Boosting the catalytic performance of Al₂O₃-supported Pd catalysts by introducing CeO₂ promoters

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Experiment details

Materials

Cerium (III) acetate hydrate ((CH₃CO₂)₃Ce·xH₂O, Aladdin, \geq 99.99%), Aluminum oxide (Al₂O₃, Aladdin, 200-300 mesh \geq 70%), Palladium nitrate solution (Pd(NO₃)₂, 15g/100g, Shanghai Tuosi Chemical Co., Ltd), Cerium (III) nitrate hexahydrate (Ce(NO₃)₃·6H₂O, Aladdin, \geq 99.95%), Sodium hydroxide (NaOH, Aladdin). All materials were used without further purification.

Synthesis

Synthesis of AlCePd catalyst. 0.0664 g of $(CH_3CO_2)_3Ce \cdot xH_2O$ and 88 µL of Pd $(NO_3)_2$ solution (2 wt%) were dissolved in 100 mL of deionized water and magnetically stirred for 30 minutes, then added 0.72 g of Al₂O₃ support. After that, it was transferred to an oil bath at 80 °C and kept for 6 h. The obtained product was separated by centrifugation three times with deionized water and then kept in a vacuum oven at 70 °C overnight. Then, the dried sample was calcined in a muffle furnace at a heating rate of 5 °C/min for 3 h at 500 °C, and subsequently treated in 5% H₂/Ar at 250 °C for 2 h to obtain the AlCePd catalyst.

Synthesis of AIPd catalyst. The contrast sample AIPd was prepared by impregnation method. 88 μ L of Pd(NO₃)₂ solution (2 wt%) and 0.72 g of Al₂O₃ were dispersed in 70 mL of deionized water, and then transferred to an oil bath at 80 °C until the solution was completely evaporated.

Synthesis of CePd catalysts. 23 μ L of Pd(NO₃)₂ solution (2 wt%) and 0.2 g of ceria nanorods were dispersed in 60 mL of deionized water, and then transferred to an oil bath at 80 °C until the solution was completely evaporated.

Synthesis of CeO₂ nanorods. 1.736 g of Ce(NO₃)₃·6H₂O and 19.2 g of NaOH were dissolved in 10 ml and 70 ml of deionized water, respectively. After that, the sodium hydroxide solution was added dropwise to the cerium nitrate solution and stirred at room temperature for 30 minutes, then transferred to a 100 ml stainless steel autoclave reactor and kept at 100 °C for 24 h. The products were collected by centrifugation, washed sequentially with deionized water and ethanol, and finally dried at 60°C overnight.

Synthesis of (AlCePd)_{co} catalysts. First, 0.72 g of Al_2O_3 support was dispersed in 70 ml of deionized water, after which 0.0223 g of $Ce(NO_3)_3 \cdot 6H_2O$ and 88 µL of $Pd(NO_3)_2$ solution were added and stirred at room temperature for 30 minutes. Then it was transferred to an oil bath at 80 °C until the solution was completely evaporated.

Characterization. The crystal structures of catalysts were analyzed using Bruker D8 Focus Powder X-ray diffraction with Cu K α radiation (λ = 0.15418 nm) at 40 kV and 40 mA. Inductively coupled plasma optical emission spectrometry (ICP-OES) analyses were performed with a Varian Liberty 200 spectrophotometer to determine the contents of Pd and Ce. Transmission electron microscope (TEM) images were obtained using TECNAI G2 high-resolution transmission electron microscope with an operating voltage of 200 kV. N₂ adsorption-desorption isotherms were measured using an Autosorb-iQ system, and the specific surface areas of the catalysts were calculated according to the Brunauer-Emmett-Teller (BET) method. The Raman measurements were performed on a Renishaw spectrometer at 532 nm on a Renishaw Microscope System RM2000. X-ray photoelectron spectroscopy (XPS) measurements were conducted on an ESCALAB-MKII 250 photoelectron spectrometer (VG Co.) with Al K α X-ray radiation as the X-ray source for

excitation. Hydrogen temperature-programmed reductions (H_2 -TPR) experiments were carried out using a ChemStar TPx Chemisorption Analyzer (USA). 100 mg of the catalyst was first treated in Ar (30 mL min⁻¹) at 250 °C for 2 h, then cooled to room temperature. After that, the flowing gas was switched to 10% H_2 /Ar, and then the samples were heated from 50 °C to 800 °C at a ramping rate of 10 °C min⁻¹. CO temperature-programmed desorption (CO-TPD) experiments were performed using a ChemStar TPx Chemisorption Analyzer (USA). 100 mg of the catalyst was first treated in He gas flow (30 ml min⁻¹) at 200 °C for 2 h, and then cooled to room temperature. Next, the flow gas was switched to 10% CO/Ar and kept at room temperature for 1 h. After that, the catalyst was flushed with He gas flow to remove physically adsorbed CO at room temperature. Then, the samples were gradually heated from 25 °C to 700 °C at a ramping rate of 10 °C min⁻¹.

Catalytic activity tests

The CO oxidation reaction was carried out in a fixed bed flow reactor system at atmospheric pressure. 50 mg of catalyst and 50 mg of quartz sand were ground to make a homogeneous mixture and then placed in a quartz tube. The reaction gas (1% CO + 9% O_2 + 90% Ar) was introduced at a flow rate of 33 ml/min and the temperature was raised from room temperature until the CO was completely converted at a ramp rate of 2 °C/min. The products were monitored online using a chromatograph equipped with a thermal conductivity detector (TCD).



Fig. S1 (a, b) TEM images and (c) EDX elemental mappings of the AlCePd catalyst.



Fig.

S2

CePd

(c,d).



Fig. S3 (a, b) HAADF-STEM images and (c) EDX elemental mappings of the AIPd catalyst. DottedorangecirclesinbdenotethePdnanoparticles.



Fig. S4 (a, b) HAADF-STEM images and (c) EDX elemental mappings of the CePd catalyst. DottedorangeboxesinbdenotethePdclusters.









Fig. S8 N_2 adsorption-desorption isotherms of fresh AlCePd, AlPd, and CePd catalysts.



Fig. S9 The profile of CO conversion versus temperature with CePd catalysts before and after long-term CO oxidation tests.



Fig. S10 The profile of CO conversion versus temperature with AICePd and AIPd catalysts beforeandafterlong-termCOoxidationtests.



Fig. S11 N2 adsorption-desorption isotherms of AlCePd, AlPd, and CePd catalysts after long-termCOoxidationtests.



Fig. S12 (a, b) HAADF-STEM images and (c) EDX elemental mappings of the AlCePd catalyst afterlong-termCOoxidationtests.



Fig. S13 (a, b) TEM images and (c) EDX elemental mappings of the AIPd catalyst after long-term CO oxidation tests.



Fig. S14 (a, b) TEM images and (c) EDX elemental mappings of the CePd catalyst after long-termCOoxidationtests.



Fig. S15 (a) The profile of CO conversion and (b) the long-term stability with AlCePd catalysts of
different Ce contents. The Ce content in AlCePd, $(AlCePd)_2$, and $(AlCePd)_3$ measured by ICP were
0.83%, 1.49%, and 1.72%, respectively.



Fig. S16 The profile of CO conversion versus temperature with different catalysts. $AICePd_{(co)}$ representsthecatalystpreparedbyco-impregnation.



Fig. S17 Pd 3d XPS spectra of AIPd catalysts before and after long-term CO oxidation tests.



Fig. S18 Pd 3d XPS spectra of CePd catalysts before and after long-term CO oxidation tests.



Fig. S19 (a) Ce 3d and (b) O 1s XPS spectra of CePd catalysts before and after long-term CO oxidation tests.

| | AlCePd fresh | AlCePd after 12 h CO oxidation | AlPd fresh | AlPd after 12 h CO oxidation | CePd fresh | CePd after 12 h CO oxidation |
|-------------------------|-----------------|--------------------------------------|---------------|------------------------------------|------------|------------------------------------|
| S _{BET} (m²/g) | 158.2 | 158.4 | 158 | 142.2 | 74.11 | 77.35 |
| Pore Diameter | 7.252 | 7.024 | 7.051 | 7.487 | 24.82 | 31.15 |

Table S1 Specific surface areas and Pore Diameter of AICePd, AIPd, and CePd before and after long-term CO oxidation tests.

| Pd content (wt%) 0.32 0.34 0.32 Ce content (wt%) 0.83 | | AlCePd | AlPd | CePd |
|---|------------------|--------|------|------|
| Ce content (wt%) 0.83 — — | Pd content (wt%) | 0.32 | 0.34 | 0.32 |
| | Ce content (wt%) | 0.83 | _ | _ |

| | (AICePd) ₂ | (AlCePd)₃ | |
|------------------|-----------------------|-----------|--|
| Pd content (wt%) | 0.36 | 0.27 | |
| Ce content (wt%) | 1.49 | 1.72 | |

Table S3 The Pd and Ce contents of $(AICePd)_2 \cdot (AICePd)_3$ catalysts.

| | AlCePd | AlPd | CePd | (AlCePd) ₂ | (AlCePd)₃ |
|----------------------|--------|------|------|-----------------------|-----------|
| T₅₀ (°C) | 143 | 186 | 55 | 133 | 106 |
| Т ₉₀ (°С) | 156 | 197 | 78 | 142 | 120 |

Table S4 The $T_{\rm 50}$ and $T_{\rm 90}$ of different catalysts.

| | AlCePd fresh | AlCePd after 12 h CO oxidation | AlPd fresh | AlPd after 12 h CO oxidation | CePd fresh | CePd after 12 h CO oxidation |
|---|-----------------|--------------------------------------|---------------|------------------------------------|---------------|------------------------------------|
| Surface content of Pd ²⁺ (%) | 40 | 40.2 | 35.0 | 34.9 | 54.6 | 100 |
| Surface content of Ce ³⁺ (%) | 30.9 | 30.95 | | _ | 19.4 | 17.5 |

Table S5 Percentages of Pd²⁺ and Ce³⁺ content based on XPS analysis of AlCePd, AlPd, and CePd catalysts before and after long-term CO oxidation tests.

| catalysts | noble metals loading (wt%) | The feed gas (CO : O ₂ : balance gas) | WHSV (ml·g _{cat} - ¹·h ⁻¹) | T ₁₀₀ (°C) | Stability | Referenc e |
|---|-------------------------------------|--|---|--------------------------|---|---------------|
| AlCePd | 0.32 | 1 : 9 : 90 (Ar) | 39600 | 160 | 35 h | This work |
| AIPd | 0.34 | 1 : 9 : 90 (Ar) | 39600 | 200 | 10 h | This work |
| CePd | 0.32 | 1 : 9 : 90 (Ar) | 39600 | 120 | 100%→44% (18 h) | This work |
| Pd-ZrO ₂ | 0.72 | 1 : 1 : 98 (He) | 180000 | >275 | 16 h | [1] |
| Pd-CeO ₂ | 0.93 | 1 : 1 : 98 (He) | 180000 | >160 | 2nd cycle | [1] |
| FeO _x /Pt/CeO ₂ | 0.61 | 1 : 20 : 79 (Ar) | 75000 | 25 | 100%→60% (36 h) | [2] |
| NiO _x /CeO ₂ | 0 | 1 : 20 : 79 (Ar) | 75000 | 200 | — | [2] |
| Pd/Ce-MOF | 5 | 4 : 20 : 76 (He) | 240000 | 90 | 8 h | [3] |
| PdO/CeO ₂ | 1 | 2 : 8 : 90 (He) | 300000 | >180 | _ | [4] |
| $Ce_{0.984}Pd_{0.016}O_{2-\delta}$ | 1 | 2 : 8 : 90 (He) | 300000 | >280 | _ | [4] |
| 5Cu/CeO ₂ | 0 | 1 : 20 : 79 (Ar) | 60000 | 142 | T ₁₀₀ 143 °C→240 °C (35 h) | [5] |
| Pd@CeO ₂ -800 (Ce:CNT=0.12) | 1 | 1 : 1.55 : 97.45 (He) | 15000 | 110 | 24 h | [6] |
| Pd/CeO_2 - ZrO_2 - Al_2O_3 | 5 | 1 : 1 : 98 (He) | 150000 | 150 | large differences in 11 cycle curves | [7] |
| Pd/Ti ₂₀ Ce ₁ | 0.5 | 1 : 10 : 89 (N ₂) | 72000 | 200 | 30 h | [8] |

Table S6 Comparison of catalysts reported in the literature for CO oxidation.

Reference

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