

## Supporting Information

### Catalyst characterization

*Phase measurement* was carried out on a X-ray diffractometer (XRD) (Rigaku D/MAX 2200PC) using Ni-filtered Cu K $\alpha$  radiation at 40 kV and 30 mA. Phase evolution during the OPDH-CO<sub>2</sub> reaction was observed on a Rigaku Smart Lab diffractometer attached an *in situ* cell. Sample of 50 mg was placed into the cell and pretreated at 550 °C for 1 h in a N<sub>2</sub> flow (10 mL·min<sup>-1</sup>). Then, a C<sub>3</sub>H<sub>8</sub>-CO<sub>2</sub> (1:1) flow (20 mL·min<sup>-1</sup>) was switched into and the spectra were recorded each 30 min during the processive 160 min with scanning speed of 0.1 s and step width of 0.01°.

*Micro morphology* was observed on a field emission scanning electron microscope (FESEM) (Czech TESCAN MIRA LMS) at 30 kV and a transmission electron microscope (TEM) (FEI Talos F200X) at 200 kV.

*Texture parameters* were measured on a surface analysis instrument (JW-BK132F) using N<sub>2</sub> physicoadsorption. Sample of 200 mg was degassed at 250 °C for 4 h prior to measurement. The specific surface area was obtained using the Brunauer-Emmett-Teller(BET) model. Pore volume and distribution were obtained using the Barrett-Joyner-Halenda (BJH) model.

*CO<sub>2</sub>/C<sub>3</sub>H<sub>8</sub> temperature-programmed desorption (CO<sub>2</sub>/C<sub>3</sub>H<sub>8</sub>-TPD)* was carried out on a chemisorption instrument (Micromeritics AutoChem II 2920). Sample of 50 mg was placed into a U-shaped quartz tube and pretreated at 350 °C for 1 h in a He flow (30 mL·min<sup>-1</sup>). Then the sample was cooled down to 50 °C and adsorbed CO<sub>2</sub>/C<sub>3</sub>H<sub>8</sub> (30 mL·min<sup>-1</sup>) for 30 min. Next, the sample was purged by the He flow for 1 h. Subsequently, as the temperature rose to 800 °C at a rate of 10 °C·min<sup>-1</sup> the desorption of CO<sub>2</sub> was recorded using TCD. For *H<sub>2</sub> temperature-programmed reduction (H<sub>2</sub>-TPR)*, sample of 50 mg was loaded into the quartz tube followed by pretreatment at 300 °C for 1 h, and cooled down to ambient temperature in the He flow. Then, the H<sub>2</sub> consumed was recorded in a 10% H<sub>2</sub>/Ar flow (30 mL·min<sup>-1</sup>) as the temperature rose to 800 °C at 10 °C·min<sup>-1</sup>.

*Surface element valence analysis* was performed using X-ray photoelectron spectroscopy (XPS) (Thermo Scientific K-Alpha spectrometer) using Al K $\alpha$  X-ray radiation source. The base pressure of the chamber was less than 5×10<sup>-8</sup> Pa. The binding energy (B.E.) was calibrated to adventitious carbon using the C1s peak at 284.8 eV.

*NH<sub>3</sub> temperature-programmed desorption (NH<sub>3</sub>-TPD)* was performed on a TP-5080 adsorption instrument. Sample of 50 mg was pretreated in a He flow (30 mL·min<sup>-1</sup>) at 550 °C for 1 h and then cooled down to ambient temperature. Then NH<sub>3</sub> was adsorbed at 100 °C for 30 min followed by purge in the He flow for 0.5 h. The desorption of NH<sub>3</sub> was recorded using TCD as the temperature was raised from ambient temperature to 600 °C at 10 °C·min<sup>-1</sup>.

*Thermogravimetric (TG) analysis* of the used catalyst samples was carried out on a thermogravimetric analyzer (NETZSCH STA 449). Sample of 20 mg was heated from ambient temperature to 800 °C at a rate of 20 °C·min<sup>-1</sup> in an air flow (30 mL·min<sup>-1</sup>) and the weight was synchronously recorded.

Raman spectra were recorded on a HORIBA Scientific LabRAM HR Evolution spectrophotometer equipped with a solid state laser (532 nm wave-length, 17 mW capacity) as the excitation source and a 5x objective lens. Spectra were collected at ambient temperature in the wave number range of 100–2000  $\text{cm}^{-1}$ .

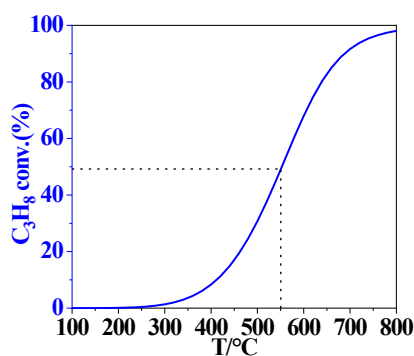


Fig. S1 Equilibrium conversions of OPDH-CO<sub>2</sub> reaction.

CO<sub>2</sub>/C<sub>3</sub>H<sub>8</sub>=1, 0.1 MPa.

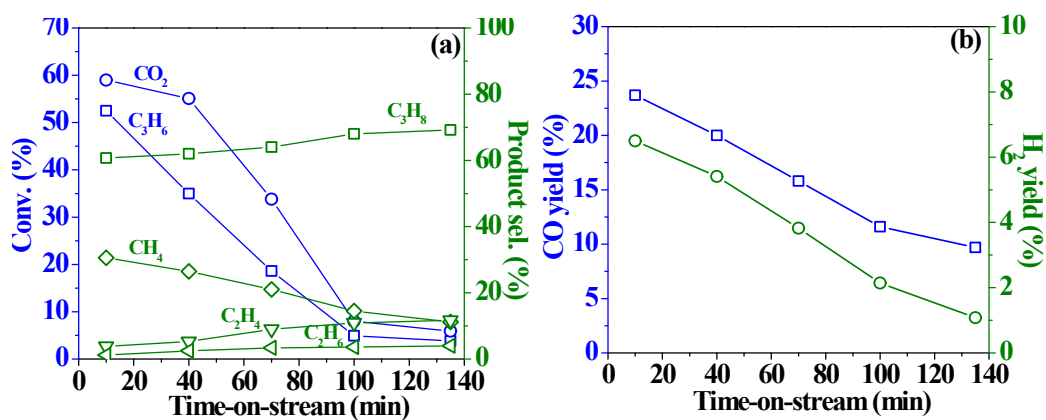


Fig. S2 C<sub>3</sub>H<sub>6</sub> reaction with CO<sub>2</sub> on Fe<sub>2</sub>O<sub>3</sub>-3ZrO<sub>2</sub>.

C<sub>3</sub>H<sub>6</sub> (CO<sub>2</sub>) conv. and product sel. (a); CO (H<sub>2</sub>) yield (b)

C<sub>3</sub>H<sub>6</sub>/CO<sub>2</sub>/Ar=1/1/1.5, W/F=12.5 g·h·mol<sup>-1</sup>, 550 °C and 0.1 MPa.

Table S1 Reported catalytic activity for OPDH-CO<sub>2</sub>

Cats	T (°C)	n(CO <sub>2</sub> )/ n(C <sub>3</sub> H <sub>8</sub> )	WHSV/ g <sub>C<sub>3</sub>H<sub>8</sub></sub> g <sub>cat</sub> <sup>-1</sup> h <sup>-1</sup>	C <sub>3</sub> H <sub>8</sub> conv. (%)	CO <sub>2</sub> conv. (%)	C <sub>3</sub> H <sub>6</sub> sel. (%)	STY/ mol <sub>C<sub>3</sub>H<sub>6</sub></sub> kg <sub>cat</sub> <sup>-1</sup> h <sup>-1</sup>	Ref.
Cr <sub>2</sub> O <sub>3</sub> /SiBeta	550	5	1.2	24.8	4.0	87.1	6.2	1
Cr-O/Al <sub>2</sub> O <sub>3</sub>	550	5	1.2	12.9	-	88.3	3.3	2
Cr <sub>2</sub> O <sub>3</sub> -ZrO <sub>2</sub>	550	2	0.3	51.1	-	81.7	2.9	3
CrO <sub>x</sub> /SBA-15	550	2	0.3	24.2	-	83.9	1.5	4
CrO <sub>x</sub> /SiO <sub>2</sub>	600	4	1.2	70	15.3	79	15.8	5
Ga <sub>2</sub> O <sub>3</sub> -Al <sub>2</sub> O <sub>3</sub>	500	2	0.15	49.7	-	91.7	1.6	6
Ga <sub>2</sub> O <sub>3</sub> -ZSM-48	600	2	0.3	52.6	-	42.2	1.6	7
In <sub>2</sub> O <sub>3</sub> -Al <sub>2</sub> O <sub>3</sub>	600	4	0.15	35	10.0	75	0.9	8
In <sub>2</sub> O <sub>3</sub> /Al <sub>2</sub> O <sub>3</sub>	600	4	0.15	14	11.0	80	0.4	9
V-MCM-41	600	4	1.0	58	10.5	90	12.4	10
V <sub>2</sub> O <sub>5</sub> -Cr <sub>2</sub> O <sub>3</sub>	550	1/3	3.5	9.9	5.0	95.9	7.9	11
V <sub>2</sub> O <sub>5</sub> -MoO <sub>3</sub>	550	1/3	3.5	10.1	3.3	96.0	8.1	11
Fe <sub>3</sub> Ni <sub>1</sub> /CeO <sub>2</sub>	550	1	11.8	2.7	4.0	58.2	3.9	12
5FeCeO <sub>2</sub>	550	1	0.59	9.50	11.0	39.0	0.5	13
Fe <sub>2</sub> O <sub>3</sub> -3ZrO <sub>2</sub>	550	1	1.1	39.9	28.2	83.7	8.7	this work

T---reaction temperature; STY---space time yield. STY--- calculated using the literatruue data.

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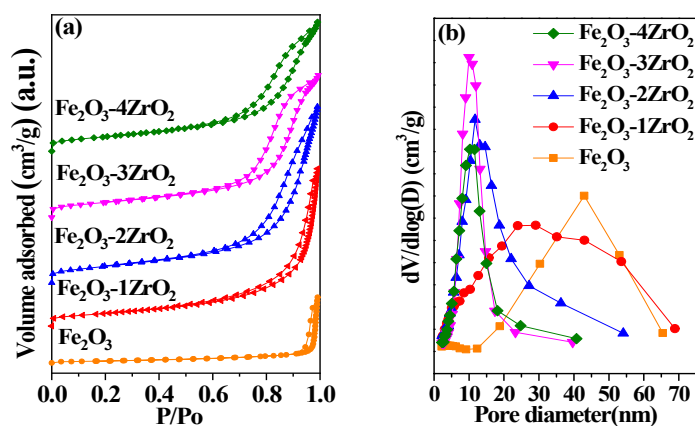


Fig. S3. N<sub>2</sub> adsorption-desorption isotherms (a) and pore distribution (b).

Table S2 Texture parameters of fresh catalysts

Catalysts	Specific surface area (m <sup>2</sup> ·g <sup>-1</sup> )	Cumulative pore volume (cm <sup>3</sup> ·g <sup>-1</sup> )	Average pore diameter(nm)
Fe <sub>2</sub> O <sub>3</sub> -4ZrO <sub>2</sub>	56.8	0.23	11.5
Fe <sub>2</sub> O <sub>3</sub> -3ZrO <sub>2</sub>	63.9	0.30	10.9
Fe <sub>2</sub> O <sub>3</sub> -2ZrO <sub>2</sub>	57.4	0.29	12.6
Fe <sub>2</sub> O <sub>3</sub> -1ZrO <sub>2</sub>	49.1	0.27	15
Fe <sub>2</sub> O <sub>3</sub>	8.1	0.11	29.7

Table S3 Surface element composition of fresh catalysts<sup>a</sup>

Catalysts	Fe (wt.%)	Zr (wt.%)	O (wt.%)	Zr/Fe (molar ratio)	Zr/Fe (nominal molar ratio)
Fe <sub>2</sub> O <sub>3</sub> -4ZrO <sub>2</sub>	6.56	23.23	70.21	2.07	2.00
Fe <sub>2</sub> O <sub>3</sub> -3ZrO <sub>2</sub>	8.20	22.10	69.70	1.58	1.50
Fe <sub>2</sub> O <sub>3</sub> -2ZrO <sub>2</sub>	11.46	19.55	68.99	1.03	1.00
Fe <sub>2</sub> O <sub>3</sub> -1ZrO <sub>2</sub>	17.34	14.59	68.07	0.52	0.50
Fe <sub>2</sub> O <sub>3</sub>	36.02	/	63.98	/	/

<sup>a</sup> Calculated from XPS measurement results.

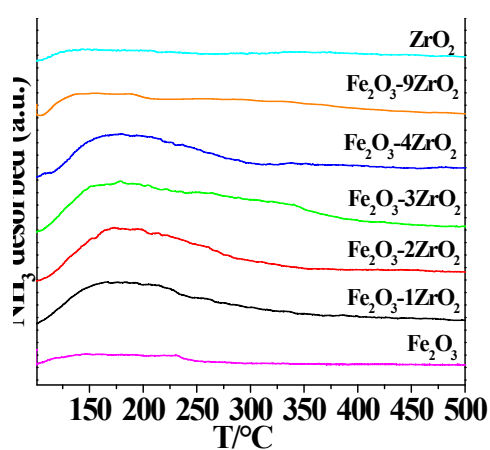


Fig. S4 NH<sub>3</sub>-TPD profiles of fresh catalysts.

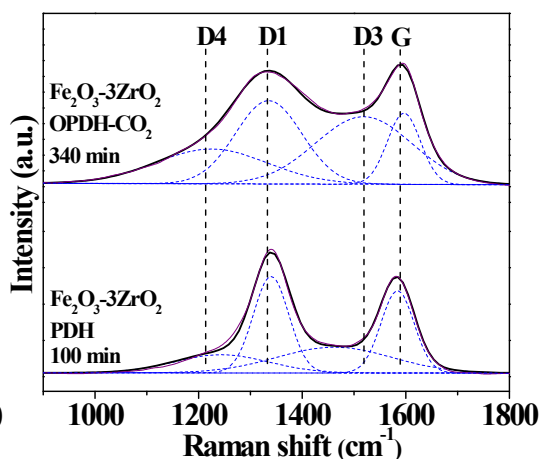


Fig. S5 Raman spectra of used catalysts.