

## Supporting Information

Insights into structure-function relationships of mesoporous H-ZSM-5  
zeolite catalysts for direct amination of cyclohexene with NH<sub>3</sub>

*Haoyu Peng<sup>a</sup>, Chao Luo<sup>a</sup>, Jincheng Leng<sup>a</sup>, Zhenjie Zhang<sup>a</sup>, Wenzhou Zhong<sup>\*,a</sup>,*

*Liqiu Mao<sup>\*,a</sup>, Gouqiang Zou<sup>b</sup> and Dulin Yin<sup>a</sup>*

<sup>a</sup> National & Local United Engineering Laboratory for New Petrochemical Materials & Fine Utilization of Resources, Key Laboratory of Chemical Biology Traditional Chinese Medicine Reserach Ministry of Education, College of Chemistry and Chemical Engineering, Hunan Normal University, Changsha 410081, China

<sup>b</sup> State Key Laboratory of Powder Metallurgy College of Chemistry and Chemical Engineering, Central South University, Changsha 410083, China

\*Corresponding author. Tel.: +86-731-88872531; Fax.: +86-731-88872531.

E-mail address: zwenz79@163.com (W. Zhou); mlq1010@126.com (L. Mao)

$$\text{Conversion of cyclohexene(\%)} = \frac{[\text{the amount (mol) of starting cyclohexene}] - [\text{the amount (mol) of cyclohexene recovered}]}{[\text{the amount (mol) of starting cyclohexene}]} \times 100\%$$
$$\text{Selectivity of cyclohexylamine (\%)} = \frac{[\text{the amount (mol) of cyclohexylamine}]}{[\text{the amount (mol) of starting cyclohexane}] - [\text{the amount (mol) of cyclohexane recovered}]} \times 100\%$$

Scheme S1 The formulas for the calculations of cyclohexene conversion and cyclohexylamine selectivity

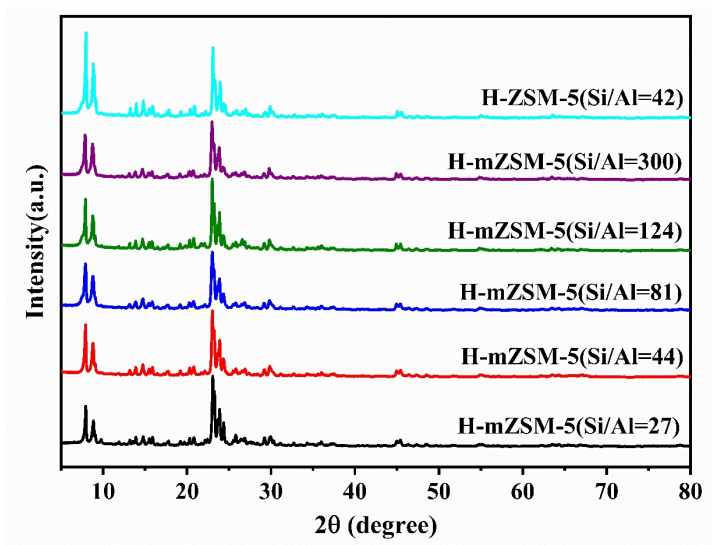


Figure S1 XRD of synthesized ZSM-5 zeolites.

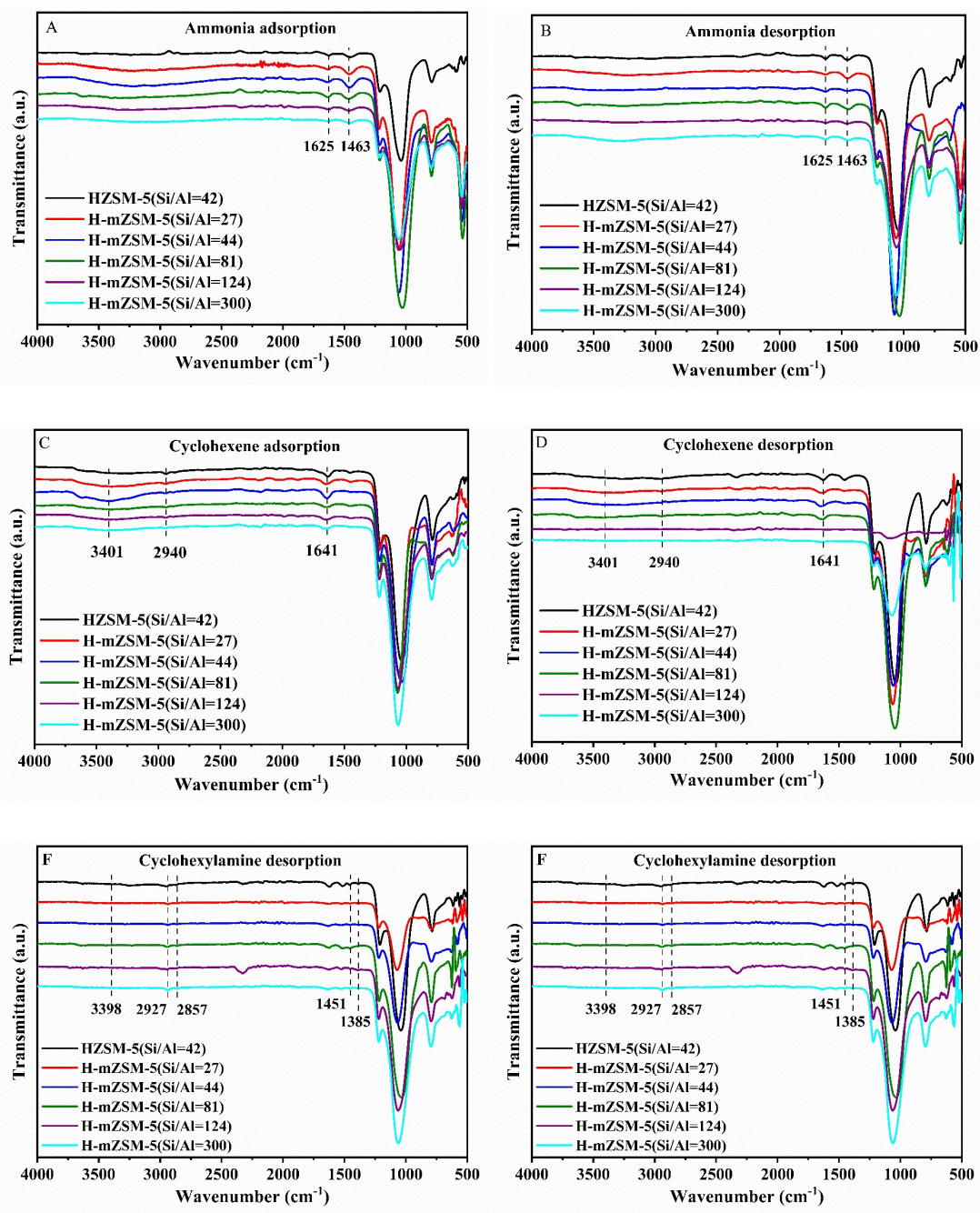


Figure S2 FT-IR spectroscopy measurements for NH<sub>3</sub> adsorption (A) and desorption (B), cyclohexene adsorption (C) and desorption (D), cyclohexylamine adsorption (E) and desorption (F) on ZSM-5 zeolites.

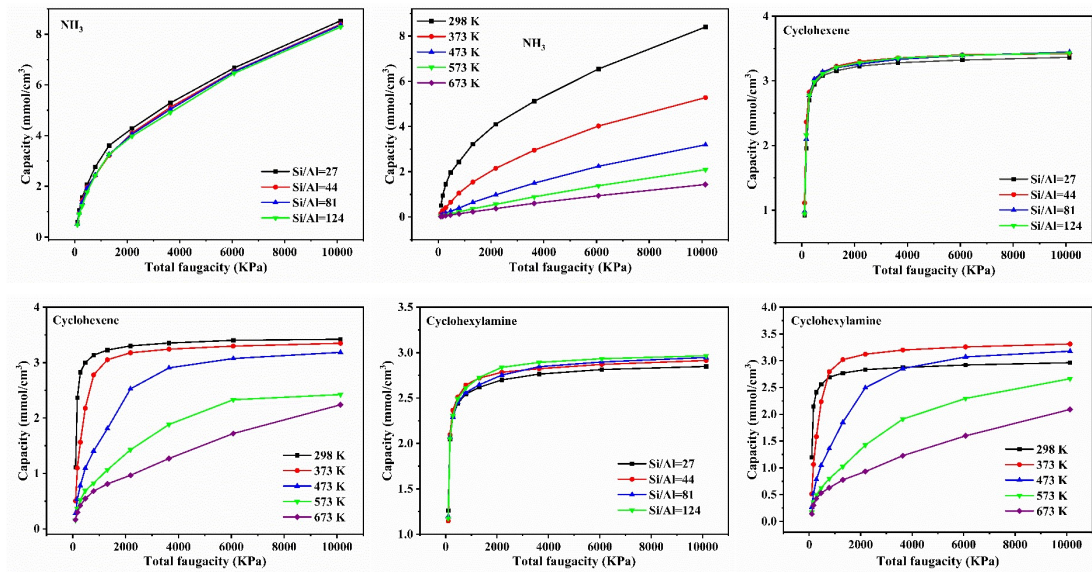


Figure S3 Adsorption capacities of pure NH<sub>3</sub>, cyclohexene and cyclohexylamine on zeolite with different Si/Al ratios and temperatures.

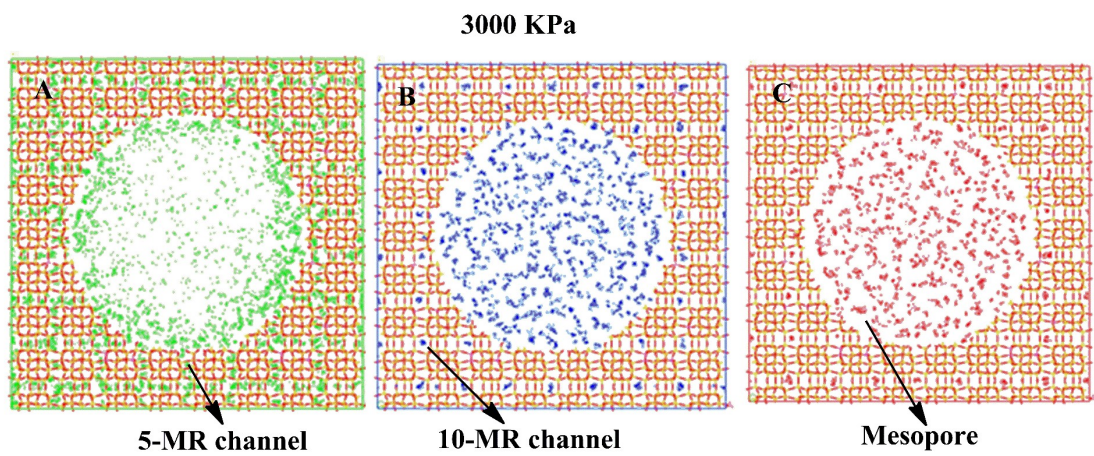


Figure S4 Configuration of adsorbed  $\text{NH}_3$  (A), cyclohexene (B) and cyclohexylamine (C) with low energy over catalysts (373K) at 3000 KPa

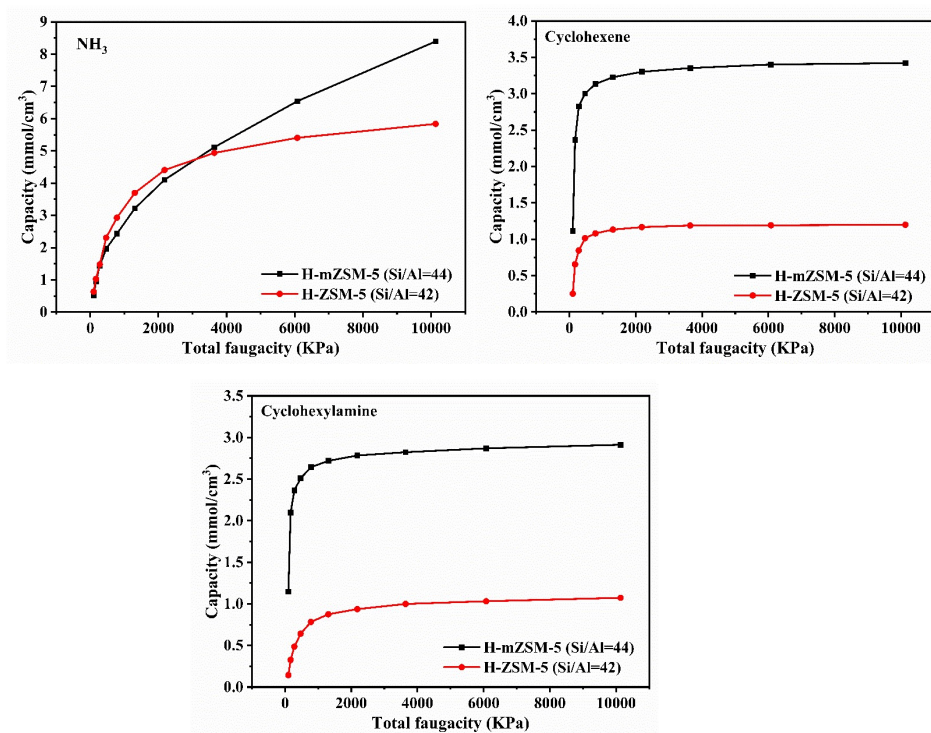


Figure S5 The comparison of the adsorption capacity between HM-ZSM-5 and HZSM-5, for NH<sub>3</sub>, cyclohexene and cyclohexylamine.

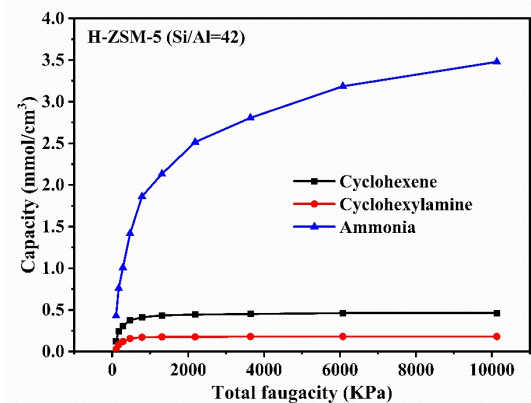


Figure S6 Adsorption capacities of NH<sub>3</sub>, cyclohexene and cyclohexylamine in a mixture on HZSM-5 zeolite.



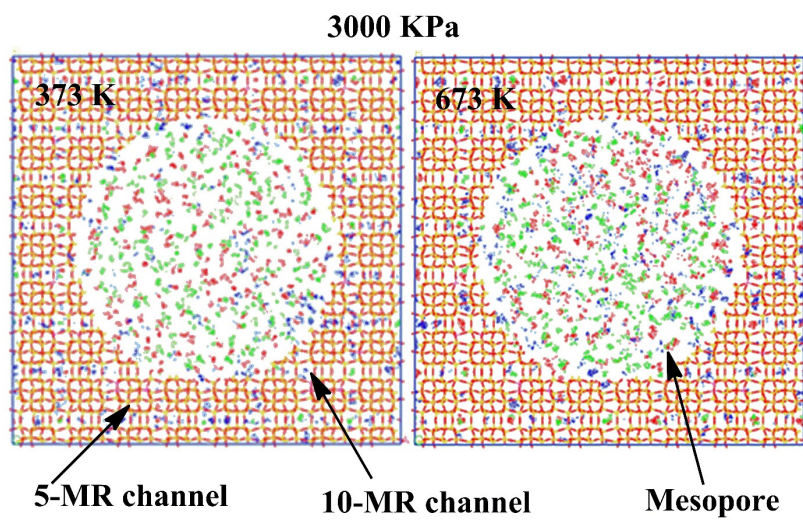


Figure S7 Configuration of adsorbed  $\text{NH}_3$ , cyclohexene and cyclohexylamine in a mixture for 573 K and 673 K with low energy over catalysts at 3000 KPa.

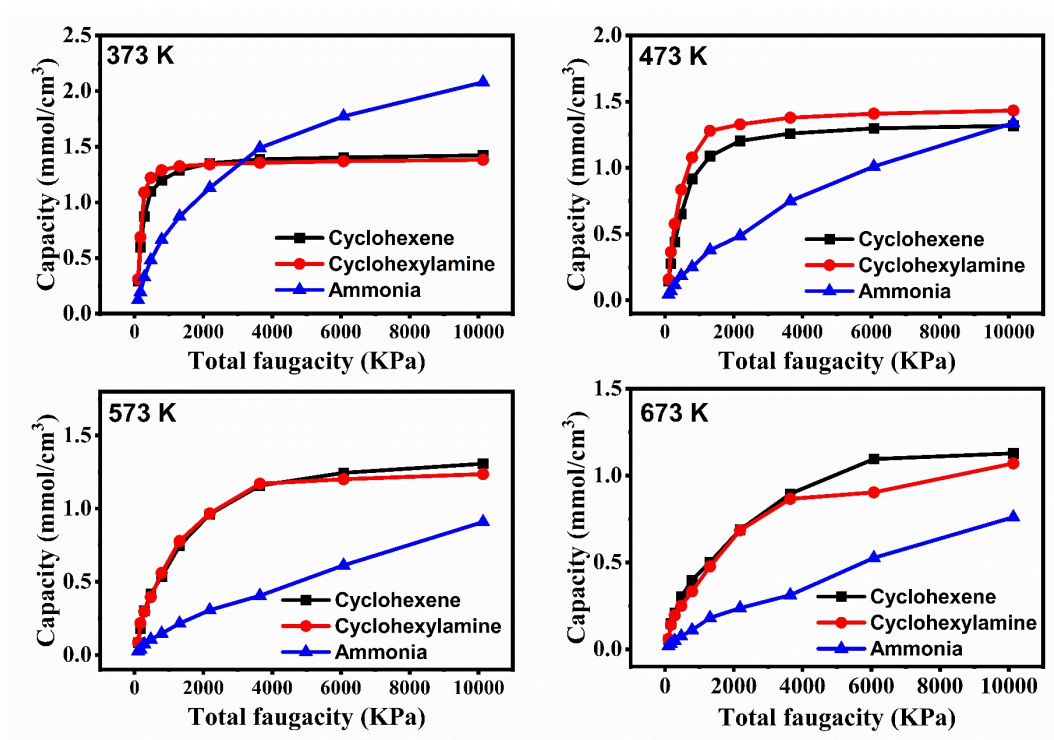


Figure S8 Adsorption capacities of  $\text{NH}_3$ , cyclohexene and cyclohexylamine in a mixture on HM-ZSM-5 zeolite with different temperatures.

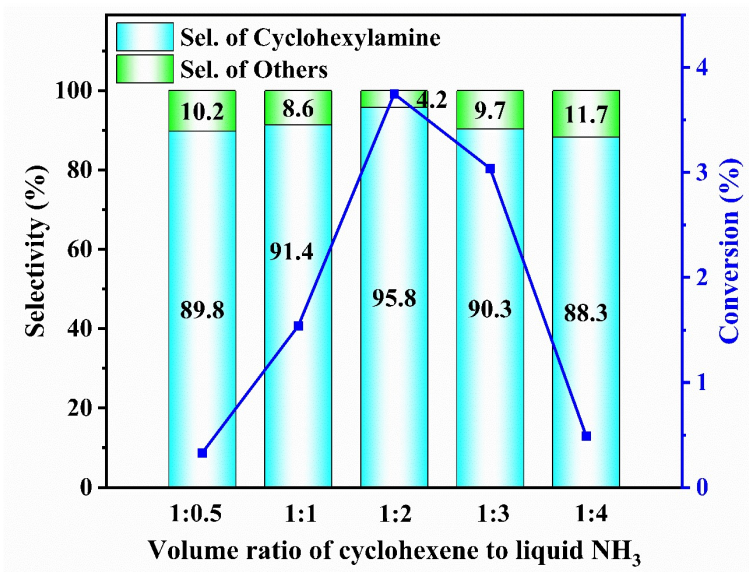


Figure S9 Effects of the volume ratio cyclohexene to ammonia on direct amination reaction

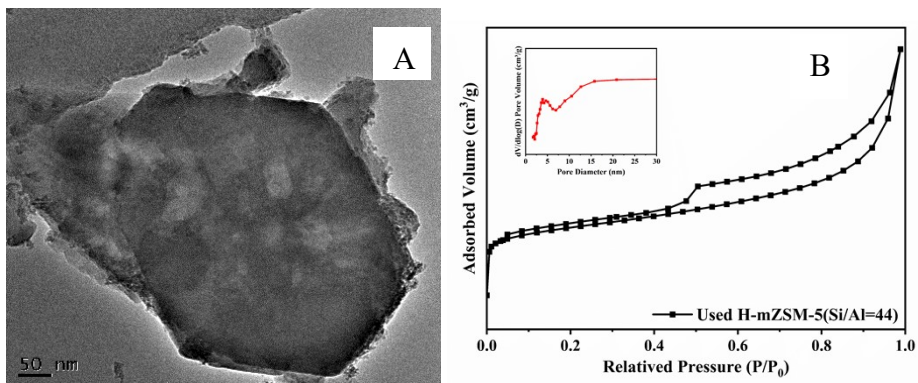


Figure S10 TEM images (A) and N<sub>2</sub> adsorption-desorption isotherms (B) of reused H-mZSM-5 zeolite.