

1 **Precise stepwise recovery of platinum group metals from high level liquid waste**
2 **based on SDB polymer modified SiO₂**

3 Kun Wu ^a, Shunyan Ning ^{b,*}, Xiangbiao Yin ^{b,*}, Sizhi Xu ^a, Yilai Zhong ^a, Zengyuan Li ^a,
4 Lifeng Chen ^b, Mohammed F. Hamza ^b, Toyohisa Fujita ^a, Yuezhou Wei ^{b,c}

5 *^aState Key Laboratory of Featured Metal Materials and Life-cycle Safety for Composite Structures,*
6 *MOE Key Laboratory of New Processing Technology for Nonferrous Metals and Materials, and*
7 *School of Resources, Environment and Materials, Guangxi University, Nanning 530004, China.*

8 *^bSchool of Nuclear Science and Technology, University of South China, 28 Changsheng West*
9 *Road, Hengyang 421001, P.R. China.*

10 *^cSchool of Nuclear Science and Engineering, Shanghai Jiao Tong University, 800 Dong Chuan*
11 *Road, Shanghai 200240, China.*

12 *Corresponding author: Shunyan Ning

13 E-mail: ningshunyan@usc.edu.cn

14 Address: School of Nuclear Science and Technology, University of South China, 28
15 Changsheng West Road, Hengyang 421001, P.R. China.

16 ORCID: 0000-0002-9573-5960

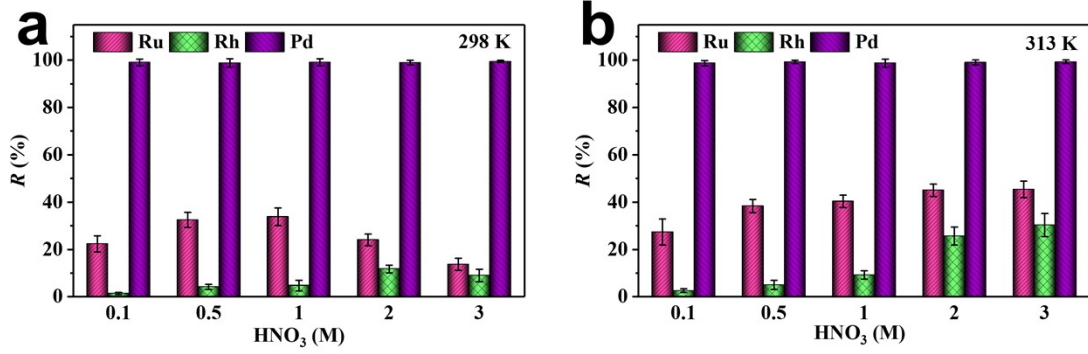
17 *Corresponding author: Xiangbiao Yin

18 Email: yinxb@usc.edu.cn

19 Address: School of Nuclear Science and Technology, University of South China, 28
20 Changsheng West Road, Hengyang 421001, PR China.

21 ORCID: 0000-0003-2319-1789

22 **3.2.1. Effects of HNO₃ concentration and temperature**



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24 **Fig. S1.** Effect of HNO₃ concentrations on the adsorption of PGMs by dNbpy/SiO₂-P at 298 K (a), 313

25 K (b) ($m/V = 0.02$ g/mL, C_0 : 1 mM, $t = 24$ h).

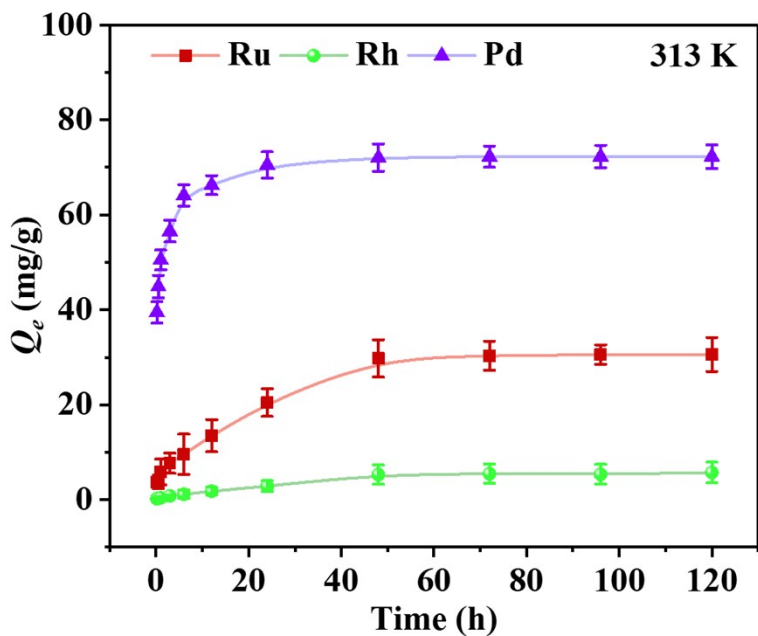
26 3.2.2 Kinetics study

Pseudo-first-order kinetics model: $\ln(Q_e - Q_t) = \ln Q_e - k_1 t$ (S1)

Pseudo-second-order kinetics model: $\frac{t}{Q_t} = \left(\frac{1}{Q_e}\right)t + \frac{1}{k_2 Q_e^2}$ (S2)

27 Where k_1 (h⁻¹) and k_2 (mg·g⁻¹·h⁻¹) are the adsorption rate constants of pseudo-first-
 28 order kinetics model and pseudo-second-order kinetics model, the equilibrium
 29 adsorption capacity and the adsorption quantity at time t (min), respectively, are Q_e
 30 (mg·g⁻¹) and Q_t (mg·g⁻¹).

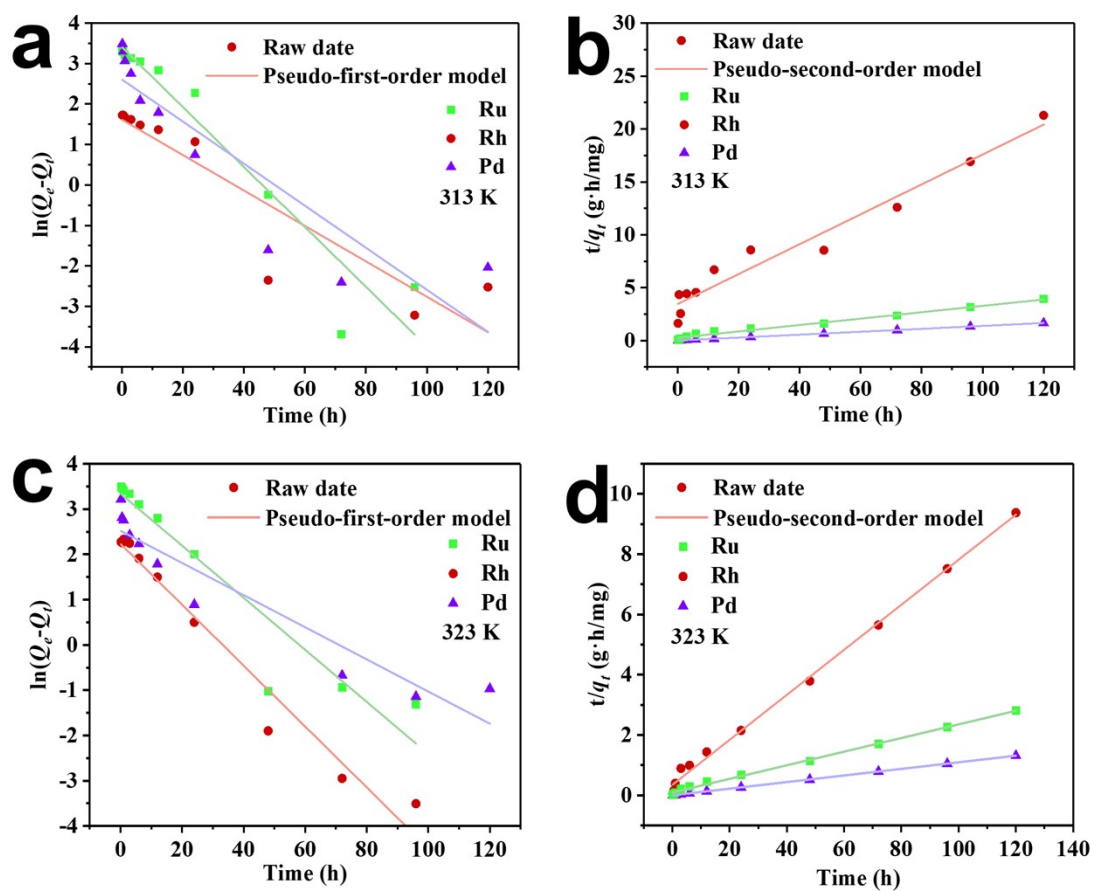
31 In this work, both pseudo-first-order kinetics model and pseudo-second-order
 32 kinetic model were applied to analyze the experimental data.



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34 **Fig. S2.** Adsorption kinetics of PGMs on dNbpy/SiO₂-P at 313 K ($m/V = 0.02$ g/mL, $C_{\text{Ru(III)}}: 10$ mM,

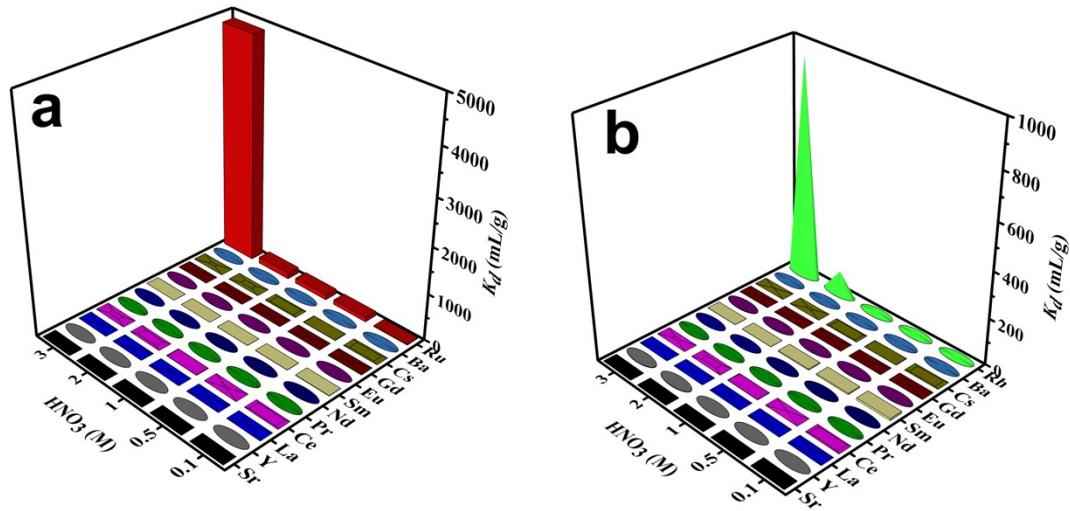
35 $C_{\text{Rh(III)}}: 5$ mM, $C_{\text{Pd(II)}}: 20$ mM, $C_{\text{HNO}_3}: 3$ mol/L).



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37 **Fig. S3.** Adsorption kinetics fitting results of PGMs on dNbpy/SiO₂-P at 313 K (a, b) and 323 K (c, d)

38 ($m/V = 0.02$ g/mL, $C_{\text{Ru(III)}} = 10$ mM, $C_{\text{Rh(III)}} = 5$ mM, $C_{\text{Pd(II)}} = 20$ mM, $C_{\text{HNO}_3} = 3$ mol/L).



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Fig. S4. Ru(III) (a) and Rh(III) (b) distribution coefficients.

41 **Table S1** SF data for PGMs.

HNO_3/M	$SF_{\text{Ru/M}}$	$SF_{\text{Rh/M}}$	$SF_{\text{Pd/M}}$
0.1	33	4	543
0.5	170	9	930
1	188	59	1412
2	230	74	3716
3	1705	336	3805

42 3.2.3. Isotherm study

$$\text{Langmuir model: } Q_e = \frac{q_m \times K_L \times C_e}{1 + K_L \times C_e} \quad (\text{S3})$$

$$\text{Freundlich model: } Q_e = K_F \times C_e^{\frac{1}{n}} \quad (\text{S4})$$

43 where Q_e ($\text{mg} \cdot \text{g}^{-1}$) and q_m ($\text{mg} \cdot \text{g}^{-1}$) are the equilibrium and computed maximum

44 adsorption capacities. C_e ($\text{mmol} \cdot \text{L}^{-1}$) stands for equilibrium ions concentration. The

45 constants in the Langmuir and Freundlich isotherm are K_L ($\text{L} \cdot \text{mg}^{-1}$) and K_F ($\text{mg}^{1-n} \cdot \text{L}^n/\text{g}$).

46 Adsorption intensity is expressed as n .

47 Langmuir model (**Eq. S4**) assumes the process is single layer adsorption that all

48 the sites are evenly distributed and have the same adsorption ability. Freundlich model
 49 (Eq. S5) assumes a heterogeneous adsorption surface with sites having different
 50 adsorption energies.

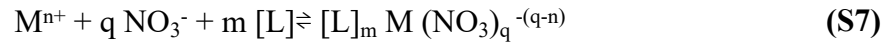
51 3.2.4. Thermodynamic analysis

$$\text{Van't Hoff equation: } \ln K_d = \frac{-\Delta H_o}{RT} + \frac{\Delta S_o}{R} \quad (\text{S5})$$

$$\text{Gibbs-Helmholtz equation: } \Delta G_o = \Delta H_o - \Delta S_o T \quad (\text{S6})$$

52 where ΔG^o , ΔH^o , and ΔS^o are the changes in Gibbs free energy (kJ/mol), enthalpy
 53 (kJ/mol), entropy (kJ/K·mol), respectively. R is the universal gas constant 8.314
 54 J/(K·mol) and K_d (mL/g) is the distribution coefficient. ΔS^o , ΔH^o are obtained according
 55 to the intercept and slope of Eq. S6 ($\ln K_d$ versus $1/T$), while then ΔG^o at different
 56 temperature can be obtained according to Eq. S7.

57 3.3.3 Slope analysis



$$\text{Partition coefficient: } D = \frac{C_1}{C_a} = \frac{(C_2 - C_a)}{C_a} \times \frac{V_a}{V_1} = \frac{[\text{L}]_m \cdot \text{M} (\text{NO}_3^-)_q}{\text{Mn}^{n+}} \quad (\text{S8})$$

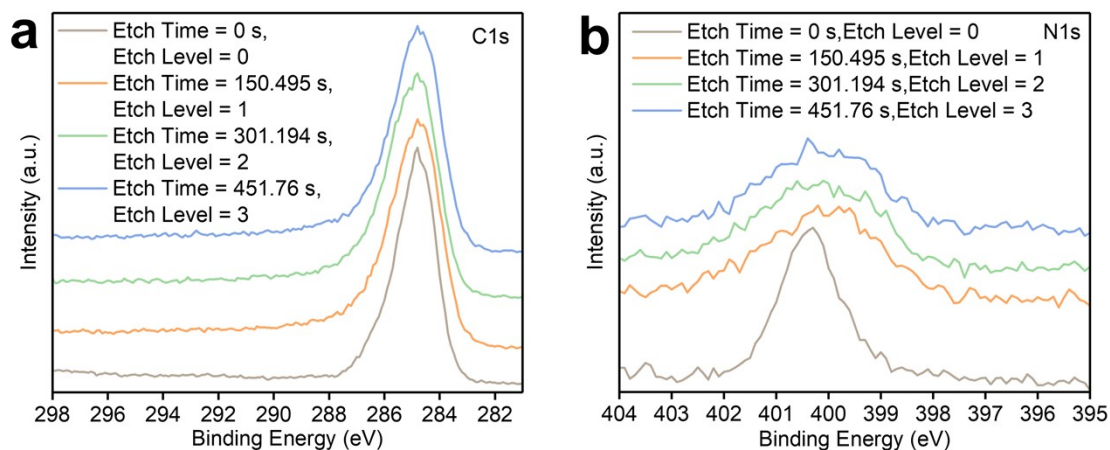
$$\text{Extraction equilibrium constant: } K' = \frac{[\text{L}]_m \cdot \text{M} (\text{NO}_3^-)_q}{\text{Mn}^{n+} [\text{L}]_m (\text{NO}_3^-)_q} \quad (\text{S9})$$

$$\text{Slope analysis equation: } \log D = \log K' + q \log [\text{NO}_3^-] + m \log [\text{L}] \quad (\text{S10})$$

58 Partition coefficient D was calculated using Eq. S9. C_1 , C_2 , and C_a represent the
 59 cation concentrations in the loaded oil phase, the initial aqueous phase before
 60 extraction, and the aqueous phase after extraction. V_a and V_1 denote the volumes of the
 61 aqueous and organic phases of the extraction experiment. Where M^{n+} represents the Ru,

62 Rh, and Pd, [L] represents dN_{bpy} , m denotes the stoichiometric coefficient. $\log D$ can
 63 be transformed from Eq. S9 and Eq. S10 to Eq. 11.

64 3.3.4 Depth-profiling XPS analysis



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Fig. S5. Fine spectra of depth-profiling XPS etched C 1s (a), N 1s (b).

67 3.4. Column experiments

68 **Table S2** Recovery yields of metal ions in the column experiment (a).

Elements	I (%)	II (%)	III (%)	IV (%)	Total (%)
Ru	0.00	99.57	0.00	0.10	99.67
Rh	0.00	99.83	0.00	0.07	99.9
Pd	0.00	0.08	0.03	99.58	99.69
Sr	0.00	99.99	0.00	0.00	99.99
Y	0.00	99.95	0.00	0.00	99.95
Cs	0.00	98.17	0.00	0.12	98.17
Ba	0.00	99.99	0.00	0.00	99.99
La	0.00	99.96	0.00	0.00	99.96
Ce	0.00	99.97	0.00	0.00	99.97
Pr	0.00	99.86	0.00	0.00	99.86
Nd	0.00	99.93	0.00	0.00	99.93
Sm	0.00	99.79	0.00	0.35	99.79
Eu	0.00	99.99	0.00	0.00	99.99

Gd	0.00	99.87	0.00	0.00	99.87
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69 **Table S3** Recovery yields of metal ions in the column experiment (b).

Elements	I (%)	II (%)	III (%)	IV (%)	Total (%)
Ru	0.00	9.43	0.00	90.35	99.78
Rh	0.00	60.92	0.00	15.37	76.29
Pd	0.00	0.00	0.00	0.00	0.00
Sr	0.00	99.32	0.00	0.07	99.39
Y	0.00	99.53	0.00	0.10	99.63
Cs	0.00	99.75	0.00	0.23	99.98
Ba	0.00	99.92	0.00	0.00	99.92
La	0.00	99.84	0.00	0.00	99.84
Ce	0.00	99.73	0.00	0.18	99.91
Pr	0.00	99.91	0.00	0.00	99.91
Nd	0.00	99.95	0.00	0.00	99.95
Sm	0.00	99.35	0.00	0.45	99.8
Eu	0.00	99.96	0.00	0.00	99.96
Gd	0.00	99.83	0.00	0.00	99.83
