Supplementary Materials

Karst-inspired hierarchical Mg/Al layered double hydroxide with high entropy-driven for interception and storage

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Text S1: Formula details

The removal efficiency (%) and phosphate adsorption capacity (mg g⁻¹) of three adsorbents were calculated using the following equations:

$$q_e = (C_0 - C_e) V/m \tag{1}$$

$$q_t = (C_0 - C_t) V/m \tag{2}$$

$$\eta = (C_0 - C_e) V/C_0 \tag{3}$$

where C_0 (mg L⁻¹) represents the phosphate concentration before adsorption; C_e (mg L⁻¹) and C_t (mg L⁻¹) represent the phosphate concentration at equilibrium and time t, respectively; V (L) represents the solution volume and m (g) represents the mass of the adsorbent.

1.1. Adsorption kinetics

The adsorption kinetics is significant in further exploring the adsorption mechanism. Pseudo-first-order,^[1] pseudo-second-order,^[2] and Elovich ^[3,4] models were applied to fit the adsorption data. The equations are as follows:

Pseudo-first-order equation:
$$q_t = q_e[1 - exp(-K_1 t)]$$
 (4)

Pseudo-second-order equation:
$$q_t = q_e^2 K_2 t / (1 + K_2 q_e t)$$
 (5)

Elovich equation:
$$q_t = alnt + b$$
 (6)

where $q_t (\text{mg g}^{-1})$ and $q_e (\text{mg g}^{-1})$ represent the amounts of phosphate adsorbed at time *t* and adsorption equilibrium, respectively; $K_1 (\text{min}^{-1})$ and $K_2 (\text{g mg}^{-1} \text{min}^{-1})$ represent the adsorption rate constants; *a* and *b* represent the rate constants fitted by the Elovich model.

1.2. Adsorption isotherms

Adsorption isotherms show the relationship between adsorption capacity (q_e) and the adsorption equilibrium concentration (C_e) under suitable reaction conditions. Langmuir,^[5] Freundlich,^[6] and Toth ^[7,8] models were applied to describe monolayer homogeneous, multilayer heterogeneous, and multilayer heterogeneous surface adsorption processes, respectively. The models can be expressed by the following equations:

Langmuir model:
$$q_e = q_m K_L C_e / (1 + K_L C_e)$$
 (7)

Freundlich model:
$$q_e = K_F C_e^{1/n}$$
 (8)

Toth model:
$$q_e = q_m C_e / [aT + C_e^Z]^{1/Z}$$
 (9)

where q_m (mg g⁻¹) and K_L represent the maximum adsorption capacity of phosphate and the constant in the Langmuir related to the heat of adsorption, respectively; K_F and n represent the adsorption capacity and favorability of adsorption, respectively; Z represents the heterogeneity of the adsorbent surface, and aT represents the adsorption affinity.

1.3. Adsorption thermodynamics

To evaluate the spontaneity and thermostability of LDHs during adsorption process, three thermodynamic parameters (ΔG^{0} , ΔS^{0} , and ΔH^{0}) were calculated.^[9] The equations are as follows:

$$\Delta G^{\theta} = -RT lnK \tag{10}$$

$$\Delta G^0 = \Delta H^0 - T \Delta S^0 \tag{11}$$

$$\ln K = -\Delta H^0 / RT + \Delta S^0 / R \tag{12}$$

where K (L mol⁻¹) and R (8.314 J K⁻¹ mol⁻¹) are the thermodynamic equilibrium constant and the gas constant, respectively.

	6			
Samples	Ratio	Mg element	Al element	[Mg]/[Al]
		content(%)	content(%)	(ICP-OES)
G-LDH	Mg ²⁺ :Al ³⁺ :Na ⁺ =4:1:1	26.04	6.40	4.51
Rock-LDH	Mg ²⁺ :Al ³⁺ :Na ⁺ =4:1:1	24.08	6.35	4.20
Karst-LDH		14.30	13.22	1.20

Table S1 Actual Mg-Al ratio of different LDHs.

Table S2 BET data of adsorbents.

Samples	Specific Surface Area (m ² g ⁻¹)	Pore Volume (m ³ g ⁻¹)	Average Pore Diameter (nm)
G-LDH	16.239	0.107	25.677
Rock-LDH	36.828	0.221	23.279
Karst-LDH	48.470	0.227	18.145

	Pseudo-first-order			Pse	eudo-second-ord	Elovich			
Samples	<i>q_e</i> (mg g ⁻¹)	<i>K</i> ₁ (min ⁻¹)	R ²	<i>q</i> _e (mg g ⁻¹)	<i>K</i> ₂ (g mg ⁻¹ min ⁻¹)	R ²	a	Ь	R ²
G-LDH	6.345	0.927	0.320	6.599	0.193	0.681	0.501	4.368	0.986
Rock-LDH	14.201	0.660	0.602	14.664	0.077	0.899	1.059	9.800	0.919
Karst-LDH	60.457	0.310	0.947	62.790	0.008	0.982	6.384	32.081	0.810

Table S3 Adsorption kinetics fitting parameters.

Table S4 Adsorption isotherms fitting parameters.

	Т	Langmuir isotherm T equation			Freundlich isotherm equation		Toth equation				
Samples	(K)	<i>q</i> _m (mg g ⁻¹)	KL	R ²	K _F	1/n	R ²	<i>q_m</i> (mg g ⁻¹)	a_T	Z	R ²
	298	16.14	0.012	0.956	1.342	0.400	0.982	39.25	0.025	0.357	0.978
G-LDH	308	22.50	0.010	0.979	1.420	0.442	0.993	53.93	0.015	0.392	0.992
	318	24.81	0.013	0.968	2.275	0.388	0.982	61.15	0.031	0.347	0.983
	298	38.36	0.013	0.893	2.954	0.422	0.976	123.76	0.039	0.291	0.962
Rock- LDH	308	44.60	0.012	0.946	3.412	0.419	0.992	142.46	0.027	0.309	0.985
LDII	318	49.96	0.012	0.979	4.146	0.400	0.996	153.78	0.026	0.314	0.996
	298	105.54	0.860	0.750	61.402	0.119	0.990	435.00	2.610*109	0.081	0.959
Karst-	308	111.41	0.900	0.795	63.554	0.125	0.992	593.40	3.066*10 ⁹	0.076	0.997
LDII	318	114.30	1.980	0.711	67.794	0.119	0.998	1230.31	4.411*10 ¹⁶	0.049	0.998

Samples	Т (К)	∆ <i>G</i> [∅] (KJ mol ⁻¹)	∆ <i>H</i> ⁰ (KJ mol ⁻¹)	∆ <i>S</i> ^θ (J K ⁻¹ mol ⁻ ¹)	%ζ _H	%ζ _S
	298	-0.728			49.321	50.679
G-LDH	308	-0.899	20.313	70.040	48.496	51.504
	318	-2.152			47.699	52.301
	298	-2.683			45.466	54.250
Rock-LDH	308	-3.142	13.330	53.655	44.649	55.351
	318	-3.760			43.861	56.139
	298	-10.201			21.640	78.360
Karst-LDH	308	-10.631	3.887	47.231	21.086	78.914
	318	-11.148			20.560	79.441

Table S5 Adsorption thermodynamic parameters.

phosphate adsorption properties of Mg-Al LDH modified by different methods.

	Adsorbent characteristics	Actual maximum	
Adsorbents	and adsorption conditions	adsorption	Ref
		capacity (mg g ⁻¹)	
Mg/Al hydroxides modified	Mg/Al ratio=3	6.10	[10]
almond shell biochar	SSA: 4.51 $m^2 g^{-1} PV$: 0.023 $cm^3 g^{-1}$		
	Dosage: 2.50 g L ⁻¹ C ₀ : 0-250 mg L ⁻		
Mg-Al-LDH/BC	SSA: 77.32 m ² g ⁻¹ PD: 16.377 nm	36.19 (P)	[11]
	C ₀ : 5-80 mg P L ⁻¹ T: 298K		
Mg-Al-La LDH/Fe ₃ O ₄ /C	SA: 19.19 $m^2 g^{-1}$ PV: 0.096 cm ³ g ⁻¹	106.21	[12]
	PD: 20.637 nm		
	Dosage: 0.6 g L ⁻¹ pH: 7 T: 328 K		
	Co: 10-100 mg L ⁻¹		
Mg/Al-201	SA: 4.32 m ² g ⁻¹ PD: 8.4 nm	52.00	[13]
	Dosage: 0.5 g L ⁻¹ T: 298 K		
Mg-Al-CO ₃ LDH-	Dosage: 0.3 g L ⁻¹ pH: 5	54.9	[14]
Chitosancomposite	Co: 10-120 mg L ⁻¹		
40% LDH/biochar composite	SA: 10.1 m ² g ⁻¹	13.23 (P)	[15]
	Dosage: 2.0 g L ⁻¹ Co: 50 mg P L ⁻¹		
Karst-LDH	SA: 48.47 $m^2 g^{-1}$ PV: 0.227 cm ³ g ⁻¹	127.17	This
	PD: 18.145 nm		work
	Dosage: 0.8 g L ⁻¹ Co: 25-300 mg L ⁻		

Note: SSA, PV, PD represent specific surface area, pore volume, pore diameter, respectively.

References

[1] S. Lagergren, K. Sven. Vetensk. Handl., 1898, 241, 1-39.

- [2] Y.S. Ho and G. McKay, Process. Biochem. 1999, 34, 451-465.
- [3] P.N. Diagboya, B.I. Olu-Owolabi and K.O. Adebowale, *RSC Adv.*, 2015, 5, 2536-2542.
- [4] M.J.D. Low, Chem. Rev., 1960, 60, 267.
- [5] I. Langmuir, J. Am. Chem. Soc., 1918, 40, 489.
- [6] H. Freundlich and W. Heller, J. Am. Chem. Soc., 1939, 61, 2228.
- [7] J.Toth, Adv. Colloid Interf. Sci., 1995, 55, 1.
- [8] J.Toth, Marcel Dekker, 2002.
- [9] S. Merrad, M. Abbas and M. Trari, Fiber. Polym., 2023, 24, 1067.
- [10] S. Li, X. Ma, Z. Ma, X. Dong, Z. Wei, X. Liu and L. Zhu, *Environ. Technol. Innov.*, 2021, 23, 101771.
- [11] J. Zhang, W. Huang, D. Yang, J. Xiang and Y. Chen, *Sci. Total Eenviron.*, 2022, 844, 156802.
- [12] Y. Wang, J. Li, Y. Yuan, Y. Si, J. Xu, M. Li and X. Peng, Colloid. Surface. A., 2021, 626, 127060.
- [13] G. Nie, L. Wu, S. Qiu, Z. Xu and H. Wang, J. Colloid. Interf. Sci., 2022, 614, 583-592.
- [14] N. Isidoro Ribeiro, O. Barreto Pessanha, M. Luiza Gomes Soares Pessanha and D. Guimarães, Sep. Purif. Technol., 2023, 307, 122717.
- [15] S. Wan, S. Wang, Y. Li and B. Gao, J. Ind. Eng. Chem., 2017, 47, 246-253.