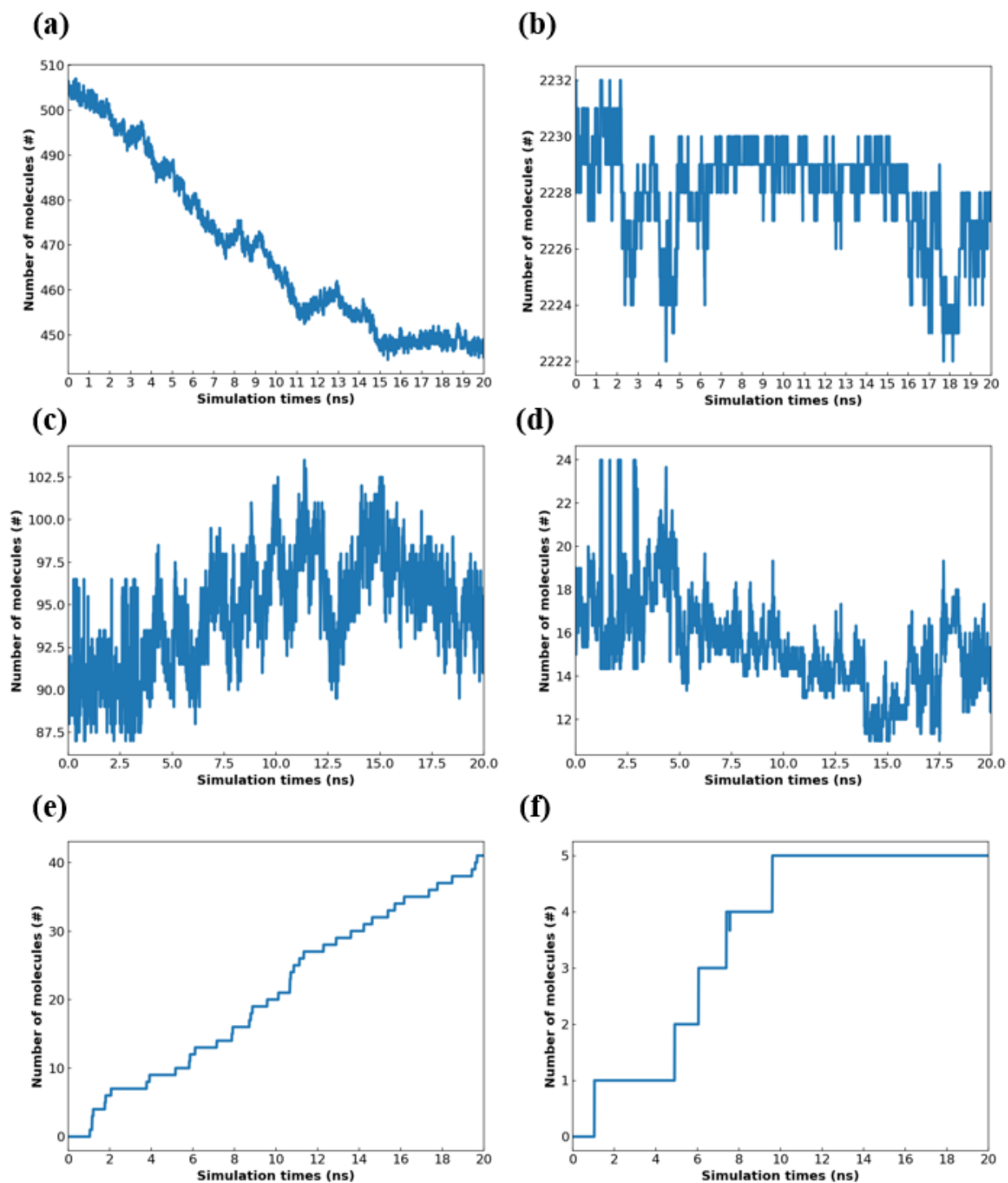
Membrane type	Separation factor ( $\alpha$ )	Thickness normalized flux (Kg Å/m <sup>2</sup> h) (J)
MFI (random seed 1)	21.61	$6.24 \times 10^5$
MFI (random seed 2)	27.68	$7.70 \times 10^5$
MFI (random seed 3)	21.29	$7.04 \times 10^5$
MFI (random seed 4)	23.69	$6.14 \times 10^5$
Zigzag (random seed 1)	118.32	$8.76 \times 10^5$
Zigzag (random seed 2)	85.83	$9.24 \times 10^5$
Zigzag (random seed 3)	110.29	$9.43 \times 10^5$
Zigzag (random seed 4)	115.28	$9.85 \times 10^5$
Zigzag-MFI (random seed 1)	268.14	$1.18 \times 10^6$
Zigzag-MFI (random seed 2)	645.21	$1.03 \times 10^6$
Zigzag-MFI (random seed 3)	176.11	$1.12 \times 10^6$
Zigzag-MFI (random seed 4)	204.60	$1.07 \times 10^6$
MFI-Zigzag (random seed 1)	29.58	$7.46 \times 10^5$
MFI-Zigzag (random seed 2)	36.18	$8.98 \times 10^5$
MFI-Zigzag (random seed 3)	21.96	$9.00 \times 10^5$
MFI-Zigzag (random seed 4)	25.68	$7.53 \times 10^5$

**Table S2.** Performance comparison between experiments and simulations. The simulation results obtained in this work are the averaged values of four independent simulations with different random seeds.

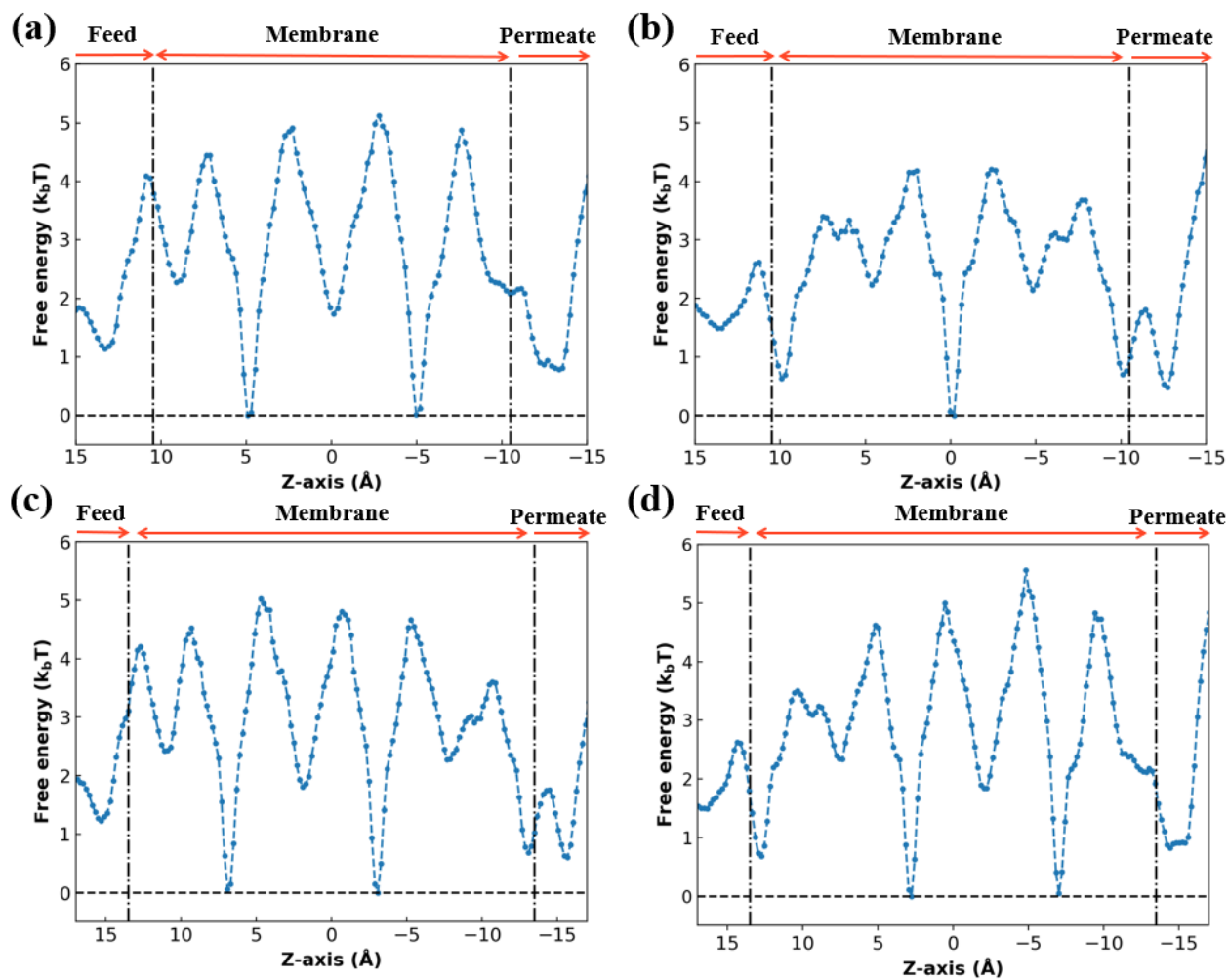
Membrane type	separation factor ( $\alpha$ )	Thickness normalized flux (Kg Å/m <sup>2</sup> h) (J)	ref
MFI/mullite tube	30-72	$8.00 \times 10^4$ - $2.26 \times 10^5$	1
MFI/YSZ fiber	47	$2.22 \times 10^5$	2
silicalite-1/ $\alpha$ - Al <sub>2</sub> O <sub>3</sub> tube	23-45	$1.01 \times 10^5$ - $1.92 \times 10^5$	3
MFI (simulation)	20.17	$5.88 \times 10^5$	4, 5
Zigzag (simulation)	136.00	$6.77 \times 10^5$	4, 5
MFI	23.57	$6.78 \times 10^5$	This work
Zigzag	107.43	$9.32 \times 10^5$	This work
Zigzag-MFI	323.52	$1.10 \times 10^6$	This work
MFI-Zigzag	28.35	$8.49 \times 10^5$	This work



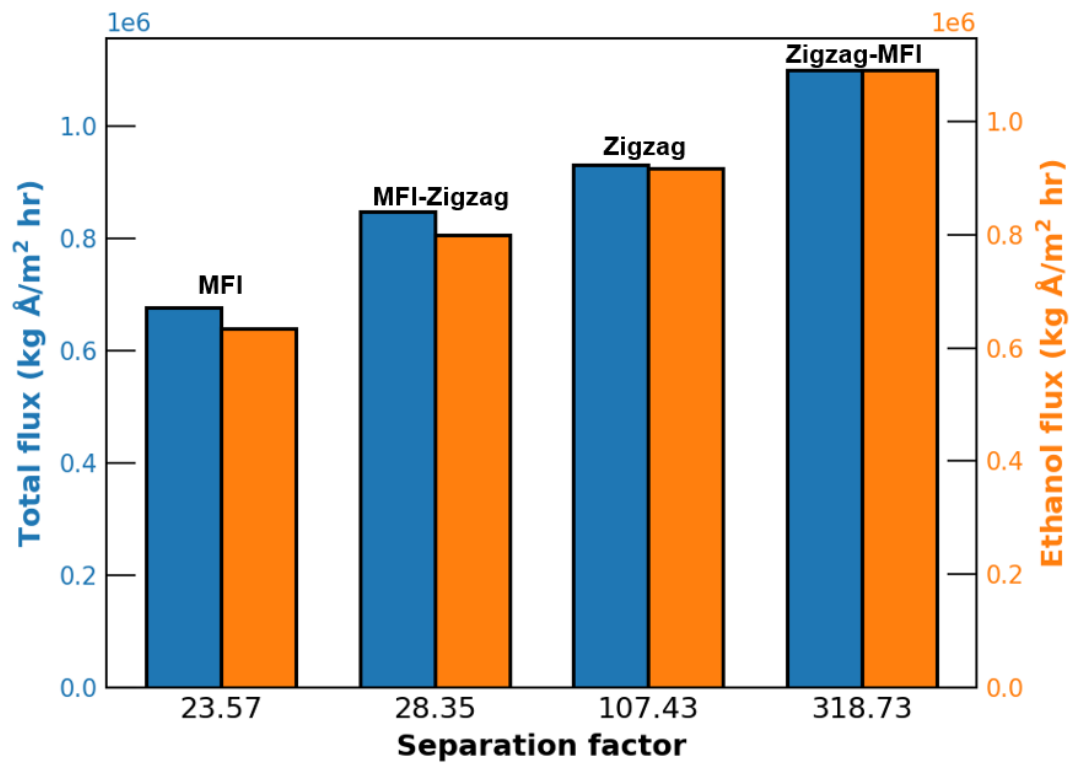
**Figure S1.** The number of (a) ethanol and (b) water molecules in the feed-side region, the number of (c) ethanol (d) water molecules within the membrane, the number of (e) ethanol and (f) water molecules on the adsorbing plate as a function of simulation time.



**Figure S2.** The number of (a) ethanol and (b) water molecules in the feed-side region, the number of (c) ethanol and (d) water molecules within the membrane, the number of (e) ethanol and (f) water molecules on the adsorbing plate as a function of simulation time observed in simulation of a smaller domain (i.e., 4-fold smaller than the simulation domain adopted to obtain all the reported main results in this work).



**Figure S3.** The free energy profiles along the permeation z-direction for ethanol in (a) MFI, (b) Zigzag, (c) MFI-Zigzag, and (d) Zigzag-MFI membranes.



**Figure S4.** Total and ethanol flux with separation factors of the four studied membranes.



## References

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